# **Supporting Information**

## The *in-situ* structural evolution of Bi<sub>2</sub>O<sub>3</sub> facilitates the electrocatalytic

hydrogenation of oxalic acid to glycolic acid

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#### Materials and methods

#### **Chemicals and materials**

The chemicals and materials utilized in this work included bismuth (III) nitrate pentahydrate (Bi(NO<sub>3</sub>)<sub>3</sub>·5H<sub>2</sub>O, 99.0%, Shanghai Mindray Biochemical Technology Co., Ltd), ethylene glycol (C<sub>2</sub>H<sub>6</sub>O<sub>2</sub>, AR, Tianjin Kermel Chemical Reagent Co., Ltd), polyvinyl pyrrolidone (PVP-K30, AR, Tianjin Guangfu Fine Chemical Research Institute) and sulfuric acid (H<sub>2</sub>SO<sub>4</sub>, 95~98 wt%, Tianjin Jiangtian Chemical Technology Co., Ltd.). Oxalic acid (C<sub>2</sub>H<sub>2</sub>O<sub>4</sub>, 98%), glyoxylic acid (C<sub>2</sub>H<sub>2</sub>O<sub>3</sub>, 98%) and glycolic acid (C<sub>2</sub>H<sub>4</sub>O<sub>3</sub>, 98%) were purchased from Tianjin Hiens Optus Technology Co., Ltd. Nafion 117 membrane (DuPont, USA) was obtained from Jingchong Electronic Technology Development Co., Ltd.

#### Characterizations

The microstructure and phase compositions of the as-prepared catalysts were characterized through field emission scanning electron microscopy (SEM) (Apreo S LoVac), JEM-F200 transmission microscopy (TEM), X-ray diffraction (XRD, SmartLab with Cu Kα radiation), X-ray photoelectron spectroscopy (XPS, Thermo Fisher Scientific K-Alpha+) and inductively coupled plasma optical emission spectrometry (ICP-OES, Agilent 5110). Electron paramagnetic resonance (EPR) spectra of the samples were collected on a Bruker EMX-plus ESR spectrometer. Products for the ECH of OX were determined by high performance liquid chromatography (HPLC, Agilent 1200) equipped with an Aminex HPX-87H column (300 × 7.8 mm) and an ultraviolet detector (UVD). Raman and *in-situ* Raman spectra were obtained from confocal Raman

microscopy (Horiba LabRAM HR Evolution) with a laser of 633 nm and 1800 g/mm diffraction grating. Electrochemical *in situ* ATR-SEIRAS measurements were performed on the FT-IR spectrometer (iS50, Nicolet) with a modified accessory (VeeMax III, PIKE Technology) and MCT-A detector cooled with liquid nitrogen.

#### **Electrochemical measurements**

Electrochemical measurements were performed utilizing the CHI760E workstation in a three-electrode system. The as-prepared electrode, Ag/AgCl electrode, and Pt plate were used as the working, reference, and counter electrode, respectively. The geometric surface area for the working electrode is 1 cm<sup>2</sup> (1.0 cm × 1.0 cm). Each potential was calibrated to the reversible hydrogen electrode by the following equation:

$$E_{RHE} = E_{Ag/AgCl} + 0.197 + 0.059pH$$

Prior to conducting any tests, the working electrodes were pre-activated by cyclic voltammograms (CV) acquiring from 0.1 to -0.9 V vs RHE at a scan rate 100 mV s<sup>-1</sup>. Linear scan voltammetry (LSV) curves occurred at a scan rate of 5 mV s<sup>-1</sup> in 0.05 M H<sub>2</sub>SO<sub>4</sub> with 100 mM OX added, complemented by 85% iR correction. The related Tafel slopes (b) were determined using the equation (E is the overpotential and j is the current density):

#### $E = a + b \log j$

Electrochemical active surface area (ECSA) was derived from the CV curves by the double-layer capacitance ( $C_{dl}$ ) method under non-Faradaic regions.<sup>1</sup> It was estimated in a potential scan range from 0.712 to 0.812 V vs RHE with the scan rates of 20, 40,

60, 80, and 100 mV·s<sup>-1</sup> in 0.05 M H<sub>2</sub>SO<sub>4</sub> with 100 mM OX added. Electrochemical impedance spectroscopy (EIS) was acquired at -0.5 V vs RHE within the frequency range from 10<sup>5</sup> to 10<sup>-2</sup> Hz.

#### **Density functional theory (DFT) calculations**

Density Functional Theory (DFT) calculations were conducted using the Vienna Ab initio Simulation Package (VASP), employing the Projector Augmented-Wave (PAW) method.<sup>2</sup> The exchange-correlation energy and potential were described using the Perdew-Burke-Ernzerhof (PBE) functional within the generalized gradient approximation (GGA).<sup>3</sup> A plane-wave basis set with a cutoff energy of 500 eV was employed. The Brillouin zone was sampled using a 2×2×1 Monkhorst-Pack grid. To prevent spurious interactions between periodic images, a vacuum layer with a thickness of 15 Å was introduced along the Z direction.

For the Bi/Bi<sub>2</sub>O<sub>3</sub> model, the simulation combined the Bi<sub>2</sub>O<sub>3</sub> (222) surface with a Bi monolayer. In the Bi configuration, the atoms in the bottommost layer were fixed, while all other atoms were permitted to relax. In the Bi/Bi<sub>2</sub>O<sub>3</sub> configuration, the bottom three layers were fixed, while the remaining atoms were fully relaxed. Structural optimizations were conducted until the convergence criteria for energy and force were met, specifically  $10^{-5}$  eV and 0.02 eV/Å, respectively. To accurately compute the density of states, the hybrid Heyd-Scuseria-Ernzerhof (HSE06) functional was used, and the K-point grid was refined to  $3 \times 4 \times 1.^4$  The reaction pathways involved in the calculation of the catalytic hydrogenation of OX are as follows:

\* + HOOCCOOH 
$$\rightarrow$$
 HOOCCOOH\* (1)

$HOOCCOOH^* + H^+ + e^- \rightarrow HOOCCO^* + H_2O$	(2)
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 $HOOCCO^* + H^+ + e^- \rightarrow HOOCCHO^*$ (3)

$$HOOCCHO^* + H^+ + e^- \rightarrow HOOCCHOH^*$$
 (4)

$$HOOCCHOH^* + H^+ + e^- \rightarrow HOOCCH_2OH^*$$
 (5)

$$HOOCCH_2OH^* \rightarrow HOOCCH_2OH + *$$
 (6)

where \* represents the group adsorbed on the surface. The Gibbs free energy (G) of the reaction intermediate is determined by the computational hydrogen electrode (CHE) model, and the G (T=298K) is expressed as:  $G = E_{DFT} + E_0 - TS$ ,

where  $E_0$  and S were considered as zero-point energy and entropy.



Fig. S1. Schematic illustration for the synthesis procedure of Bi<sub>2</sub>O<sub>3</sub>@CC-700.



Fig. S2. High-resolution XPS spectra of  $Bi_2O_3@CC$  synthesized at various thermal treatment temperatures: (a) Bi 4f and (b) O 1s.



Fig. S3. The SEM images of  $Bi_2O_3@CC$  synthesized at various thermal treatment temperatures: (a) 500 °C, (b) 600 °C, and (c) 700 °C.



Fig. S4. The mass loadings of Bi for  $Bi_2O_3@CC-500$ ,  $Bi_2O_3@CC-600$ ,  $Bi_2O_3@CC-700$ ,  $Bi/Bi_2O_3@CC-700$  (ECH for 9 h) and  $Bi_2O_3@CC-800$  respectively, determined by ICP-OES.



Fig. S5. HPLC spectra of the reactant and products for ECH of 100 mM OX under 10 mA cm<sup>-2</sup> for 9 h.



Fig. S6. The HPLC standard curves for (a) OX, (b) GX and (c) GA.



Fig. S7. CV curves of (a) Pure CC, (b) 500 °C, (c) 600 °C and (d) 700 °C measured in non-Faradaic region (0.712  $\sim$  0.812 V vs RHE) of the voltammogram at different scan rates of 20, 40, 60, 80 and 100 mV s<sup>-1</sup> in 0.05 M H<sub>2</sub>SO<sub>4</sub> with 100 mM OX added.



Fig. S8. The photographs of the electrolysis cell used in the *in-situ* Raman measurements.



Fig. S9. Time-dependent Raman spectra of OX on  $Bi_2O_3@CC-700$  in 0.05 M  $H_2SO_4$  with 100 mM OX at -0.5 V vs RHE (The red curve is the Raman spectrum after ECH for 9h at the same condition.).



Magnetic field (G)

Fig. S10. EPR spectra of Bi<sub>2</sub>O<sub>3</sub>@CC-700 before and after ECH for 9 h.



Fig. S11. (a, b) SEM images of  $Bi_2O_3@CC-700$  after ECH for 9 h. (c) TEM image. (d, e) HRTEM images and (f) SAED pattern of  $Bi_2O_3@CC-700$  after ECH for 9 h. (g-i) The corresponding elemental mappings.



Fig. S12. The SEM images of  $Bi_2O_3@CC$  synthesized at various thermal treatment temperatures after ECH for 9 h: (a) 500 °C, (b) 600 °C, and (c) 700 °C.



Fig. S13. The photographs of the electrolysis cell used in the *in-situ* ATR-SEIRAS measurements.



Fig. S14. (a) Bode plots of increasing gradient concentration of OX at -0.5 V vs RHE over Bi<sub>2</sub>O<sub>3</sub>@CC-700. (b) The corresponding correlation between the interface reaction charge transfer process resistance ( $R_{ct}$ ) and the concentration of OX.



Fig. S15. The theoretical models of (a)  $Bi/Bi_2O_3$  and (b) Bi.



Fig. S16. Schematic illustrations of the reaction processes of OX on Bi.

Catalvst	Temperature	Electrolvte	Applied potential	OX Conversion	GA Selectivity	Faradaic efficiency	Ref.	
,	(°C)		(V vs RHE)	(%)	(%)	(%)		
Bi <sub>2</sub> O <sub>3</sub> @CC-	25	0.05 M H <sub>2</sub> SO <sub>4</sub> +	-0.5	82	87	61	This	
700	25	100 mM OX	0.5	0.5 02	07	01	work	
TiO₂/Ti-M	60	0.03 M OX	2	_	50	_	5	
			(Cell voltage)				0	
MWNT/PyPB	60	0.2 M Na <sub>2</sub> SO <sub>4</sub> +	2.4	51 2	38 7	_	6	
I/TiO <sub>2</sub>	00	30 mM OX	(Cell voltage)	51.2	50.7		Ū	
$Ti_1 \sqrt{2}r_2 O_2$	50	0.2 M Na <sub>2</sub> SO <sub>4</sub> +	-0.7	40.8	_	80	7	
	50	30 mM OX	0.7					
g-C <sub>3</sub> N <sub>4</sub> /TiO <sub>2</sub> -	ВТ	0.2 M Na <sub>2</sub> SO <sub>4</sub> +	-1.3	_	76	88	8	
NTF		30 mM OX	(vs Ag/AgCl)				0	
TiNT60-E F	RТ	0.2 M Na <sub>2</sub> SO <sub>4</sub> +	-0.8	48	78	86	9	
		30 mM OX	0.0	40	70	00	5	
GaSnO <sub>x</sub> /C	80	1 M OX	-0.8	~30	—	91.7	10	
M-TiO <sub>2</sub>	RТ	100 mM OX	-0.5	_	_	73 9	11	
spheres			0.5			73.5		
TiO <sub>2</sub>	50	200 mM OX	-0.74	—	70	64	12	
TNT-90	60	0.2 M Na <sub>2</sub> SO <sub>4</sub> +	-1.0	_	Q1	67	13	
	00	30 mM OX	(vs Ag/AgCl)		51	07	15	
TINT-HS	25	0.2 M Na <sub>2</sub> SO <sub>4</sub> +	-1.1	-1.1 20	_	60.8	14	
11111-113	20	30 mM (	30 mM OX	(vs Ag/AgCl)	50		00.0	7

Table S1. Summary of ECH of OX on different electrocatalysts.

Abbreviations: OX, oxalic acid; GA, glycolic acid; R.T., room temperature.

Catalyst	Bi content (mg cm <sup>-2</sup> )
Bi <sub>2</sub> O <sub>3</sub> @CC-500	2.43
Bi <sub>2</sub> O <sub>3</sub> @CC-600	2.34
Bi <sub>2</sub> O <sub>3</sub> @CC-700	1.89
Bi/Bi <sub>2</sub> O <sub>3</sub> @CC-700	1.42
Bi <sub>2</sub> O <sub>3</sub> @CC-800	0.008

Table S2. Bi contents of various catalysts determined by ICP-OES.

Table S3. The ECH performance under different reaction conditions <sup>a</sup>.

NO.	Catalyst	Reaction Temperat ure (°C)	Current density (mA cm <sup>-2</sup> )	Applied potential (V vs RHE)	Reaction time (h)	OX Conversion (%)	GA Selectivity (%)	GX Selectivity (%)	FE (%)
1	Pure CC	25	10	_	9	38.05	56.52	29.39	24.50
2	Bi₂O₃@CC -500	25	10	_	9	72.04	67.32	17.55	56.48
3	Bi₂O₃@CC - 600	25	10	_	9	96.26	55.45	20.40	50.19
4	Bi <sub>2</sub> O <sub>3</sub> @CC - 700	25	10	_	9	96.70	62.82	20.18	55.73
5	Bi₂O₃@CC - 700	25	40/3	_	9	97.75	59.80	21.98	40.89
6	Bi₂O₃@CC - 700	25	50/3	_	9	96.58	85.79	4.88	40.79
7	Bi₂O₃@CC - 700	25	60/3	_	9	99.87	70.23	11.11	30.21

8	Bi <sub>2</sub> O <sub>3</sub> @CC -	25	_	-0.45	_	28.24	82.24	18.76	31.12
	700								
9	Bi <sub>2</sub> O <sub>3</sub> @CC -	25	_	-0.50	_	82.49	86.56	13.64	61.17
	700								
10	Bi <sub>2</sub> O <sub>3</sub> @CC -	25	_	-0.55	_	85 67	74 77	19 49	57 49
10	700	23		0.00		00.07	,,	10.10	57.15
11	Bi <sub>2</sub> O <sub>3</sub> @CC -	25	_	-0.60	_	84.60	53,41	42.13	50.03
	700	20		0.00		0 1100	00112	12120	50.05
12	Bi <sub>2</sub> O <sub>3</sub> @CC -	25	_	-0.65	_	90.06	51.11	42.30	50.41
	700						•		
13	Bi <sub>2</sub> O <sub>3</sub> @CC -	25	_	-0.70	_	94.71	52.87	40.08	54.84
10	700	23		••••••		•	52.07	10100	5
14	Bi <sub>2</sub> O <sub>3</sub> @CC -	35	10	_	9	89.36	81.57	12.33	62.26
	700		10		2	00.00	01.07	12100	02.20
15	Bi <sub>2</sub> O <sub>3</sub> @CC -	45	10	_	9	79,97	89.97	6.64	59.25
10	700	10	10		2	, , , , , , , , , , , , , , , , , , , ,	00.07		00120
16	Bi <sub>2</sub> O <sub>3</sub> @CC -	55	10	_	9	72 84	88 93	3 55	63 15
10	700		10		5	/ 2.04	00.55	5.55	00.10

Reaction conditions: catholyte:  ${}^{a}$  0.05 M H<sub>2</sub>SO<sub>4</sub> with 100 mM OX; anolyte: 0.05 M H<sub>2</sub>SO<sub>4</sub>.

Catalyst	Overpotential at 20 mA cm <sup>-2</sup> (mV)	Tafel slope (mV dec⁻¹)	C <sub>dl</sub> (mF cm⁻²)	R <sub>ct</sub> (Ω)
Pure CC	669	393	0.5	490.8
Bi <sub>2</sub> O <sub>3</sub> @CC-500	519	251	11.7	20.06
Bi <sub>2</sub> O <sub>3</sub> @CC-600	525	206	12.4	19.29
Bi <sub>2</sub> O <sub>3</sub> @CC-700	507	156	16.3	11.09

Table S4. Electrochemical properties of Pure CC,  $Bi_2O_3@CC-500$ ,  $Bi_2O_3@CC-600$ , and  $Bi_2O_3@CC-700$ .

Table S5. Charge transfer resistances of  $Bi_2O_3@CC-700$  in Fig. S13.

OX Concentration (mM)	$R_{\rm ct}(\Omega)$
0	34.4
100	8.646
200	4.997
300	3.756
400	2.956

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