Supplementary Information

Delivering low-energy carbon capture with photo-responsive hypercrosslinked polymers derived from polystyrene waste

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1. Experimental Configuration for Photo-modulated Desorption

The experimental configuration for dynamic photo-modulated desorption was established by adding a visible light outside the metal retainer. The light rays can irradiate the spent adsorbents in the quartz container through the hole of the metal retainer.



Figure S1. Experimental configuration for photo-modulated desorption: (1) N_2 gas cylinder and regular, (2) CO2 gas cylinder and regular, (3) zeolite/silica drying column of N_2 gas, (4) zeolite/silica drying column of CO2 gas, (5) mass flow controller of N_2 , (6) mass flow controller of CO2, (7) fibre-optic temperature sensor and signal conditioner, (8) data analysis workstation, (9) metal retainer, (10) visible light, (11) quartz container, (12) water condenser, (13) non-dispersive infrared CO₂ sensor, (14) mass flow meter and (15) gas exit.

2. BET Analysis

N2 adsorption-desorption isotherms at 77 K and CO₂ adsorption isotherms at 273 K of HCPs, HCPs@Azo, *cis*-HCPs@Azo and *trans*-HCPs@Azo were measured on a Quadrasorb Evo Quantachrome in our previous paper [1]. The pore size distributions and pore volumes were obtained using the model of non-local density functional theory (NLDFT) [2].



Figure S2. (a) N₂ adsorption and desorption curves at 77 K temperature, (b) pore size distribution and (c) CO2 adsorption curves at 273 K of HCPs, HCPs@Azo, *cis*-HCPs@Azo and *trans*-HCPs@Azo.

Table S1. BET surface areas, pore volumes of different size and total pore volumes of HCPs, HCPs@Azo, *cis*-HCPs@Azo and *trans*-HCPs@Azo.

	HCPs	HCPs@Azo	cis-HCPs@Azo	trans-HCPs@Azo
Pore volume (5 Å – 10 Å) (cm ³ g ⁻¹)	0.308	0.254	0.228	0.223
Pore volume (10 Å – 20 Å) (cm ³ g ⁻¹)	0.212	0.183	0.231	0.163
Pore volume (20 Å – 40 Å) (cm³g-1)	0.64	0.462	0.488	0.398
Pore volume (> 40 Å) (cm ³ g ⁻¹)	0.06	0.058	0.062	0.048
Total pore volume (cm ³ g ⁻¹)	1.22	0.957	1.009	0.832
BET surface area (m ² g ⁻¹)	1225	984	1024	862



3. CO₂ adsorption and CO₂/N₂ Selectivity

Figure S3. CO₂ adsorption rates and adsorption profiles of (black) HCPs, (green) visible light irradiated *trans*-HCPs@Azo and (red) UV light irradiated *cis*-HCPs@Azo at different CO₂ concentration of (a) 1 v/v %, (b) 10 v/v %, (c) 20 v/v %, (d) 40 v/v % at room temperature and atmosphere pressure.

The ideal CO_2/N_2 selectivity ($S_{CO2/N2 ideal}$) can be calculated by dividing the adsorbed amounts of CO_2 and N_2 pure gas [3, 4] as the equations in the following table:

Pure CO ₂ component	$V_{pure CO_2} = \int_0^t V_{gas blank} - \int_0^t V_{mfm}$	(1)
	$n_{pure \ CO_2} = \frac{P \times V_{pure \ CO_2}}{R \times T}$	(2)
Pure N ₂ component	$V_{pure N_2} = \int_0^t V_{gas \ blank} - \int_0^t V_{mfm}$	(3)
	$n_{pure N_2} = \frac{P \times V_{pure N_2}}{R \times T}$	(4)
Ideal selectivity	$S_{co_2/N_2 \ ideal} = \frac{n_{pure \ CO_2}}{n_{pure \ N_2}}$	(5)

Table S2. Equations of adsorbed amounts of pure CO₂ and N₂ and CO₂/N₂ ideal selectivity

, where V_{pure CO2} (mL) and V_{pure N2} (mL) are the adsorbed volumes of pure CO₂ and N₂, n_{pure CO2} (mmol) and n_{pure N2} (mmol) are the adsorbed amounts of CO₂ and N₂, V_{gas blank} (mL s⁻¹) and V_{mfm} (mL s⁻¹) are the volumes of blank gas at input and mass flow meter reading at output, R is the gas constant (8.314 J mol⁻¹ K⁻¹), P (KPa) and T (K) are the pressure and temperature of adsorption process, t (s) is the adsorption duration.

The practical selectivity of CO_2/N_2 (S_{CO2/N_2}) in the mixed CO_2 and N_2 gas is determined by the ratio of the molar fractions of gas after and before adsorption process [5, 6], the equations are shown as following:

CO ₂ component	$V_{CO_2} = \int_0^t V_{CO_2 \ blank} - \int_0^t \frac{C_{CO_2}}{C_{CO_2 \ blank}} V_{CO_2 \ blank}$	(6)
	$n_{CO_2} = \frac{P \times V_{CO_2}}{R \times T}$	(7)
	$n_{CO_2 blank} = \frac{P \times V_{CO_2 blank}}{R \times T}$	(8)
N ₂ component	$V_{N_{2}} = \int_{0}^{t} V_{gas \ blank} - \int_{0}^{t} V_{mfm} - \int_{0}^{t} V_{CO_{2}}$	(9)
	$n_{N_2} = \frac{P \times V_{N_2}}{R \times T}$	(10)
	$n_{N_2 blank} = \frac{P \times V_{N_2 blank}}{R \times T}$	(11)
Selectivity	$S_{co_2/N_2} = \frac{n_{CO_2}/n_{N_2}}{n_{CO_2 blank}/n_{N_2 blank}}$	(12)

Table S3. Equations of adsorbed amounts of CO₂ and N₂ and CO₂/N₂ selectivity in the mixed gas

, where V_{CO2} (mL) and V_{N2} (mL) are the adsorbed volumes of CO₂ and N₂ respectively in the mixed gas, n_{CO2} (mmol) and n_{N2} (mmol) are the adsorbed amounts of CO₂ and N₂, C_{CO2} (mg L⁻¹ s⁻¹)and $C_{CO2 \ blank}$ (mg L⁻¹ s⁻¹)are the CO₂ concentrations at output and input, $V_{gas \ blank}$ (mL s⁻¹)and V_{mfm} (mL s⁻¹)are the volumes of blank total gas at input and mass flow meter reading at output, $V_{CO2 \ blank}$ (mL s⁻¹) and $V_{N2 \ blank}$ (mL s⁻¹) are the volumes of CO₂ and N₂ in blank gas, $n_{CO2 \ blank}$ (mmol s⁻¹)and $n_{N2 \ blank}$ (mmol s⁻¹) are the amounts of CO₂ and N₂ in blank gas, R is the gas constant (8.314 J mol⁻¹ K⁻¹), P (KPa) and T (K) are the pressure and temperature of adsorption process, t (s) is the adsorption duration.



Figure S4. The CO₂ adsorption process experimental data of (a) HCPs, (b) *trans*-HCPs@Azo and (c) *cis*-HCPs@Azo was fitted by (blue) Pseudo-first order kinetic model, (green) Pseudo-second order kinetic order and (red) Avrami's fractional order kinetic model.

4. Adsorption Kinetic Models



5. Desorption Efficiency and Kinetic Models

Figure S5. (a) The CO₂ desorption efficiency of HCPs, *cis*-HCPs@Azo and *trans*-HCPs@Azo with and without visible irradiation, and the desorption process experimental data of (b) HCPs, (c) HCPs-vis, (d) *cis*-HCPs@Azo, (e) *cis*-HCPs@Azo-vis and (f) *trans*-HCPs@Azo was fitted by (blue) Pseudo-first order kinetic model, (green) Pseudo-second order kinetic order and (red) Avrami's fractional order kinetic model.

6. Energy Consumption and Cost Evaluation

The energy consumption and cost of regenerating pristine HCPs and HCPs@Azo were evaluated. Pristine HCPs were regenerated using the traditional thermal approach where these adsorbents were regenerated in a vacuum environment at 110 C for 24 hours, while HCPs@Azo were regenerated using UV-vis irradiation. The equipment used in the thermal-vacuum regeneration method included a vacuum oven (Fistreem International Limited - OVA031.XX3.5) and a vacuum pump (KNF Neuberger - N816.3KT.18). The light used in our photo-modulated method included a UV light (ZLUV LAMP - 365nm, 6W) and a visible light (ZLUV LAMP - 450nm, 6W). Based on the Energy Guide UK [7], the price of electricity in the UK in 2023 was set at £0.34 per kWh.

____ Table S4. Energy consumption and cost evaluation of adsorption-desorption in traditional method of HCPs and photomodulated method of HCPs@Azo

		Vacuum oven	Vacuum pump	UV light	Visible light	Total power consumption	Total cost
Power		0.4 kW	0.1 kW	6 × 10 ⁻³ kW	6 × 10 ⁻³ kW	-	£ 0.34 /kWh
HCPs	Adsorption	-	-	-	-	-	-
	Desorption	12 h	12 h	-	-	-	-
	Power consumption	4.8 kWh	1.2 kWh	-	-	6 kWh	£ 2.04
HCPs@Azo	Adsorption	-	-	1 h	-	-	-
	Desorption	-	-	-	1 h	-	-
	Power consumption	-	-	6 × 10⁻³ kWh	6 × 10⁻³ kWh	1.2 × 10 ⁻² kWh	£ 4.08 × 10 ⁻³

7. References

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