1	Supporting Information
2	Chemical upcycling of Ni from electroplating wastewater to
3	well-defined catalyst for electrooxidation of glycerol to
4	formate
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14 Experiment section

Materials and reagents: Except noted, all chemicals were purchased and used without 15 further purification. Deionized water was used throughout the experiments. potassium 16 permanganate (KMnO₄), nickel sulfate (NiSO₄•6H₂O), potassium hydroxide (KOH), 17 sodium hydroxide (NaOH), ethylenediamine tetraacetic acid disodium salt (EDTA) and 18 Sodium hypophosphite (NaH₂PO₄•H₂O) were purchased from Sinopharm Chemical 19 Reagent (Beijing Co., Ltd.). Glycerol ($C_3H_8O_3$, $\geq 99\%$) and oxalic acid, tartaric acid, 20 pyruvic acid, glyceric acid, glycolic acid, lactic acid, formic acid, and acetic acid were 21 obtained from Shanghai Macklin Biochemical Co., Ltd. All the above chemicals were 22 used as received without further purification. Abbreviation: glycerol (GLY), oxalic acid 23 (OA), tartaric acid (TA), pyruvic acid (PA) glyceric acid (GLA), glycolic acid (GA), 24 lactic acid (LA), formic acid (FA) and acetic acid (AA) 25

The remediation performance to simulated Ni-electroplating solution: The effect 26 of mole ratio of NaOH/Ni²⁺: For example, firstly, 0.424 g NaH₂PO₄•H₂O was dissolved 27 in 50 mL simulated Ni-electroplating solution to ensure the mole ratio of NaH₂PO₄/Ni²⁺ 28 was 3. After that, 0.3 g NaOH was introduced into the above solution with vigorous 29 stirring for 30 minutes. Then, the solution was transformed in a 100 mL Teflon-lined 30 stainless-steel autoclave. After sealing the autoclave, it was heated to 160 °C for 6 h. 31 After the reaction, the mixture solution (8 ml) was filtered through a 0.2-micron 32 membrane filter, then the filtrates were analyzed using ICP-OES to detect the residual 33 Ni²⁺ concentration. The precipitate was obtained by centrifugation and washed with 34 deionized water and dried in oven. With the mole ratio of NaH₂PO₄/Ni²⁺ kept constant, 35 different amounts of NaOH were added to explore the effect to remove Ni²⁺ from 36 solution. 37

The effect of mole ratio of NaH₂PO₄/Ni²⁺: For example, firstly, 0.4 g NaOH was 38 dissolved in 50 mL simulated Ni-electroplating solution to ensure the mole ratio of 39 NaOH/Ni²⁺ was 4. After that, 0.159 g NaH₂PO₄•H₂O was introduced into the above 40 solution with vigorous stirring for 30 minutes. Then, the solution was transformed in a 41 100 mL Teflon-lined stainless-steel autoclave. After sealing the autoclave, it was heated 42 to 160 °C for 6 h. After the reaction, the mixture solution (8 ml) was filtered through a 43 0.2-micron membrane filter, then the filtrates were analyzed using ICP-OES to detect 44 the residual Ni²⁺ concentration. The precipitate was obtained by centrifugation and 45 washed with deionized water and dried in oven. With the mole ratio of NaOH/Ni²⁺ kept 46 constant, different amounts of NaH₂PO₄•H₂O were added to explore the effect to 47 remove Ni²⁺ from solution. 48

The remediation performance to actual Ni-electroplating solution: Firstly, 1.2 g 49 NaOH and 1.5 g NaH₂PO₄•H₂O were dissolved in 50 mL actual Ni-electroplating 50 solution with vigorous stirring for 30 minutes. Then, the solution was transformed in a 51 100 mL Teflon-lined stainless-steel autoclave. After sealing the autoclave, it was heated 52 to 160 °C for 6 h. After the reaction, the mixture solution (8 ml) was filtered through a 53 0.2-micron membrane filter, then the filtrates were analyzed using ICP-OES to detect 54 the residual Ni²⁺ concentration. The precipitate was obtained by centrifugation and 55 washed with deionized water and dried in oven. 56

57 **Preparation of working electrode:** The carbon cloth was firstly immersed in 0.5mol/L 58 potassium permanganate solution for 30 min, then washed with deionized water and 59 dried in a 60°C oven. Mixed 16 mg electrocatalyst, 1.6 ml ethanol and 16 μ L Nafion 60 solution (5%, Macklin) together thoroughly, and ultrasonic for 30 min, after that, the 61 mixture was deposited on the treated carbon cloth of 2*2.5 cm², and dried for 30 min.

Electrochemical measurement: All electrochemical measurements for glycerol 62 oxidation were performed in 1 M KOH electrolyte at room temperature on an 63 electrochemical workstation (CHI 760E, CH Instruments, Inc.). The electrochemical 64 tests were performed in a three-electrode system in a membrane-free glass beaker, 65 using Ag/AgCl electrode (with saturated KCl) and Pt foil as reference and counter 66 electrode, respectively. Linear scan voltammetry (LSV) curves of catalysts were 67 acquired from -0.2 V to 0.7 V vs. Ag/AgCl at a scan rate of 10 mV s⁻¹. All of the 68 electrocatalytic reactions were conducted at ambient pressure and temperature, unless 69 otherwise specified. All potentials measured against Ag/AgCl were converted to the 70 reversible hydrogen electrode (RHE) scale using the following equations: 71

$$E_{\rm RHE} = E_{\rm Ag/AgCl} + E_{\rm Ag/AgCl \nu s. NHE} + 0.059 \text{ pH}$$
(1)
where

74 $E_{Ag/AgCl vs. NHE}$ in eq (1) is 0.197 V at 20 °C.

The selectivity of the products was calculated based on total moles of GLY 75 oxidation products using the following equations. 76

Selectivity = $\frac{n_{\text{product}}}{n_{\text{total}}} \times 100\%$ 77 (2)

The liquid products were quantified by high performance liquid chromatography 78 (HPLC; Angilent 1200 Infinity Series) equipped with organic acid column (Coregel 79 87H3) using 5 mM aqueous H₂SO₄ as mobile phase and detected by UV detector (210 80 nm) and refractive index detector. 81

The product yield rate can be expressed using the following formula: 82

$${
m Yield} \ ({
m mmol} \ {
m h}^{-1} \ {
m g}^{-1}) = rac{{
m Amount \ of \ product \ (mmol)}}{{
m Catalyst \ mass \ (g) imes {
m Reaction \ time \ (h)}}}$$

84

85 This formula can be adapted to express the yield of any product generated during 86 the reaction, including formic acid or other products of glycerol oxidation.

87 Characterizations.

X-ray diffraction patterns were collected on a Shimadzu XRD-6000 88 diffractometer using a Cu K α source, with a scan range of 5–80° and scan step of 10° 89 min⁻¹. X-ray photoelectron spectra (XPS) were performed on a Thermo VG 90 ESCALAB 250 X-ray photoelectron spectrometer at a pressure of about 2×10^{-9} Pa 91 using Al Ka X-rays as the excitation source. Scanning electrode microscope (SEM) 92 images were recorded by a Zeiss SUPRA 55 Field Emission SEM with an accelerating 93 voltage of 20 kV. Transmission electron microscopy (TEM) images were recorded 94 with JEOL JEM-2010 high resolution (HR-)TEM with an accelerating voltage of 200 95 kV. Metal contents in catalysts were determined by ICP-MS on a Thermo ICAP6300 96 Radial. 97

In situ Raman spectra were recorded on a confocal Raman microspectrometer (Renishaw, inVia-Reflex, 532 nm) using a 532 nm laser and the power was set at 2 mW under different potentials monitored by a CHI 760E electrochemical workstation equipped with an in situ Raman cell (Beijing Scistar Technology Co. Ltd). The applied potentials during the in situ Raman tests were not corrected by the solution resistance, which is constant with the LSV test without I-R correction (Fig. 4a), ensuring clear comparison of the results by using different techniques.

In situ FT-IR spectra were recorded by a Bruker Equinox 55 spectrometer,
between 4000 and 400 cm-1 with a resolution of 4 cm-1 after 600 scans per spectrum.
The electrochemical measurements were monitored by a CHI 760E electrochemical

108 workstation equipped with an in-situ FTIR cell (Beijing Scistar Technology Co. Ltd). 109 The FTIR cell is a three-electrode system, using Ag/AgCl electrode (with saturated 110 KCl) and Pt wire as reference and counter electrode, respectively. The working 111 electrode was prepared by loading S-C/Ni-P_x catalyst on glassy carbon electrode 112 (Figure S19). For the in-situ FTIR test, we first stabilized the catalyst in 1 M KOH at 113 1.6 V vs. RHE for 10 min, then 0.1 M GLY was added in the electrolyte and set this 114 time point as 0 min. The FTIR spectrum of S-C/Ni-P_x from 5 to 605s is shown in Figure 115 5d.

117 Supplementary Figures



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Figure S1. XPS survey spectra of the obtained precipitate from simulated Ni-electroplating solution



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122 Figure S2. XRD patterns of the obtained precipitate



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125 Figure S3. LSV curves of carbon cloth electrode at a scan rate of 10 mV/s in 1.0 M KOH with or

126 without 0.1 M glycerol.





Figure S4. HPLC chromatogram of glycerol oxidation products over S-C/Ni-P_x at different
potential.



135 Figure S5. HPLC calibration curves of glycerol, reaction intermediates, and products with

136 refractive index detector.



138 139 Figure S6. Yield of the detected products from glycerol electrooxidation versus the reaction time

140 catalyzed by S-C/Ni-P_x.Reaction conditions: 1.0 M KOH with 0.1 M glycerol at 1.6 V vs. RHE.





144 Figure S7. i-t experiments with glycerate and glycolate as substrates on S-C/Ni-Px catalyst were 145 performed at the applied potential of 1.6 V vs RHE in 1 M KOH solution with 0.1 M of the

146 substrates.



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148 Figure S8. SEM image of the obtained precipitate

150 Supplementary Tables

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152 Table S1. The main components and concentrations of simulated Ni-electroplating solution

	Main components	Ni ²⁺	H ₂ PO ₂ -	$\mathrm{NH_4^+}$	C ₆ H ₅ O ₇ ³⁻	pН
-	Concentrations	3.0	4.5	9.0	2	4.8
	(mg/L)					

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154

155 Table S2. Comparison of Residual Nickel Concentrations and Compliance across Different

156 Remediation Methods

Remediation	Initial Nickel	Post-	Recovery of Ni ²⁺	Ref.
Method	Concentration	Treatment	(%)	
	(mg/L)	Nickel		
		Concentration		
		(mg/L)		
Sodium	3000	0.32	99.99	This
hypophosphite				work
oxidation method				
Two-Chamber	325	λ	82.34	1
Electrodeposition-				
Electrodialysis				
combination				
RCE bench scale	1220	\	97	2
and RCE pilot				
plant				
reactors				
Solar Light	8.1	1.5	81.48	3
Responsive				
Photocatalyst				
integrated	53694.2	١	>55	4
electrodeposition				
with adsorption				
pretreatment				
technique				
Electrocoagulation	300	λ	97	5
treatment				
processes				
Chemical	X	0.003	99.88	6
precipitation				
Ion exchange	X	λ	>50	7

	Comparison	of	X		١	ç	99		8
	processes	and							
	combined								
	processes								
	extraction		500	,	\	9	90		9
157	Ministry of Envi	ronmen	tal Protec	tion of Chin	a. Dischar	ge Standard	d of Polluta	ints for Ele	ctroplating
158	(GB 21900-2008).							
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160									
160 161	Table S3 The ele	ectropla	ting wast	ewater comp	position an	alysis			
161	Table S3 The ele	ectropla	ting wast	ewater comp	position an	alysis	Cl-	EDT	
161	Table S3 The ele Main compor	ectropla nents	ting wast Ni ²⁺	ewater comp H ₂ PO ₂ -	NH4 ⁺	alysis SO4 ^{2–}	Cl-	EDT A	рН
161	Table S3 The eld Main comport Concentration	ectropla nents ons	ting waste Ni ²⁺ 8.7	$H_2PO_2^{-1}$ 30.8	NH4 ⁺	alysis SO4 ²⁻ 1.2	C1- 3.4	EDT A 4.6	рН 5.5
161	Table S3 The eld Main compon Concentration (g/L)	ectropla nents ons	ting waste Ni ²⁺ 8.7	H ₂ PO ₂ -	NH4 ⁺	alysis SO4 ^{2–} 1.2	Cl- 3.4	EDT A 4.6	рН 5.5

Table S4. Comparisons of S-C/Ni- P_x with reported electrocatalysts to glycerol electrooxidation

Catalyst	Electrolyte	Value-added products	Voltage (V)	Selectivity /FE	Ref.
FeCoNi/C	0.1 M NaOH +0.1 M Glycerol	Formate	-	Sel. 34.1%	10
Bi-Co ₃ O ₄	1.0 M KOH + 0.1 M Glycerol	Formate	1.223 1.297 1.446	Sel.97.01± 1.73%	11
CuCo ₂ O ₄ /CFC	1.0 M KOH + 0.1 M Glycerol	Formate	1.26	Sel. 80.6%	12
NixB	1.0 M KOH + 0.1 M Glycerol	Formate	1.535	Sel. 80%	13
CuNi/ ACF	0.1M KOH+0.1 M Glycerol	Formate	1.897	Sel.97.4%	14

	Glycerol				wor
C/Ni-P _x	1.0 M KOH 0.1 N	+ M Formate	1.6	Sel.96.4%	This
	GlyceroL				
NiO	0.1 N	M Formate	1.7	Sel.97%	21
	0.1 M KOH -	ł			
	M Glycerol				
NiCrO-V _{Cr,O}	0.1	Formate	1.37	Sel.98%	20
	1 M KOH	+			
	GlyceroL	i i onnute	1.00	~~~~~	17
Ni(OH) ₂	1 M KOH +	M Formate	1.65	Sel.81.3%	19
	Glycerol				
Ni-Mo-N/CFC	0.1 N	M Formate	1.35	Sel.92.48%	18
	1 M KOH +				
	M Glycerol				
Pt-in-VGCC	0.6	Formate	1.23	Sel.79%	17
	1 M KOH	+			
5()2(5-)	Glycerol				
$Co_3(PO_4)_2(CoP)$	0.1 N	⊤ M Formate	1.33	Sel.82%	16
	Glycerol	1			
CuCo-oxide	0.1 N	M Formate	1.31	Sel.62.9%	15
				a 1 (a a) (

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