

## Supporting Information

### Mechanism and Selectivity of MOF-Supported Cu Single-Atom Catalysts for the Preferential CO Oxidation

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## Supporting Tables:

**Table S1.** Summary of structural characteristic of the Cu/UiO-66

Catalyst	Cu loading (wt. %) <sup>a</sup>	Cu/Zr <sub>6</sub> <sup>a</sup>	BET surface area (m <sup>2</sup> /g)
UiO-66	-	-	1561
Cu/UiO-66	2.0	0.8	1511

<sup>a</sup> Determined by ICP analysis

**Table S2.** Fit parameters of EXAFS data collected during CO oxidation (COX) at different temperatures (250, 180 and 120 °C).

Measurement	CN	DWF / Å <sup>-2</sup>	R / Å	E <sub>0</sub>
H250	2.0 ± 0.5	0.00228 ± 0.001	1.98 ± 0.02	-14.307 ± 0.6

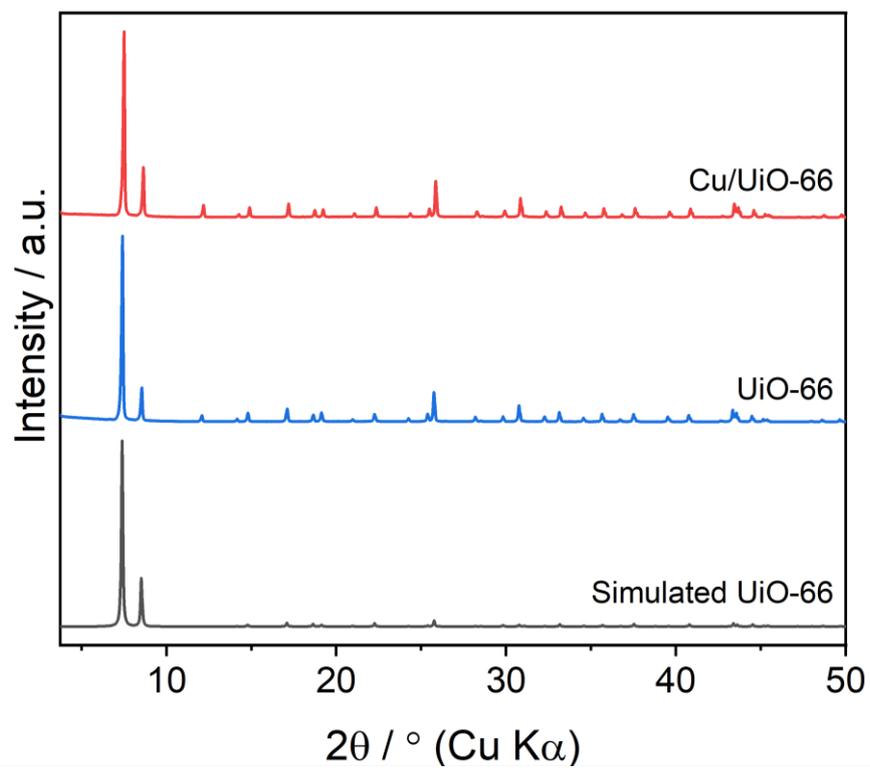
CN: Cu-O first shell coordination number.  $\sigma^2$ : mean square displacement, which is included in the Debye-Waller-Factor (DWF) according to this expression [ $\exp(-2\sigma^2 k^2)$ ]; with k being the wave vector. R: Cu-O bond distance. E<sub>0</sub>: energy reference parameter. In these fits, the amplitude correction factor ( $S_0^2$ ) was kept at a value between 0.85, which was determined from the calibration of the experimental references by FEFF models. For CN numbers in the range given the quality of the fit essentially did not change, while outside it decreased measurably. Therefore, we prefer to give ranges for CN rather than error bars.

**Table S3** The effect of confinement on the adsorption energy and activation energy barrier.

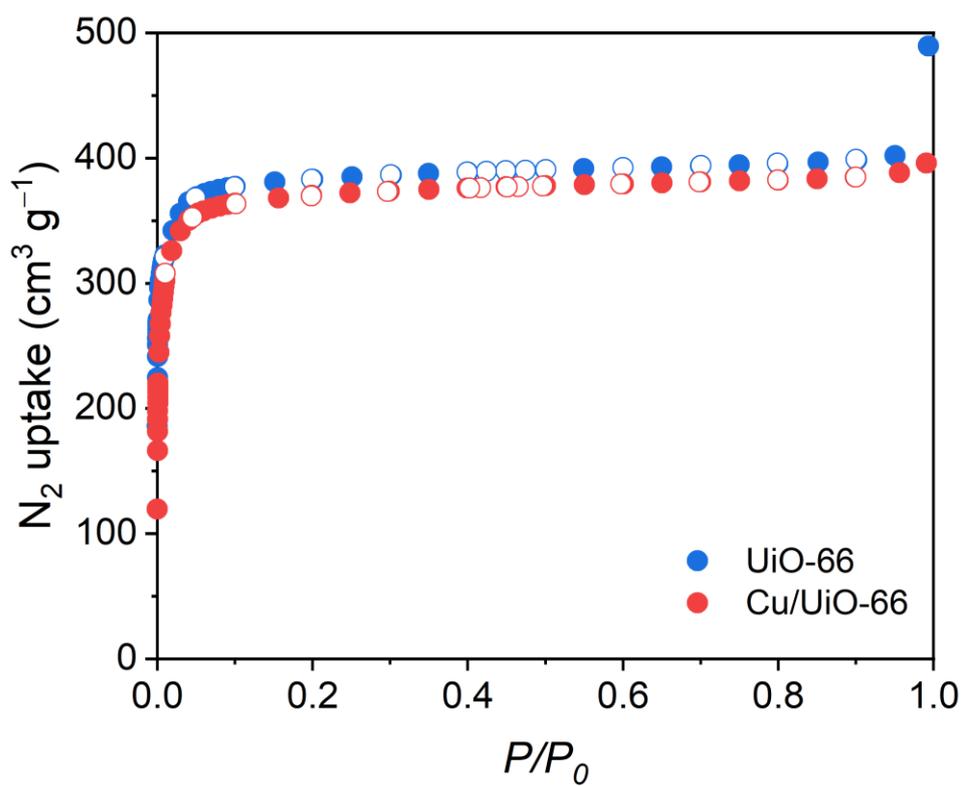
<b>Reaction species</b>	<b>Zr-acetate cluster</b>	<b>Zr-benzoate cluster</b>
II	-122 kJ/mol	-120 kJ/mol
III	-154 kJ/mol	-159 kJ/mol
TS I	-60 kJ/mol ( $E_a = 94$ kJ/mol)	-63 kJ/mol ( $E_a = 96$ kJ/mol)

To investigate the effect of confinement on the adsorption energy and activation energy barrier, we did test calculations by using benzoate groups as linkers. We calculated the adsorption energies of O<sub>2</sub> (intermediate **I**), H<sub>2</sub>/O<sub>2</sub> co-adsorption (intermediate **II**), and the energy barrier for **TS I** on the triplet spin state. As shown in Table S3, the adsorption energies and energy barrier calculated with benzoate groups are similar to those obtained with acetate groups. This suggests that increasing the size of the catalyst model to account for the confinement effect of UiO-66 MOF, does not significantly alter the calculated adsorption energies and activation energy barrier of small molecules such as O<sub>2</sub> and H<sub>2</sub>.

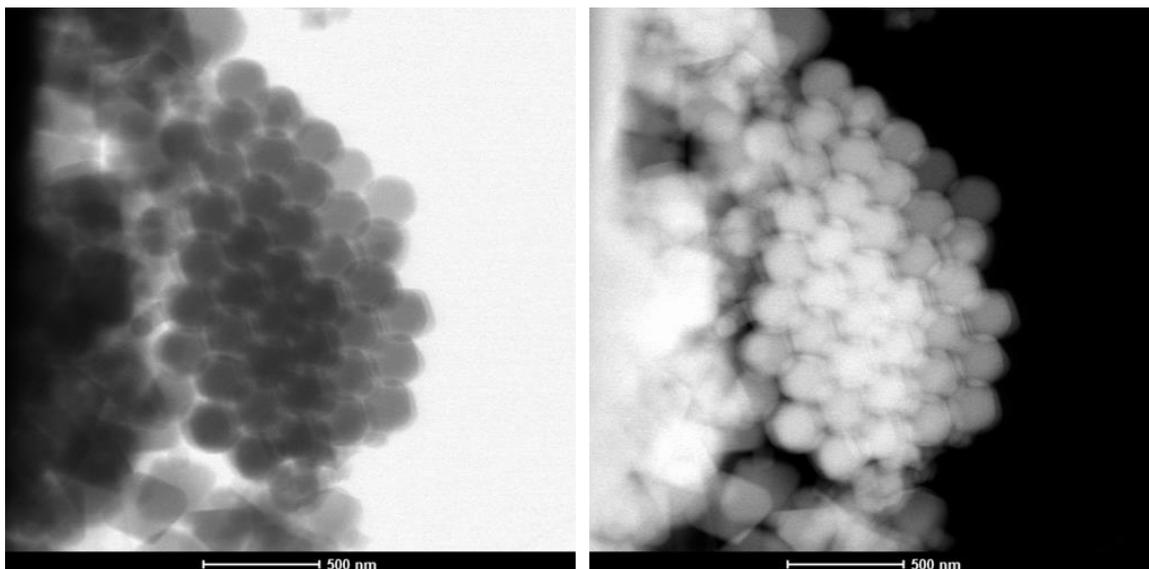
## Additional results



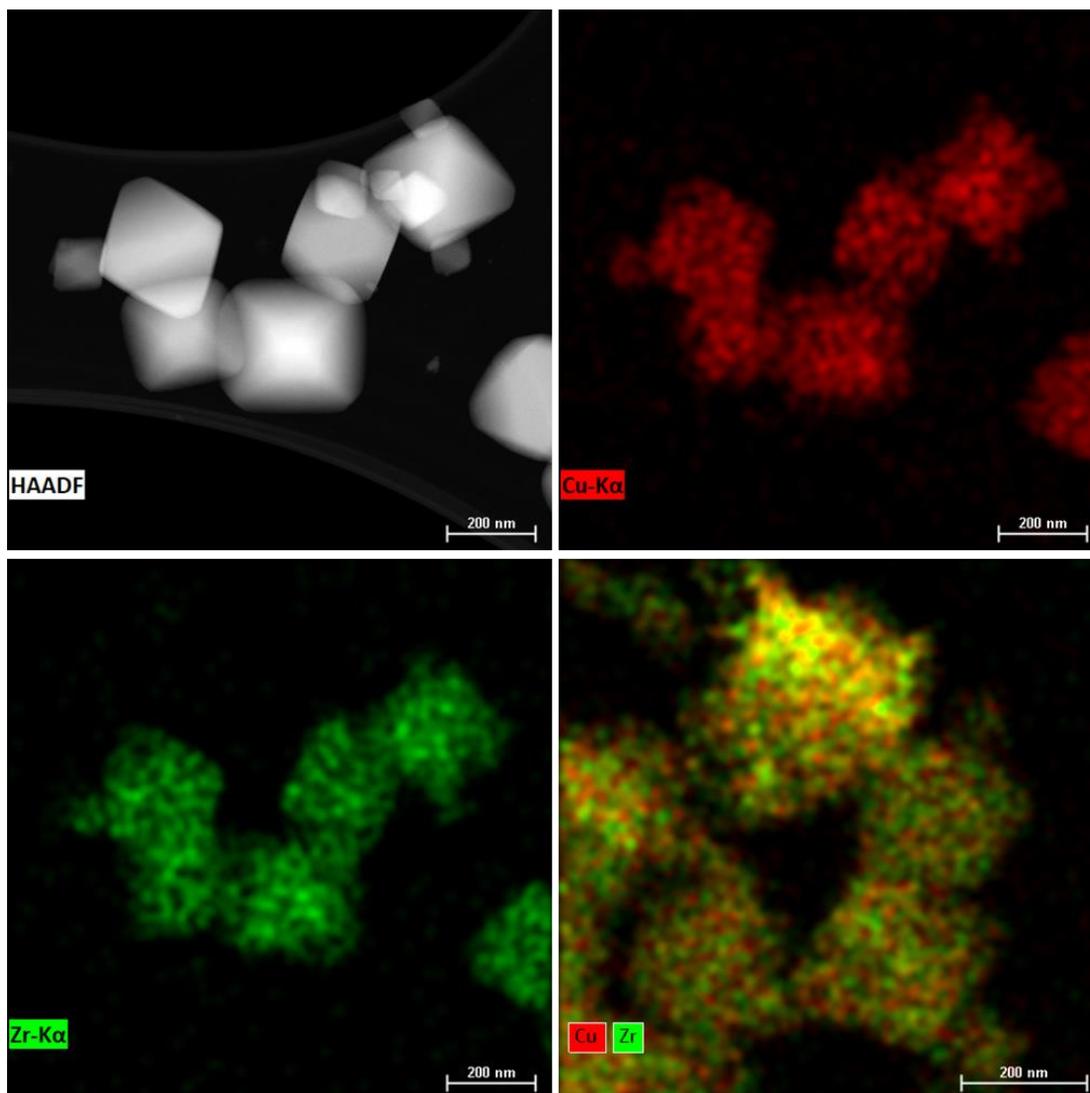
**Figure S1.** PXRD of UiO-66 and Cu/UIO-66 overlaid with the simulated pattern of UiO-66.



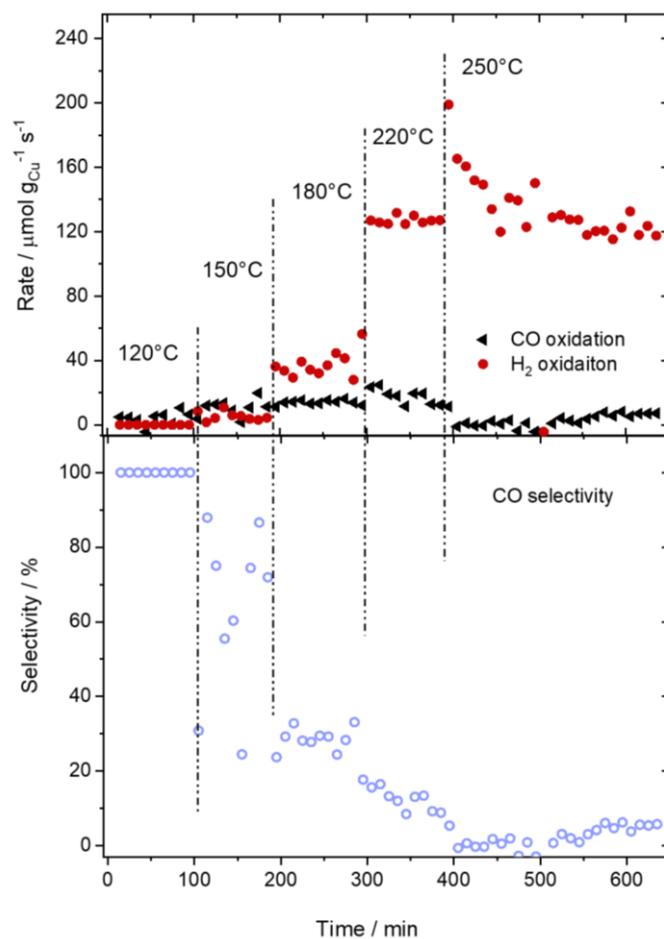
**Figure S2.** N<sub>2</sub> adsorption-desorption isotherms recorded at 77 K of UiO-66 and Cu/UiO-66.



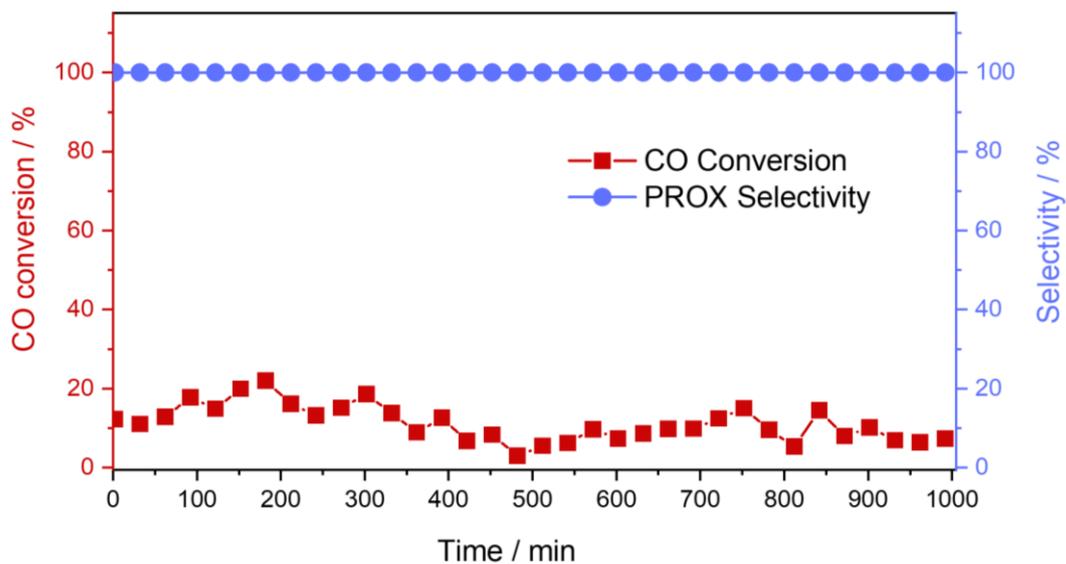
**Figure S3.** Bright and dark field scanning transmission electron microscopy (a: BF-STEM; b: HAADF STEM) results of the fresh reduced Cu1/Uio-66 catalyst.



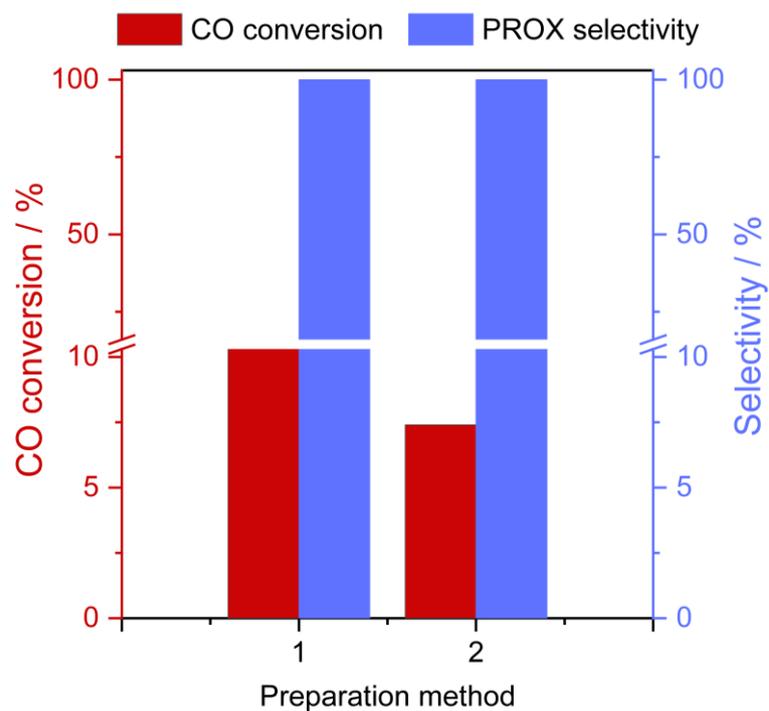
**Figure S4.** HADDF STEM (a) micrograph and corresponding EDS maps of Cu(b), Zr (c) and the hybrid Cu/Zr map (d) of the Cu1/UiO-66 after H250 treatment.



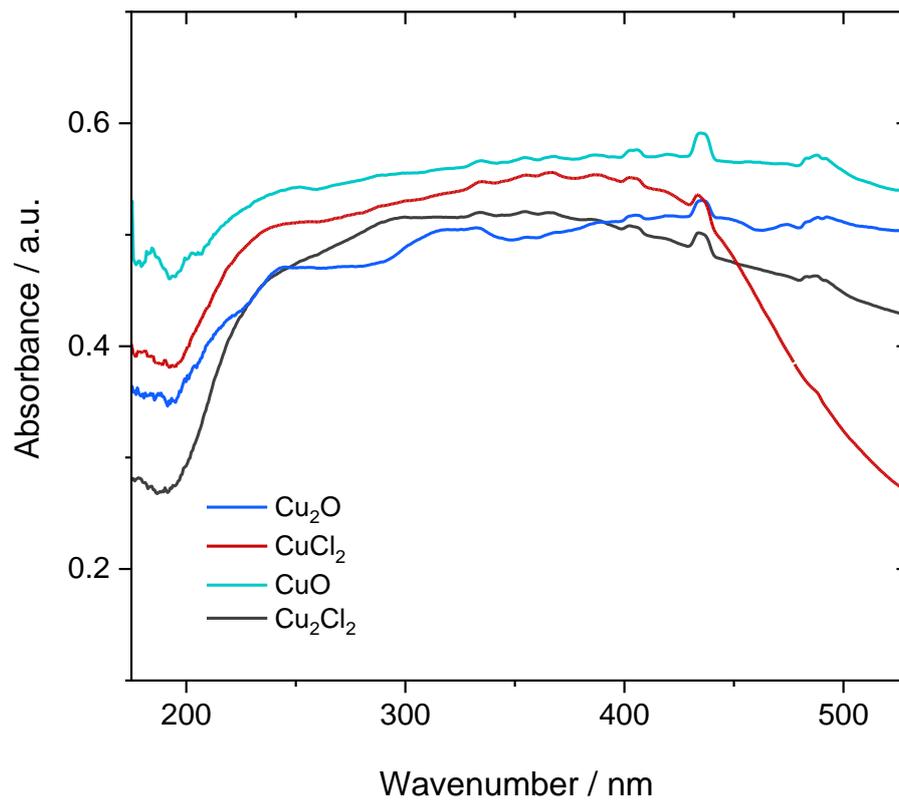
**Figure S5.** (a) Reaction rates for the oxidation of CO and H<sub>2</sub> PROX reaction (1% CO, 1% O<sub>2</sub>, 80% H<sub>2</sub> and N<sub>2</sub>) on Cu/UiO-66 catalyst (prepared by solvothermal method) at different temperatures with time on stream, after the H250 pretreatment (1 h in 10% H<sub>2</sub>/Ar at 250°C) and (b) corresponding selectivity changes. Calculated gas hourly space velocity (GHSV) = 10975 h<sup>-1</sup>.



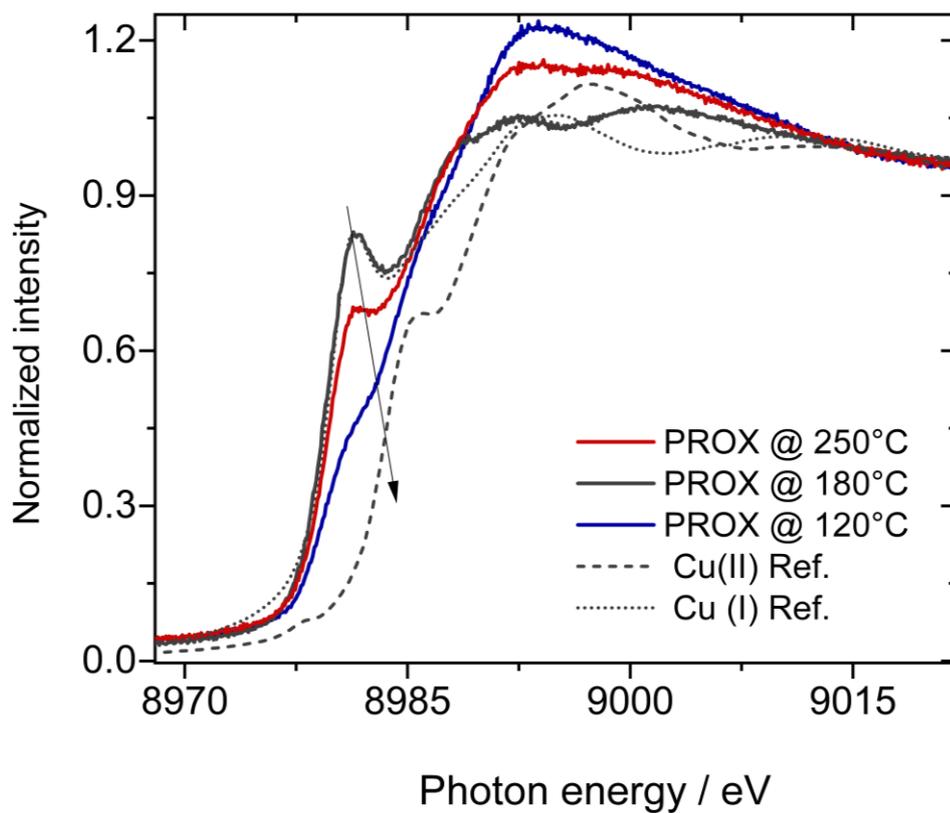
**Figure S6.** Time-on-stream CO oxidation activity and corresponding PROX selectivity (as measured CO conversion) on Cu1/UiO-66 catalyst (prepared by solvothermal method) during PROX reaction (1% CO, 1% O<sub>2</sub>, 80% H<sub>2</sub> and Ar) at 120°C directly after the H250 pretreatment (1 h in 10% H<sub>2</sub>/Ar at 250°C). Calculated gas hourly space velocity (GHSV) = 3658 h<sup>-1</sup>.



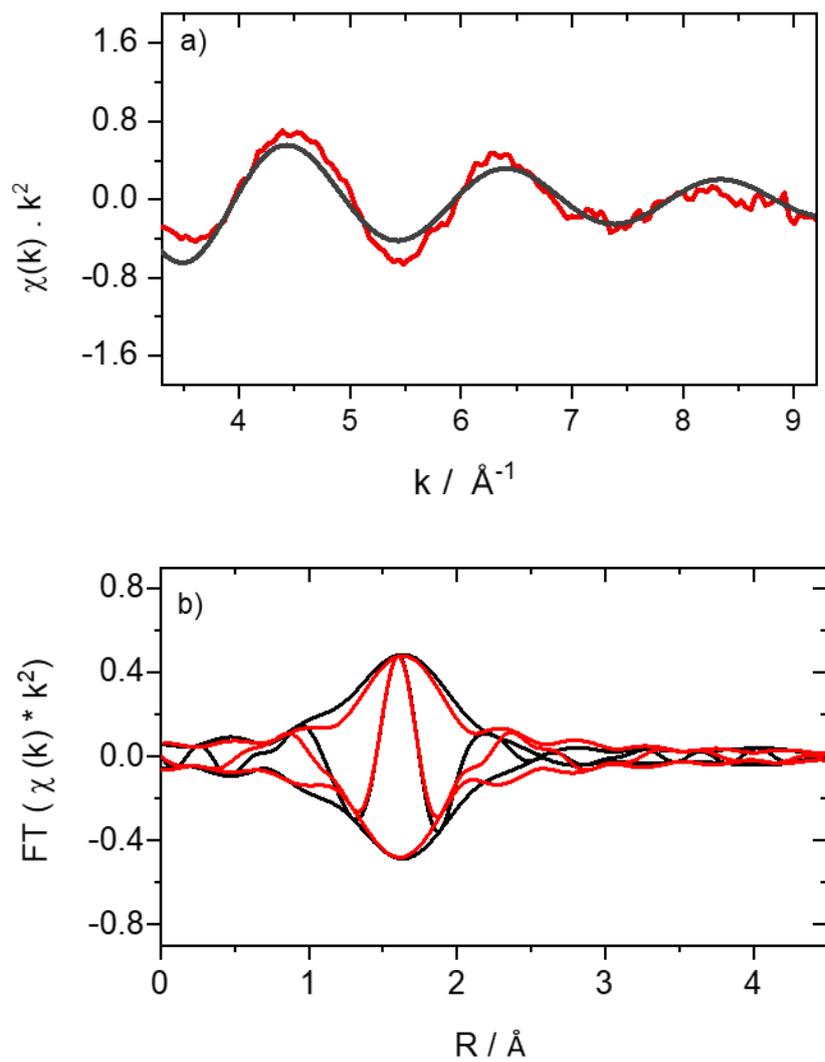
**Figure S7.** Comparison of the steady state CO conversion and corresponding PROX selectivity prepared on Cu1/UiO-66 catalysts by solvothermal method (1) and using mechanical mixing method (2) during PROX reaction (1% CO, 1% O<sub>2</sub>, 80% H<sub>2</sub> and Ar) at 120°C directly after the H250 pretreatment (1 h in 10% H<sub>2</sub>/Ar at 250°C). Calculated gas hourly space velocity (GHSV) = 3658 h<sup>-1</sup>.



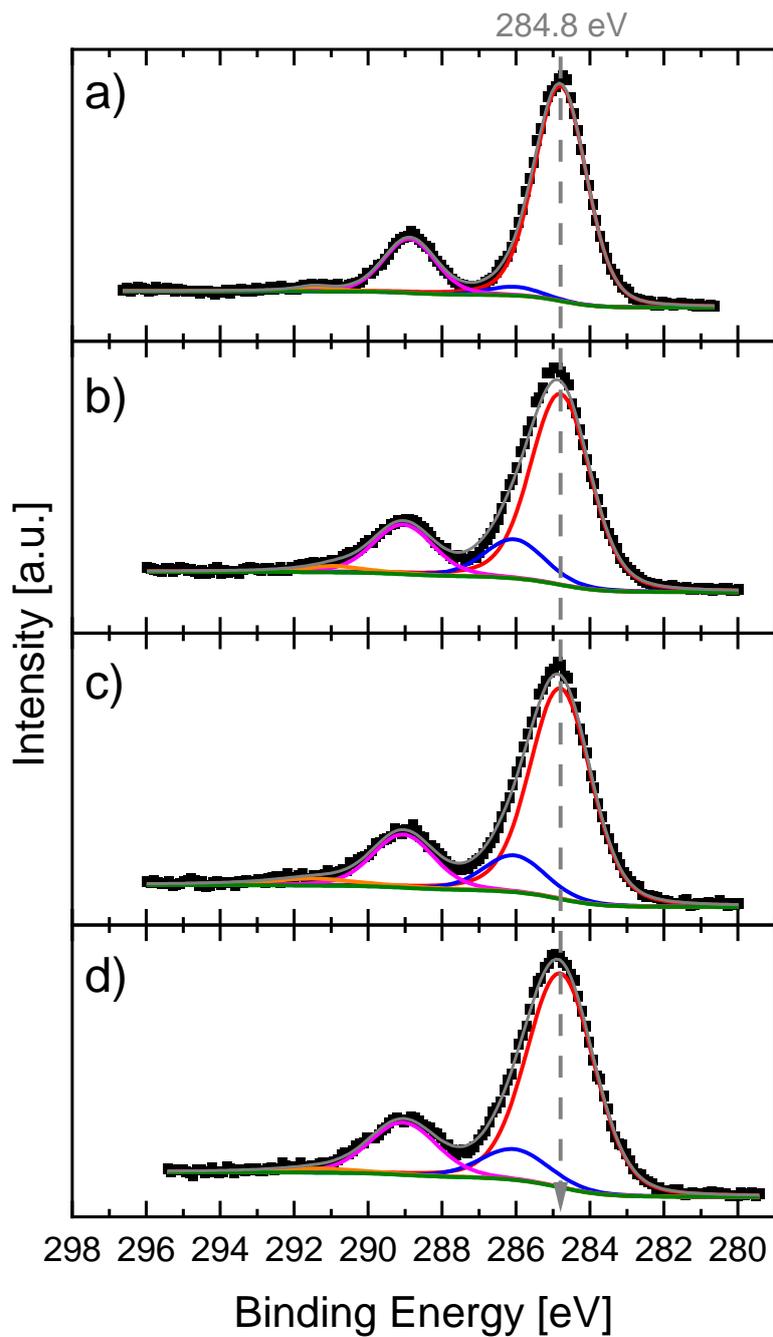
**Figure S8.** Measured spectra of different reference materials of Cu(I) and Cu(II) recorded under flow of Ar at room temperature.



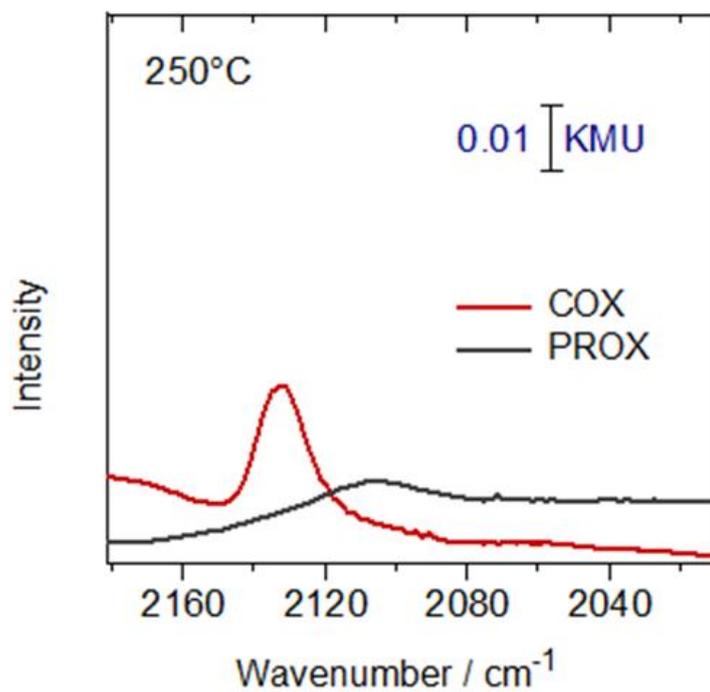
**Figure S9.** Cu K-edge XANES spectra recorded during PROX reaction at different temperatures in standard gas mixture (1% CO, 1% CO, 80% H<sub>2</sub>, balance N<sub>2</sub>) compared to reference spectra for Cu(I) and Cu (II) ions taken on Cu<sub>2</sub>O and CuO powders.



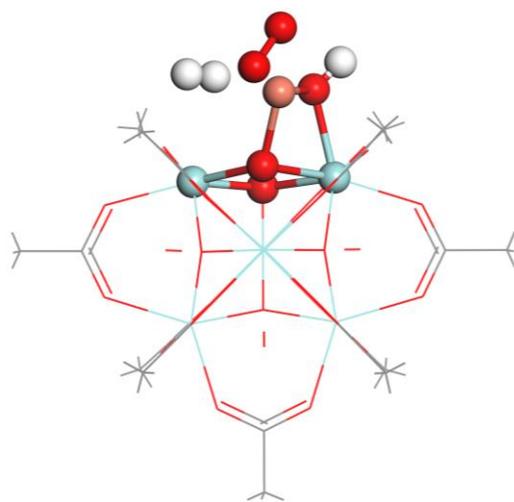
**Figure S10.** EXAFS spectra after the reductive treatment of Cu/UiO-66 in hydrogen at 250°C



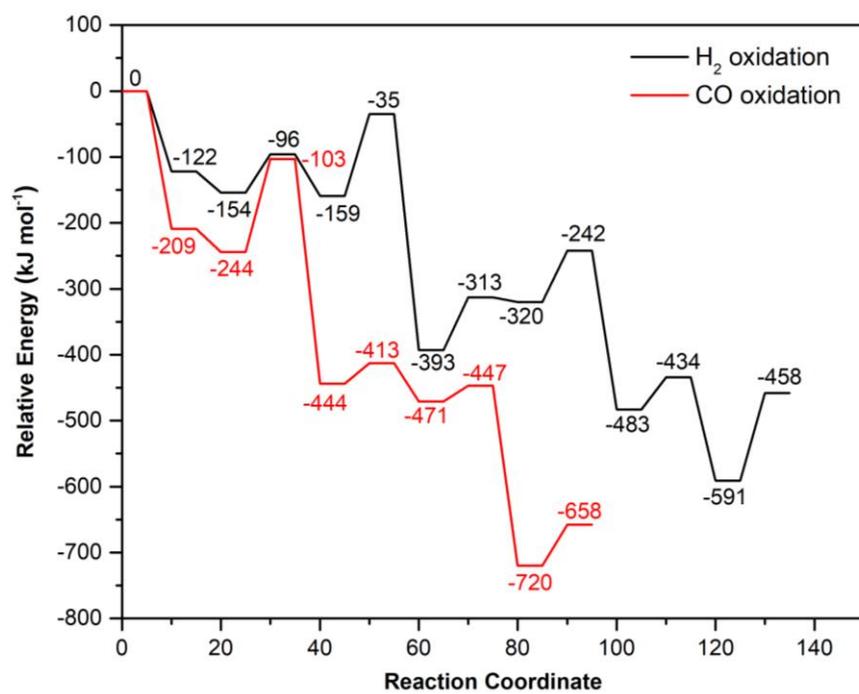
**Figure S11.** NAP-XP spectra for the C1 region at 250°C and a pressure 2 mbar and different feed gases (a, e: in He after heating from RT; b, f: in 10% H<sub>2</sub>/He; c, g: in PROX gas ( 1% CO, 1% O<sub>2</sub>, 80% H<sub>2</sub>, He balance); d, h: back again in He).



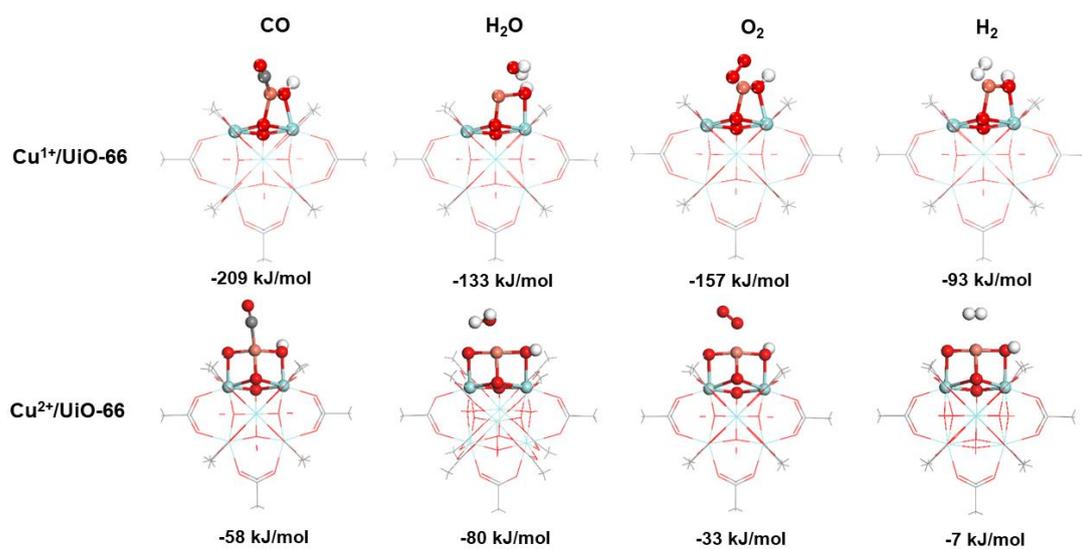
**Figure S12.** CO<sub>ad</sub> bands during preferential CO oxidation (1%CO, 1% O<sub>2</sub>, 80% and N<sub>2</sub> balance) and CO oxidation (1%CO, 1% O<sub>2</sub>, 80% and N<sub>2</sub> balance) at 250°C.



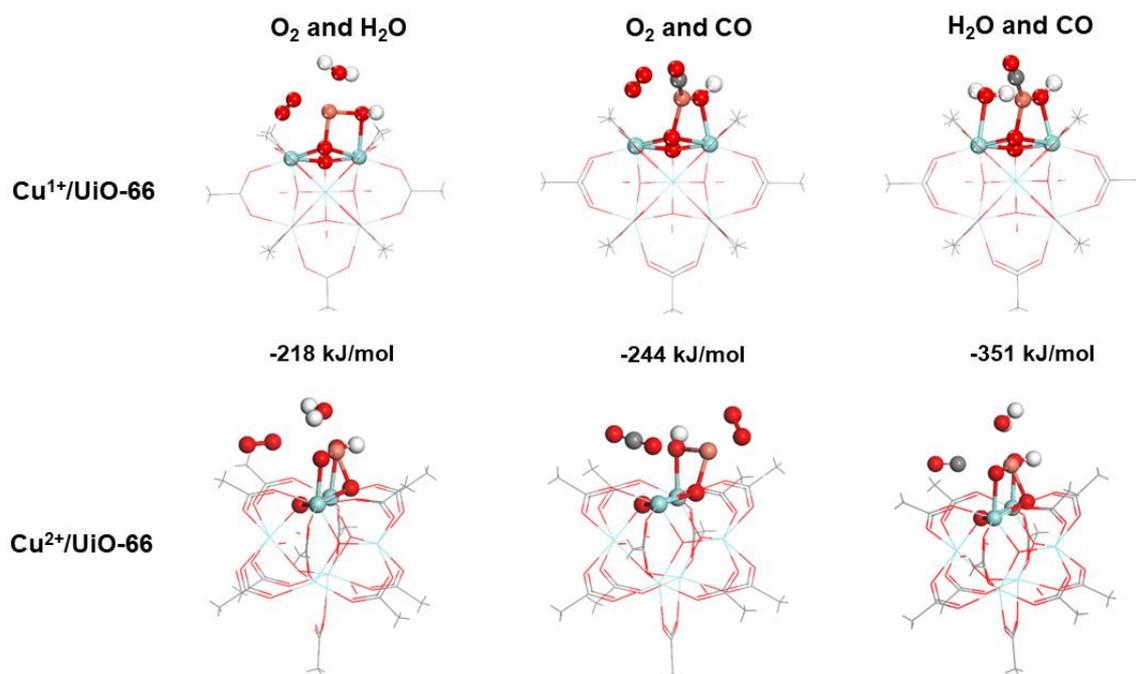
**Figure S13.** The optimized structure of co-adsorption configuration of O<sub>2</sub> and H<sub>2</sub> with the adsorbed O<sub>2</sub> on Cu site.



**Figure S14.** Comparison of the energy profile of the CO and H<sub>2</sub> oxidation

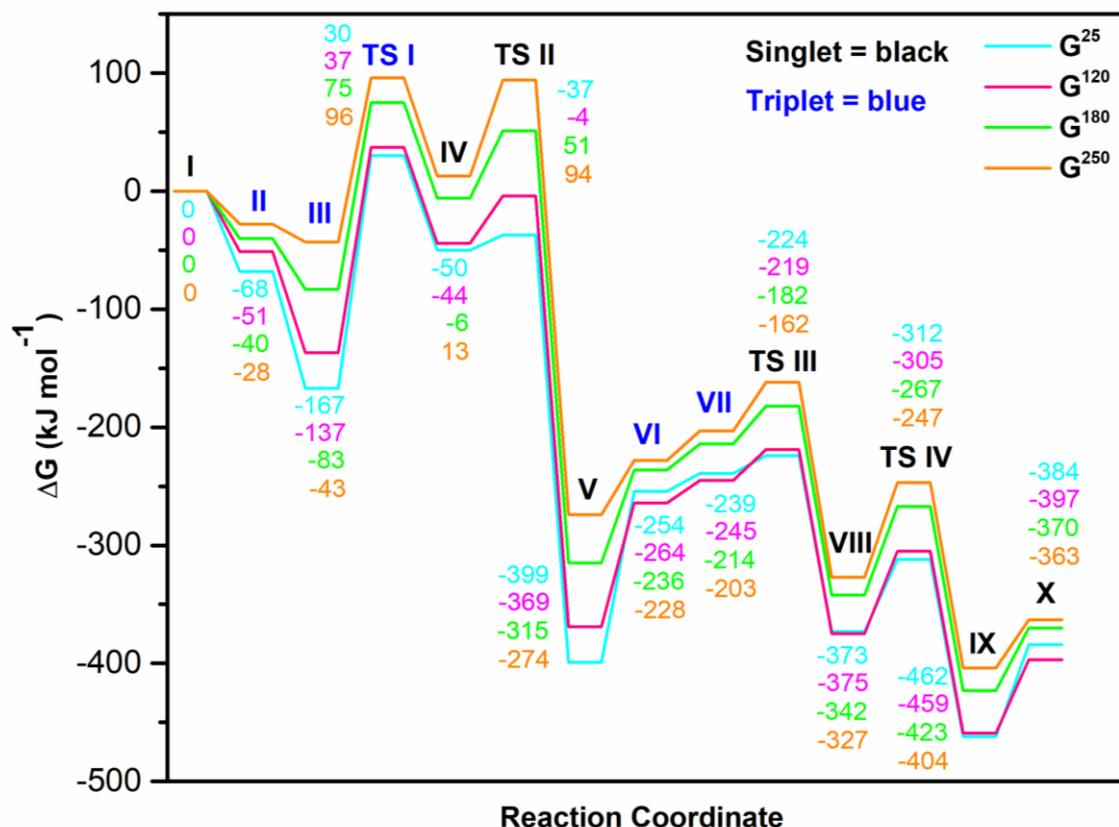


**Figure S15.** The optimized structures of the most stable adsorption of CO, H<sub>2</sub>O, O<sub>2</sub> and H<sub>2</sub> on the Cu<sup>1+</sup> and Cu<sup>2+</sup> sites.



**Figure S16.** The optimized structures of the most stable co-adsorption of O<sub>2</sub>/H<sub>2</sub>O, O<sub>2</sub>/CO and H<sub>2</sub>O/CO on the Cu<sup>1+</sup> and Cu<sup>2+</sup> sites.

We note here that the optimization of CO and O<sub>2</sub> co-adsorption on the Cu<sup>2+</sup> site results in co-adsorption of CO<sub>2</sub> and O<sub>2</sub> on the Cu<sup>1+</sup> site according to the CO oxidation by the adsorbed O<sub>br</sub> atom.

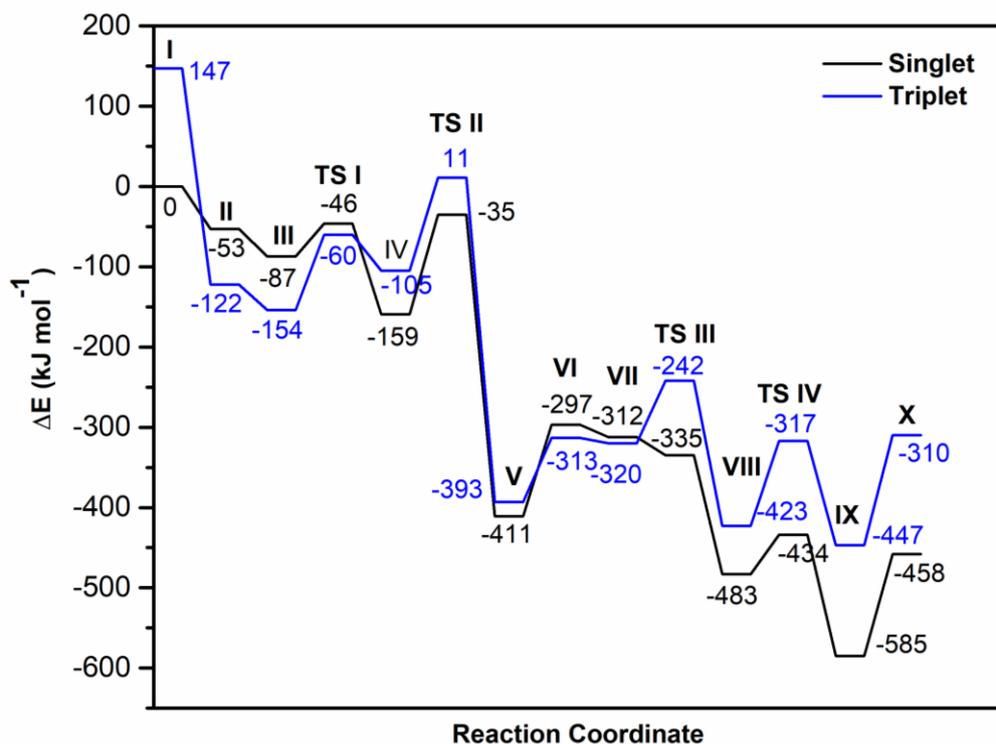


**Figure S17.** Gibbs free energy profile at the temperatures of 25, 120, 180 and 250 °C and 1 atm for the H<sub>2</sub> oxidation by O<sub>2</sub> on the Cu/UiO-66 catalyst.

**Related Discussion to data in Figure S18:** The comparison of relative Gibbs free energy ( $\Delta G$ ) at 25, 120, 180 and 250 °C reveals that both steps of H<sub>2</sub> oxidation are exergonic, similar to that the relative electronic energy ( $\Delta E$ ). Interestingly, the first transition state (TS I) emerges as the rate-determining step, which is in contrast to  $\Delta E$  calculations, where the second transition state (TS II) was predicted to be the rate-determining step. Following the formation of intermediate IV, the reaction appears to progress towards TS II, leading to the formation of intermediate V. Notably, at 250 °C although the formation of intermediate V seems more energetically favorable than H<sub>2</sub>/O<sub>2</sub> co-adsorption (III), the calculated Gibbs free energies for the backward step (83 kJ/mol from IV to III via TSI) is very close to that for the forward step (81 kJ/mol from IV to V via TSII).

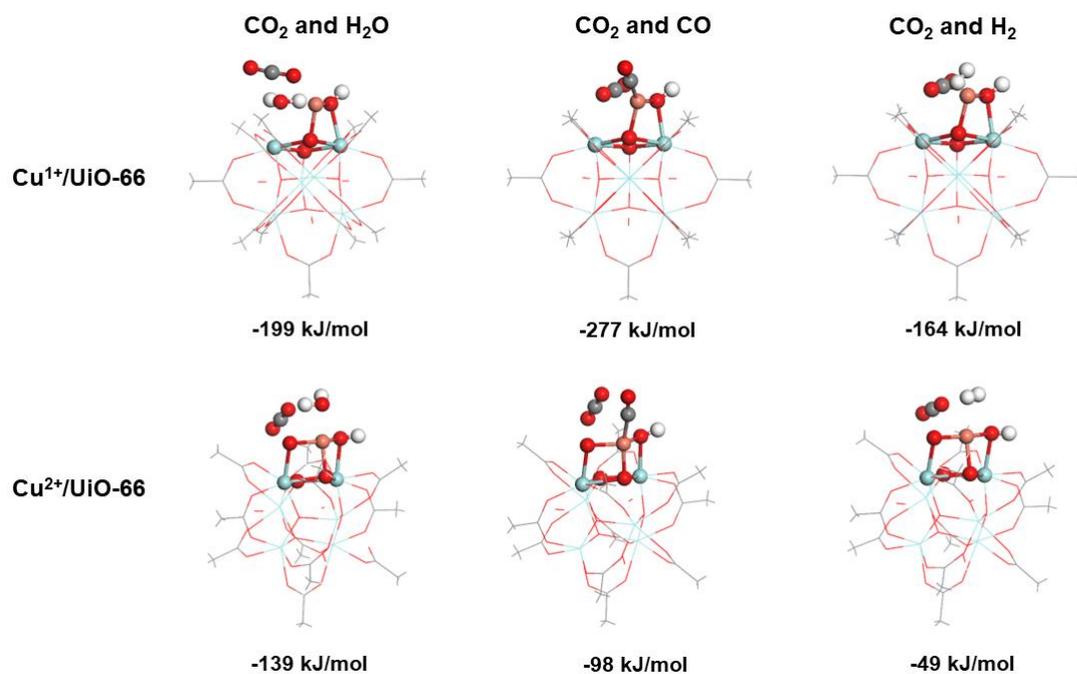
This near equal energy barrier slows down H<sub>2</sub> oxidation, in line with experimental observations discussed in section 3.2 of the main manuscript.

The Gibbs free energy profile also reveals that the adsorption of second H<sub>2</sub> molecule (intermediate VII) is energy-consuming, suggesting the weak adsorption ability of the Cu<sup>2+</sup> sites for H<sub>2</sub>. Furthermore, with increasing temperature the calculated  $\Delta G$  for the second H<sub>2</sub> oxidation become less favorable (-462, -459, -423, and -404 kJ/mol for 25, 120, 180 and 250 °C, respectively). Overall, this computational result suggests the significant effect of temperature on the activity of Cu/UiO-66 catalyst for H<sub>2</sub> oxidation, with higher reaction temperatures leading to reduced activity.



**Figure S18.** Energy profile for H<sub>2</sub> oxidation by O<sub>2</sub> on the Cu/UiO-66 model catalyst. The inserted values are the relative energies ( $\Delta E$ ).

In our study, we considered singlet and triplet spin states. Our calculations showed that the singlet state is the ground spin state for Cu<sup>1+</sup> (intermediate **I**) with the triplet state being 147 kJ/mol higher in energy. During the reaction, spin state changes occurred. Following O<sub>2</sub> adsorption, the spin state changed from singlet to triplet and then returned to singlet after the first transition state **TS I**. During the first H<sub>2</sub> oxidation step (intermediate **VI**), a spin state change from singlet to triplet occurred, suggesting the oxidation of Cu<sup>1+</sup> to Cu<sup>2+</sup>. Then the spin state returned to singlet for the second H<sub>2</sub> oxidation step (from **TS III** to **X**), signifying the change in the oxidation state of Cu active site from +2 to +1.



**Figure S19.** The optimized structures of the most stable co-adsorption of CO<sub>2</sub>/H<sub>2</sub>O, CO<sub>2</sub>/CO and CO<sub>2</sub>/H<sub>2</sub> on the Cu<sup>1+</sup> and Cu<sup>2+</sup> sites.