# **Experimental Section**

#### Synthesis of amorphous NiB<sub>2</sub>

All chemicals were used as received without further purification. Amorphous  $NiB_2$  was prepared by a reflux method with Ar protection[1]. Typically, 2.6 g  $Ni_2SO_4.6H_2O$  was dissolved in 20 mL deionized water in three-necked flask. Then, 0.75 g NaBH<sub>4</sub> dissolved in 5 mL deionized water was rapidly added into the reaction flask. After refluxing for 2 h, the precipitates were collected and washed with deionized water/ethanol and then dried under vacuum.

### **Electrochemical measurements**

Electrochemical measurements were carried out with an electrochemical workstation (CHI-760E Instruments, Shanghai Chenhua Instrument Corp., China). A conventional three-electrode cell was employed with a carbon cloth (CC) sample as working electrode, an Ag/AgCl electrode as reference electrode, and a graphite rod as counter electrode. Before coating catalyst on CC, the CC substrate was pretreated by soaking it in 0.5 M H<sub>2</sub>SO<sub>4</sub> for 12 h, and then washed with deionized water several times and dried at 60 °C for 24 h. All potentials were referenced to reversible hydrogen electrode (RHE) by following equation:  $E_{\rm RHE}$ (V)= $E_{Ag/AgCl}$ +0.197+0.059×pH. The NORR tests were performed using an gastight Htype two-compartment electrochemical cell separated by a Nafion 211 membrane. Before the NORR measurements, all the feeding gases were purified through two glass bubblers containing 4 M KOH solution and the cathodic compartment was purged with Ar for at least 30 min to remove residual oxygen[2]. During each NORR electrolysis, high-purity NO gas (99.9%) was continuously purged into the cathodic chamber at a flow rate of 20 mL min<sup>-1</sup>. After NORR electrolysis at specified potentials for 1 h, the aqueous and gas product are detected by the colorimetric methods and gas chromatography (GC), respectively.

## **Determination of NH3**

The generated NH<sub>3</sub> was determined by the indophenol blue method[3]. Typically, 0.5 mL of electrolyte was removed from the electrochemical reaction vessel and

diluted 10 times with deionized water. Then 2 mL of diluted solution was removed into a clean vessel followed by sequentially adding NaOH solution (2 mL, 1 M) containing salicylic acid ( $C_7H_6O_3$ , 5 wt.%) and sodium citrate ( $C_6H_5Na_3O_7$ , 5 wt.%), sodium hypochlorite (NaClO, 1 mL, 0.05 M), and sodium nitroprusside ( $C_5FeN_6Na_2O$ , 0.2 mL, 1wt.%) aqueous solution. After the incubation for 2 h at room temperature, the mixed solution was subjected to UV-vis measurement using the absorbance at 655 nm wavelength. The concentration-absorbance curves were calibrated by the standard NH<sub>4</sub>Cl solution with a series of concentrations.

The detailed procedure for colorimetric determination of N<sub>2</sub>H<sub>4</sub> was provided in our previous publications[4].

#### Calculations of NH<sub>3</sub> yield rate and NH<sub>3</sub>-Faradaic efficiency

NH<sub>3</sub> yield rate (
$$\mu$$
g h<sup>-1</sup> cm<sup>-2</sup>) =  $\frac{c_{\rm NH_3} \times V}{t \times A}$  (1)

NH<sub>3</sub>-Faradaic efficiency (%) = 
$$\frac{5 \times F \times c_{\text{NH}_3} \times V}{17 \times Q} \times 100\%$$
 (2)

where  $c_{\rm NH3}$  (µg mL<sup>-1</sup>) is the measured NH<sub>3</sub> concentration, V (mL) is the volume of the electrolyte, t (h) is the reduction time, A (cm<sup>-2</sup>) is the surface area of CC (1×1 cm<sup>2</sup>), F (96500 C mol<sup>-1</sup>) is the Faraday constant, Q (C) is the quantity of applied electricity.

### Characterizations

diffraction (XRD) carried X-ray pattern was out on а Rigaku D/max 2400 diffractometer. Transmission electron microscopy (TEM), highresolution transmission electron microscopy (HRTEM), selected area electron diffraction (SAED) and high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) were recorded on a Tecnai G<sup>2</sup> F20 microscope. X-ray photoelectron spectroscopy (XPS) analysis was recorded on a PHI 5702 spectrometer. Online differential electrochemical mass spectrometry (DEMS, QAS 100) was performed by QAS 100 spectrometer.

#### **Calculation details**

The Cambridge sequential total energy package (CASTEP) module of the Materials Studio software was conducted for the quantum chemistry calculations. The Perdew-Burke-Ernzerhof (PBE) generalized gradient approximation (GGA) functional was used for the exchange-correlation potential. The van der Waals interaction was described by using the empirical correction in Grimme's scheme (DFT+D). The convergence criteria for structure optimization were (1) energy tolerance of  $1 \times 10^{-5}$  eV, (2) maximum force tolerance of 0.02 eV Å<sup>-1</sup>, (3) Monkhorst-Pack k-point sampling:  $3 \times 3 \times 1$ . The electron wave functions were expanded using plane waves with a cutoff energy of 400 eV. NiB<sub>2</sub> (001) was modeled by a  $3 \times 3$  supercell, and a vacuum region of 15 Å was used to separate adjacent slabs. The amorphous NiB<sub>2</sub> was built by relaxing the crystalline NiB<sub>2</sub> (001) at 600 K, and the atomic arrangement could be disordered.

The free energies ( $\Delta$ G, 298 K) for each reaction were given after correction[5]:

$$\Delta G = \Delta E + \Delta Z P E - T \Delta S \tag{3}$$

where  $\Delta E$  is the adsorption energy,  $\Delta ZPE$  is the zero-point energy difference and T $\Delta S$  is the entropy difference between the gas phase and adsorbed state.

The Forcite module was employed for the MD simulations. The electrolyte system was modeled by a cubic cell with placing catalyst at the center of the cell and randomly filling 1000  $H_2O$ , 50 NO molecules, and 50 H atoms. After geometry optimization, the MD simulations were performed under the universal field with the total simulation time of 5 ns at a time step of 1 fs.

The radial distribution function (RDF) is calculated by[6]

$$g(\mathbf{r}) = \frac{dN}{4\pi\rho r^2 dr} \tag{4}$$

where dN is the amount of NO in the shell between the central particle r and r+dr,  $\rho$  is the number density of NO, H<sub>2</sub>O, and H.



Fig. S1. XPS B1s spectra of NiB<sub>2</sub>.



Fig. S2. DOS profile of NiB<sub>2</sub>.



Fig. S3. Average potential profiles along c-axis direction for calculating the work function of NiB<sub>2</sub>.



Fig. S4. (a) UV-vis absorption spectra of  $NH_4^+$  assays after incubated for 2 h at ambient conditions. (b) Calibration curve used for the calculation of  $NH_3$  concentrations.



Fig. S5. (a) UV-vis absorption spectra of  $N_2H_4$  assays after incubated for 20 min at ambient conditions. (b) Calibration curve used for calculation of  $N_2H_4$  concentrations.



Fig. S6. Partial current densities of various products over NiB<sub>2</sub> after 1 h of NORR electrolysis at different potentials.



Fig. S7. (a) TEM image, (b) XRD pattern (inset: FFT pattern) and (c) Ni/B atom ratio of NiB<sub>2</sub> after stability tests.



Fig. S8. (a) XRD pattern of crystalline NiB<sub>2</sub> (c-NiB<sub>2</sub>). (b) NH<sub>3</sub> yield rates and (c)  $FE_{NH3}$  of c-NiB<sub>2</sub> and a-NiB<sub>2</sub>.

The crystalline NiB<sub>2</sub> (c-NiB<sub>2</sub>) is prepared by directly annealing amorphous NiB<sub>2</sub> (a-NiB<sub>2</sub>) in Ar. The XRD pattern (Fig. S8a) shows the clear crystalline structure of c-NiB<sub>2</sub>. Impressively, the NORR performance of c-NiB<sub>2</sub> is much inferior to that of a-NiB<sub>2</sub> in terms of both NH<sub>3</sub> yield rate (Fig. S8b) and FE<sub>NH3</sub> (Fig. S8c), and the main cause for their performance disparity arises from their difference in electrochemical surface areas (ECSA), where a-NiB<sub>2</sub> exhibits a much higher ECSA than c-NiB<sub>2</sub> (Fig. S9).



Fig. S9. CV measurements for determining the ECSA of (a) a-NiB<sub>2</sub> and (b) c-NiB<sub>2</sub>.



Fig. S10. Amounts of produced  $NH_3$  on  $NiB_2$  under different conditions at -0.4 V.



Fig. S11. Switching Ar/NO cycling tests on  $NiB_2$  at -0.4 V.



Fig. S12. <sup>1</sup>H NMR spectra of <sup>15</sup>NH<sub>4</sub><sup>+</sup> standard sample and those fed by <sup>15</sup>NO and Ar after NORR electrolysis on NiB<sub>2</sub> at -0.4 V.



Fig. S13. Charge density differences of absorbed NO on (a) B and (b) Ni sites of NiB<sub>2</sub> (Yellow: accumulation, cyan: depletion).



Fig. S14. FTIR spectra of NiB<sub>2</sub> with and without NO adsorption.

We perform FTIR measurement to experimentally investigate the NO adsorption behavior of NiB<sub>2</sub>. It is seen that upon the adsorption of NO, the FTIR spectra show two distinct infrared peaks, where ~1850 cm<sup>-1</sup> is assigned to NO adsorption on Ni species (Ni-\*NO)[7], and ~800 cm<sup>-1</sup> corresponds to B-\*NO[8]. Obviously, the B-\*NO peak area is much larger than Ni-\*NO area, suggesting the stronger NO adsorption on B sites of NiB<sub>2</sub>.



Fig. S15. (a) Online DEMS spectra of NiB<sub>2</sub> during the NORR electrolysis. (b) Schematic of two typical NORR pathways.

The online DEMS data (Fig. S15a) reveal an obvious sign of NH<sub>2</sub>OH intermediate (m/z=33) but no detection of N intermediate (m/z=14), implying that NiB<sub>2</sub> prefers to adopt a NHO pathway (\*NO  $\rightarrow$  \*NHO  $\rightarrow$  \*NHOH  $\rightarrow$  \*NH<sub>2</sub>OH $\rightarrow$  \*NH<sub>2</sub> $\rightarrow$  \*NH<sub>3</sub>) rather than NOH pathway (\*NO  $\rightarrow$  \*NOH  $\rightarrow$  \*N  $\rightarrow$  \*NH $\rightarrow$  \*NH<sub>2</sub> $\rightarrow$  \*NH<sub>3</sub>) to drive the NORR process[9], as illustrated in Fig. S15b.

$\geq$	*NO	*NHO	*NHOH	*NH <sub>2</sub> OH	*NH <sub>2</sub>	*NH <sub>3</sub>
Fe site						
B site			2000 B			20 8 8 8 8 8 9 8 9 8 9 8 9 8 9 8 9 9 9 9

Fig. S16. Optimized structures of NORR intermediates on B and Ni sites of NiB<sub>2</sub>.



Fig. S17. Integrated RDF curves of \*NO,  $*H_2O$ , and \*H on Ni sites of NiB<sub>2</sub>.

Catalyst	Electrolyte	NH3 yield rate (μmol h <sup>-1</sup> cm <sup>-2</sup> )	FE <sub>NH3</sub> (%)	Potential (V vs. RHE)	Ref.
Mo <sub>2</sub> C	0.5 M Na <sub>2</sub> SO <sub>4</sub>	122.7	86.3	-0.4	[10]
Ni <sub>2</sub> P/CP	0.1 M HCl	33.47	76.9	-0.2	[11]
Ru <sub>0.05</sub> Cu <sub>0.95</sub>	$0.05 \text{ M} \text{ Na}_2 \text{SO}_4$	17.68	64.9	-0.5	[12]
Co <sub>1</sub> /MoS <sub>2</sub>	0.5M Na <sub>2</sub> SO <sub>4</sub>	217.6	87.7	-0.5	[9]
MoS <sub>2</sub> /GF	0.1 M HCl	99.6	76.6	0.1	[13]
NiO/TM	0.1 M Na <sub>2</sub> SO <sub>4</sub>	125.3	90	-0.6	[14]
a-B <sub>2.6</sub> C@TiO <sub>2</sub> /Ti	0.1 M Na <sub>2</sub> SO <sub>4</sub>	216.4	87.6	-0.9	[15]
FeP/CC	0.2 M PBS	85.62	88.49	-0.2	[16]
Bi NDs	0.1 M Na <sub>2</sub> SO <sub>4</sub>	70.2	89.2	-0.5	[17]
CoP/TM	$0.2 \text{ M} \text{Na}_2 \text{SO}_4$	47.22	88.3	-0.2	[18]
$CoS_{1-x}$	$0.2 \text{ M} \text{Na}_2 \text{SO}_4$	44.67	53.62	-0.4	[19]
HCNF	$0.2 \text{ M} \text{Na}_2 \text{SO}_4$	22.35	88.33	-0.6	[20]
Cu <sub>2</sub> O@CoMN <sub>2</sub> O 4	$0.1 \text{ M} \text{ Na}_2 \text{SO}_4$	94.18	75.05	-0.9	[21]
MoC/NCS	0.1 M HCl	79.4	89	-0.8	[22]
NiB <sub>2</sub>	0.5 M Na <sub>2</sub> SO <sub>4</sub>	167.1	89.6	-0.4	This work

Table S1. Comparison of the optimum  $NH_3$  yield and  $NH_3$ -Faradic efficiency (FE<sub>NH3</sub>) for recently reported state-of-the-art NORR electrocatalysts at ambient conditions.

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