

## *Supplemental Information*

### **Dual-Function Thiourea for Photochemical Recovery of Precious Metals in Fe(III)-Oxalate Based System**

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## ***EXPERIMENTAL SECTION***

***Materials and Reagents.*** Spent Pt-/Pd-containing catalysts used in this work were obtained from chemical industries. Deactivated Au-containing catalyst was obtained after lab test. All the catalysts were scrapped (Loss on ignition, LOI >5 wt.%), and they were used in the form of powder (60 meshes) throughout the experiment. Iron oxide ( $\text{Fe}_2\text{O}_3$ ,  $\geq 99.0\%$ ), cerium nitrate hexahydrate ( $\text{Ce}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$ ,  $\geq 99.0\%$ ), oxalic acid dihydrate ( $\text{H}_2\text{C}_2\text{O}_4 \cdot 2\text{H}_2\text{O}$ ,  $\geq 99.5\%$ ), thiourea ( $\text{CH}_4\text{N}_2\text{S}$ ,  $\geq 99.0\%$ ), *tert*-butyl alcohol ( $\text{C}_4\text{H}_{10}\text{O}$ ,  $\geq 99.5\%$ ), methanol ( $\text{CH}_3\text{OH}$ ,  $\geq 99.5\%$ ), sodium chloride ( $\text{NaCl}$ ,  $\geq 99.5\%$ ), urea ( $\text{CH}_4\text{N}_2\text{O}$ ,  $\geq 99.0\%$ ), ammonium sulfate ( $(\text{NH}_4)_2\text{SO}_4$ ,  $\geq 99.0\%$ ), ammonium persulfate ( $(\text{NH}_4)_2\text{S}_2\text{O}_8$ ,  $\geq 98.0\%$ ), and thioacetamide ( $\text{C}_2\text{H}_5\text{NS}$ ,  $\geq 99.0\%$ ) of analytical grade and were purchased from Sinopharm Chemical Reagent Co., Ltd. Chloroplatinic acid hydrate ( $\text{H}_2\text{PtCl}_6 \cdot \text{H}_2\text{O}$ ,  $\geq 99.0\%$ ), Gold chloride hydrate ( $\text{HAuCl}_4 \cdot \text{H}_2\text{O}$ ,  $\geq 99.0\%$ ), Ammonium tetrachloropalladate ( $(\text{NH}_4)_2\text{PdCl}_4$ ,  $\geq 99.0\%$ ), Ammonium thiosulfate ( $(\text{NH}_4)_2\text{S}_2\text{O}_3$ , 98%) and *p*-Benzoquinone ( $\text{C}_6\text{H}_4\text{O}_2$ , 99%) and 5,5-dimethyl-1-pyrroline-N-oxide ( $\text{C}_7\text{H}_{12}\text{N}_2\text{O}$ , 97%) were purchased from Aladdin Chemical Reagent Co., Ltd.

### ***Photocatalytic Dissolution of Au, Pt, and Pd***

#### **1. Screening Experiments for Sulfide Ligands**

Some sulfides, such as ammonium sulfate, ammonium thiosulfate, ammonium persulfate, thioacetamide, and thiourea, were used as ligand for photochemical dissolution in FOC-based system. In these lixivants, the volume ratio of parent Fe(III)-oxalate addition (The concentration of parent FOC was approximately  $0.1 \text{ mol} \cdot \text{L}^{-1}$  detected by ICP-OES.) was 50 vol.% ( $\sim 0.05 \text{ mol} \cdot \text{L}^{-1}$ ), and the concentration of sulfides was  $60 \text{ g} \cdot \text{L}^{-1}$ . In the dissolution experiments, 50 mL FOC-sulfide lixivants was mixed with 0.05 g Au/CeZr, 0.5 g Pt/CM, and 0.5 g Pd/ $\text{Al}_2\text{O}_3$  catalyst powders to

photochemical reaction for 4 hours, respectively. To investigate the effect of thiocarbonyl group, the comparison study of FOC-urea lixiviant was carried out, and the experimental conditions are the same as the aforementioned FOC-sulfide lixiviant.

## **2. Optimal Conditions for Single Precious Metal Photochemical Dissolution**

The volume ratio of parent Fe(III)-oxalate addition, thiourea concentration in the lixiviant, solid-to-liquid ratio of PMs-containing catalysts, and the dissolution time were investigated in sequence.

For the single-factor test of addition amount of parent Fe(III)-oxalate, 0.05 g Au/CeZr, 0.5 g Pt/CM, or 0.5 g Pd/Al<sub>2</sub>O<sub>3</sub> catalyst powders were put into 50 mL lixiviant to photochemically dissolve for 4 h, respectively. The thiourea concentration was 60 g·L<sup>-1</sup> in the lixiviant, and the addition amounts of FOC solution were ranged into 0 vol.% (0 mol·L<sup>-1</sup>), 25 vol.% (~0.02 mol·L<sup>-1</sup>), 50 vol.% (~0.05 mol·L<sup>-1</sup>), 75 vol.% (~0.07 mol·L<sup>-1</sup>), and 100 vol.% (~0.1 mol·L<sup>-1</sup>), respectively.

For the single-factor test of thiourea concentration in the lixiviant, the component was changed from 20 g·L<sup>-1</sup> to 100 g·L<sup>-1</sup>. The usage of spent catalysts was still 0.05 g Au/CeZr, 0.5 g Pt/CM, or 0.5 g Pd/Al<sub>2</sub>O<sub>3</sub> catalyst powders in 50 mL lixiviant, reaction for 4 h. While the addition amount of FOC was 25 vol.% in Au dissolution experiment, and was 50 vol.% in Pt or Pd dissolution experiment.

For the single-factor test of solid-to-liquid (S-L) ratio of PMs-containing catalysts and lixiviant, the usages of spent catalysts were quite different due to their different contents of PMs. In the experiment of Au dissolution, 50 mL lixiviant containing 25 vol.% FOC and 40 g·L<sup>-1</sup> thiourea was used to react for 4 h. The usages of Au/CeZr powder were 0.01 g (S-L=0.2 mg·mL<sup>-1</sup>), 0.02 g (S-L=0.4 mg·mL<sup>-1</sup>), 0.03 g (S-L=0.6 mg·mL<sup>-1</sup>), 0.04 g (S-L=0.8 mg·mL<sup>-1</sup>), and 0.05 g (S-L=1.0 mg·mL<sup>-1</sup>), respectively. In the experiment of Pt dissolution, 50 mL lixiviant containing 50 vol.% FOC and 60 g·L<sup>-1</sup>

thiourea was used to react for 4 h. The usages of Pt/CM powder were 0.1 g (S-L=2 mg·mL<sup>-1</sup>), 0.2 g (S-L=4 mg·mL<sup>-1</sup>), 0.3 g (S-L=6 mg·mL<sup>-1</sup>), 0.4 g (S-L=8 mg·mL<sup>-1</sup>), and 0.5 g (S-L=10 mg·mL<sup>-1</sup>), respectively. In the experiment of Pd dissolution, 50 mL lixiviant containing 50 vol.% FOC and 60 g·L<sup>-1</sup> thiourea was used to react for 4 h. The usages of Pd/Al<sub>2</sub>O<sub>3</sub> powder were 0.5 g (S-L=10 mg·mL<sup>-1</sup>), 0.6 g (S-L=12 mg·mL<sup>-1</sup>), 0.7 g (S-L=14 mg·mL<sup>-1</sup>), 0.8 g (S-L=16 mg·mL<sup>-1</sup>), and 0.9 g (S-L=18 mg·mL<sup>-1</sup>), respectively. Herein, the PM dissolution efficiency ( $\eta$ ) was calculated in accordance with **eq. S1**.

$$\eta_i (\%) = \frac{V_i \times C_i}{\omega_i \times m_i} \times 100 \quad (\text{S1})$$

Where  $i$  represents the PMs of gold, platinum and palladium, respectively.  $\omega$  is the mass concentration of PMs in the wastes, mg·kg<sup>-1</sup>.  $m$  is the mass of waste addition, kg.  $V$  is the volume of PM-containing lixivium, L.  $C$  is the PM concentration in the lixivium, mg·L<sup>-1</sup>.

Apparently, the dissolution rate of  $r$  was necessary to be introduced to describe the dissolution amount of PMs for per hour in the whole process when the PMs were dissolved from the secondary resources under the optimal conditions, as followed in the **eq. S2**.

$$r_i = \frac{M_i}{t} \quad (\text{S2})$$

Where  $M$  is the mass of PMs in the leaching solution under the optimal condition, mg.  $t$  is the reaction time, h.

### **3. Photochemical Dissolution Performance for Blended Precious Metals**

Considering about the dissolution priority of PMs in a blended feeding, so it was necessary to discuss the co-dissolution performance for PMs recovery. In this section, the FOC-T lixiviant contained 50 vol.% FOC and 60 g·L<sup>-1</sup> thiourea. The changes of

photochemical dissolution efficiency with 0.17 g Pt/CM (~0.1 mg Pt) + 0.24 g Pd/Al<sub>2</sub>O<sub>3</sub> (~0.1 mg Pd) powder or 0.01 g Au/CeZr (~0.1 mg Au) + 0.24 g Pd/Al<sub>2</sub>O<sub>3</sub> (~0.1 mg Pd) powder in 100 mL FOC-T lixiviant were recorded within 6 hours. Then, the dissolution efficiencies of lixiviant mixed with 0.17 g Pt/CM (~0.1 mg Pt) + 0.47 g Pd/Al<sub>2</sub>O<sub>3</sub> (~0.2 mg Pd) powder, 0.34 g Pt/CM (~0.2 mg Pt) + 0.24 g Pd/Al<sub>2</sub>O<sub>3</sub> (~0.1 mg Pd) powder, and 0.34 g Pt/CM (~0.2 mg Pt) + 0.47 g Pd/Al<sub>2</sub>O<sub>3</sub> (~0.2 mg Pd) powder were investigated after the photochemical dissolution for 5 h. Meanwhile, 0.01 g Au/CeZr (~0.1 mg Au) + 0.47 g Pd/Al<sub>2</sub>O<sub>3</sub> (~0.2 mg Pd) powder, 0.02 g Au/CeZr (~0.2 mg Au) + 0.24 g Pd/Al<sub>2</sub>O<sub>3</sub> (~0.1 mg Pd) powder, and 0.02 g Au/CeZr (~0.2 mg Au) + 0.47 g Pd/Al<sub>2</sub>O<sub>3</sub> (~0.2 mg Pd) powder were also mixed with FOC-T lixiviant to react for 4 h to obtain the dissolution performance for blended precious metals of Au and Pd.

#### 4. Kinetics Rate Calculation and Additional Experiments of Single Precious Metal

To make sure the comparability among dissolution kinetics rates, the input amount of single PMs should be consistent. 0.51 g Pt/CM (~0.3 mg Pt), 0.71 g Pd/Al<sub>2</sub>O<sub>3</sub> (~0.3 mg Pd), or 0.03 g Au/CeZr (~0.3 mg Au) powders was added into 50 mL FOC-T lixiviant to react within 1 h, respectively. All the lixiviants contained 50 vol.% FOC and 60 g·L<sup>-1</sup> thiourea. Herein, the chemical reaction control model (eq. S3) and the diffusion control model (eq. S4) were used to simulate the dissolution kinetics of PMs and evaluate the dissolution rate during the photocatalytic dissolution<sup>1</sup>.

$$1 - (1 - x_i)^{\frac{1}{3}} = k_1 t \quad (\text{S3})$$

$$1 - \frac{2}{3} x_i - (1 - x_i)^{\frac{2}{3}} = k_2 t \quad (\text{S4})$$

Where x denotes the PMs dissolution efficiency, %. k<sub>1</sub> and k<sub>2</sub> are the reaction rate constants of the two models, respectively, h<sup>-1</sup>. t is the reaction time, h.

When it came to study on the effect of FOC and thiourea in FOC-T system, the

optimal dissolution conditions were applied for Au, Pt or Pd recovery according to section S1. The photochemical dissolution efficiencies of Au, Pt, and Pd were investigated with the lixivants of bare FOC under darkness or irradiation, bare thiourea under darkness or irradiation, and FOC-T under darkness. Additionally, the thiourea ligand was replaced by NaCl to determine the differences during photochemical dissolution of PMs. The concentration of ligand was still 40 g·L<sup>-1</sup> for Au dissolution, 60 g·L<sup>-1</sup> for Pt and Pd dissolution. Then, photochemical liquid oxidant of FOC was changed into the TiO<sub>2</sub> (P25) or g-C<sub>3</sub>N<sub>4</sub> photocatalysts, and the total volume was 50 mL containing 50 mg solid catalysts and a certain concentration of thiourea in deionized water to dissolve PMs for a period of irradiation. It evaluated the differences of photochemical dissolution performance among different ligands and photochemical oxidants for the PMs recovery.

### ***Computational Methods***

A plane wave (PW) energy cutoff of 450 Ry was employed for the calculation of electrostatic energy terms, while a relative cutoff of 50 Ry was utilized for Gaussian mapping on multigrid levels. the adsorption energy ( $\Delta E_{\text{ads}}$ ) between the thiourea molecule and PMs were defined as followed in **eq. S5**.

$$\Delta E_{ad} = E_{Total}^{Thio-M} - E_{Frag}^{Thio} - E_{atom}^M \quad (\text{S5})$$

Where the  $M$  represents the PMs, i.e. Au, Pt, and Pd.  $Thio-M$  denotes the adsorbed states between thiourea and PMs.  $E_{Total}^{Thio-M}$  is the total energies of adsorbed states.  $E_{Frag}^{Thio}$  is the energy of thiourea fragment.  $E_{atom}^M$  is the energy of PM atoms.

The formation energy ( $\Delta E_f$ ) of thiourea oxidization in FOC-T and TiO<sub>2</sub>-thiourea systems were given out as followed in **eq. S6**.

$$\Delta E_f = E_{Sol}^{(Thio)^*O} - E_{Sol}^{Thio} - E_{Sol}^{*O} \quad (\text{S6})$$

Where  $(Thio)^*O$  denotes the oxidization product of thiourea.  $Sol$  is the liquid phase compositions of FOC or  $H_2O$  ( $TiO_2$ ). condition PMs-Thiourea complexes.  $E_{Sol}^{(Thio)^*O}$  is the total energy of thiourea oxidization in FOC or  $H_2O$  ( $TiO_2$ ).  $E_{Sol}^{Thio}$  is the energy of an isolated thiourea molecule in FOC or  $H_2O$  ( $TiO_2$ ), and  $E_{Sol}^{*O}$  is the energy of reactive oxygen atom in FOC or  $H_2O$  ( $TiO_2$ ).

### ***Characterization.***

All the spent catalyst powders were dissolved in the aqua regia solution to determine the contents of precious metals by inductively coupled plasma–optical emission spectrometry (ICP-OES). Fourier transform infrared spectroscopy (FTIR) was used to estimate the chemical structures in range from  $4000\text{ cm}^{-1}$ – $400\text{ cm}^{-1}$  with a resolution of  $4\text{ cm}^{-1}$ . X-ray photoelectron spectroscopy (XPS) was used to analyze the valence bands related to Au 4f, Pt 4f and Pd 3d of PMs, and S 2p in the PMs(Thio). XPS was equipped with an Al K $\alpha$  anode monochromatic X-ray source (1486.6 eV), whose binding energy values were regulated with referenced to the adventitious C 1s position at 284.8 eV. Confocal laser Raman spectrometer equipped with 532 nm (5 mW) wave-length laser and the data was collected by corresponding software (Wire) in the Raman shift from 200 to  $2000\text{ cm}^{-1}$ . The Raman shift was calibrated to  $520\text{ cm}^{-1}$  using a Si wafer. The crystal phases of samples were measured using an X-ray diffraction (XRD) equipped with Cu K $\alpha$  radiation source ( $\lambda = 1.54\text{ \AA}$ ) from  $10^\circ$  to  $60^\circ$  in  $2\theta$  range with  $0.020^\circ$  step interval and 2 sec  $\text{step}^{-1}$  counter time. The UV-vis spectrophotometer from 190 to 900 nm was recorded with a UV2600 spectrophotometer. FTIR, XPS, Raman, and UV-vis analysis were applied for the final product powder obtained after the washing and drying from the product powder. Electron paramagnetic resonance (EPR) was used to qualitatively analyze the formation

of  $\cdot\text{OH}$ ,  $\text{SO}_4^{\cdot-}$  and  $\text{O}_2^{\cdot-}$ . EPR spectra were measured by the trapping agent of DMPO at room temperature with a center field of 3500 G, resonance frequency of 9.88 GHz, microwave power of 1.65 mW, modulation frequency of 100 kHz, sweep width of 200 G. Laser flash photolysis (LFP) spectrometer equipped with LP920-KS system was used to detect the generation of active radicals and evaluate their lifetime in the solution under the irradiation.  $[\text{Fe}_2(\text{C}_2\text{O}_4)_3] \approx 1.83 \times 10^{-3}$  M,  $[\text{H}_2\text{C}_2\text{O}_4] \approx 2.62 \times 10^{-2}$  M. The pump laser is a Nd:YAG laser (10 Hz rep rate) operating at 355 nm with pulse duration 7 ns. The system is normally operated at 1 Hz. The probe is a 450 W pulsed Xenon arc lamp for kinetic and spectral measurements. The spectral range is 200-850 nm, and the temporal resolution is 50 ns.

### ***Catalyst Preparation and Catalytic Activity Measurement for Toluene Degradation***

#### **1. PMs/CeO<sub>2</sub> Catalysts Prepared by Commercial Reagents and Recovered Lixiviums**

CeO<sub>2</sub> nanocubes were synthesized by a hydrothermal method at 180 °C for 24 h under autogenous pressure and static conditions as mentioned by Sun et al.<sup>2</sup> The recovered Au, Pt, and Pd-containing lixiviums were approximately concentrated to 0.1 g/L (PMs contents) detected by ICP-OES. Then, a total 0.4 g of CeO<sub>2</sub> nanocube was dispersed into the 20 mL PMs-containing lixivium and stirred at room temperature for 1 h. 2 mL NaBH<sub>4</sub> and NaOH mixing solution (NaBH<sub>4</sub>/NaOH = 1/5, molar ratio) was added to the suspension mentioned above, and the suspension was then stirred for another 1 h. Finally, the samples were washed with deionized water four times and ethanol once, and dried in the oven at 80 °C for 12 h, as denoted PMs (Pt, Pd, Au)/CeO<sub>2</sub>-R. At the same time, the commercial PMs reagents were also prepared into 0.1 g/L solution, the follow-up method was the same as aforementioned synthesis procedure. The catalysts are denoted as PMs (Pt, Pd, Au)/CeO<sub>2</sub>-C.



## 2. Catalytic Activity Measurement of Toluene Oxidation Degradation

The catalytic activity of toluene oxidation was performed at atmospheric pressure in a tubular fixed-bed reactor system of 4 mm inner diameter. The reaction mixtures were flowed into 0.1 g (40-60 meshes) catalysts with a weight hourly space velocity (WHSV) of 60000 mL·g<sup>-1</sup>·h<sup>-1</sup>. The component of the feed gases was 1000 ppm toluene, 20% O<sub>2</sub>/N<sub>2</sub>, and the total flow rate was 100 mL/min. The 1000 ppm toluene in the gas mixture was produced through a bottle filled with pure toluene by using an N<sub>2</sub> bubbler. All reaction gas lines were heated to 100 °C by a heating belt to prevent toluene condensation on the tube walls. The reactants and products were in-situ analyzed online by using a gas chromatograph (Shimadzu, GC-2014) equipped with a flame ionization detector (FID) and thermal conductivity detector (TCD). The conversion of toluene was calculated according to **eq. S7**.

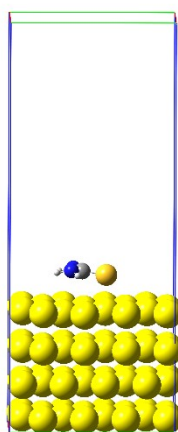
$$X_{Toluene} = \frac{[Toluene]_{in} - [Toluene]_{out}}{[Toluene]_{in}} \times 100\% \quad (S7)$$

where [Toluene]<sub>in</sub> represents the inlet toluene concentration, and [Toluene]<sub>out</sub> is the outlet toluene concentration.

## Structural Parameters of Adsorption Model with Thiourea Molecule and Au

|    |       |            |             |            |
|----|-------|------------|-------------|------------|
|    | Tv_1: | 9.989800   | 0.000000    | 0.000000   |
|    | Tv_2: | 0.000000   | 11.535200   | 0.000000   |
|    | Tv_3: | 0.000000   | 0.000000    | 28.598672  |
| Au |       | 4.79644193 | 1.94838087  | 0.74077596 |
| Au |       | 9.79143664 | 4.83113774  | 0.74634355 |
| Au |       | 1.47935392 | 1.94609309  | 3.23040732 |
| Au |       | 6.46533473 | 4.82777777  | 3.19746022 |
| Au |       | 8.14796539 | 1.94194515  | 5.64622237 |
| Au |       | 3.15720646 | 4.82758144  | 5.62860874 |
| Au |       | 4.82404135 | 1.91679057  | 8.09982856 |
| Au |       | 9.82388491 | 4.83099436  | 8.13154363 |
| Au |       | 7.29287297 | 0.50975260  | 0.74136109 |
| Au |       | 2.29906186 | 3.38838448  | 0.74041390 |
| Au |       | 3.97530845 | 0.50425539  | 3.21857234 |
| Au |       | 8.96907001 | 3.38687591  | 3.22197758 |
| Au |       | 0.65550081 | 0.50062480  | 5.65241684 |
| Au |       | 5.64292973 | 3.39132873  | 5.65855498 |
| Au |       | 7.32275496 | 0.49506702  | 8.12931065 |
| Au |       | 2.31591066 | 3.37433138  | 8.09596603 |
| Au |       | 9.79261563 | 1.94938766  | 0.76003573 |
| Au |       | 4.79378824 | 4.83011561  | 0.70633486 |
| Au |       | 6.46852767 | 1.95396552  | 3.23196681 |
| Au |       | 1.48018857 | 4.83146211  | 3.21425336 |
| Au |       | 3.15261395 | 1.94043346  | 5.63927833 |
| Au |       | 8.14584006 | 4.82274012  | 5.61527918 |
| Au |       | 9.82001036 | 1.93910772  | 8.13592781 |
| Au |       | 4.82986810 | 4.82612697  | 8.11133381 |
| Au |       | 2.29732174 | 0.50615073  | 0.74790418 |
| Au |       | 7.29244032 | 3.38880517  | 0.73751828 |
| Au |       | 8.96954233 | 0.50631961  | 3.22612782 |
| Au |       | 3.97538017 | 3.38786275  | 3.21335708 |
| Au |       | 5.65448614 | 0.50041036  | 5.63136651 |
| Au |       | 0.65334761 | 3.38939901  | 5.64053352 |
| Au |       | 2.32598947 | 0.49313384  | 8.12931522 |
| Au |       | 7.33940816 | 3.38216401  | 8.11034687 |
| Au |       | 4.79236190 | 7.71908084  | 0.69141436 |
| Au |       | 9.78670347 | 10.60274830 | 0.73343296 |
| Au |       | 1.46519807 | 7.71832194  | 3.18588177 |
| Au |       | 6.47473313 | 10.60509214 | 3.19002943 |
| Au |       | 8.14243074 | 7.72451738  | 5.60255363 |
| Au |       | 3.15172576 | 10.59452520 | 5.63210607 |
| Au |       | 4.81905365 | 7.74897800  | 7.94021051 |
| Au |       | 9.81544752 | 10.59172630 | 8.13803038 |

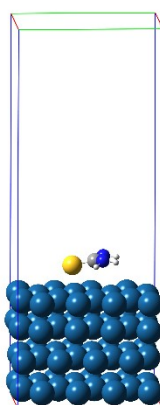
|    |            |             |             |
|----|------------|-------------|-------------|
| Au | 7.28949392 | 6.27367529  | 0.71257481  |
| Au | 2.29496794 | 9.16328950  | 0.71414058  |
| Au | 3.96970597 | 6.27197754  | 3.17218586  |
| Au | 8.96193579 | 9.16262830  | 3.20189187  |
| Au | 0.63484899 | 6.27319289  | 5.60882103  |
| Au | 5.65908464 | 9.17348465  | 5.56778508  |
| Au | 7.34521543 | 6.27908173  | 8.03041587  |
| Au | 2.32253789 | 9.15748164  | 8.12115145  |
| Au | 9.78691665 | 7.71766962  | 0.72828034  |
| Au | 4.79432230 | 10.60276676 | 0.71912819  |
| Au | 6.46235397 | 7.71072786  | 3.17951627  |
| Au | 1.47350809 | 10.59892957 | 3.21815365  |
| Au | 3.13541841 | 7.71898568  | 5.56496554  |
| Au | 8.15056474 | 10.59960600 | 5.63851703  |
| Au | 9.81788194 | 7.71869914  | 8.13915374  |
| Au | 4.82581614 | 10.58779303 | 8.13295297  |
| Au | 2.29597841 | 6.27538539  | 0.71259769  |
| Au | 7.28990670 | 9.16092109  | 0.711121408 |
| Au | 8.95973894 | 6.27241923  | 3.19587815  |
| Au | 3.96841568 | 9.16313862  | 3.17763791  |
| Au | 5.64066005 | 6.25877481  | 5.59834562  |
| Au | 0.64782624 | 9.15582495  | 5.63460359  |
| Au | 2.30608579 | 6.28592464  | 8.02583036  |
| Au | 7.31892238 | 9.15216714  | 8.12409968  |
| C  | 4.78885458 | 6.44814715  | 10.92290329 |
| S  | 4.66925280 | 4.75797885  | 10.66840199 |
| N  | 3.67853746 | 7.21020180  | 11.04104211 |
| H  | 2.81390778 | 6.77934143  | 10.72329371 |
| H  | 3.73637620 | 8.21403770  | 10.87979736 |
| N  | 5.99384124 | 7.05071197  | 11.04007176 |
| H  | 6.07796255 | 8.04539227  | 10.83582862 |
| H  | 6.79058423 | 6.49298344  | 10.74282546 |



## Structural Parameters of Adsorption Model with Thiourea Molecule and Pt

|    |       |            |             |            |
|----|-------|------------|-------------|------------|
|    | Tv_1: | 9.611600   | 0.000000    | 0.000000   |
|    | Tv_2: | 0.000000   | 11.098500   | 0.000000   |
|    | Tv_3: | 0.000000   | 0.000000    | 29.268817  |
| Pt |       | 4.63416787 | 1.89765294  | 1.14907649 |
| Pt |       | 9.43621156 | 4.67089862  | 1.12769181 |
| Pt |       | 1.44830588 | 1.88971241  | 3.43081609 |
| Pt |       | 6.24918743 | 4.66196432  | 3.45101275 |
| Pt |       | 7.85104928 | 1.88784519  | 5.67019758 |
| Pt |       | 3.05717084 | 4.66234800  | 5.71425475 |
| Pt |       | 4.66070579 | 1.85588285  | 7.96301455 |
| Pt |       | 9.46471159 | 4.66037114  | 7.97662367 |
| Pt |       | 7.03984341 | 0.50160670  | 1.12514220 |
| Pt |       | 2.23328563 | 3.28536088  | 1.14686464 |
| Pt |       | 3.84340606 | 0.50339877  | 3.43176762 |
| Pt |       | 8.66105198 | 3.28343507  | 3.42968573 |
| Pt |       | 0.63950829 | 0.49842476  | 5.67471756 |
| Pt |       | 5.44865457 | 3.27919622  | 5.71531868 |
| Pt |       | 7.06703617 | 0.49032662  | 7.96614719 |
| Pt |       | 2.23729819 | 3.26458992  | 7.96956228 |
| Pt |       | 9.44061127 | 1.89650136  | 1.13824176 |
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| Pt |       | 6.24919493 | 1.89471250  | 3.42906377 |
| Pt |       | 1.45231507 | 4.66676864  | 3.43269603 |
| Pt |       | 3.04331428 | 1.88228196  | 5.68544663 |
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| Pt |       | 9.46502512 | 1.87947415  | 7.96844626 |
| Pt |       | 4.65537644 | 4.65850337  | 8.06880581 |
| Pt |       | 2.23399295 | 0.50885402  | 1.13953017 |
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| Pt |       | 3.85033997 | 3.28061460  | 3.46214719 |
| Pt |       | 5.45076027 | 0.50000552  | 5.66895746 |
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| Pt |       | 7.84770771 | 7.44062019  | 5.65247823 |
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| Pt |       | 9.46210665 | 10.20158460 | 7.97015907 |

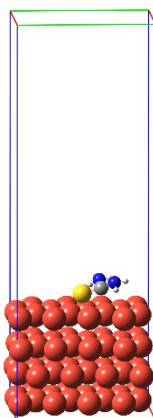
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| Pt | 8.64357001 | 8.82658422  | 3.41750171  |
| Pt | 0.63504226 | 6.04883555  | 5.66228885  |
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| Pt | 7.08650148 | 6.05303333  | 7.92867315  |
| Pt | 2.24957729 | 8.81869763  | 7.97256848  |
| Pt | 9.43993471 | 7.44742135  | 1.12770820  |
| Pt | 4.63698801 | 10.21882157 | 1.13289142  |
| Pt | 6.24230495 | 7.43650842  | 3.41436907  |
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| Pt | 3.03272508 | 7.44116180  | 5.65866069  |
| Pt | 7.85365143 | 10.21287866 | 5.66870487  |
| Pt | 9.46346083 | 7.43366087  | 7.97367923  |
| Pt | 4.65900174 | 10.20185618 | 7.97509262  |
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| Pt | 7.03935841 | 8.83840823  | 1.11222441  |
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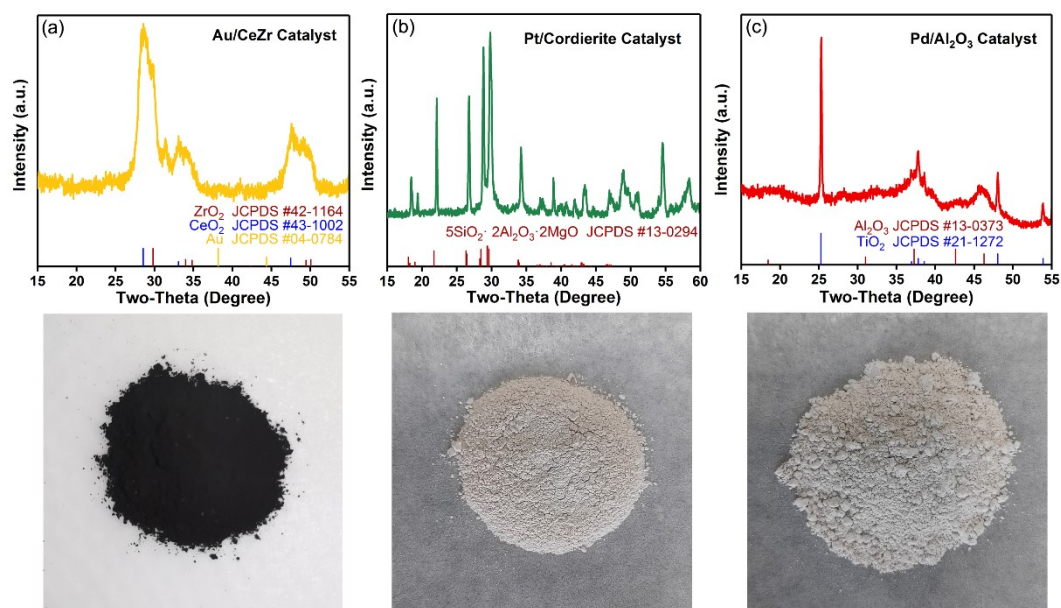
## Structural Parameters of Adsorption Model with Thiourea Molecule and Pd

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|    | Tv_2: | 0.000000   | 11.004600  | 0.000000   |
|    | Tv_3: | 0.000000   | 0.000000   | 31.605712  |
| Pd |       | 4.12192958 | 3.78058378 | 1.10812534 |
| Pd |       | 8.88964324 | 6.53182193 | 1.11483555 |
| Pd |       | 0.94397851 | 3.78353720 | 3.39981348 |
| Pd |       | 5.72042717 | 6.53667022 | 3.40244529 |
| Pd |       | 7.31012609 | 3.78636120 | 5.61544911 |
| Pd |       | 2.54226367 | 6.52973931 | 5.66931789 |
| Pd |       | 4.12262891 | 3.76187970 | 7.95766215 |
| Pd |       | 8.86244004 | 6.55862484 | 7.93253782 |
| Pd |       | 6.50592350 | 2.40320909 | 1.09086325 |
| Pd |       | 1.74157381 | 5.15627763 | 1.13001198 |
| Pd |       | 3.32737660 | 2.40750704 | 3.38333079 |
| Pd |       | 8.10613919 | 5.15882398 | 3.39260359 |
| Pd |       | 0.13630121 | 2.40608217 | 5.61604299 |
| Pd |       | 4.92439196 | 5.15980570 | 5.64363414 |
| Pd |       | 6.49835624 | 2.41015662 | 7.89697065 |
| Pd |       | 1.67177205 | 5.15640187 | 7.96505346 |
| Pd |       | 8.88732349 | 3.78151235 | 1.10381211 |
| Pd |       | 4.12337445 | 6.53142510 | 1.12766146 |
| Pd |       | 5.71357810 | 3.77897733 | 3.38586082 |
| Pd |       | 0.95289372 | 6.53101793 | 3.41360685 |
| Pd |       | 2.53340906 | 3.78220223 | 5.64219987 |
| Pd |       | 7.31715261 | 6.54276303 | 5.62602849 |
| Pd |       | 8.86004787 | 3.77444420 | 7.93425401 |
| Pd |       | 4.16108174 | 6.58588048 | 7.96211950 |
| Pd |       | 1.73950223 | 2.40489191 | 1.10782003 |
| Pd |       | 6.50251255 | 5.15549245 | 1.11047744 |
| Pd |       | 8.08804372 | 2.40242952 | 3.37186676 |
| Pd |       | 3.33590146 | 5.15664023 | 3.41639099 |
| Pd |       | 4.90616440 | 2.42371374 | 5.63233510 |
| Pd |       | 0.17142828 | 5.15706248 | 5.67495319 |
| Pd |       | 1.71347268 | 2.39010096 | 7.86587473 |
| Pd |       | 6.52110282 | 5.16739877 | 7.87823194 |
| Pd |       | 4.12654286 | 9.28068132 | 1.10946858 |
| Pd |       | 8.88901663 | 1.02846868 | 1.08887398 |
| Pd |       | 0.94741386 | 9.28565045 | 3.39226351 |
| Pd |       | 5.70242205 | 1.02584705 | 3.37245811 |
| Pd |       | 7.29272766 | 9.28521048 | 5.62814228 |
| Pd |       | 2.53080360 | 1.02676439 | 5.60428534 |
| Pd |       | 4.12641163 | 9.32502348 | 7.92982384 |
| Pd |       | 8.87397635 | 1.03570420 | 7.90584079 |

|    |            |             |             |
|----|------------|-------------|-------------|
| Pd | 6.50855307 | 7.90706734  | 1.10803210  |
| Pd | 1.74121738 | 10.65737527 | 1.09490910  |
| Pd | 3.33745870 | 7.90477838  | 3.41292796  |
| Pd | 8.08627120 | 10.65904423 | 3.37805010  |
| Pd | 0.15735866 | 7.91251054  | 5.63656047  |
| Pd | 4.91222094 | 10.65993439 | 5.62041342  |
| Pd | 6.51757836 | 7.93806070  | 7.93285324  |
| Pd | 1.73562420 | 10.67562926 | 7.90511291  |
| Pd | 8.89233657 | 9.28189249  | 1.10133043  |
| Pd | 4.12397791 | 1.02886847  | 1.09251939  |
| Pd | 5.70960743 | 9.28178475  | 3.38995819  |
| Pd | 0.93675576 | 1.02927774  | 3.37698278  |
| Pd | 2.53744091 | 9.28683718  | 5.63295836  |
| Pd | 7.28526885 | 1.03416378  | 5.61191465  |
| Pd | 8.88500517 | 9.30605694  | 7.90890338  |
| Pd | 4.11715257 | 1.04103054  | 7.90000859  |
| Pd | 1.74378310 | 7.90797258  | 1.12866400  |
| Pd | 6.51037887 | 10.65588888 | 1.08766254  |
| Pd | 8.10071412 | 7.91382427  | 3.38902203  |
| Pd | 3.32343710 | 10.65604569 | 3.37520306  |
| Pd | 4.91661226 | 7.89542392  | 5.67351102  |
| Pd | 0.14422852 | 10.66263987 | 5.61813054  |
| Pd | 1.72838592 | 7.94546734  | 7.91999035  |
| Pd | 6.50175194 | 10.67924053 | 7.91380511  |
| C  | 3.89210680 | 4.08710932  | 10.08599648 |
| S  | 3.04905369 | 5.65555952  | 9.75544878  |
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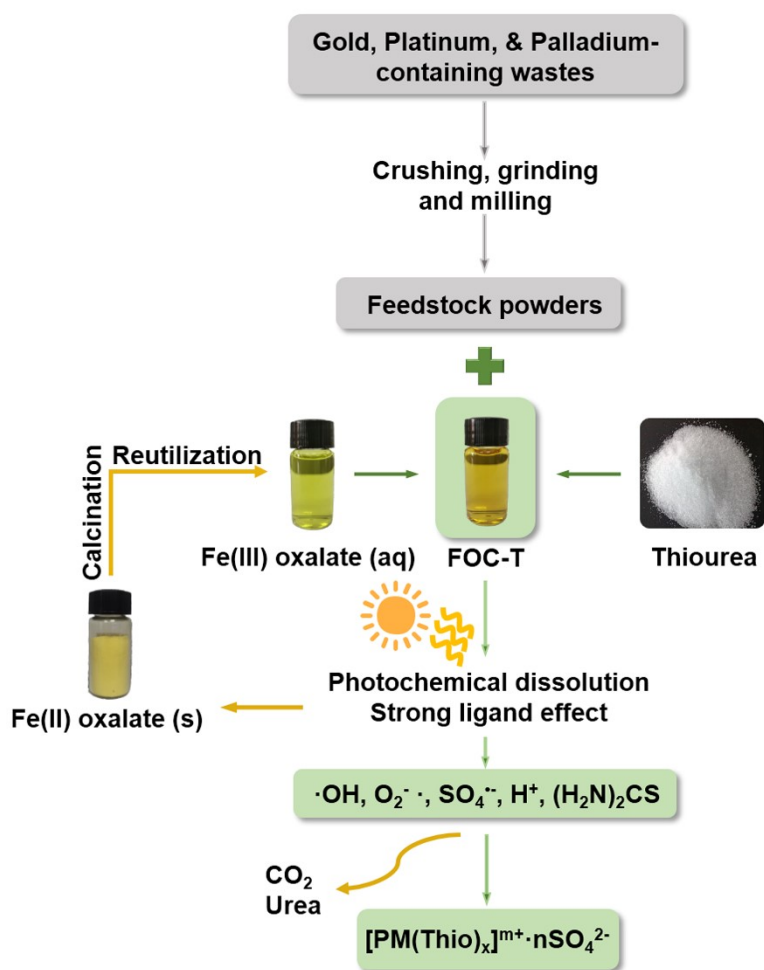
## Figures



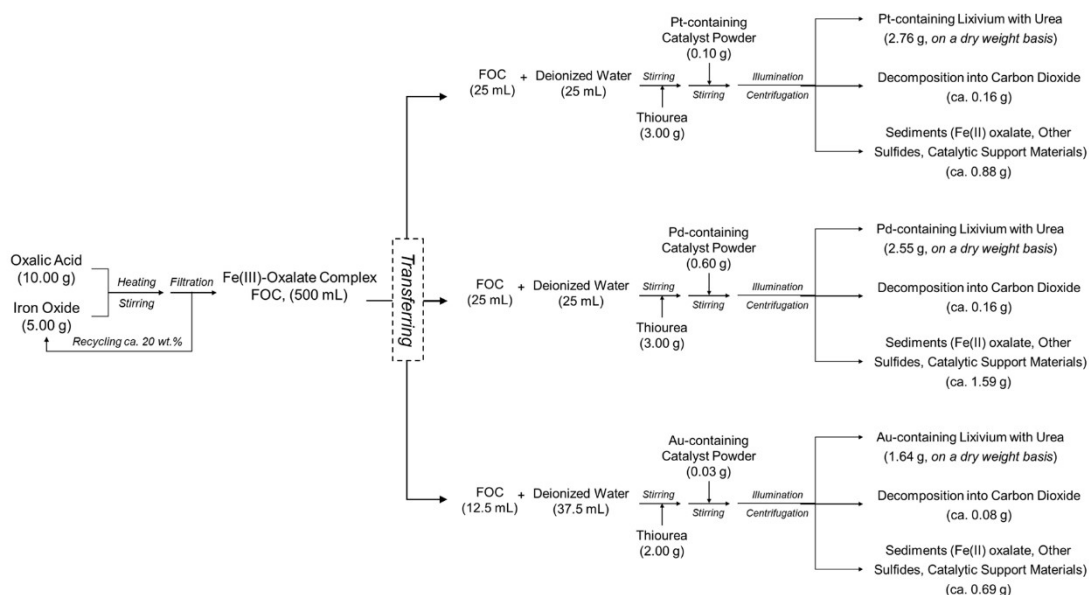
**Figure S1** Original forms of PMs-containing spent catalysts. (a) Au/CeZr powder catalyst, (b) Pt/CM catalyst, and (c) Pd/Al<sub>2</sub>O<sub>3</sub> spherical catalyst.

XRD analysis showed that Au/CeZr catalyst had a poor crystallization of ZrO<sub>2</sub> and CeO<sub>2</sub>, and a weak peak of Au crystal could be observed. Pt/Cordierite and Pd/Al<sub>2</sub>O<sub>3</sub> catalyst only showed the crystal peaks of supported materials, while the Pt and Pd were difficult to be detected due to their relatively low content. They were all used in the forms of powder.



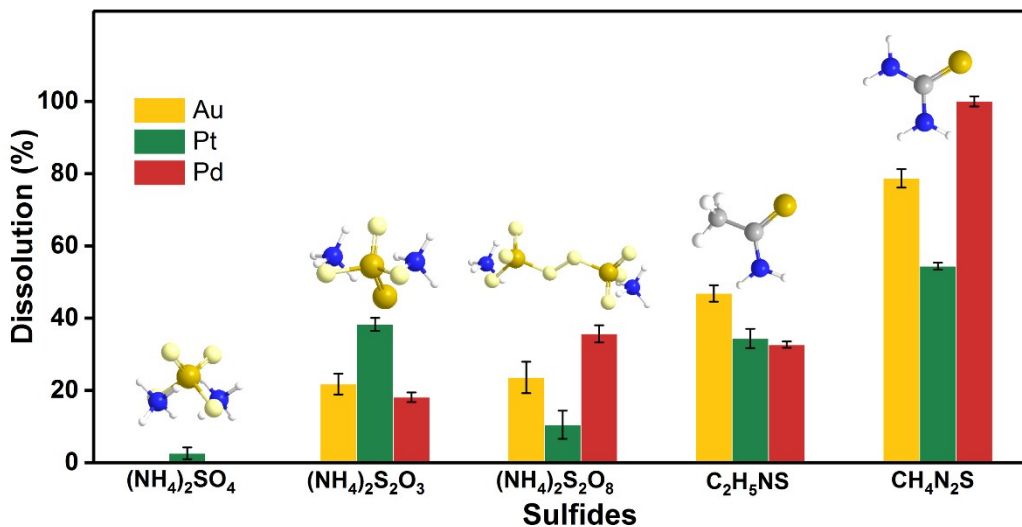


**Scheme S1** Experimental flowchart of photochemical dissolution of Au, Pt, and Pd in the FOC-T system under SSL irradiation.



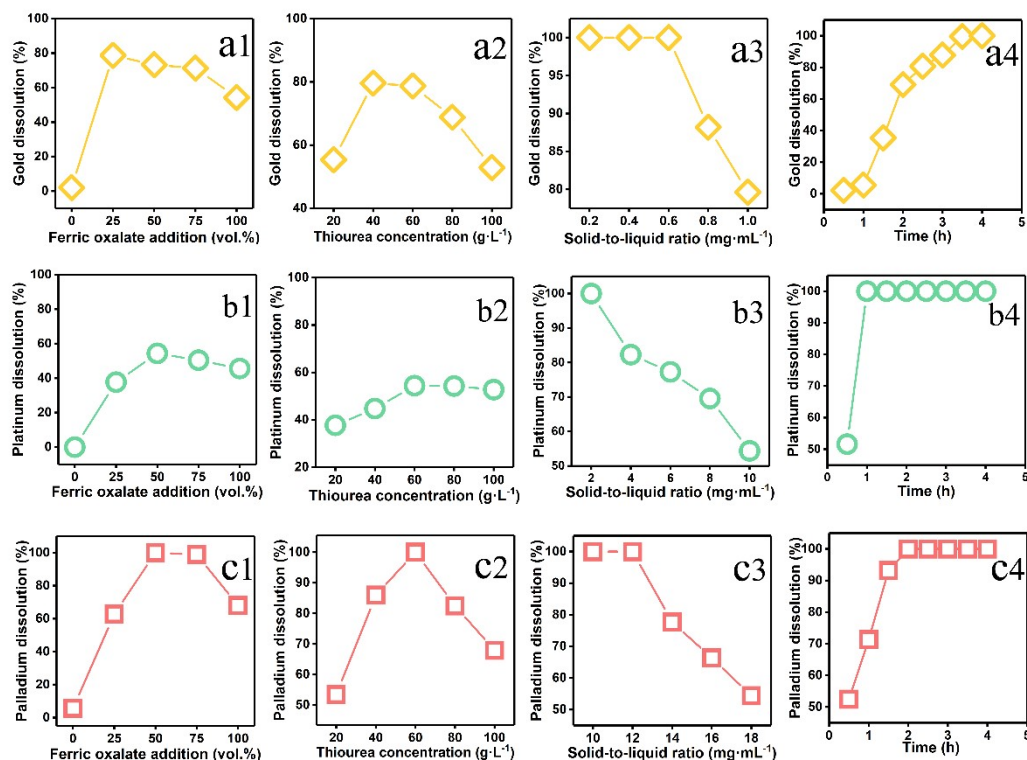
**Figure S2** Pictorial flow-sheet with mass balance for Pt, Pd, and Au recovery in FOC-T system under their own optimal conditions.

In the recovery process, the lixiviant consists of Fe (III)-oxalate (FOC) and thiourea. Bulk FOC is synthesized by the oxalic acid and iron oxide with 500 mL DI water at the temperature of 98 °C, and transferred to be as a leaching agent. Then, the Pt/Pd/Au-containing catalyst powder is added into the system under their own optimal conditions including FOC addition volume ratio, thiourea concentration, solid-to-liquid ratio between catalyst powder and FOC-T lixiviant, and dissolution time. After the sufficient irradiation, Pt/Pd/Au is dissolved into liquid phase blended with urea which comes from the chemical transformation of thiourea. After separation, the Pt/Pd/Au-containing lixivium can be used as a chemical precursor.



**Figure S3** Common sulfides as lixiviants for PMs photochemical dissolution in Fe(III)-oxalate complexes. (0.05 mol·L<sup>-1</sup> FOC, 60 g·L<sup>-1</sup> sulfides, 10 g·L<sup>-1</sup> Pt/CM or Pd/Al<sub>2</sub>O<sub>3</sub> catalyst or 1 g·L<sup>-1</sup> Au/CeZr catalyst, RT, 300 rpm/min and SSL irradiation for 4 h)

On the one hand, thiourea was chemically stable under acidic condition, and the sulfur radicals could be generated available in photochemistry. On the contrary, thioacetamide and ammonium thiosulfate might break down into hydrogen sulfide, sulfates and other sulfur-containing materials in an acidic solution<sup>2</sup>, and an odor similar to rotten eggs can be smelled during the experiment. This behavior would greatly reduce the recovery performance of precious metals. On the other hand, thiocarbonyl and amino groups of thiourea could reduce the surface tension of liquids<sup>3</sup>, promoting full contact between the solution and the metal surface. These groups could strongly bind the precious metals to form stable complexes.



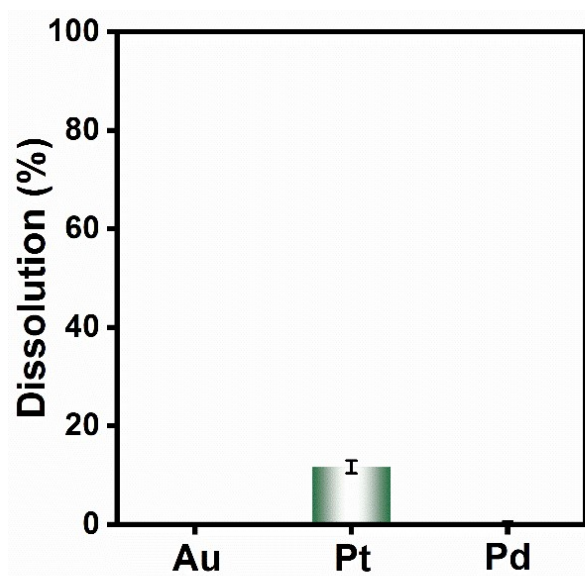
**Figure S4** Factors optimization for PMs dissolution in the FOC-T system: PMs dissolution of (a) Au, (b) Pt, and (c) Pd under the conditions of (1) FOC addition, (2) thiourea concentration, (3) solid-to-liquid ratio of feedstocks, and (4) dissolution time.

**The optimal conditions of PMs recovery in FOC-T system (RT, 300 rpm/min):**

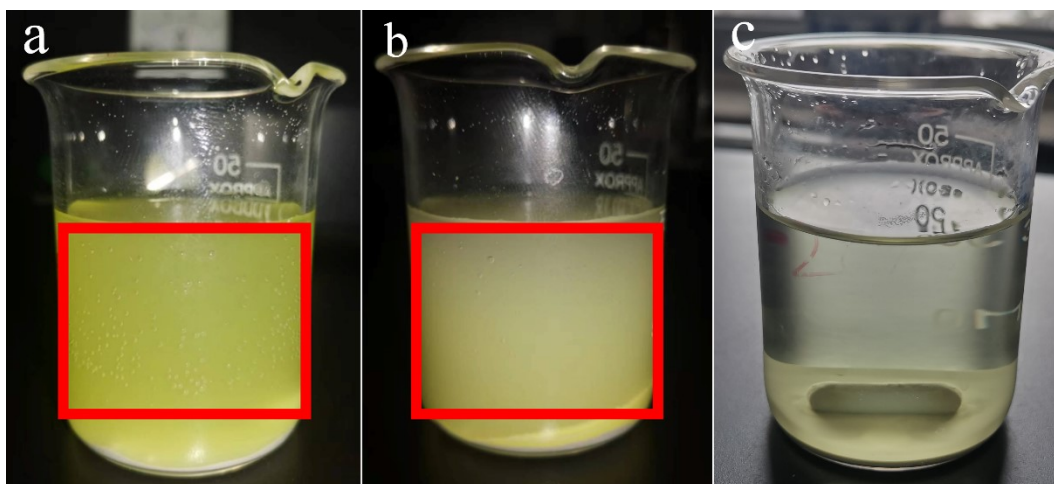
For Au dissolution, it was 25 vol.% FOC ( $0.02 \text{ mol}\cdot\text{L}^{-1}$ ) addition,  $40 \text{ g}\cdot\text{L}^{-1}$  thiourea concentration,  $0.6 \text{ g}_{\text{spent catalyst}}\cdot\text{L}^{-1}$  solid-to-liquid ratio, and reaction time for 3.5 h.

For Pt dissolution, it was 50 vol.% FOC ( $0.05 \text{ mol}\cdot\text{L}^{-1}$ ) addition,  $60 \text{ g}\cdot\text{L}^{-1}$  thiourea concentration,  $2 \text{ g}_{\text{spent catalyst}}\cdot\text{L}^{-1}$  solid-to-liquid ratio, and reaction time for 1 h.

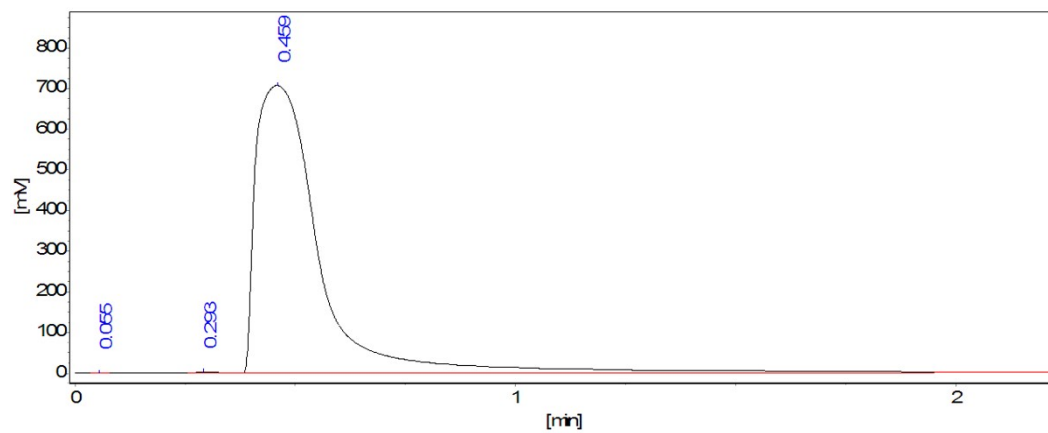
For Pd dissolution, it was 50 vol.% FOC ( $0.05 \text{ mol}\cdot\text{L}^{-1}$ ) addition,  $60 \text{ g}\cdot\text{L}^{-1}$  thiourea concentration,  $12 \text{ g}_{\text{spent catalyst}}\cdot\text{L}^{-1}$  solid-to-liquid ratio, and reaction time for 2 h.



**Figure S5** Photochemical dissolution performance of PMs in FOC-urea system. (0.05 mol·L<sup>-1</sup> FOC vol.% FOC, 60 g·L<sup>-1</sup> urea, 10 g·L<sup>-1</sup> Pt/CM catalyst or 10 g·L<sup>-1</sup> Pd/Al<sub>2</sub>O<sub>3</sub> catalyst or 1 g·L<sup>-1</sup> Au/CeZr catalyst, RT, 300 rpm/min and SSL irradiation for 4 h)

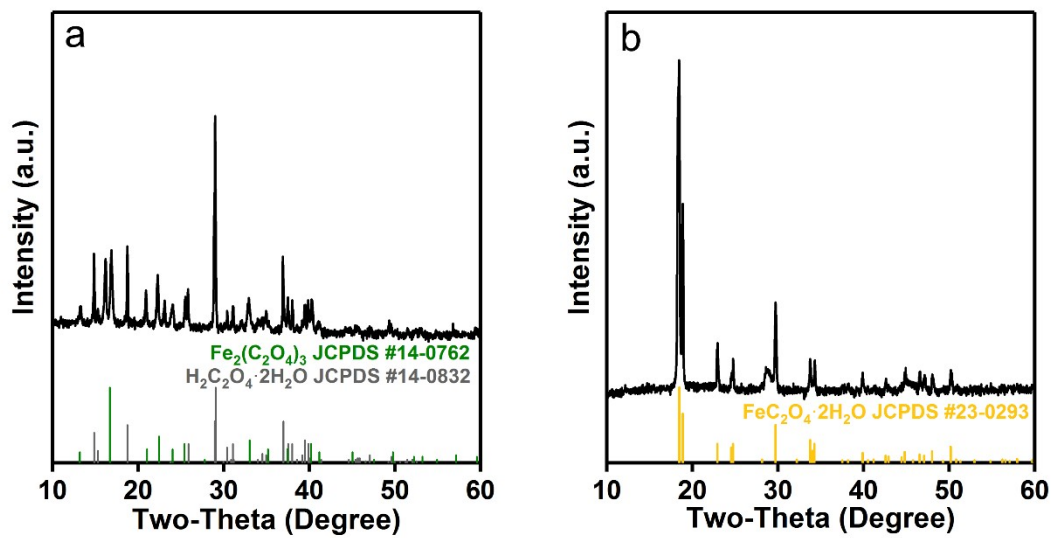


**Figure S6** Record for the gas generation from the Fe(III) oxalate photo-degradation reaction mixed with spent catalyst powder: (a) reaction in the progress, (b) reaction in the end, and (c) standing treatment.



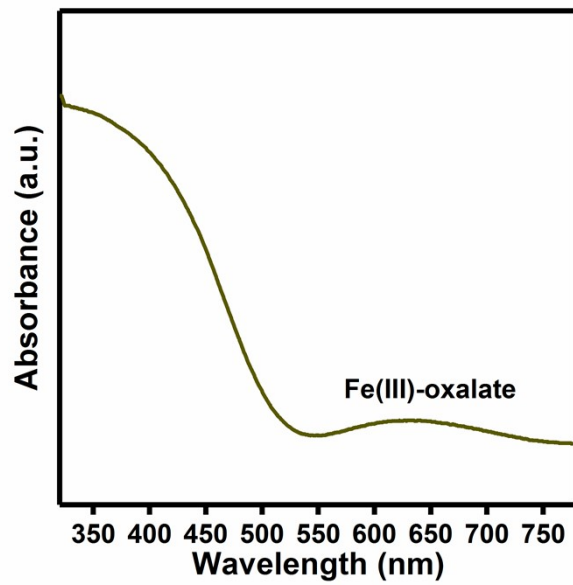
**Figure S7** Gas chromatography analysis during FOC photodegradation.

The peak at 0.459 min is assigned to carbon dioxide. It indicates that the main component in the tail gas is carbon dioxide.

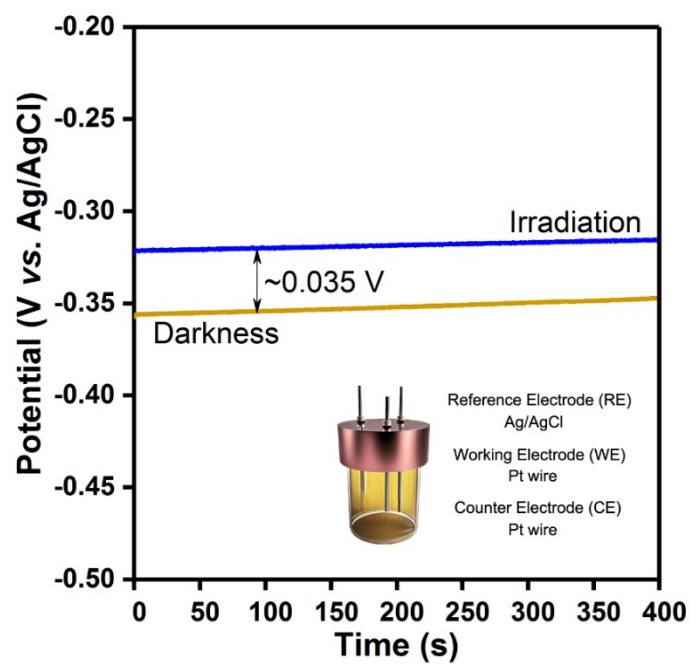


**Figure S8** XRD patterns of (a) FOC and (b) the sediment after FOC photodegradation.

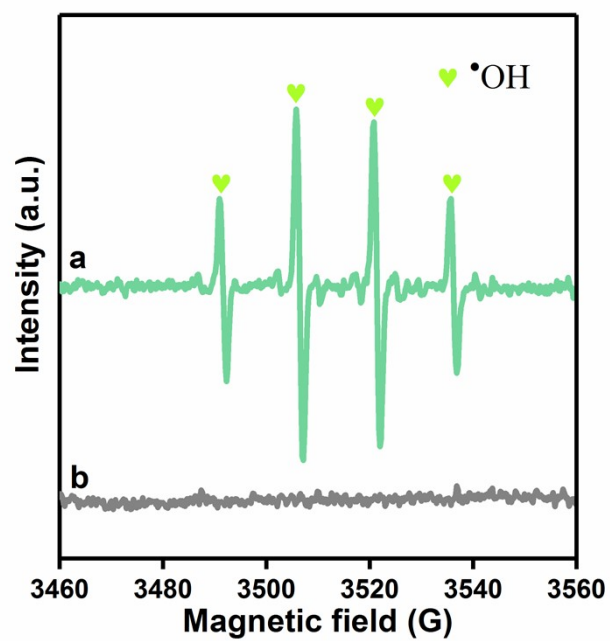




**Figure S9** UV-vis spectroscopy of FOC.



**Figure S10** Open circuit potential curves of the FOC-T lixiviant in darkness and under irradiation.



**Figure S11** EPR spectra of DMPO-radical adduct with irradiation for 30 min in (a) bare FOC system and (b) bare thiourea system.

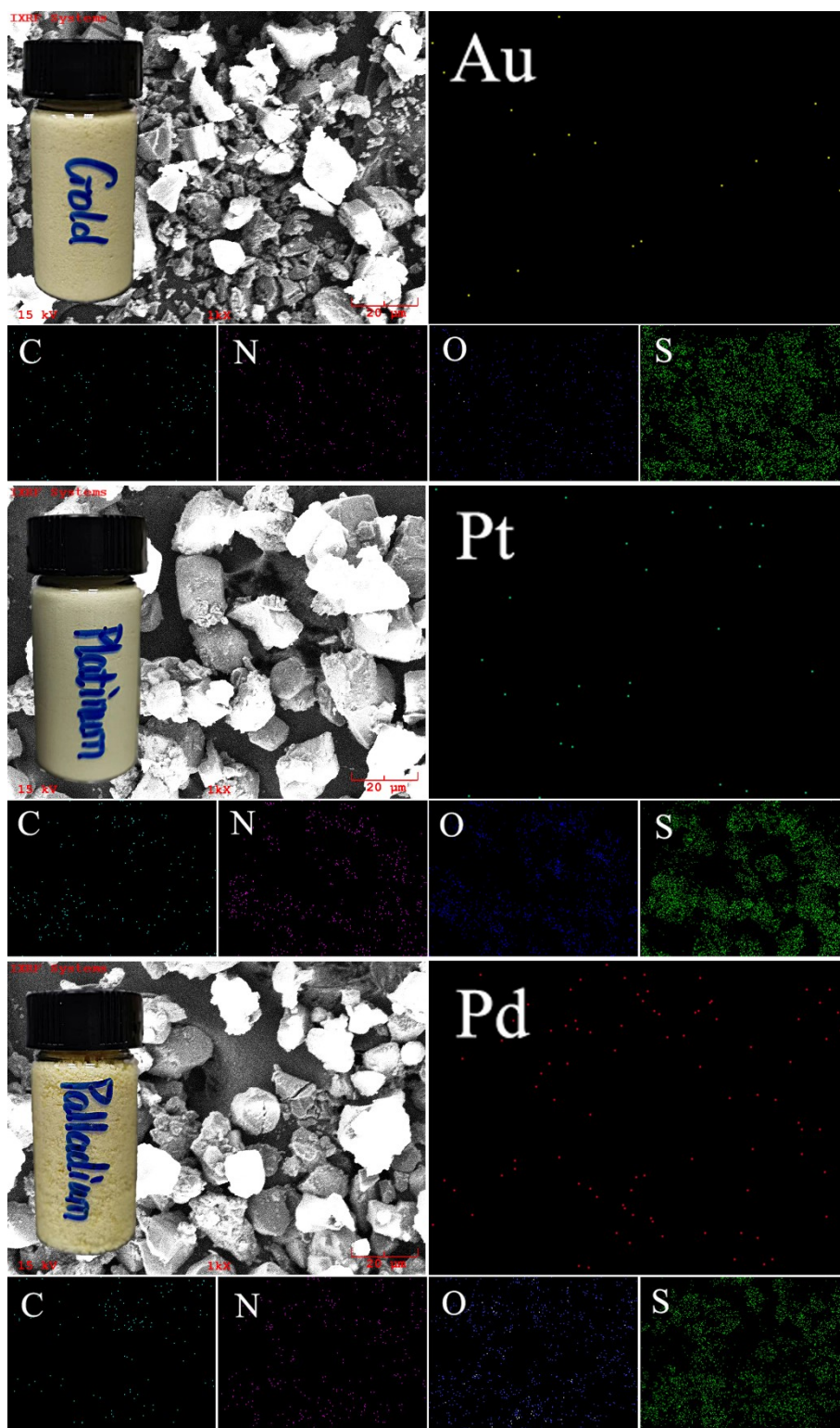
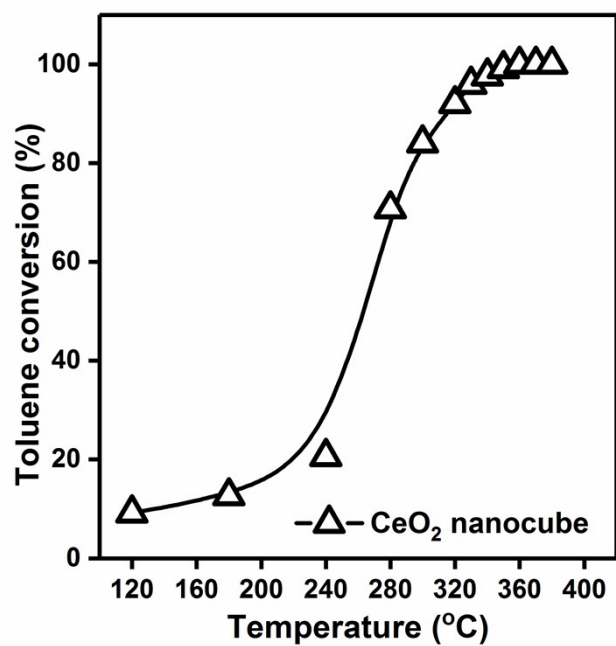
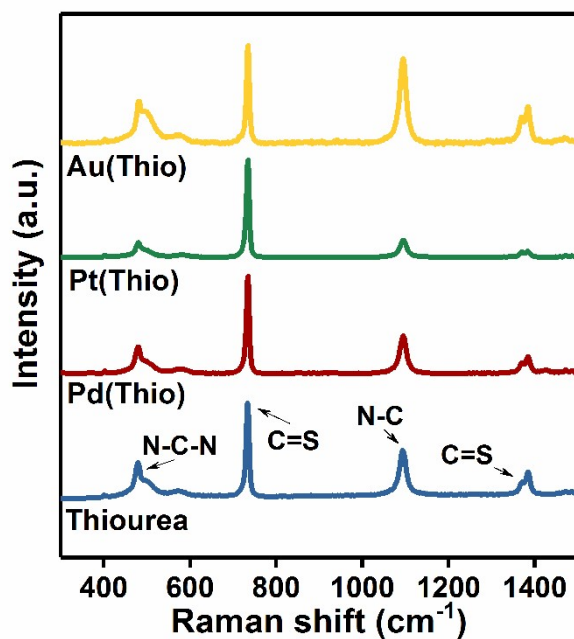


Figure S12 SEM-EDX analysis of Au(Thio), Pt(Thio), and Pd(Thio).

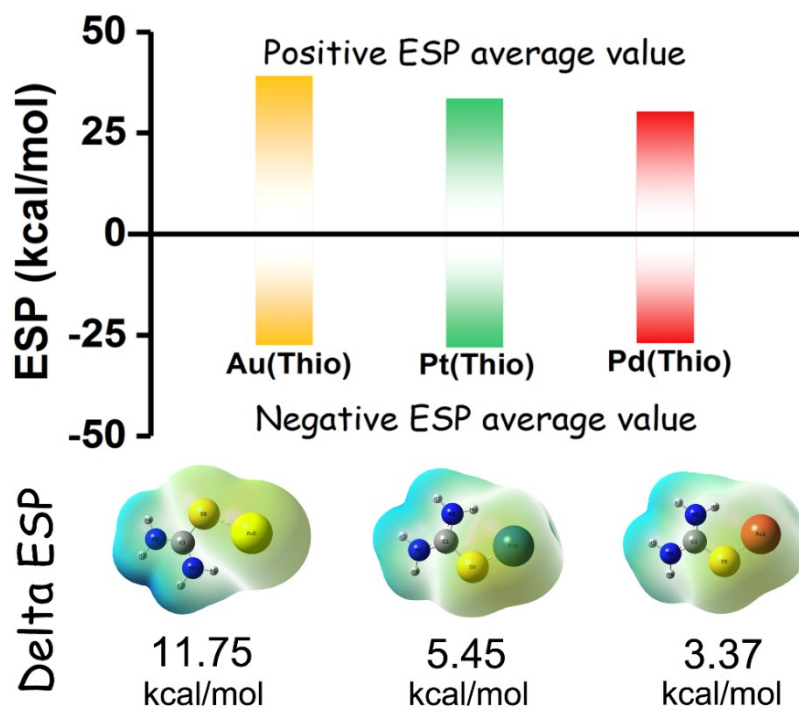


**Figure S13** Catalytic performance of CeO<sub>2</sub> catalysts for toluene oxidation.



**Figure S14** Raman spectra of Au(Thio), Pt(Thio), Pd(Thio), and thiourea.

Two signal peaks at 730 and 1380  $\text{cm}^{-1}$  were assigned to the C=S stretching vibration, and those at 479 and 1094  $\text{cm}^{-1}$  was corresponding to the bending and stretching vibration of N-C=S.<sup>4</sup>



**Figure S15** Computational ESP mapped over the electron density isosurface of PMs(Thio) complexes.

## Tables

**Table S1** Chemical compositions of the support for Pt/CM catalyst (wt%)

| Al <sub>2</sub> O <sub>3</sub> | TiO <sub>2</sub> | MgO   | CaO  | SiO <sub>2</sub> | CeO <sub>2</sub> | Fe <sub>2</sub> O <sub>3</sub> | La <sub>2</sub> O <sub>3</sub> | SO <sub>3</sub> | K <sub>2</sub> O | P <sub>2</sub> O <sub>5</sub> |
|--------------------------------|------------------|-------|------|------------------|------------------|--------------------------------|--------------------------------|-----------------|------------------|-------------------------------|
| 31.63                          | 0.52             | 13.26 | 1.00 | 50.19            | 1.93             | 0.64                           | 0.36                           | 0.04            | 0.16             | 0.09                          |

**Table S2** Chemical compositions of the support for Pd/Al<sub>2</sub>O<sub>3</sub> catalyst (wt%)

| Al <sub>2</sub> O <sub>3</sub> | TiO <sub>2</sub> | Na <sub>2</sub> O | CaO  | SiO <sub>2</sub> | SO <sub>3</sub> | Fe <sub>2</sub> O <sub>3</sub> |
|--------------------------------|------------------|-------------------|------|------------------|-----------------|--------------------------------|
| 92.72                          | 6.65             | 0.36              | 0.09 | 0.08             | 0.04            | 0.04                           |



**Table S3** PMs dissolution performance under different dissolution conditions

| NO. | Lixiviant composition         | Illumination | Dissolution efficiency                |
|-----|-------------------------------|--------------|---------------------------------------|
| 1   | Fe(III) oxalate               | No           | Au: 0 %<br>Pt: 0 %<br>Pd: 0 %         |
| 2   | Fe(III) oxalate               | Yes          | Au: 0 %<br>Pt: 0 %<br>Pd: 0 %         |
| 3   | Thiourea                      | No           | Au: 14.66 %<br>Pt: 0 %<br>Pd: 1.19 %  |
| 4   | Thiourea                      | Yes          | Au: 14.74 %<br>Pt: 0 %<br>Pd: 3.29 %  |
| 5   | Fe(III) oxalate &<br>Thiourea | No           | Au: 11.82 %<br>Pt: 0 %<br>Pd: 30.39 % |
| 6   | Fe(III) oxalate &<br>Thiourea | Yes          | Au: 99.55 %<br>Pt: 100 %<br>Pd: 100 % |

**Table S4** Current studies about PMs recovery via photochemical oxidization reactions

| Precious Metals            | Radical sources             | Solution                              | Reactive species   | Illuminant                           | Temp. /°C | Hazardous risk | Ref.                       |
|----------------------------|-----------------------------|---------------------------------------|--|--------------------------------------|-----------|----------------|----------------------------|
| Au, Ag, Pt, Pd, Ru, Rh, Ir | TiO <sub>2</sub>            | Acetonitrile, Dichloromethane         | h <sup>+</sup> , e <sup>-</sup> , ·OH, ·O <sub>2</sub> <sup>-</sup> , CH <sub>2</sub> CN <sup>·</sup> , CHCl <sub>2</sub> <sup>·</sup> | 100 W ultraviolet LED lamp           | RT        | Yes            | Chen et al. <sup>5</sup>   |
| Au, Pt                     | TiO <sub>2</sub>            | Acetonitrile, Dichloromethane         | h <sup>+</sup> , e <sup>-</sup> , ·OH, ·O <sub>2</sub> <sup>-</sup> , CN <sup>·</sup> , Cl <sup>·</sup>                                | 100 W ultraviolet LED lamp           | RT        | Yes            | Chen et al. <sup>6</sup>   |
| Au, Pd                     | TiO <sub>2</sub>            | NH <sub>4</sub> Br, NH <sub>4</sub> I | h <sup>+</sup> , e <sup>-</sup> , ·OH, ·O <sub>2</sub> <sup>-</sup>  | 100 W ultraviolet LED lamp           | RT        | No             | Cao et al. <sup>7</sup>    |
| Au, Pt, Pd, Ru, Rh, Ir     | P-TiO <sub>2</sub>          | Acetonitrile, Dichloromethane         | h <sup>+</sup> , e <sup>-</sup> , ·OH, ·O <sub>2</sub> <sup>-</sup> , CH <sub>2</sub> CN <sup>·</sup> , CHCl <sub>2</sub> <sup>·</sup> | 100 W ultraviolet LED lamp           | RT        | Yes            | Qiao et al. <sup>8</sup>   |
| Au, Pt                     | CeO <sub>2</sub>            | Acetonitrile, Dichloromethane         | h <sup>+</sup> , e <sup>-</sup> , ·OH, ·O <sub>2</sub> <sup>-</sup> , CH <sub>2</sub> CN <sup>·</sup> , CHCl <sub>2</sub> <sup>·</sup> | 100 W ultraviolet LED lamp           | RT        | Yes            | Chen et al. <sup>9</sup>   |
| Au                         | TiO <sub>2</sub>            | Acetonitrile, NaOH                    | h <sup>+</sup> , e <sup>-</sup> , ·OH, ·O <sub>2</sub> <sup>-</sup> , CH <sub>2</sub> CN <sup>·</sup> , CN <sup>·</sup>                | 100 W ultraviolet LED lamp           | RT        | Yes            | Shang et al. <sup>10</sup> |
| Au                         | Benzaldehyde, Benzylalcohol | Acetonitrile                          | ·OH, CH <sub>2</sub> CN <sup>·</sup> , CN <sup>·</sup>   | 100 W high-pressure mercury lamp     | RT        | Yes            | Li et al. <sup>11</sup>    |
| Au, Pd                     | Peroxydisulfate             | NaCl                                  | ·OH, SO <sub>4</sub> <sup>·-</sup>   | 50 W Xe lamp<br>85W ultraviolet lamp | 60        | No             | Ding et al. <sup>12</sup>  |
| Pt, Pd                     | Fe(III) oxalate             | NaCl                                  | ·OH, ·O <sub>2</sub> <sup>-</sup>  | LED lamp/sunlight                    | RT        | No             | Zhao et al. <sup>13</sup>  |
| Au, Pt, Pd                 | Fe(III) oxalate             | Thiourea                              | ·OH, ·O <sub>2</sub> <sup>-</sup> , SO <sub>4</sub> <sup>·-</sup>  | 500 W Xe lamp                        | RT        | No             | This work                  |



**Table S5** Economic benefit estimation of recovery of per gram precious metal in comparison with commercial chlorinated compounds

| Precious Metals      | Purchase Cost <sup>a</sup> | Fe(III)-oxalate Cost <sup>b</sup> | Thiourea Cost <sup>b</sup> | Commercial Price/\$ <sup>c</sup> |
|----------------------|----------------------------|-----------------------------------|----------------------------|----------------------------------|
| Gold                 | \$ 40.00                   | \$ 0.63                           | \$ 10.02                   | 108.16                           |
| <b>Total Cost/\$</b> |                            | <b>50.65</b>                      |                            | <b>Value/ \$ +57.51</b>          |
| Platinum             | \$ 47.60                   | \$ 6.25                           | \$ 75.02                   | 156.12                           |
| <b>Total Cost/\$</b> |                            | <b>128.87</b>                     |                            | <b>Value/ \$ +27.25</b>          |
| Palladium            | \$ 134.40                  | \$ 1.50                           | \$ 18.00                   | 206.01                           |
| <b>Total Cost/\$</b> |                            | <b>153.90</b>                     |                            | <b>Value/ \$ +52.11</b>          |

<sup>a</sup> The purchase prices of spent precious metal-containing catalyst are determined by market quotation.

<sup>b</sup> The dosages of Fe(III)-oxalate and thiourea are in line with the optimal conditions of PMs dissolution.

<sup>c</sup> The commercial prices of chlorinated compounds comes from *Aladdin Chemical Reagent Co., Ltd.*

HAuCl<sub>4</sub> CAS: 16961-25-4; H<sub>2</sub>PtCl<sub>6</sub> CAS: 16941-12-1; (NH<sub>4</sub>)<sub>2</sub>PdCl<sub>4</sub> CAS: 13820-40-1.

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