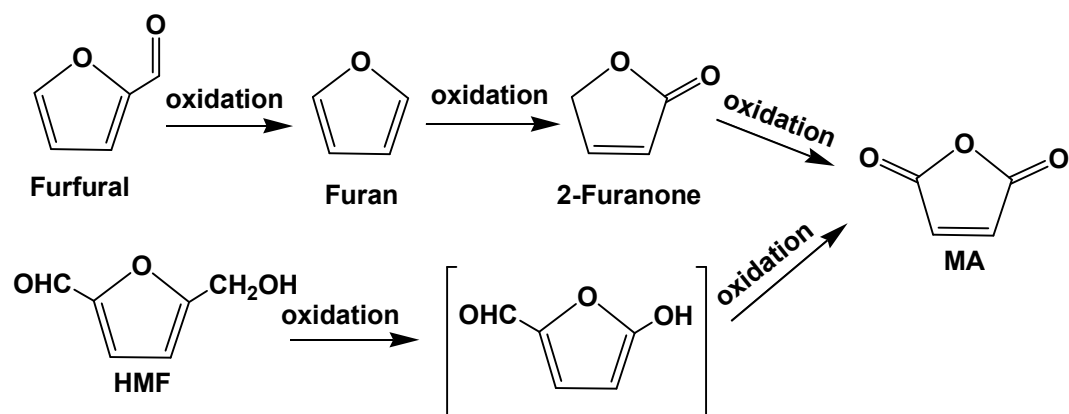


## **Supporting Information**

For

### **One-pot synthesis of 1,4-butanediol via the deep hydrogenation of maleic anhydride over Cu-xMo/SiO<sub>2</sub> catalysts**

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**Scheme S1** Selective oxidation of furfural or HMF to maleic anhydride.

**Table S1** Quantitative acidity according to NH<sub>3</sub>-TPD for various Cu-xMo/SiO<sub>2</sub> catalysts.

| Catalyst                   | Acid amount (mmol·g <sup>-1</sup> ) |          |        |               |
|----------------------------|-------------------------------------|----------|--------|---------------|
|                            | Weak                                | Moderate | Strong | Total acidity |
| Cu/SiO <sub>2</sub>        | 0.15                                | 0.14     | 0.08   | 0.37          |
| Cu-0.02Mo/SiO <sub>2</sub> | 0.22                                | 0.39     | 0      | 0.61          |
| Cu-0.03Mo/SiO <sub>2</sub> | 0.22                                | 0.28     | 0      | 0.50          |
| Cu-0.1Mo/SiO <sub>2</sub>  | 0.35                                | 0.36     | 0      | 0.71          |
| Cu-0.25Mo/SiO <sub>2</sub> | 0.22                                | 0.37     | 0      | 0.59          |
| Mo/SiO <sub>2</sub>        | 0                                   | 0        | 0      | 0             |

**Table S2** Quantitative hydrogen uptake for various Cu-xMo/SiO<sub>2</sub> catalysts.

| Sample                     | Cu content (wt%) | Amount of H <sub>2</sub> consumption |
|----------------------------|------------------|--------------------------------------|
|                            |                  | (mmol/g <sub>Cu</sub> )              |
| Cu/SiO <sub>2</sub>        | 37.7             | 4.38                                 |
| Cu-0.03Mo/SiO <sub>2</sub> | 32.1             | 5.54                                 |
| Cu-0.25Mo/SiO <sub>2</sub> | 31.7             | 5.84                                 |

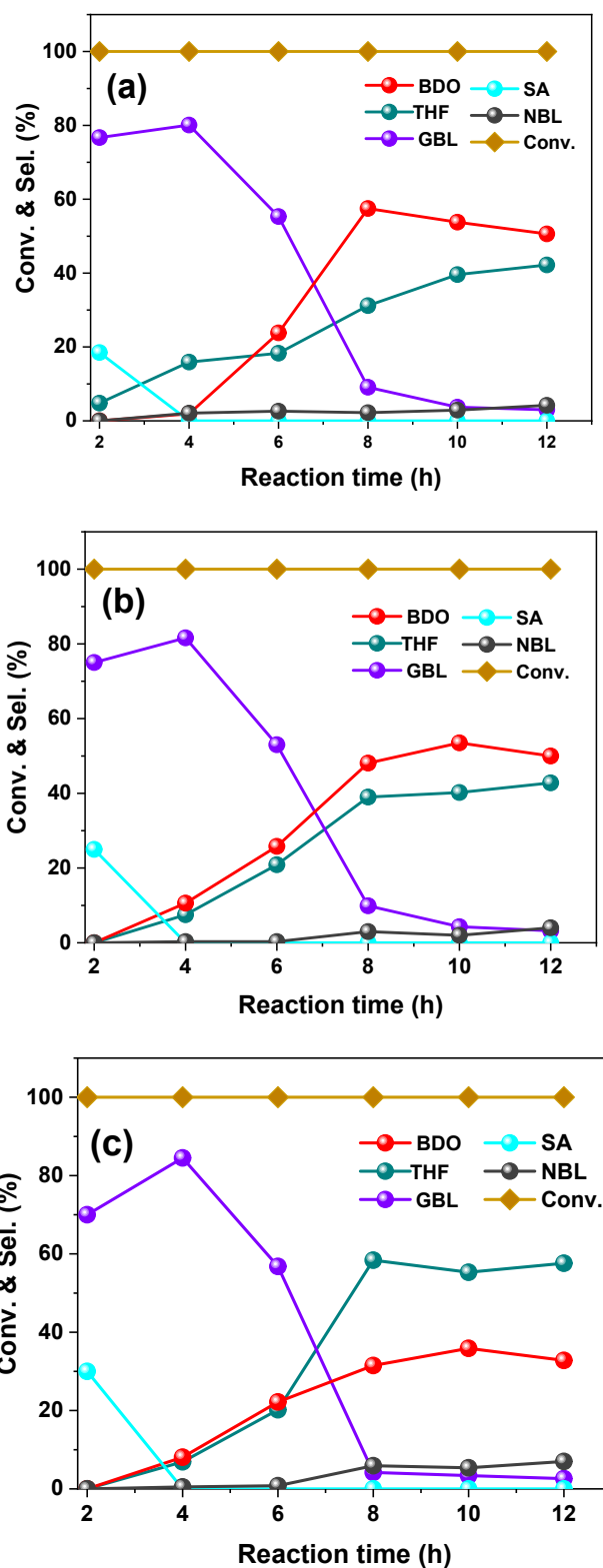
**Table S3** Physicochemical properties of the spent Cu-0.03Mo/SiO<sub>2</sub> catalyst.

| Catalyst                          | S <sub>BET</sub> <sup>a</sup><br>(m <sup>2</sup> ·g <sup>-1</sup> ) | V <sub>p</sub> <sup>a</sup><br>(cm <sup>3</sup> ·g <sup>-1</sup> ) | Cu loading <sup>b</sup><br>(wt%) | d <sub>Cu</sub> <sup>c</sup><br>(nm) |
|-----------------------------------|---------------------------------------------------------------------|--------------------------------------------------------------------|----------------------------------|--------------------------------------|
| Cu-0.03Mo/SiO <sub>2</sub> -used  | 291                                                                 | 0.50                                                               | 31.4                             | 14.1                                 |
| Cu-0.03Mo/SiO <sub>2</sub> -fresh | 357                                                                 | 0.61                                                               | 32.1                             | 3.8                                  |

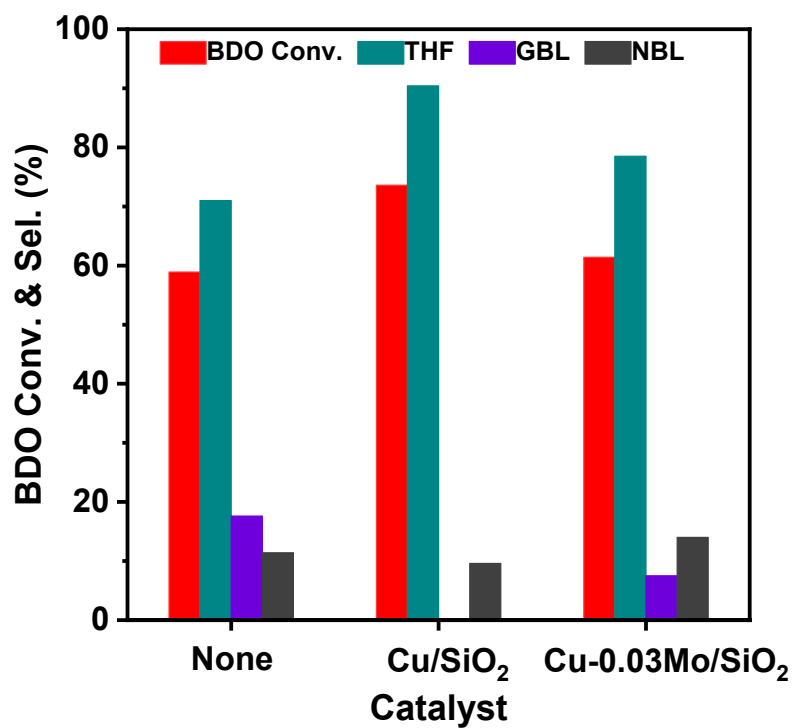
<sup>a</sup> Determined by N<sub>2</sub> physisorption.

<sup>b</sup> Determined by ICP-OES analysis.

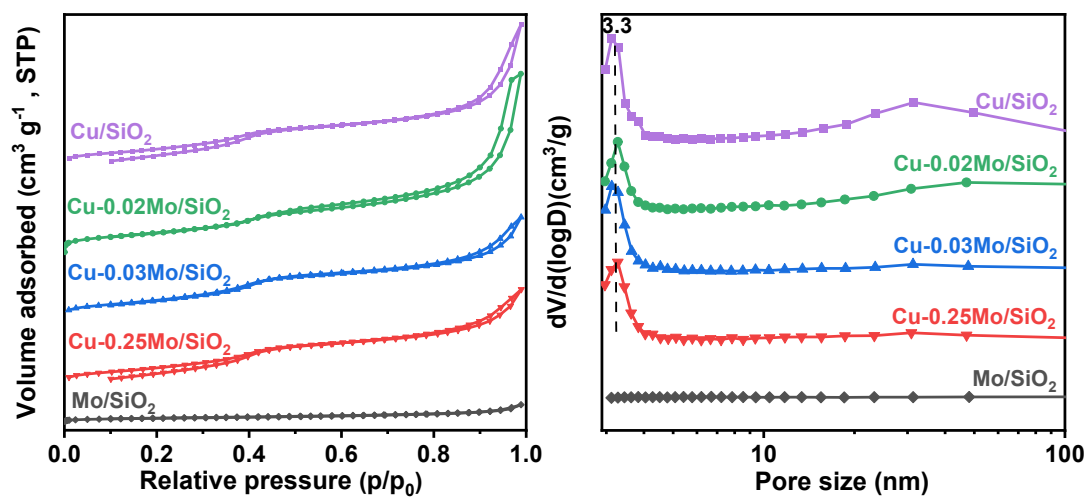
<sup>c</sup> Cu particle size was calculated by the Scherrer equation.



**Fig. S1** Kinetic profiles for the hydrogenation of MA with (a) Cu-0.02Mo/SiO<sub>2</sub>, (b) Cu-0.1Mo/SiO<sub>2</sub>, and (c) Cu-0.25Mo/SiO<sub>2</sub> catalysts. General conditions: 0.2 g of catalyst, 0.2 g of MA, 10 mL of 1,4-dioxane, 5MPa H<sub>2</sub>, 200 °C.

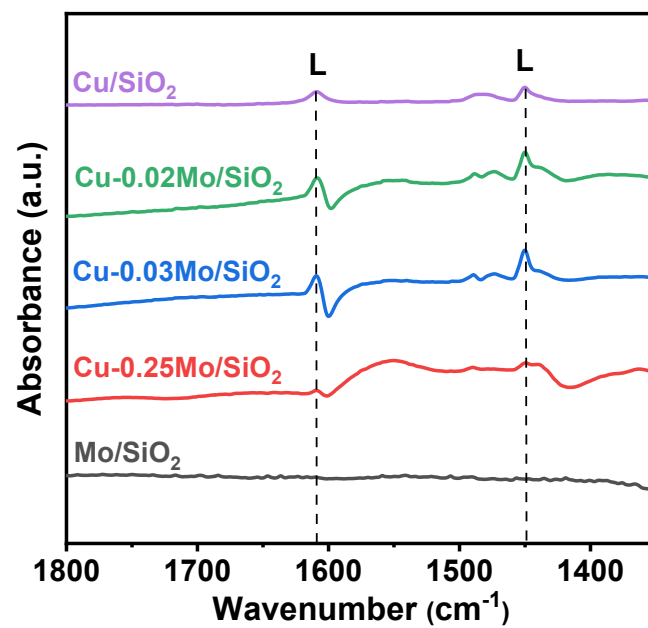


**Fig. S2** Product distribution in the hydrogenation of BDO. Reaction conditions: 0.2 g of catalyst, 0.2 g of BDO, 10 mL of 1,4-dioxane, 200 °C, 5MPa H<sub>2</sub>, 10 h.

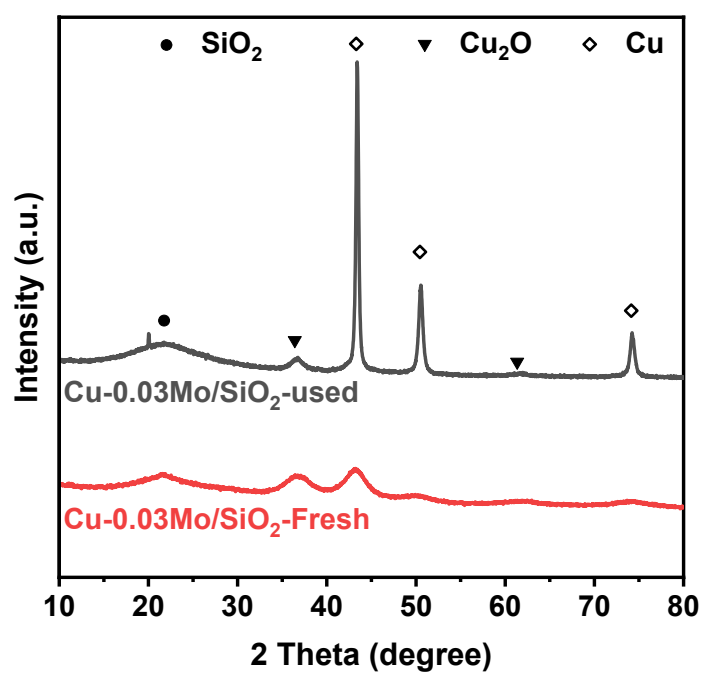


**Fig. S3** (a) N<sub>2</sub> adsorption-desorption isotherms and (b) pore size distributions of various Cu-xMo/SiO<sub>2</sub> catalysts.

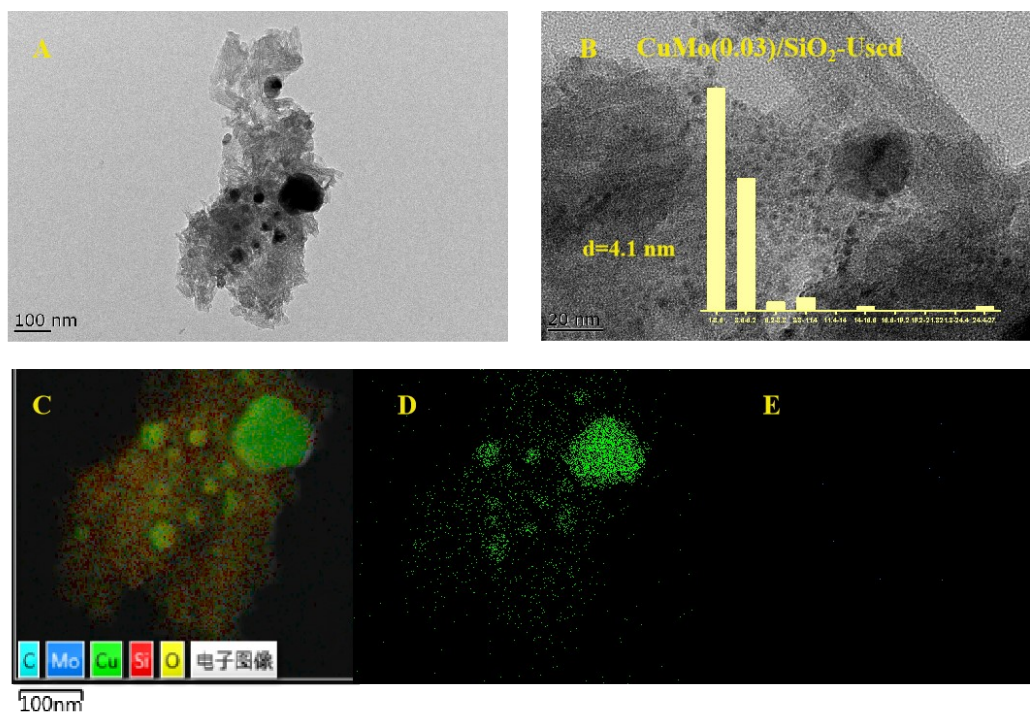




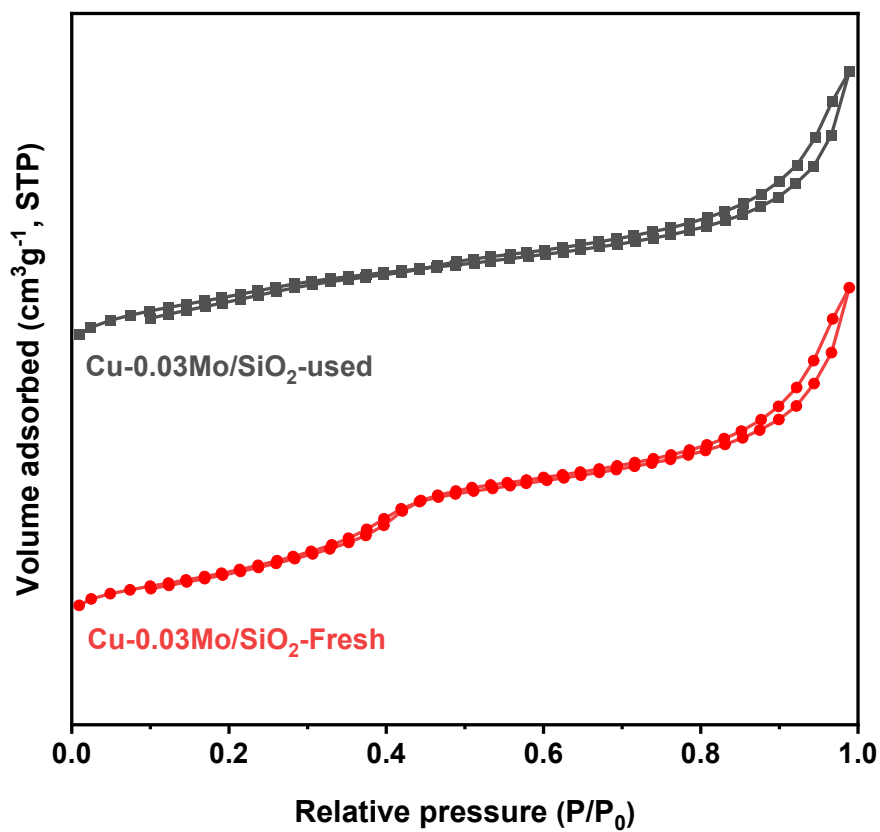
**Fig. S4** FTIR spectra of pyridine adsorbed on Cu-xMo/SiO<sub>2</sub> catalysts at 150 °C.



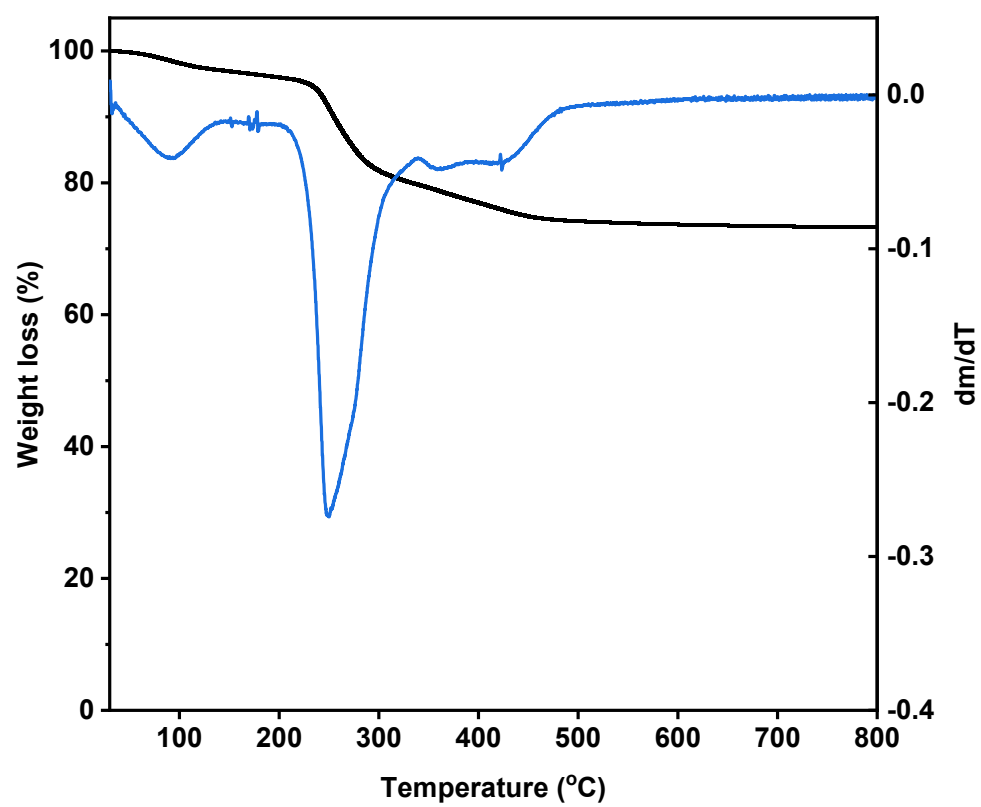
**Fig. S5** XRD patterns of Cu-0.03Mo/SiO<sub>2</sub> before and after long-term stability test.



**Fig. S6** (A) TEM image and (B) high-resolution TEM image of used Cu-0.03Mo/SiO<sub>2</sub>. (C) HAADF-STEM-EDX mapping of used Cu-0.03Mo/SiO<sub>2</sub> and (D) Cu element, (E) Mo element.



**Fig. S7** N<sub>2</sub> sorption isotherms of the Cu-0.03Mo/SiO<sub>2</sub> catalyst before and after long-term stability test.



**Fig. S8** TG curve of the used Cu-0.03Mo/SiO<sub>2</sub> catalyst.