

Supplementary Material

Boosting Urea Synthesis in Simulated Flue Gas Electroreduction by Adjusting W-W Electronic Properties

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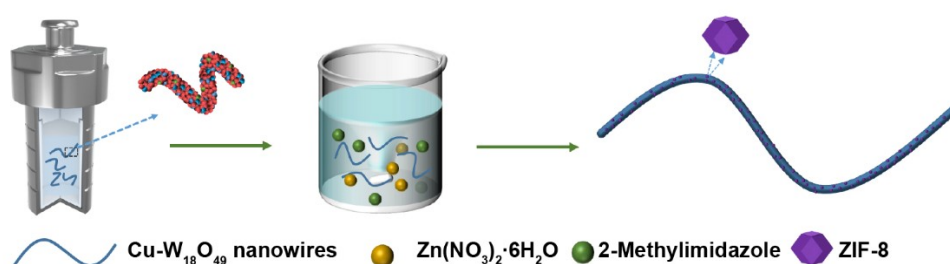
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Materials

The raw materials for Cu-W₁₈O₄₉@ZIF-8 synthesis were purchased in Macklin. Other reagents and solvents applied in the synthesis and photocatalysis were purchased from Aladdin and Sigma-Aldrich.

Synthesis of Cu-W₁₈O₄₉@ZIF-8 composite

50 mg WCl₆ was dissolved in 10 mL of ethanol, which was vigorously stirred to obtain a yellow solution, then 6.88 mg CuCl₂·2H₂O was added to the solution. After further stirring for 10 min, the resultant solution was transferred to a 15 mL Teflon-lined autoclave, which was heated at 210 °C, 12 h. After cooling down to room temperature, the grey-blue product was separated by centrifugation and washed with water and ethanol several times. The obtained product was dried in the vacuum overnight at 50 °C. Then, 7.5 mg Cu-W₁₈O₄₉ and 81 mg dimethylimidazole were dispersed in 5 mL methanol, after stirring for 30 min, 5 mL methanol solution containing 36.66 mg Zn(NO₃)₂·6H₂O was added into the solution, which was further stirred for 45 min. The mixture was kept stationary for 2 hours at room temperature. The product was washed with water and methanol three times and dried in the vacuum overnight at 40 °C.



Scheme S1: Diagram of the preparation detail process for Cu-W₁₈O₄₉@ZIF-8 composite.

Characterization

A powder X-ray diffraction (PXRD) pattern was recorded by a Siemens D5005 diffractometer with Cu-K α ($\lambda = 1.5418$ Å). ICP spectroscopy was conducted on Agilent 7500a Inductively Coupled Plasma Mass Spectrometry (ICP-MS 7500). TEM

images were recorded on a JEM-2010 transmission electron microscope at an accelerating voltage of 200 kV. UV-Vis absorption spectroscopy was obtained on a U-3900 spectrophotometer (Hitachi, Japan). Infrared spectra were obtained from KBr pellets in a wavelength ranging from 4000-400 cm^{-1} on a Nicolet 380 FT-IR spectrophotometer. XPS was performed using an Escalab 250 instrument. Nitrogen gas porosimetry measurements were performed on automatic volumetric adsorption equipment (ASIQM0G002-3) and a porosity analyzer after the samples were outgassed under a vacuum at 100 °C for 12 h. X-ray Absorption Near Edge Structure (XANES) and Extended X-ray Absorption Fine Structure (EXAFS) data were collected at Beamline 11B at Shanghai Synchrotron Radiation Facility (SSRF). In situ IR was carried out on a 6700 Flex FTIR spectrometer equipped with a smart iTRTM attenuated total reflectance (ATR) sampling accessory in the range of 500-4000 cm^{-1} .

Electrochemical measurements

Electrochemical measurement was carried out on a CHI660E electrochemical workstation in an H-cell with a three-electrode system. A Nafion 117 proton exchange membrane separated the H-type cell. The two compartments were filled with 0.25 M K_2SO_4 electrolyte. The as-prepared catalyst, platinum foil, and saturated Ag/AgCl electrode (filled with saturated KCl) acted as the working electrode, the counter electrode, and the reference electrode, respectively. To avoid contamination with nitrogen-containing species in the air, electrodes were used either immediately after preparation or kept in a vacuum before being used in electrochemical experiments. Potential without iR-compensated were converted to RHE scale via the following equation: $E (\text{vs. RHE}) = E (\text{vs. Ag/AgCl}) + 0.0591 \times \text{pH} + 0.197$ (pH = 4.7 in CO_2 -saturated electrolyte and $\text{N}_2 + \text{CO}_2$ -saturated electrolyte in 0.25 M K_2SO_4 ; pH = 6.2 for N_2 -saturated electrolyte in 0.25 M K_2SO_4). The catalyst ink for the working electrode was prepared by dispersing 10 mg of catalyst in a 1ml Nafion (0.5 wt% to sonication for 30 minutes. Mass loading of 0.4 mg cm^{-2} was used for the electrochemical study. All experiments were carried out at room temperature (25 °C). To remove the impurities in the inlet gas, such as NO_x , the pre-purification of high-purity N_2 (purity 99.999%)

and CO₂ (purity 99.99%) by passing through a saturator filled with 0.05 M NaOH and a saturator filled with 0.05 M H₂SO₄ solution to remove any possible contaminants. Before carrying out all the electrochemical characterizations, the 0.25 M K₂SO₄ electrolyte solution was purged with CO₂ + N₂ for 30 minutes. In table S1, we summarized ink preparation process:

Table S1: Ink preparation proces

Catalyst quality	Nafion(5wt%)	H ₂ O	Ultrasound time	Ink concentration
e.g. Cu-W ₁₈ O ₄₉ @ZIF- 8 10mg	0.1ml	0.9ml	30 minutes	10 mg/ml

Synthesis of H₂S and SO_x

100mg Na₂S₂O₃ was put in a 20 mL sealed headspace reaction bottle to prepare H₂S. The sealed headspace reaction bottle is connected to the gas-gathering device with a catheter and a needle. Next, 1mL 0.1 M H₂SO₄ was injected into the reactor with a 1 mL syringe, and the gas with the odor was generated and stored in a gas collection bag. For SO_x, replace Na₂S₂O₃ with FeSO₄, and inject 0.5 M H₂SO₄. The concentrations of H₂S and SO_x is 0.2%, respectively.

Urea determination

The identification of urea was first achieved by the diacetyl monoxime method [1]. 500 mg of diacetylmonoxime (DAMO) and 10 mg of thiosemicarbazide (TSC) were dissolved in distilled water and diluted to 100 mL, denoted as DAMO-TSC solution. Then, 10 mL of concentrated phosphoric acid was mixed with 30 mL of concentrated sulfuric acid and 60 mL of distilled water, then 10 mg FeCl₃ was dissolved in the above solution, denoted as an acid-ferric solution. The preparation of the diacetyl monoxime colorant is summarized in Table S2. Typically, 1 mL of the sample solution was removed from the cathodic chamber. Afterward, 1 mL of DAMO-TSC solution and 2

mL of acid-ferric solution were added into 1 mL of sample solution. Next, the mixed solution was heated to 100 °C and maintained at this temperature for 15 min. When the solution cooled to 25 °C, the UV-Vis absorption spectrum was collected at a wavelength of 525 nm. For high-performance liquid Chromatography spectroscopy. The quantification of urea was achieved by HPLC (SHIMADZU SPD-15C) spectroscopy. HPLC was performed on a Luna 5 µm NH₂ column (250 mm × 4.6 mm). The corresponding mobile phase, flow rate, and detected wavelength were acetonitrile-water (80:20), 0.2 mL min⁻¹, and 195 nm. For the ¹H NMR tests, dimethyl sulfoxide-d₆ (DMSO-d₆) was adopted as a deuterated reagent. First, 0.35 mL of extracted electrolyte without postprocessing was mixed well with 0.15 mL DMSO-d₆. Then, the liquid was transferred into the ¹H NMR tube for the test.

Table S2: Preparation of Diacetyl Monoxime Method Colorant.

DAMO-TSC solution	Diacetylmonoxime (DAMO)	Thiosemicar bazide (TSC)	H ₂ O
	500 mg	10 mg	100 ml
Acid-Ferric solution	Acid	FeCl ₃	H ₂ O
	10ml phosphoric acid 30ml sulfuric acid	10 mg	60 ml

Determination of ammonia (NH₃):

The produced NH₃ was spectrophotometrically determined by the indophenol blue method [2]. Typically, 1 mL of the sample solution was removed from the cathodic chamber. Afterward, 1 mL of 1.0 M NaOH solution containing 5 wt% salicylic acid and 5 wt% sodium citrate was added, followed by 0.5 mL NaClO solution (0.05 M) and 0.1 mL of an aqueous solution of sodium nitroferricyanide (1 wt%) were added. After standing at room temperature for 2 hours, the UV-Vis absorption spectrum was collected at a wavelength of 655 nm.

Calculation of Faradaic efficiency (FE) and yield rate.

$$FE_{urea} = \frac{6 \times F \times C_{urea} \times V}{Q \times 60.06} \times 100\%$$

$$R_{urea} = \frac{C_{urea} \times V}{60.06 \times m_{cat} \times t}$$

$$FE_{NH_3} = \frac{3 \times F \times C_{NH_3} \times V}{Q \times 17} \times 100\%$$

$$R_{NH_3} = \frac{C_{NH_3} \times V}{17 \times m_{cat} \times t}$$

Where V is the electrolyte volume, C_{urea}/C_{NH_3} is the concentration of urea / NH_3 , F is the Faraday constant, Q is the electric quantity, m_{cat} is the mass of the catalyst, t is the electrolysis time.

Computation Method

Spin-polarized density functional theory (DFT) [1-3] simulations were performed with the Vienna *ab initio* simulation package (VASP) [4]. The Perdew-Burke-Ernzerhof (PBE) functional within the generalized gradient approximation (GGA) and the projector augmented-wave (PAW) potential were employed [5,6]. The $W_{18}O_{49}$ (-101) facet was built from the optimized $W_{18}O_{49}$ bulk until cell with lattice parameters of $a = 14.13 \text{ \AA}$, $b = 3.81 \text{ \AA}$, $c = 17.84 \text{ \AA}$, $\beta = 110.53^\circ$. The slab model consisting of $1 \times 2 \times 1$ supercell was considered in this simulation, including 36 W atoms and 98 O atoms. Top two atom layers of this slabs were relaxed, while bottom two atom layers were fixed during optimization. The vacuum region of $15 \text{ \AA}$ was used in the vertical direction to the $W_{18}O_{49}$ surface to avoid superficial interactions between periodical

slabs. The plane-wave cutoff energy of 500 eV and the Monkhorst-Pack k -points mesh of $3 \times 5 \times 1$ were adopted for all computations. The convergence criteria were set at 10^{-5} eV for total energy change and 0.05 eV $\text{\AA}^{-1}$ for the maximum forces on each atom, respectively. The Grimme's semiempirical DFT-D3 method of dispersion correction was included to properly describe the vander Waals (vdW) interactions [7]. The Gibbs free energy diagram and the adsorbed free energy during the electrocatalytic urea production were calculated using the computational hydrogen electrode (CHE) model developed by Nørskov et al [8,9].

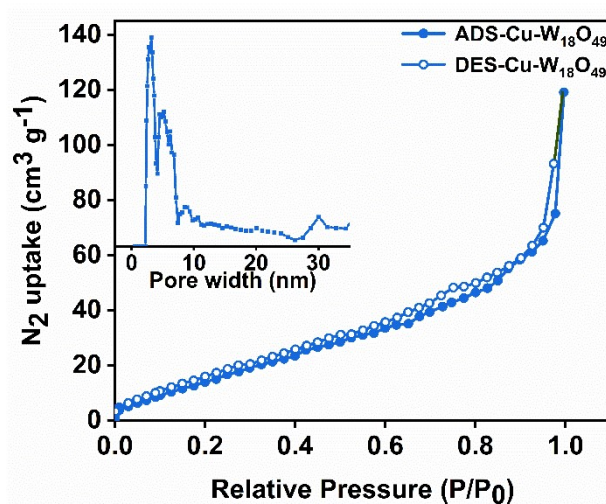


Fig. S1 Pore size distribution curve of $\text{Cu-W}_{18}\text{O}_{49}$.

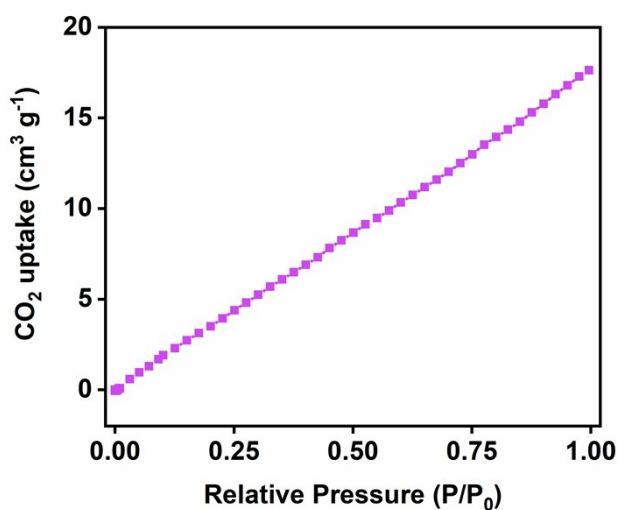


Fig. S2 CO_2 adsorption isotherm of $\text{Cu-W}_{18}\text{O}_{49}@\text{ZIF-8}$

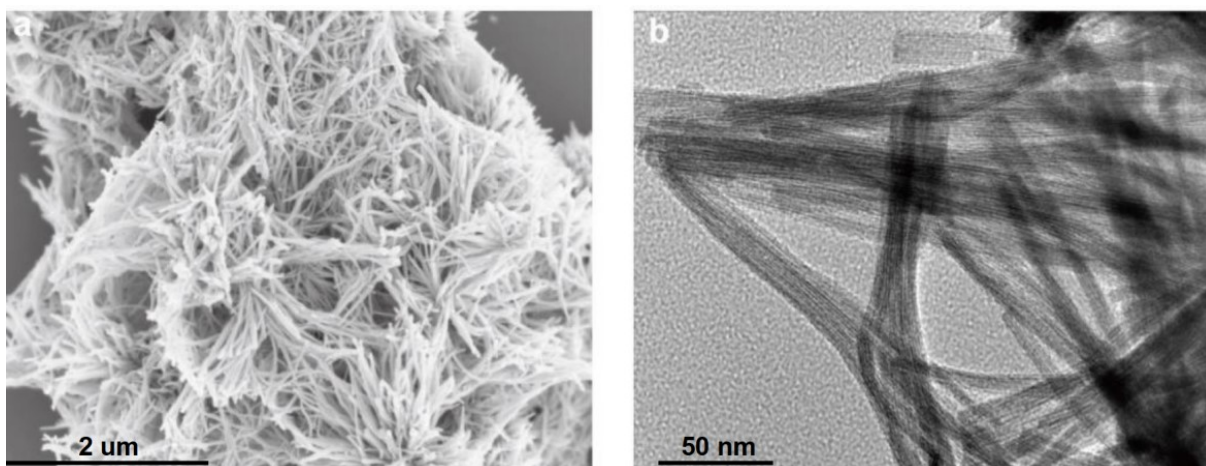


Fig. S3 SEM (a) and (b) image of Cu-W₁₈O₄₉.

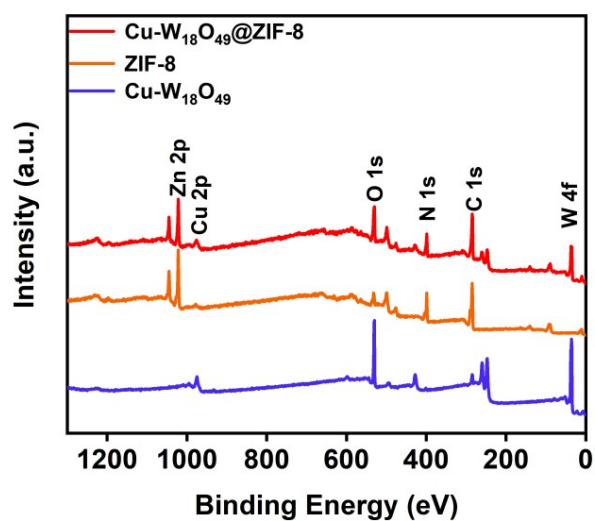


Fig. S4 XPS survey spectra of Cu-W₁₈O₄₉@ZIF-8.

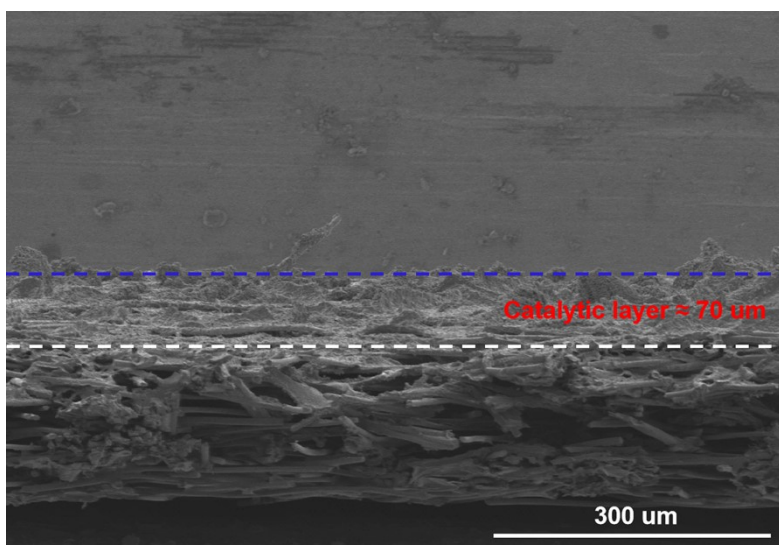


Fig. S5 SEM images of the thickness of the catalytic layer of the electrode.

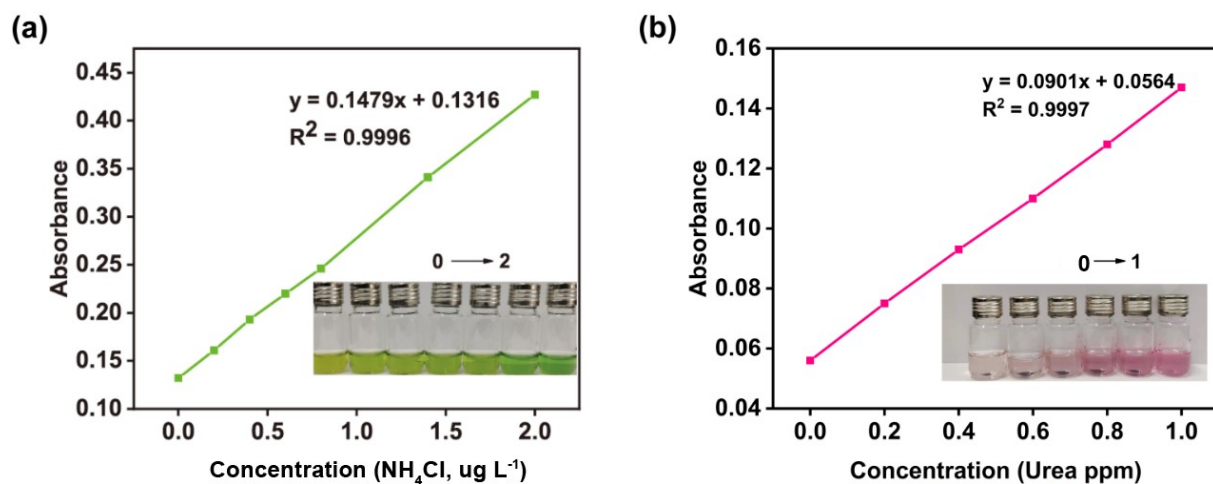


Fig. S6 (a) Concentration-absorbance of NH_4Cl solution with a series of standard concentration (0- 2 $\mu\text{g mL}^{-1}$) in 0.25 M K_2SO_4 and (b) Concentration-absorbance of urea solution with a series of standard concentration (0.2-1.0 $\mu\text{g mL}^{-1}$) in 0.25 M K_2SO_4 .

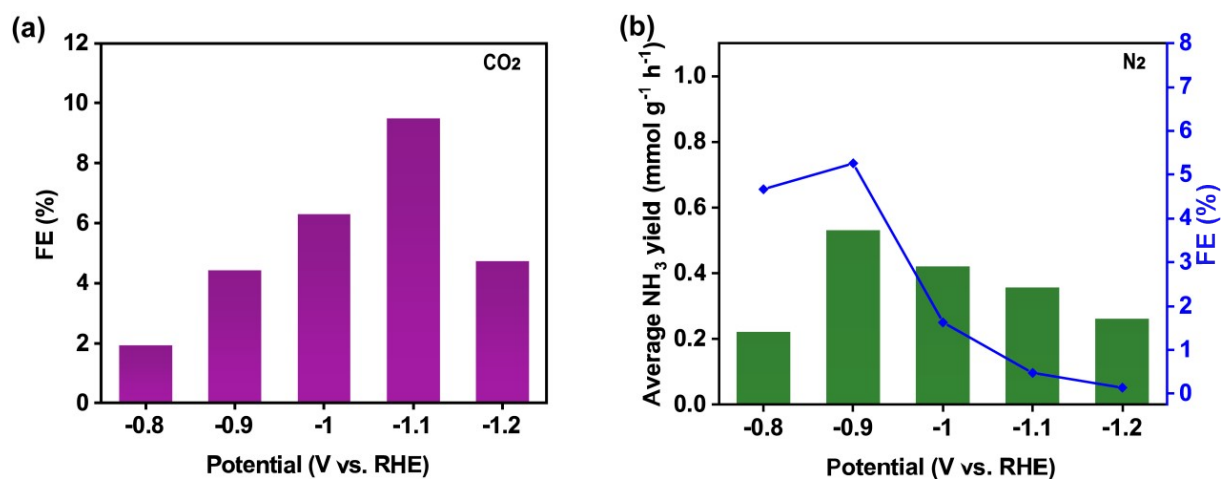


Fig. S7 (a) CO generate and (b) Ammonia product at various potentials for $\text{Cu-W}_{18}\text{O}_{49}@\text{ZIF-8}$.

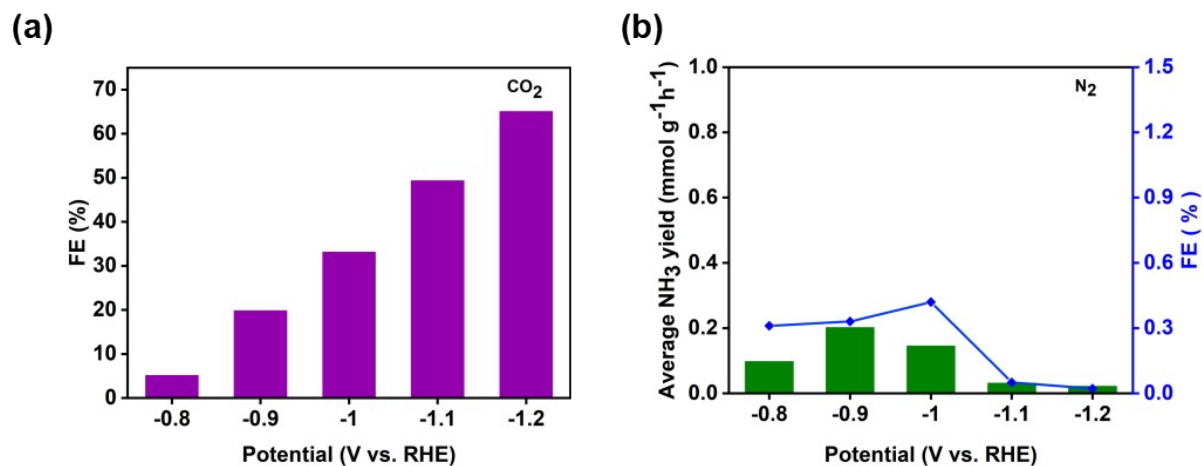


Fig.S8 (a) CO generate and (b) Ammonia product at various potentials for ZIF-8.

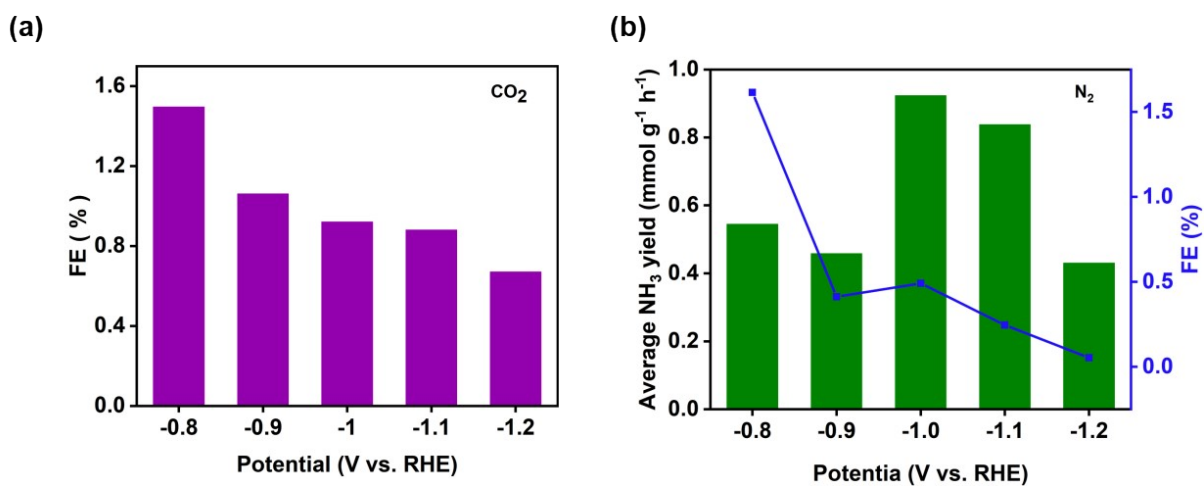


Fig. S9 (a) CO generate and (b) Ammonia product at various potentials for Cu-W₁₈O₄₉.

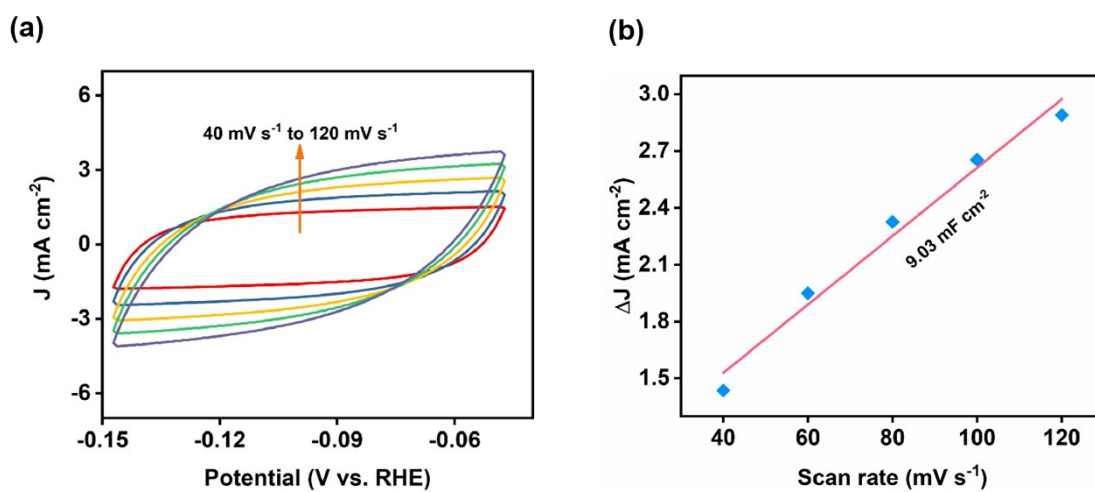


Fig.S10 (a) Different scan rate of Cu-W₁₈O₄₉@ZIF-8 (b) charging current density at different rates of Cu-W₁₈O₄₉@ZIF-8.

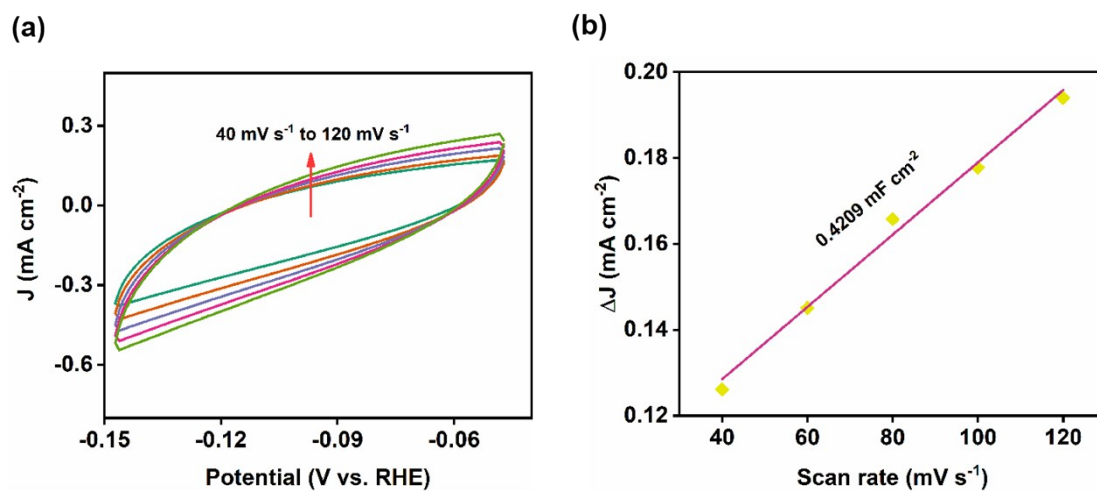


Fig. S11 (a) Different scan rate of $W_{18}O_{49}@ZIF-8$ (b) charging current density at different rates of $W_{18}O_{49}@ZIF-8$.

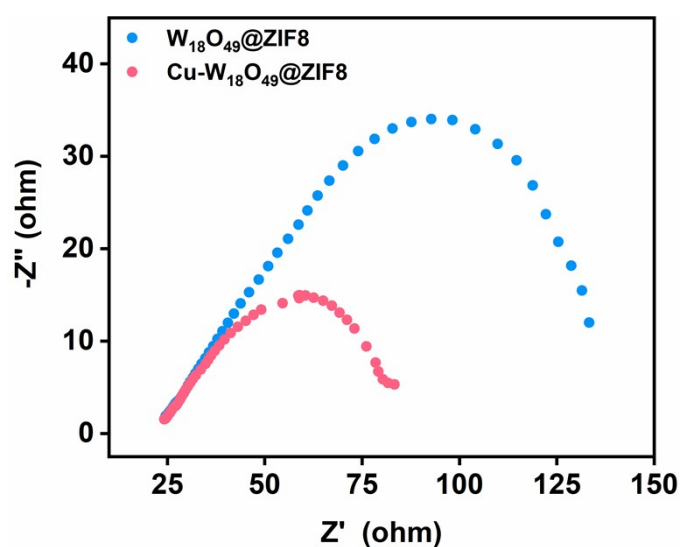


Fig. S12 Nyquist plots of $W_{18}O_{49}@ZIF-8$ and $Cu-W_{18}O_{49}@ZIF-8$.

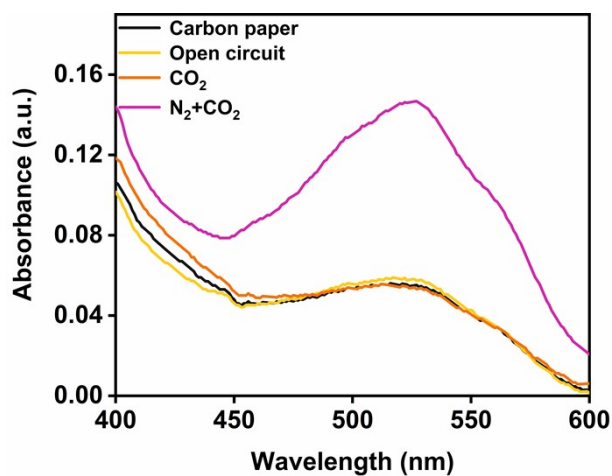


Fig. S13 The yield rate of urea under different reaction conditions ($V_{N_2}:V_{CO_2}=3:1$ at -1 V vs. RHE).

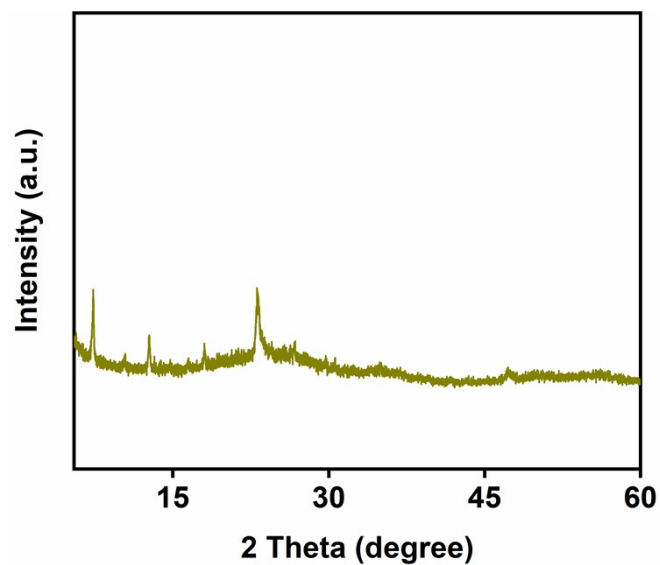


Fig. S14 XRD pattern of Cu-W₁₈O₄₉@ZIF-8 after electroreduction.

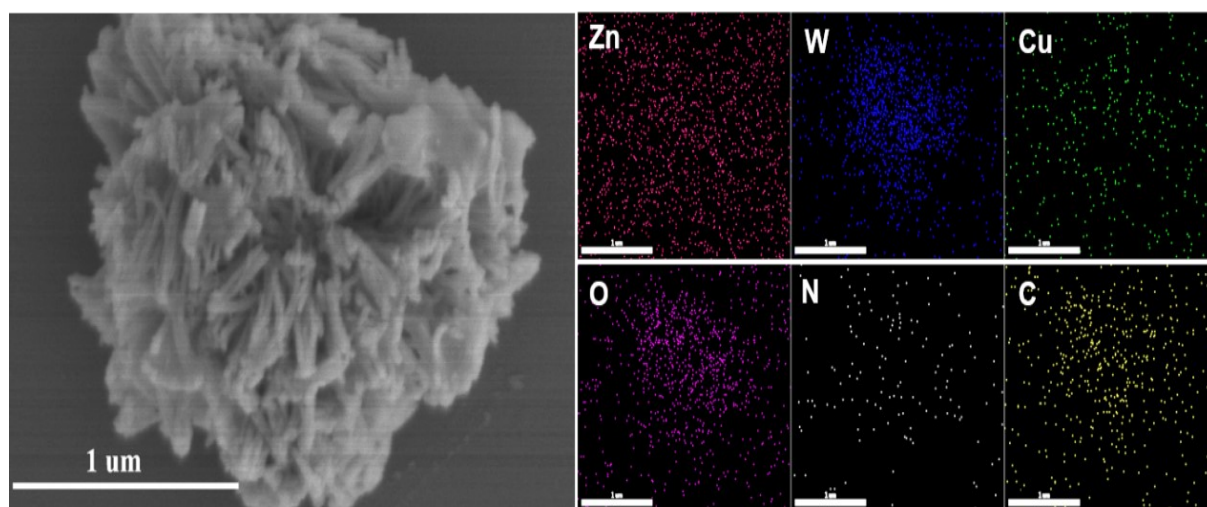


Fig. S15 SEM images of Cu-W₁₈O₄₉@ZIF-8 after electroreduction.

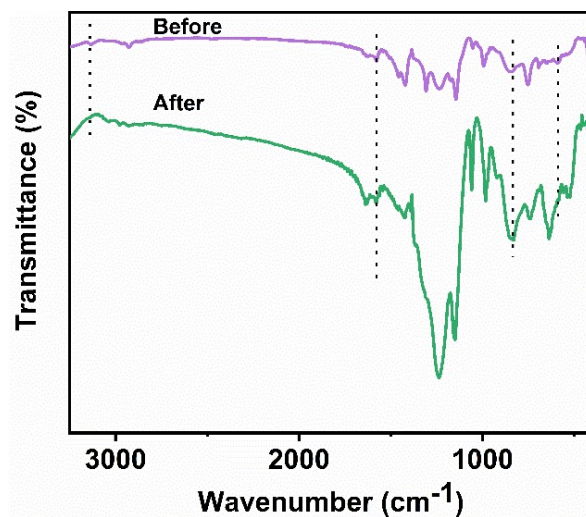


Fig. S16 FT-IR spectra of Cu-W₁₈O₄₉@ZIF-8 after electroreduction.

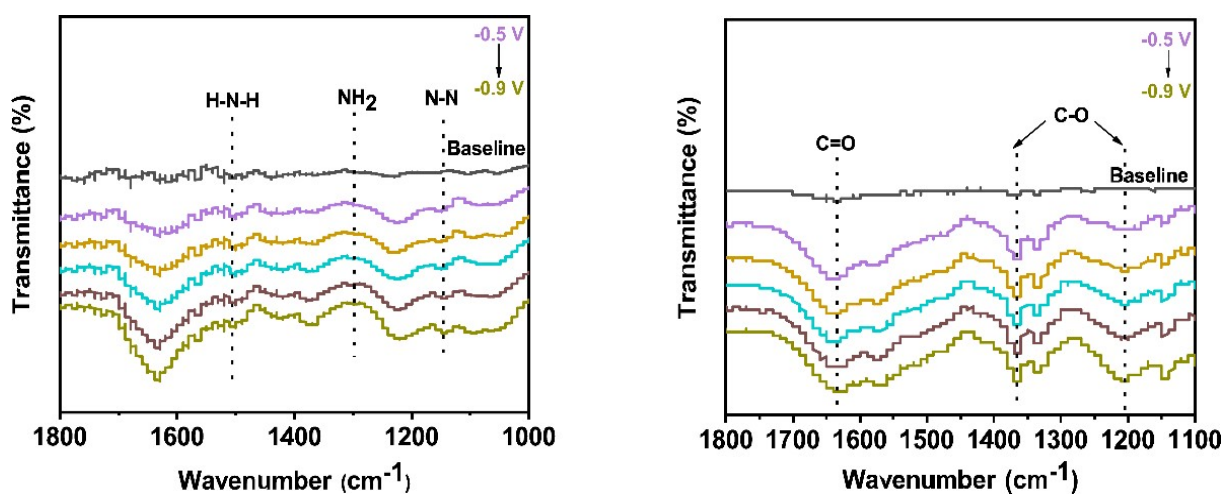


Fig. S17 In situ FT-IR spectra over Cu-W₁₈O₄₉@ZIF-8 with (a) N₂ and (b) CO₂ as the feeding gas.

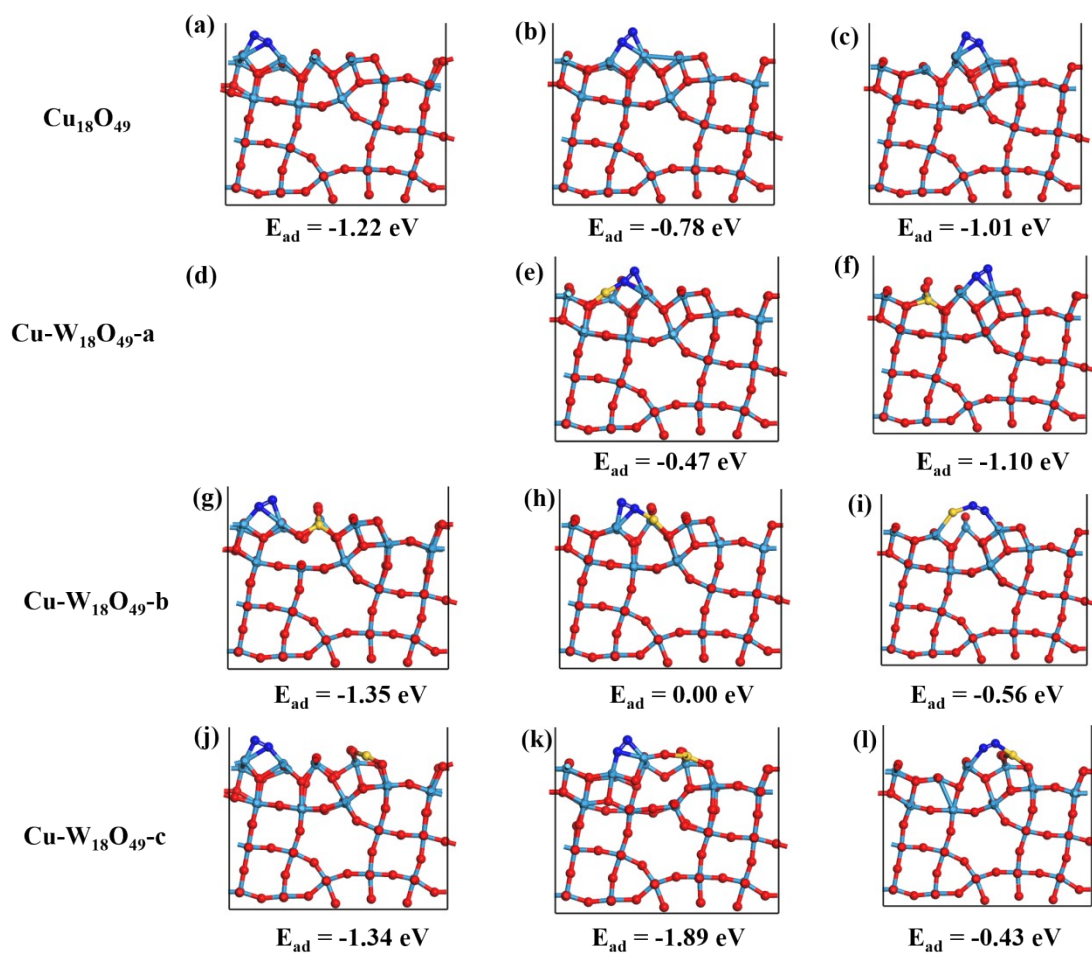


Fig. S18 Optimized structures and computed adsorption energies of $^*\text{N}_2$ intermediates on the different catalytic sites of $\text{W}_{18}\text{O}_{49}$ and $\text{Cu-W}_{18}\text{O}_{49}$. Note that the $^*\text{N}_2$ intermediate with side-on configuration in (d) can't be stable.

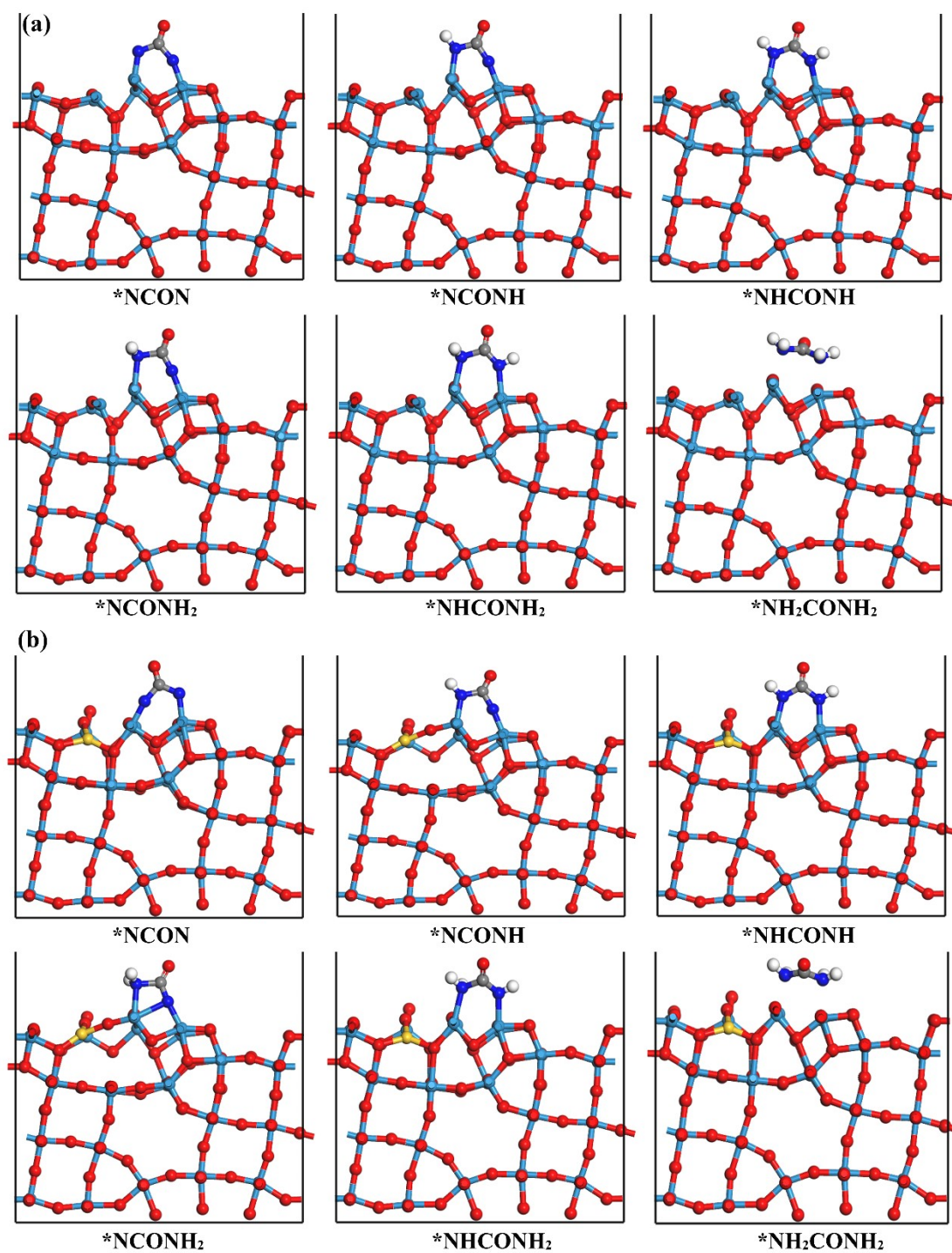


Fig. S19 Optimized structures of various intermediates for urea production on the (a) $W_{18}O_{49}$ and (b) $Cu-W_{18}O_{49-a}$.

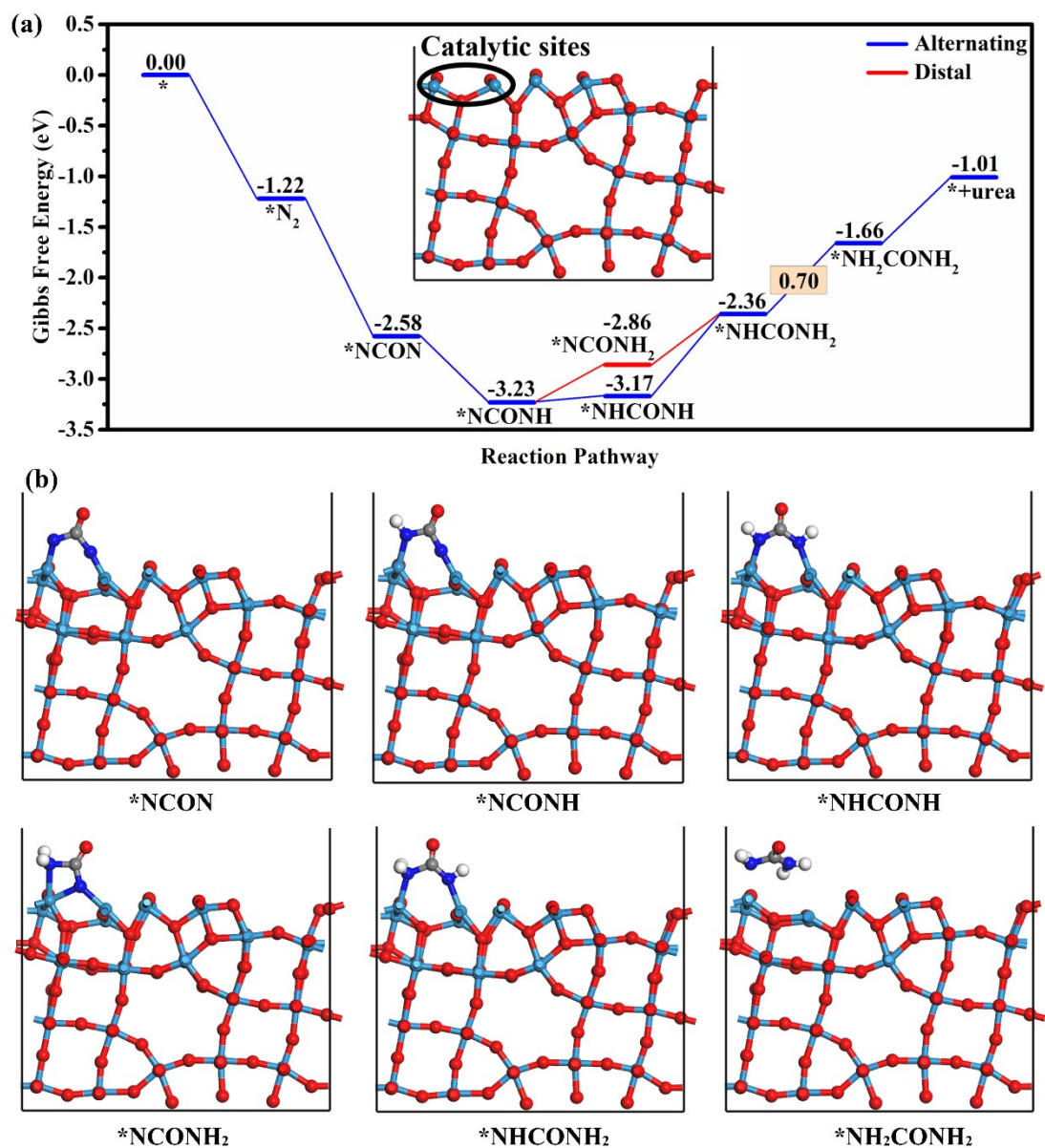


Fig. S20 (a) Gibbs free energy diagram and (b) optimized structures of various intermediates for urea production on the site $*N_2$ -a of $W_{18}O_{49}$.

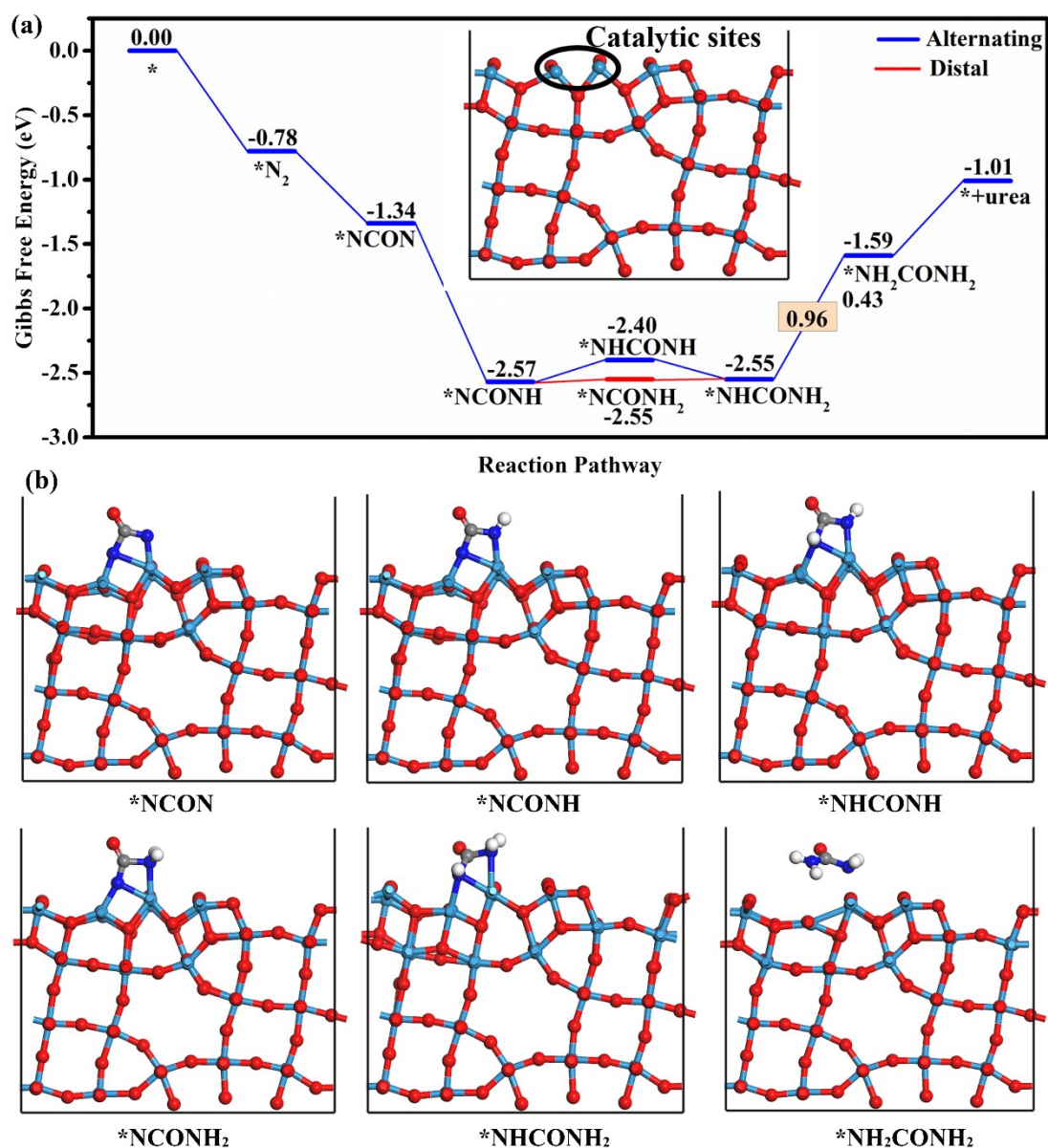


Fig. S21 (a) Gibbs free energy diagram and (b) optimized structures of various intermediates for urea production on the site $*N_2$ -b of $W_{18}O_{49}$.

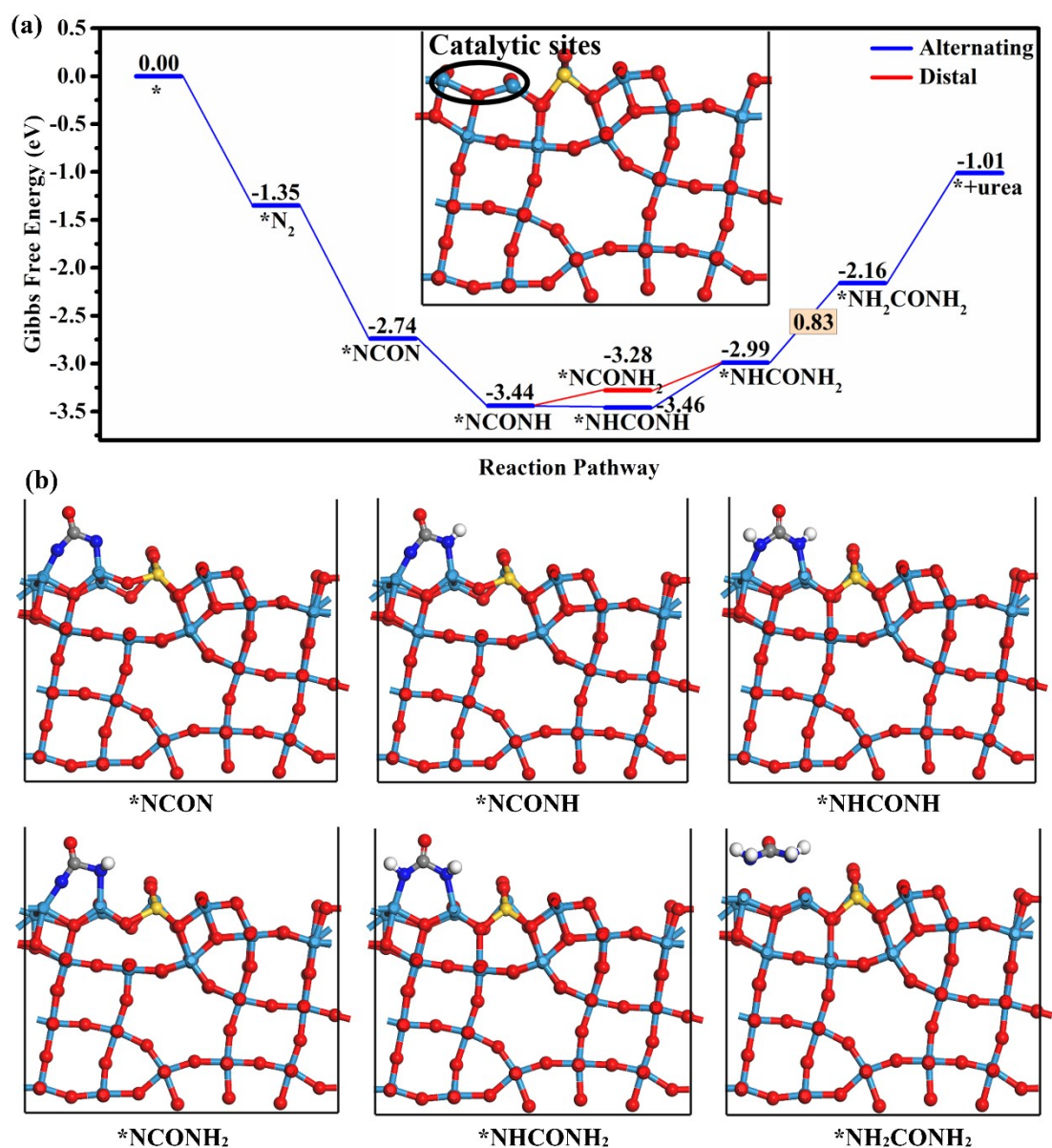


Fig. S22 (a) Gibbs free energy diagram and (b) optimized structures of various intermediates for urea production on the site $*N_2$ -g of Cu-W₁₈O₄₉-b.

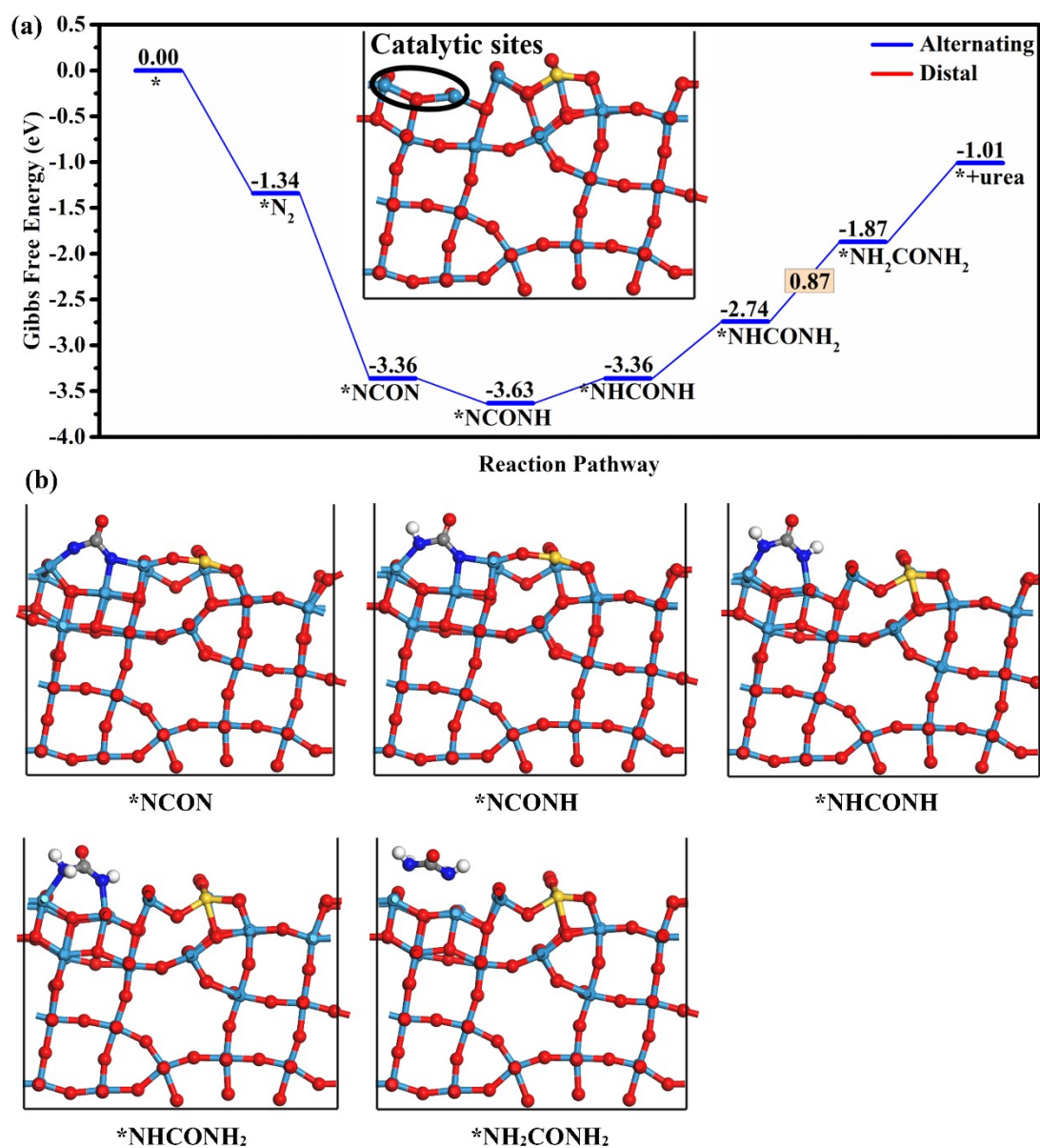


Fig. S23 (a) Gibbs free energy diagram and (b) optimized structures of various intermediates for urea production on the site $*N_2$ -j of Cu-W₁₈O₄₉-c.

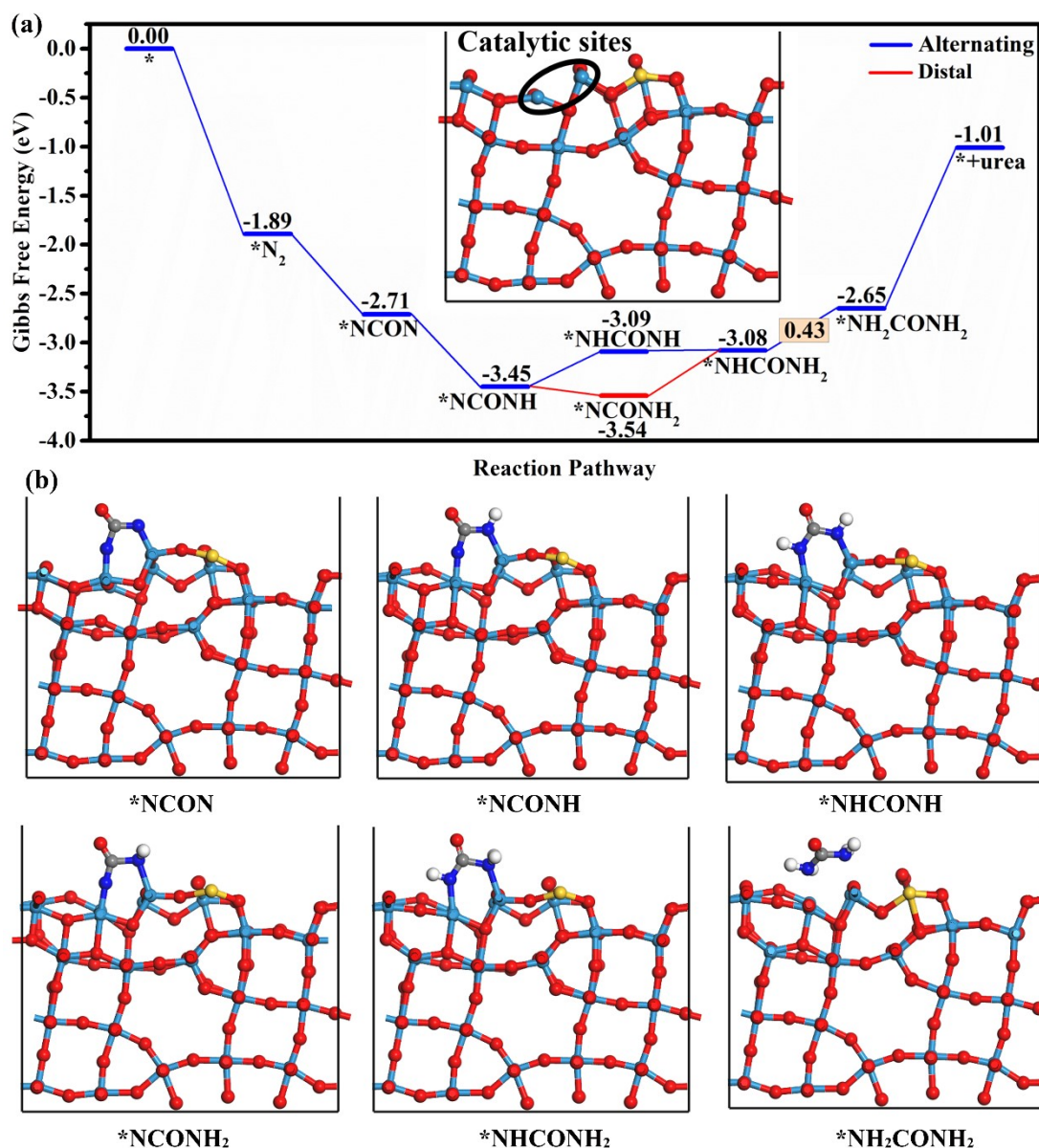


Fig. S24 (a) Gibbs free energy diagram and (b) optimized structures of various intermediates for urea production on the site $*N_2$ -k of Cu-W₁₈O₄₉-b.

Table S3. The weight ratio of Cu, W and Zn in Cu-W₁₈O₄₉@ZIF-8

Cu (wt%)	W (wt%)	Zn (wt%)
0.37	4.17	6.52

Table S4. Comparison of urea yield rate and FEs among $W_{18}O_{49}@ZIF-8$ and other reported urea synthesis electrocatalysts

Catalysts	$V_{N_2} : V_{CO_2}$	Urea yield (mmol $g^{-1} h^{-1}$)	Faradaic Efficiency (%)	ref
Cu-Pd alloy	1:1	3.36	8.92	34
Bi-BiVO ₄	1:1	5.91	12.55	35
BiFeO ₃ /BiVO ₄	1:1	4.94	17.18	36
Ni ₃ (BO ₃) ₂	1:1	9.7	20.36	37
InOOH	1:1	6.85	20.97	38
Co-PMDA-2-mnIM	1:1	14.5	48.97	39
CuPc NTs	1:1	2.39	12.99	40
MoP	1:1	0.206	36.5	41
PPy-coated Pt	1:1	2.4		42
Cu ₁ Pd ₁ -TiO ₂	1:1	166.67	22.54	43
		$mol_{urea} mol_{Pd}^{-1} h^{-1}$		
defective Cu-Bi	1:1	3.72	8.7 ± 1.7	44
V _N -Cu ₃ N-300	1:1	$81 \mu g h^{-1} cm^{-2}$	28.7	45
ZnMn-N ₂ Cl	1:1	4	63.5	46
Fe-N-C	1:1	0.156	2.13	47
Bi ₂ S ₃ /N-RGO	1:1	4.4	7.5	48
Sb _x Bi _{1-x} O _y	9:1	5.13	10.9	49
Cu ^{III} -HHTP	1:1	7.78	23.09	50
Cu- $W_{18}O_{49}@ZIF-8$	Simulated flue gas	1.33	16.1	This work

Table S5. Computed Gibbs free energies (ΔG , eV) of reaction $*N_2 + CO \rightarrow *NCON$ and $*N_2 + H^+ + e^- \rightarrow *NNH$ on the different catalytic sites of $W_{18}O_{49}$ and $Cu_{18}O_{49}-Cu$.

Sites	$\Delta G (*N_2 + CO \rightarrow *NCON)$	$\Delta G (*N_2 + H^+ + e^- \rightarrow *NNH)$
*N ₂ -a on $W_{18}O_{49}$	-1.36	-0.01
*N ₂ -b on $W_{18}O_{49}$	-0.56	0.27
*N ₂ -c on $W_{18}O_{49}$	-1.35	-0.16
*N ₂ -e on $Cu-W_{18}O_{49}$ -a	-0.03	-0.69
*N ₂ -f on $Cu-W_{18}O_{49}$ -a	-0.49	0.10
*N ₂ -g on $Cu-W_{18}O_{49}$ -b	-1.39	0.00
*N ₂ -h on $Cu-W_{18}O_{49}$ -b	0.58	-0.73
*N ₂ -i on $Cu-W_{18}O_{49}$ -b	0.99	0.09
*N ₂ -j on $Cu-W_{18}O_{49}$ -c	-2.02	0.29
*N ₂ -k on $Cu-W_{18}O_{49}$ -c	-0.82	0.32
*N ₂ -l on $Cu-W_{18}O_{49}$ -c	0.86	-0.48

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