

## Supplementary Information

### Effects of Catalyst Morphology on Oxygen Defects at Ni-CeO<sub>2</sub> Interfaces for CO<sub>2</sub> Methanation

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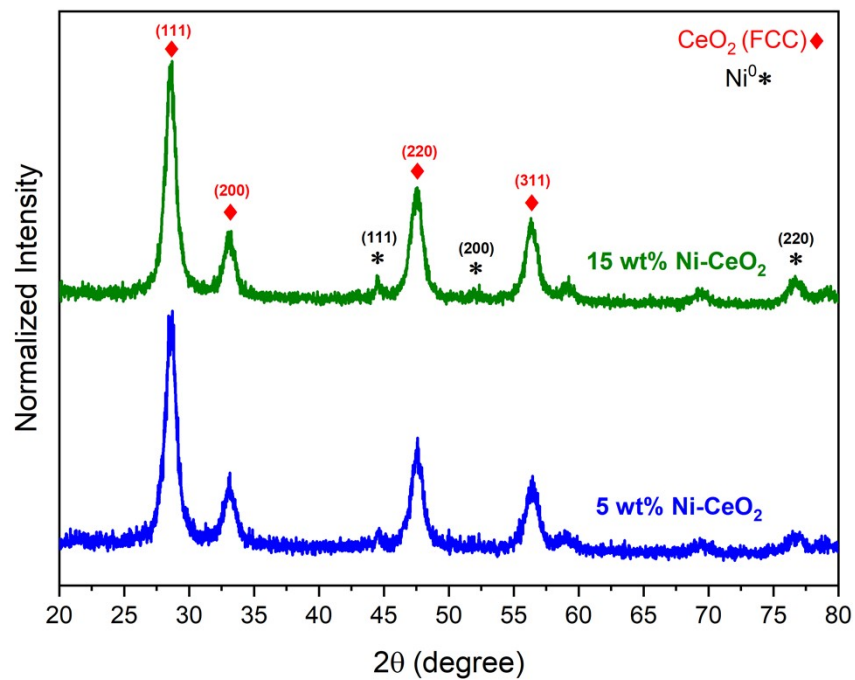


Figure S1. XRD patterns of 5 wt% and 15 wt% Ni-CeO<sub>2</sub> catalysts showing the increase in the Ni (111) peak intensity as a function of Ni loading.

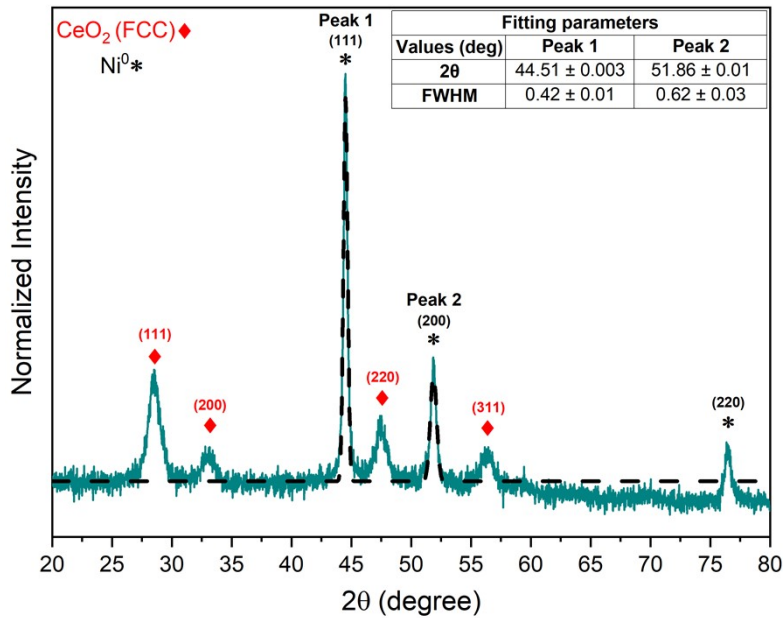


Figure S2. XRD pattern for the 60 wt% Ni-CeO<sub>2</sub> catalyst along with the fitting parameters (inset table) obtained for the Ni(111) and Ni(200) peaks post Gaussian peak fitting.

The Ni crystallite size was determined by averaging the absolute crystallite sizes (D) obtained from the (111) and (200) Ni peaks using the Scherrer equation –

$$D \text{ (nm)} = \frac{k \lambda}{\beta \cos \theta}$$

The shape factor or (k) and X-ray wavelength ( $\lambda$ ) were assumed to be 0.9 and 0.15 nm, respectively. The full width half maximum (FWHM,  $\beta$ ) and diffraction angle ( $\theta$ ) in radians were obtained from Gaussian fitting of the diffraction peaks and are presented in the inset table in Fig S2.

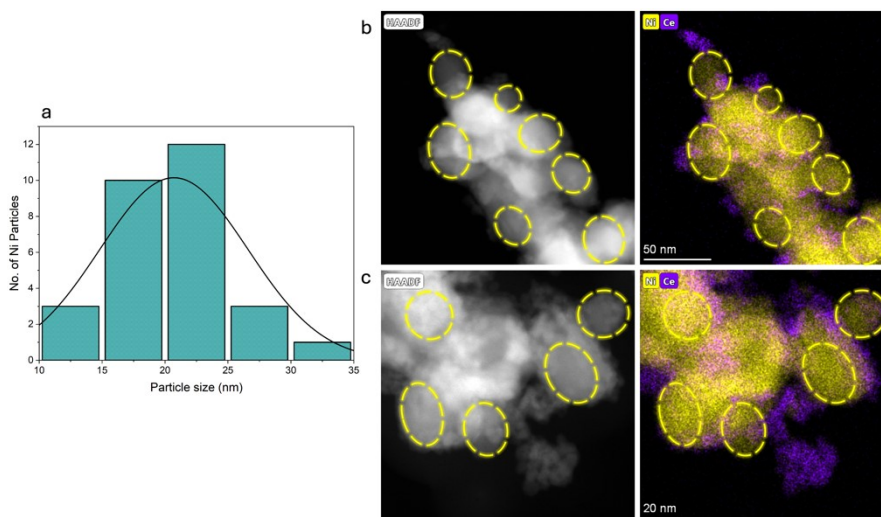


Figure S3. (a) Size distribution histogram for 60wt% Ni-CeO<sub>2</sub> catalyst obtained by measuring 30 Ni NPs. (b, c) HAADF-STEM images along with EDS elemental mapping for 60 wt% Ni-CeO<sub>2</sub> catalyst outlining the Ni particles (yellow dashes) measured for particle size distribution.

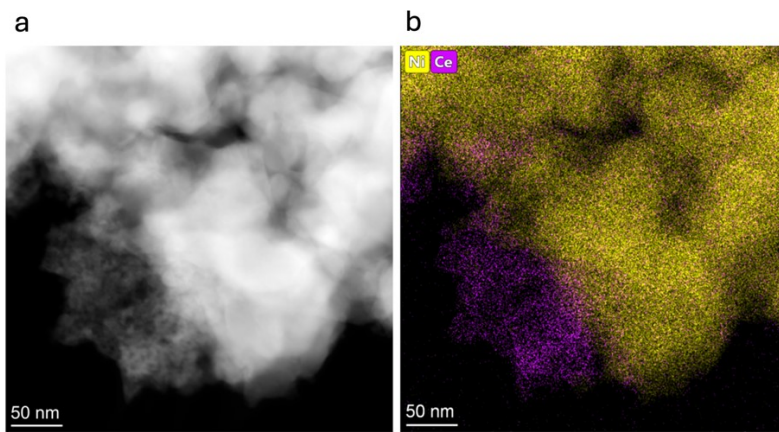


Figure S4. (a) HAADF-STEM image and (b) EDS elemental mapping of 40 wt% Ni-CeO<sub>2</sub> catalyst depicting an inverse catalytic structure.

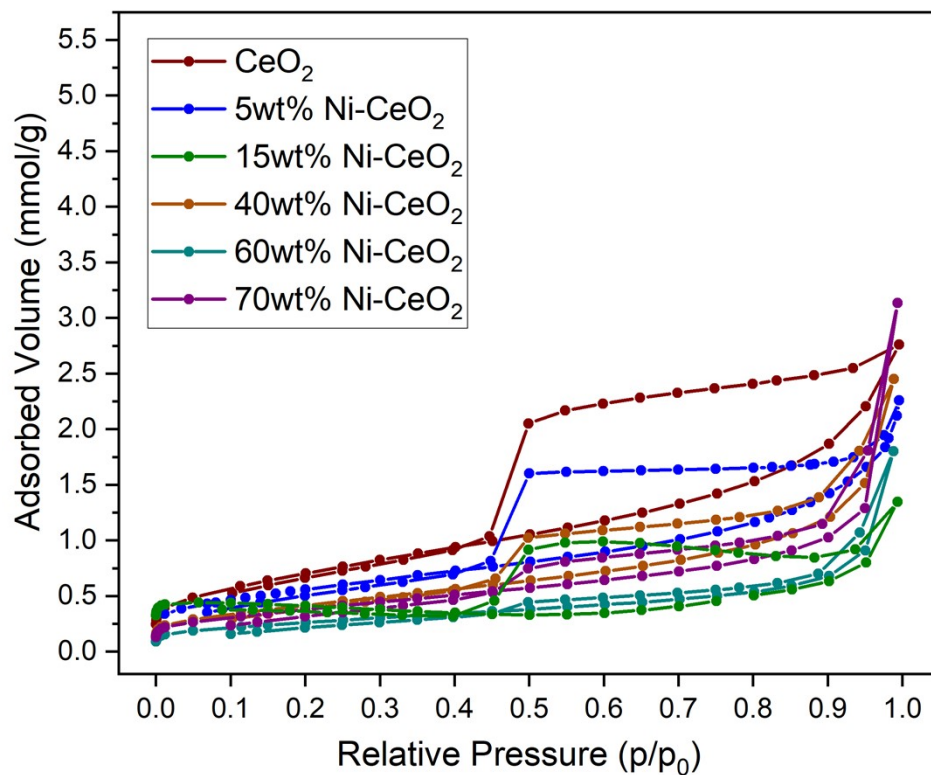


Figure S5. Nitrogen adsorption-desorption isotherms for X wt% Ni-CeO<sub>2</sub> catalysts (where X = 5, 15, 40, 60, 70).

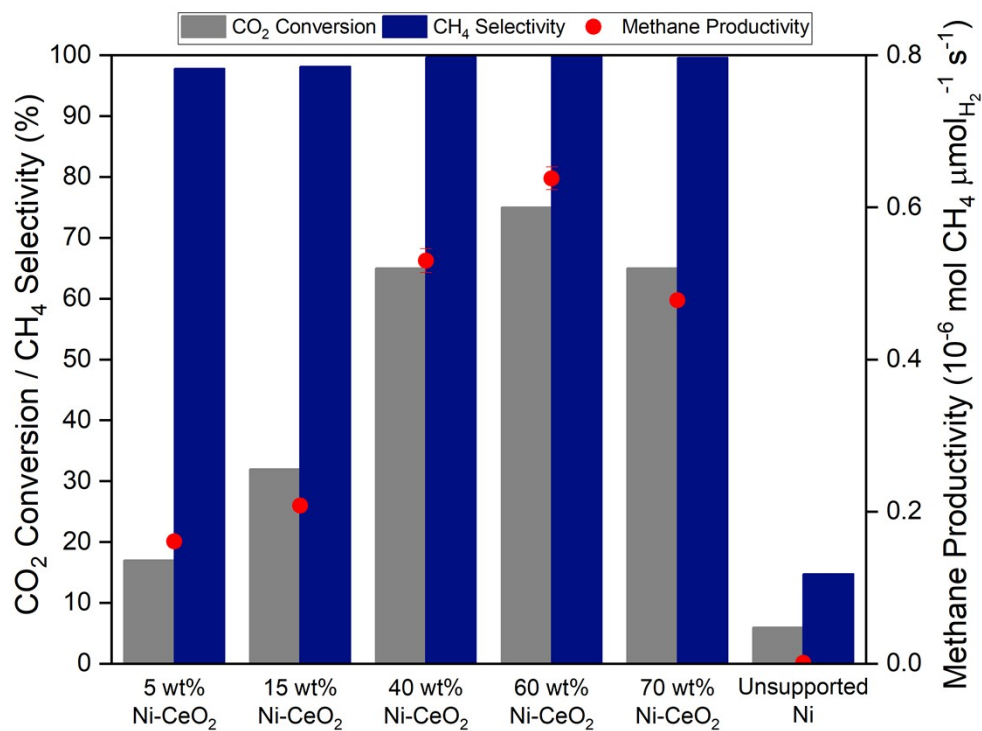


Figure S6. Catalytic performance for CO<sub>2</sub> methanation over X wt% Ni-CeO<sub>2</sub> catalysts (where X = 5, 15, 40, 60, 70) at 275°C. Methane productivity is normalized with respect to μmoles of H<sub>2</sub> adsorbed based on H<sub>2</sub> pulse chemisorption. Reaction conditions: P = 1 atm, GHSV = 15,000 mL g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>, T = 275°C, H<sub>2</sub>/CO<sub>2</sub> = 4.

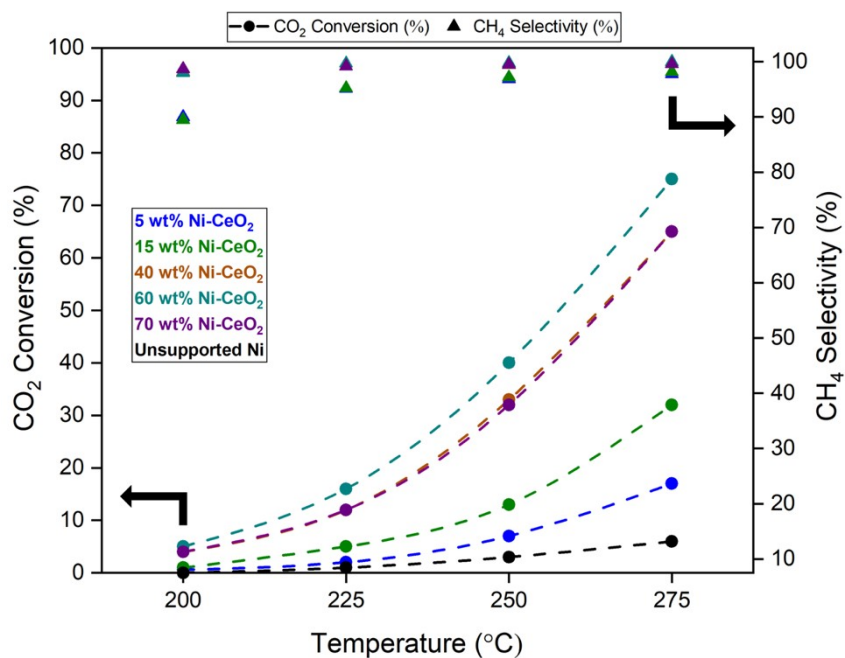


Figure S7. Catalytic performance of X wt% Ni-CeO<sub>2</sub> catalysts (where X = 5, 15, 40, 60, 70) in CO<sub>2</sub> methanation. Reaction conditions: P = 1 atm, GHSV = 15,000 mL g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>, H<sub>2</sub>/CO<sub>2</sub> = 4, T = 200-275°C.



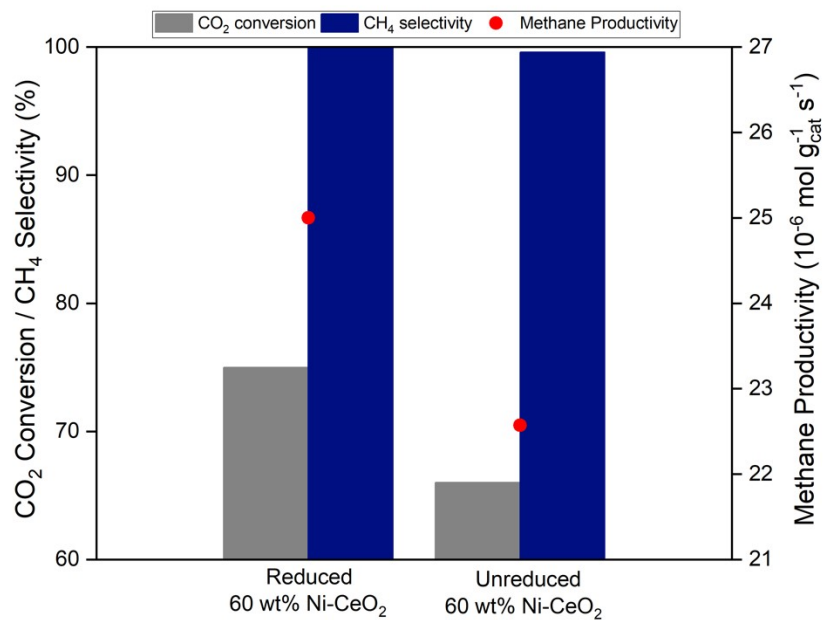


Figure S8. Catalytic performance of inverse 60 wt% Ni-CeO<sub>2</sub> catalyst reduced in-situ prior to catalytic testing at 425 °C (5°C/min ramp, 4 h hold) under a flow of H<sub>2</sub> at 40 mL/min and the unreduced catalyst post ex-situ calcination at 400 °C (5°C/min ramp, 3 h hold). Reaction conditions: P = 1 atm, GHSV = 15,000 mL g<sub>cat</sub><sup>-1</sup>h<sup>-1</sup>, T = 275 °C, H<sub>2</sub>/CO<sub>2</sub> = 4.

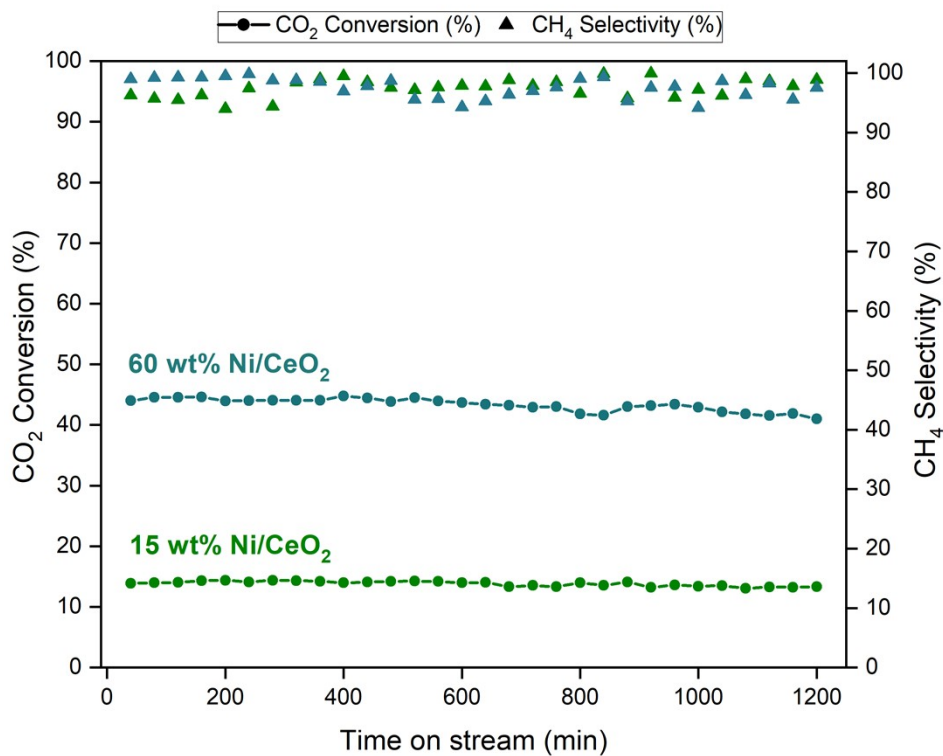


Figure S9. Stability test of the best performing inverse 60 wt% Ni-CeO<sub>2</sub> and supported 15 wt% Ni-CeO<sub>2</sub> catalyst. Reaction conditions: P = 1 atm, GHSV = 15,000 mL g<sub>cat</sub><sup>-1</sup>h<sup>-1</sup>, T = 250 °C, H<sub>2</sub>/CO<sub>2</sub> = 4.

Table S1. Intensity ratios of D<sub>1</sub> and F<sub>2g</sub> peaks obtained from Raman studies of Ni-CeO<sub>2</sub>

<b>Entries</b>	<b>Catalyst</b>	<b>I<sub>D1</sub>/I<sub>F2g</sub></b>
1	5 wt% Ni-CeO <sub>2</sub>	0.29
2	15 wt% Ni-CeO <sub>2</sub>	0.57
3	40 wt% Ni-CeO <sub>2</sub>	0.64
4	60 wt% Ni-CeO <sub>2</sub>	1.30
5	70 wt% Ni-CeO <sub>2</sub>	0.96
6	60 wt% Ni 1 wt% Gd-CeO <sub>2</sub>	1.16
7	60 wt% Ni 1 wt% La-CeO <sub>2</sub>	1.58
8	60 wt% Ni 1 wt% Pr-CeO <sub>2</sub>	1.90

catalysts.

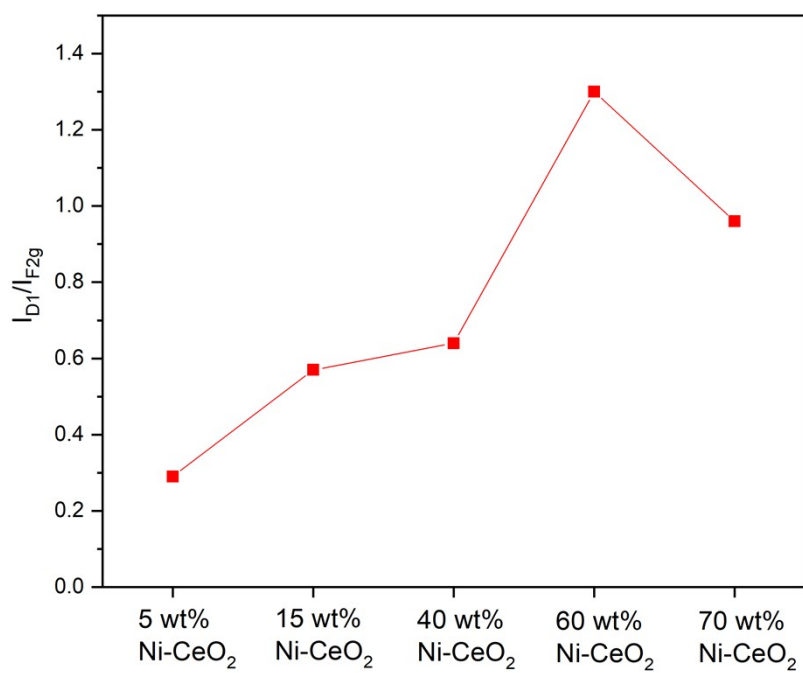


Figure S10. Intensity ratios of the Raman D<sub>1</sub> to F<sub>2g</sub> bands ( $I_{D1}/I_{F2g}$ ) as a function of Ni loading in Ni-CeO<sub>2</sub> catalysts.

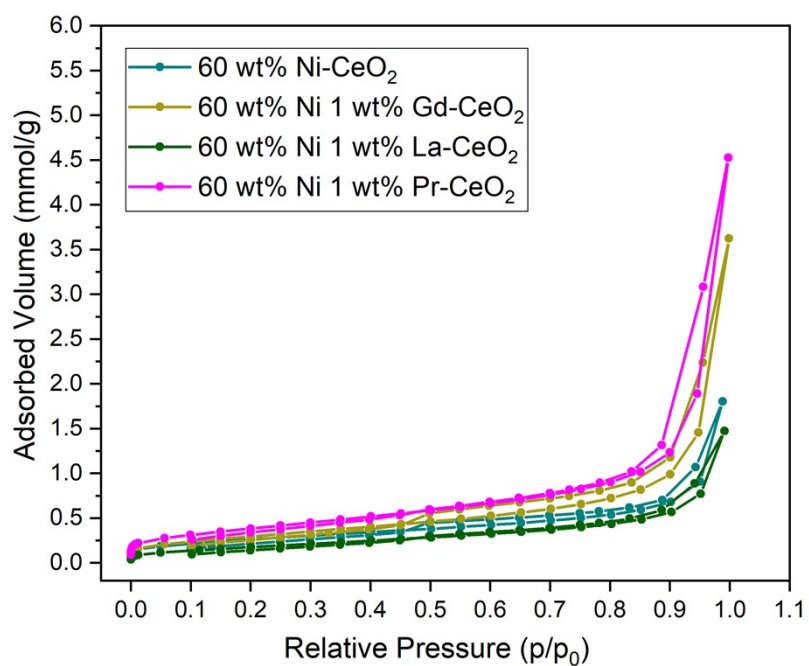


Figure S11. Nitrogen adsorption-desorption isotherms for 1 wt% Pr, La, or Gd doped 60 wt% Ni-CeO<sub>2</sub> and 60 wt% Ni-CeO<sub>2</sub> catalysts.

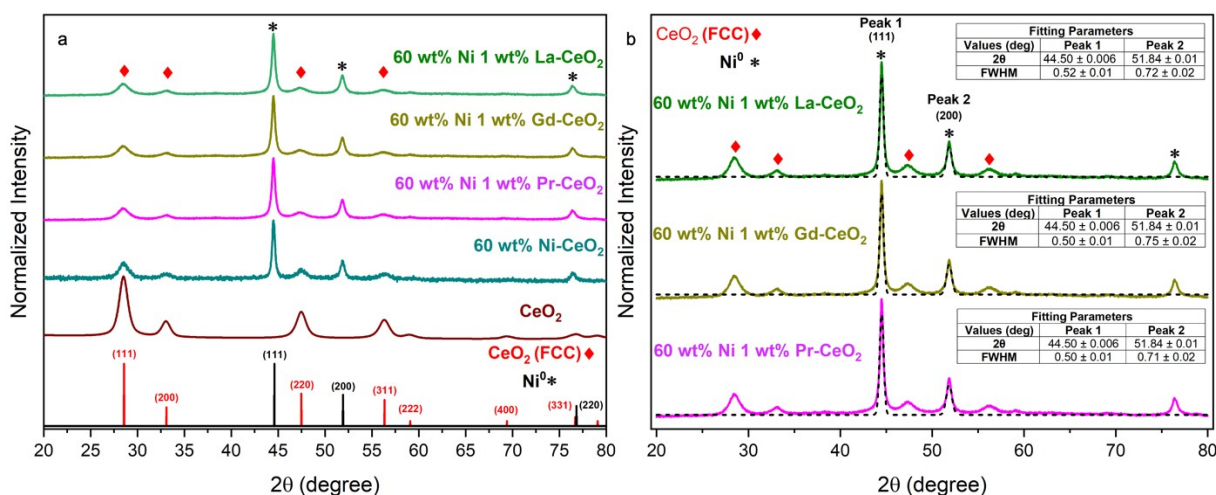


Figure S12. (a) XRD pattern of 60 wt% Ni-CeO<sub>2</sub>, 1 wt% Pr, La, or Gd doped 60 wt% Ni-CeO<sub>2</sub>, and CeO<sub>2</sub>. (b) XRD pattern for the 1 wt% Pr, La, and Gd doped 60 wt% Ni-CeO<sub>2</sub> catalyst along with the fitting parameters (inset tables) obtained for the Ni(111) and Ni(200) peaks post Gaussian peak fitting.

The Ni crystallite size was determined by averaging the absolute crystallite sizes (D) obtained from the (111) and (200) Ni peaks using the Scherrer equation –

$$D \text{ (nm)} = \frac{k \lambda}{\beta \cos \theta}$$

The shape factor or (k) and X-ray wavelength ( $\lambda$ ) were assumed to be 0.9 and 0.15 nm, respectively. The full width half maximum (FWHM,  $\beta$ ) and diffraction angle ( $\theta$ ) in radians were obtained from Gaussian fitting of the diffraction peaks and are presented in the inset table in Fig S12.

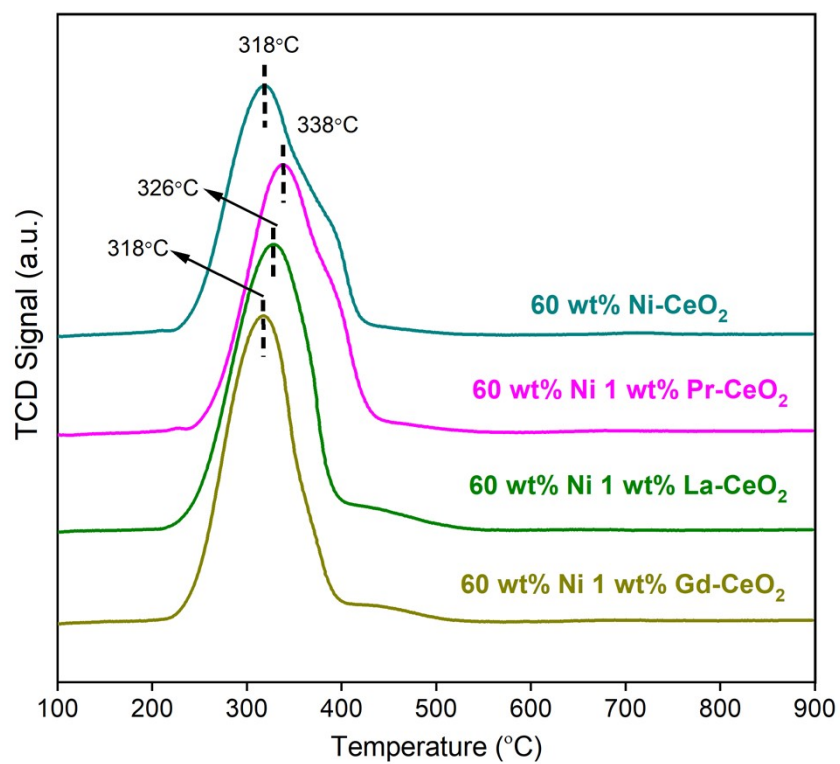


Figure S13. H<sub>2</sub>-TPR profiles for 1 wt% Pr, La, or Gd doped 60 wt% Ni-CeO<sub>2</sub> and 60 wt% Ni-CeO<sub>2</sub>.

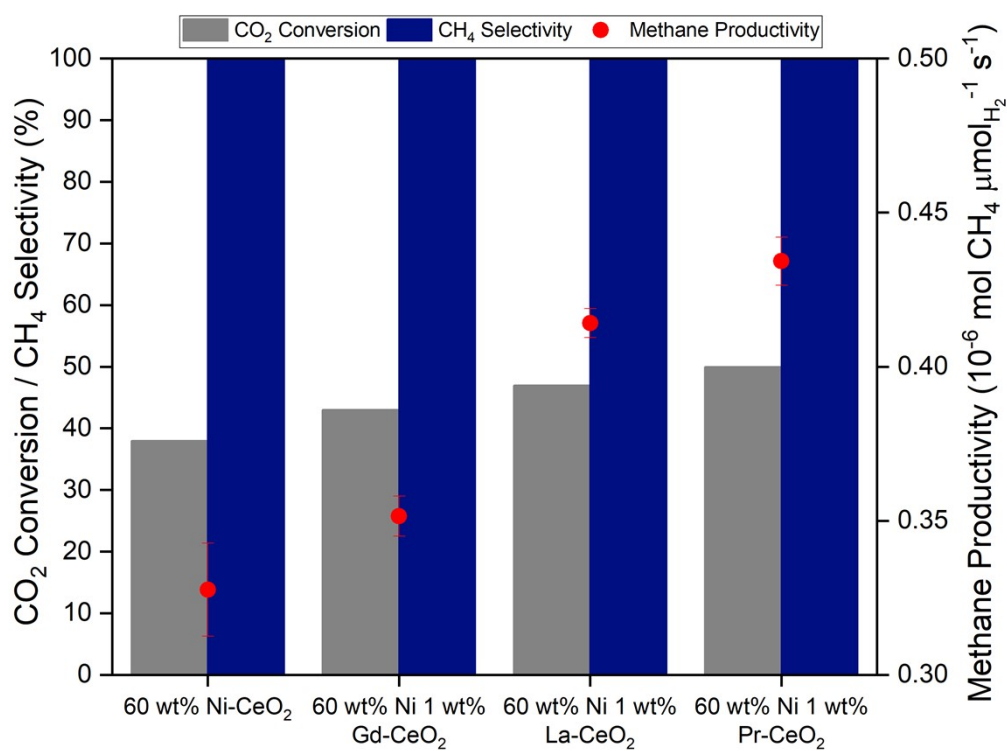


Figure S14. Catalytic performance for CO<sub>2</sub> methanation over 1 wt% Pr, La, or Gd doped 60 wt% Ni-CeO<sub>2</sub> and 60 wt% Ni-CeO<sub>2</sub> at 250°C. Methane productivity is normalized with respect to μmoles of H<sub>2</sub> adsorbed based on H<sub>2</sub> pulse chemisorption. Reaction conditions: P = 1 atm, GHSV = 15,000 mL g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>, T = 250°C, H<sub>2</sub>/CO<sub>2</sub> = 4.



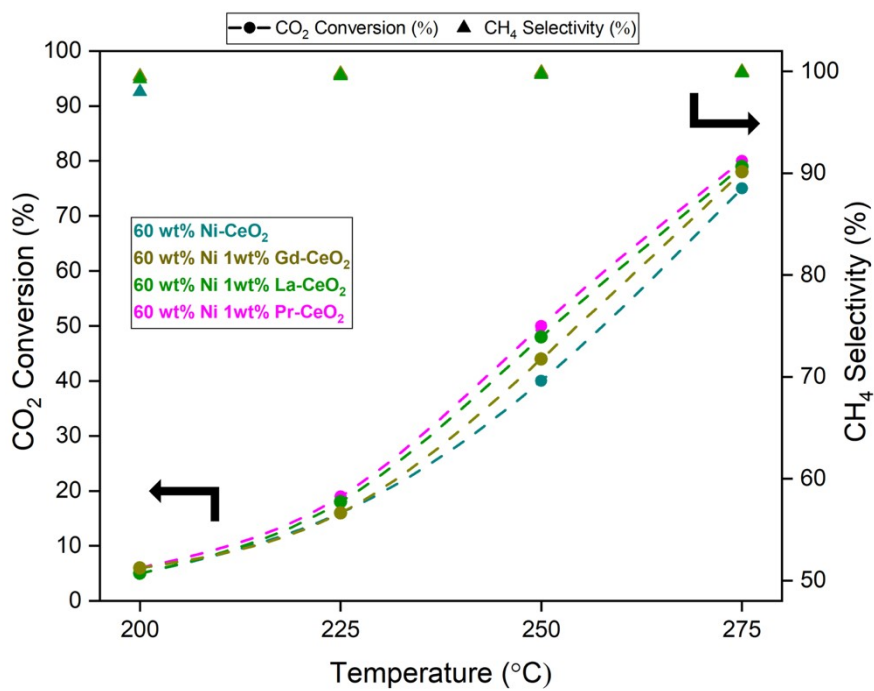


Figure S15. Catalytic performance of 1 wt% Pr, La, or Gd doped 60 wt% Ni-CeO<sub>2</sub> and 60 wt% Ni-CeO<sub>2</sub> in CO<sub>2</sub> methanation. Reaction conditions: P = 1 atm, GHSV = 15,000 mL g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>, H<sub>2</sub>/CO<sub>2</sub> = 4, T = 200-275°C.

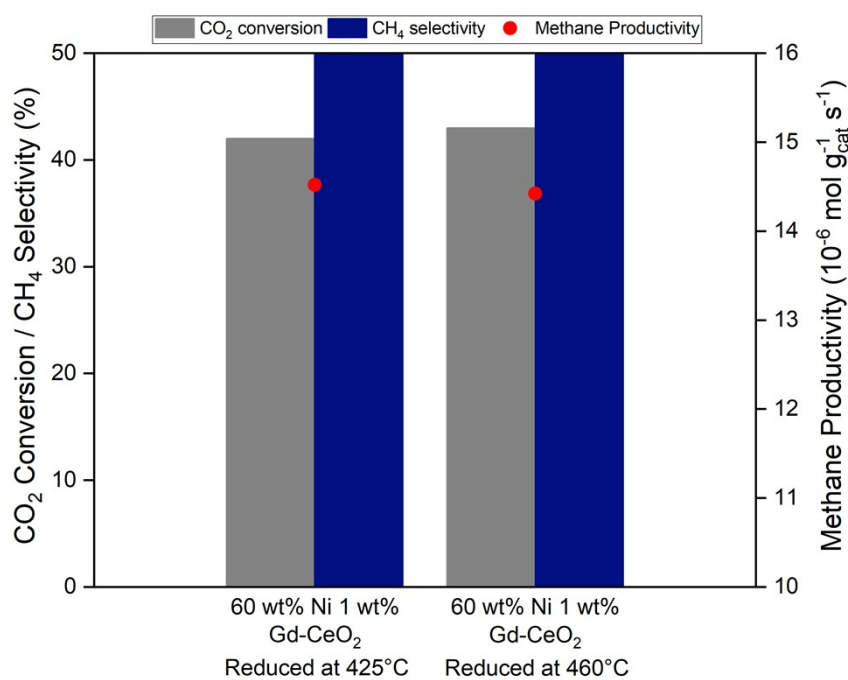


Figure S16. CO<sub>2</sub> conversion/CH<sub>4</sub> selectivity and methane productivity (secondary y-axis) of 60 wt% Ni 1 wt% Gd-CeO<sub>2</sub> reduced in situ at 425°C and 460°C (5°C/min ramp, 4 h hold) under a flow of H<sub>2</sub> at 40 mL/min prior to catalytic testing. Reaction conditions: P = 1 atm, GHSV = 15,000 mL g<sub>cat</sub><sup>-1</sup>h<sup>-1</sup>, T = 250 °C, H<sub>2</sub>/CO<sub>2</sub> = 4.

The natural log of the Arrhenius equation was used to determine the apparent activation energy for methane formation as shown below:

$$\ln(k) = -\frac{E_A}{R}\left(\frac{1}{T}\right) + \ln(A)$$

Where  $k$  represents the reaction rate constant which scales with the rate of methane formation,  $A$  is the preexponential or frequency factor,  $E_A$  is the activation energy,  $R$  is the ideal gas constant ( $8.3145 \text{ J K}^{-1} \text{ mol}^{-1}$ ) and  $T$  is the temperature.

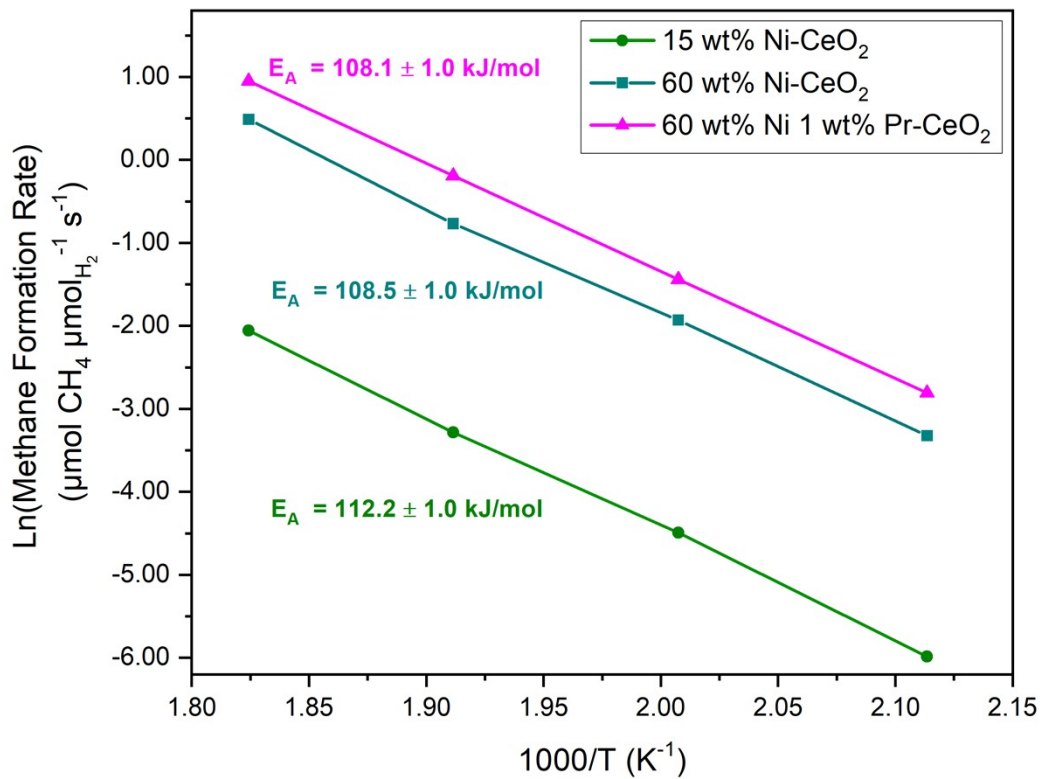


Figure S17. Arrhenius plot for 15 wt% Ni-CeO<sub>2</sub>, 60 wt% Ni-CeO<sub>2</sub>, and 60 wt% Ni 1 wt% Pr-CeO<sub>2</sub> catalysts.