# Supporting Information

Structure identification and mechanism exploration of ultralow-content of metal-

doped Cu for efficient electrochemical production of ammonia in dilute nitrate

concentrations

Jiayu Zhan, Lu-Hua Zhang, Yaohua Hong, and Fengshou Yu\*

National-Local Joint Engineering Laboratory for Energy Conservation in Chemical Process Integration and Resources Utilization, School of Chemical Engineering and Technology, Hebei University of Technology, Tianjin 300130 (P. R. China) E-mail: <u>yfsh@hebut.edu.cn</u> (F. Yu)

#### **Experimental Process**

### Chemicals

Ferric trichloride (FeCl<sub>3</sub>), sodium hydroxide (NaOH), sodium Nitrate (NaNO<sub>3</sub>) were purchased from aladdin. Sodium sulfate (Na<sub>2</sub>SO<sub>4</sub>), sodium dihydrogen phosphate (NaH<sub>2</sub>PO<sub>4</sub>), disodium hydrogen phosphate (Na<sub>2</sub>HPO<sub>4</sub>) were purchased from Bide Pharmatech Ltd. Cobalt nitrate hydrate (Co(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O), copper nitrate hydrate (Cu(NO<sub>3</sub>)<sub>2</sub>·3H<sub>2</sub>O) were purchased from Macklin. Nickel nitrate hydrate (Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O) was purchased from DAMAO. All samples require no further purification before application.

#### Synthesis of Fe-CuO precursors

The ultra-low content Fe was doped into CuO nanosheet by a simple solvothermal method<sup>1</sup>. Specifically, 4.1 mg FeCl<sub>3</sub> was dissolved in 4 mL of anhydrous ethanol, followed by the addition of 1208 mg Cu(NO<sub>3</sub>)<sub>2</sub>·3H<sub>2</sub>O. Then 40 mL of deionized water at 0 °C was added forming a homogeneous solution under stirring. Subsequently, 10 mL of 1.2 M NaOH solution was added by dropping in 1 min and stirred vigorously for 15 min. Then the mixture was transferred into a 100 mL Teflon-lined stainless steel autoclave, and heated at 130 °C for 2 h. After cooling to room temperature, the production was collected by diafiltration and washed three times with water and ethanol, then dried under vacuum at 60 °C overnight. The Co- and Ni-doped CuO were also obtained by a similar method with Co and Ni precursors, respectively.

#### Characterization

UV-Vis detection of ion concentrations was carried out with TU-1900. XRD patterns were collected on a JEMARM300F microscope. SEM images were taken on Czech TESCAN MIRA LMS. XPS spectroscopy was performed on a Thermo Scientific ESCALAB 250X. <sup>1</sup>H NMR was used to test the isotope labeling experiments on a BRUKER AVANCE 400.

#### **Electrochemical Testing**

The electrochemical investigations were carried out with the CHI760E electrochemical workstation. 4 mg of catalyst was ultrasonically for 5 min with 950  $\mu$ L of a mixture of ethanol and water (1:1), followed by adding 50  $\mu$ L of Nafion

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solution with 30 min sonication. Then 50 µL of catalyst ink was dropped evenly on the carbon paper and the catalyst loading was 0.2 mg cm<sup>-2</sup>. The H-type electrolytic cell was adopted for electrocatalytic nitrate reduction reaction (NO<sub>3</sub><sup>-</sup>RR). The 1 cm<sup>2</sup> carbon paper (with catalyst) was applied as the working electrode, Ag/AgCl as the reference electrode, and platinum wire as the counter electrode. The obtained Fe-CuO precursors were in-situ reduced to Fe-Cu during the NO<sub>3</sub><sup>-</sup>RR process. Postelectrolysis samples were protected by Ar before characterisation.

## <sup>15</sup>N Isotope Labeling Experiments

The isotopic labeling  $NO_3$ -RR experiments were carried out using the aforementioned electrochemical methods with  $Na^{15}NO_3$  as N-source. Subsequently, 500 µL of the electrolyte was blended with 200 µL of d<sup>6</sup>-DMSO for <sup>1</sup>H NMR measurement.

### Computation of conversion rate, yield and Faraday efficiency (FE)

The conversion of  $NO_3^-$  was computed by Eq. (1):

$$NO_{3}^{-} \text{ conversion} = \Delta C_{NO_{3}}^{-}/C_{0} \times 100\%$$
 (1)

The yield of  $NH_4^+$  was computed by Eq. (2):

$$Yield_{NH_4^+} = (C_{NH_4^+} \times V)/(M_{NH_4^+} \times t \times m)$$
(2)

The FE was computed by Eq. (3) and (4):

$$FE_{NH_4^+} = (8 \times F \times c \times v) / (M_{NH_4^+} \times Q)$$
(3)

$$FE_{NH_4^+} = (2 \times F \times c \times v) / (M_{NH_4^+} \times Q)$$
(4)

where  $\Delta C_{NO_3^-}$  is the change in NO<sub>3</sub><sup>-</sup> concentration before and after electrolysis, C<sub>0</sub> is the onset concentration of NO<sub>3</sub><sup>-</sup>, C<sub>NH4</sub><sup>+</sup> is the concentration of NH<sub>4</sub><sup>+</sup>(aq.), C<sub>NO2</sub><sup>-</sup> is the concentration of NO<sub>2</sub><sup>-</sup> (aq.), V is the electrolyte volume (30 mL), t is the electrolysis time, m is the mass of catalyst, F is the Faradaic constant (96485 C mol<sup>-1</sup>), and Q is the total charge passing the electrode.

## **DFT calculations**

The DFT calculations were performed by Vienna Ab initio Simulation Package (VASP)<sup>2, 3</sup> with the projector augmented wave (PAW) method<sup>4</sup>. The generalized gradient approximation (GGA) of Perdew-Burke-Ernzerhof (PBE)<sup>5</sup> functional was applied to treat the exchange-functional. Dispersion forces have been calculated based on Grimme's D3 parameters<sup>6</sup>. The energy cutoff for the plane wave basis expansion was set to 450 eV and the force on each atom less than 0.02 eV/Å was set for convergence criterion of geometry relaxation. The Brillouin zone integration is treated using  $3\times3\times1$  k-point sampling. The self-consistent calculations apply a convergence energy threshold of  $10^{-5}$  eV. A  $4\times4$  layer of Cu (111) supercell was built as a model catalyst. To prevent interaction between periodic structures, a vacuum of 20 Å was added along the z direction. We explored the effect of solvation effects on reaction pathways using an implicit solvation model.

The binding strength of different configurations for Fe-Cu catalysts was determined by the binding energy, which is defined as:

$$\Gamma_a = E_{Fe-Cu} - E_{Cu} - E_{Fe}$$

where  $E_{Fe-Cu}$ ,  $E_{Cu}$ ,  $E_{Fe}$  are total energies of Fe-doped Cu (111), of Cu (111) slab, and of a single Fe, respectively. In general, the catalyst is thermodynamically more stable when  $\Gamma_a$  is more negative (Table S4). According to DFT calculations, Fe is most stable located at the centre of the Cu surface.

The Gibbs free energy change ( $\Delta$ G) was used to determine the different adsorption modes and active sites. In general, reaction intermediates are more easily adsorbed with lower  $\Delta$ G (Table S5).

The binding energy to determine the different adsorption sites of \*H on Fe-Cu, which is defined as:

$$\Gamma_b = E_{Fe(H)Cu} - E_{FeCu} - E_H; \Gamma = E_{FeCu(H)} - E_{FeCu} - E_H$$

where  $E_{Fe(H)Cu}$ ,  $E_{FeCu(H)}$ ,  $E_{FeCu}$ ,  $E_{H}$  are total energies of H adsorbed on the Fe atom, on Cu, FeCu slab, and a single H atom, respectively. Our DFT calculations show that \*H prefers to adsorb on Fe sites (Table S6).

The free energies of the NO<sub>3</sub>-RR were calculated by the equation:  $\Delta G = \Delta E_{DFT} + \Delta E_{ZPE} - T\Delta S$ , where  $\Delta E_{DFT}$  represents the DFT electronic energy difference of every steps. The corrections for zero-point energy ( $\Delta E_{ZPE}$ ) and entropy variation ( $\Delta S$ ) were obtained through VASPKIT. The calculations were performed at a temperature of T = 298.15 K



Figure S1. Procedure for Fe-Cu synthesis.



**Figure S2.** a) TEM and b) high-resolution TEM images of Fe-Cu sample obtained by *in situ* electrochemical reconstitution.



Figure S3. Wide-survey XPS spectra of a) Fe-CuO and b) pure CuO.



Figure S4. Fe 2p XPS spectra of a) Fe-CuO and b) Fe-Cu.



Figure S5. a) Ultraviolet absorption and b) concentration-absorbance calibration

## curves of $NH_4^+$ .



Figure S6. a) Ultraviolet absorption and b) concentration-absorbance calibration

curves of NO<sub>3</sub><sup>-</sup>.



Figure S7. a) Ultraviolet absorption and b) concentration-absorbance calibration

curves of NO<sub>2</sub><sup>-</sup>.







**Figure S9.** FE of  $NH_4^+$ ,  $H_2$  and  $NO_2^-$  productions with a) Cu, b)  $Fe_{0.25\%}$ -Cu, c)  $Fe_{0.5\%}$ -Cu,

and d) Fe<sub>0.75%</sub>-Cu electrodes.



**Figure S10.** FE of  $NH_4^+$ ,  $H_2$  and  $NO_2^-$  productions with a) Cu, b) Fe/Cu, and c) Fe-Cu electrodes.



**Figure S11.** FE of  $NH_4^+$ ,  $H_2$  and  $NO_2^-$  products with a) Co-Cu and b) Ni-Cu.



Figure S12. Cu 2p XPS spectra for a) Co-Cu and b) Ni-Cu; c) Co 2p XPS spectra of Co-

Cu; d) Ni 2p XPS spectra of Ni-Cu.



Figure S13. XRD pattern for Co-Cu and Ni-Co.



Figure S14. CV curves at various scan rates of a) Cu and b) Fe-Cu; c) the corresponding  $C_{dl}$  by ECSA of Cu and Fe-Cu samples; d) ECSA normalized LSV of Cu

and Fe-Cu samples.



Figure S15. <sup>1</sup>H NMR spectra of the electrolyte after the NO<sub>3</sub><sup>-</sup> reduction at -0.6 V for 2 h with Na<sup>14</sup>NO<sub>3</sub><sup>-</sup> and Na<sup>15</sup>NO<sub>3</sub><sup>-</sup> as N-source, respectively.



Figure S16. In situ Raman spectra for local magnification of Fe-Cu.



Figure S17. In situ Raman spectra of  $NO_3$ -RR with CuO catalyst in 0.5 M  $Na_2SO_4$  and 0.1 M PBS (with 0.1 M  $NO_3$ -N)



**Figure S18.** The integration area of  $NH_2OH$  and  $NO_2^-$  (left Cu and right is Fe-Cu).



Figure S19. Gibbs free energy diagram of  $NO_3^-$  to  $*NO_2H$  conversion calculated with the solvation effect

Sample	(wt. %)	(at. %)
Fe-CuO	0.26	0.32
Fe-Cu	0.22	0.43

Table S1. The contents of Fe in Fe-CuO and Fe-Cu determined by ICP-MS

Table S2. The contents of Fe in Fe $_{0.25\%}$ -Cu, Fe $_{0.5\%}$ -Cu and Fe $_{0.75\%}$ -Cu determined by

	ICP-MS	
Sample	(wt. %)	(at. %)
Fe <sub>0.25%</sub> -Cu	0.10	0.26
Fe <sub>0.5%</sub> -Cu	0.22	0.43
Fe <sub>0.75%</sub> -Cu	0.31	0.61

**Table S3.** Comparison of NH<sub>4</sub><sup>+</sup> yield rate by NO<sub>3</sub><sup>-</sup>RR on various catalysts.

Catalysts	Electrolyte	Potential (vs. RHE)	NH₃ yield rate (mmol h⁻¹ g <sub>cat</sub> ⁻¹)	Ref.
Fe-Cu	100 ppm NO <sub>3</sub> <sup>-</sup> -N,	-0.9 V	323.1	This work
	$0.5 \text{ IVI Na}_2 SO_4$			
	100 ppm NO <sub>3</sub> <sup>-</sup> -N,	-1 0 V	07.2	7
	0.5 M Na <sub>2</sub> SO <sub>4</sub>	-1.0 V	57.5	
CuBc@Myono	50 ppm NO₃ <sup>-</sup> -N,	-1.06 V	84.7	8
CuPC@Ivixene	0.5 M Na <sub>2</sub> SO <sub>4</sub>			-
Plasma	50 ppm NO₃⁻-N,	0 5 0 1/	82.0	9
treated $Cu_2O$	$0.5 \text{ M} \text{ Na}_2 \text{SO}_4$	-0.58 V	83.0	5
Pd-Cu <sub>2</sub> O	50 ppm NO₃⁻-N,	1 2 1/		10
CEO	0.5 M Na <sub>2</sub> SO <sub>4</sub>	-1.3 V	54.4	10
TiO <sub>2-X</sub>	50 ppm NO₃⁻-N,	07414	45.0	11
	0.5 M Na <sub>2</sub> SO <sub>4</sub>	-0.74 V		11
10Cu/TiO <sub>2-X</sub>	200 ppm NO₃⁻-N,	0.75.1	1110	12
	0.5 M Na <sub>2</sub> SO <sub>4</sub>	-0.75 V	114.3	12

# **Table S4.** Binding energies ( $\Gamma$ ) of Fe doping at different sites of Cu (111).

	On Surface		
	Centre	Edge	Corner
Γ (kJ/mol)	-301	-289	-298
Structure			
	On Subsurface		

	First Subsurface Layer	Second Subsurface Layer
Γ (kJ/mol)	-276	-269
Structure		

**Table S5.** Dependence of  $\Delta G$  for NO<sub>3</sub><sup>-</sup> adsorption on the adsorption site and the corresponding structure.

	Bridge adsorption		
Adsorption sites	Cu	Cu and Fe	
$\Delta$ G (eV)	0.79	0.85	
Structure			
	top adsorption		
Adsorption sites	Cu	Fe	
$\Delta$ G (eV)	1.22	1.38	
Structure			

**Table S6.** Binding energies ( $\Gamma$ ) of \*H at different sites of Fe and Cu.

	*H occupies the Fe	*H occupies the Cu
Г (kJ/mol)	-353	-344

Structure



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