

# **Supplementary Information: Scaling theory for the kinetics of mechanochemical reactions with convective flow**

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## S1 Mass conservation

We here summarize the consistency condition of the jump of the volume fraction of reactants at the interface between the product-rich phase and the reactant-rich phase.<sup>1</sup> The volume fraction  $\psi_B$  of reactant B follows the diffusion equation

$$\frac{\partial}{\partial t}\psi_B = D_B \frac{\partial^2}{\partial z^2} \left( \frac{\Pi(\psi_B)v_B}{k_B T} \right), \quad (\text{S1})$$

where  $z$  is the position in the system and  $t$  is the time.  $D_B$  is the diffusion constant.  $\Pi(\psi_B)$  is the osmotic pressure.  $v_B$  is the volume per molecule.  $k_B$  is the Boltzmann constant and  $T$  is the absolute temperature. Integrating both sides of Eq. S1 with respect to  $z$  around  $z = h(t)$ , where the volume fraction  $\psi_B$  jumps between  $\psi_{B1}$  and  $\psi_{B2}$ , leads to

$$\int_{h(t)-\Delta z}^{h(t)+\Delta z} dz \frac{\partial}{\partial t}\psi_B = D_B \frac{\partial^2}{\partial z^2} \left( \frac{\Pi(\psi_B)v_B}{k_B T} \right). \quad (\text{S2})$$

The right side of Eq. S2 is evaluated as

$$\begin{aligned} D_B \frac{\partial^2}{\partial z^2} \left( \frac{\Pi(\psi_B)v_B}{k_B T} \right) &= D_B \frac{\partial}{\partial z} \left( \frac{\Pi(\psi_B)v_B}{k_B T} \right) \Big|_{h(t)+\Delta z} - D_B \frac{\partial}{\partial z} \left( \frac{\Pi(\psi_B)v_B}{k_B T} \right) \Big|_{h(t)-\Delta z} \\ &= -J_B(z = h(t) + \Delta z) + J_B(z = h(t) - \Delta z). \end{aligned} \quad (\text{S3})$$

The last form of Eq. S5 is derived by using the fact that the flux has the form

$$J_B(z) = -D_B \frac{\partial}{\partial z} \left( \frac{\Pi(\psi_B)v_B}{k_B T} \right). \quad (\text{S4})$$

The left side of Eq. S2 is evaluated as

$$\begin{aligned} \int_{h(t)-\Delta z}^{h(t)+\Delta z} dz \frac{\partial}{\partial t}\psi_B &= \frac{d}{dt} \left( \int_{h(t)-\Delta z}^{h(t)+\Delta z} dz \psi_B \right) - \frac{dh(t)}{dt} (\psi_B(z = h(t) + \Delta z) - \psi_B(z = h(t) - \Delta z)) \\ &= -\frac{dh(t)}{dt} (\psi_B(z = h(t) + \Delta z) - \psi_B(z = h(t) - \Delta z)). \end{aligned} \quad (\text{S5})$$

The last form of eq. (S5) is derived by using the fact that

$$\int_{h(t)-\Delta z}^{h(t)+\Delta z} dz \psi_B = \psi_{B1} \Delta z + \psi_{B2} \Delta z \quad (\text{S6})$$

for  $\Delta z \rightarrow 0$  and this integral thus does not depend on time. Eqs. S3 and S5 lead to the form

$$(\psi_B(z = h(t) + \Delta z) - \psi_B(z = h(t) - \Delta z)) \frac{dh(t)}{dt} = J_B(z = h(t) + \Delta z) - J_B(z = h(t) - \Delta z). \quad (\text{S7})$$

Taking the limit  $\Delta z \rightarrow 0$  to both sides of Eq. S7 leads to the form

$$(\psi_{B2} - \psi_{B1}) \frac{dh(t)}{dt} = J_{B2} - J_{B1}, \quad (\text{S8})$$

with  $J_{B1} = \lim_{\Delta z \rightarrow 0} J_B(z = h(t) - \Delta z)$  and  $J_{B2} = \lim_{\Delta z \rightarrow 0} J_B(z = h(t) + \Delta z)$ . Eq. S8 indeed represents the mass conservation at  $z = h(t)$ . The jump of the volume fraction  $\psi_B$  at  $z = h(t)$  is consistent with Eq. S1 as long as the time evolution of the interface is given by Eq. S8 and the condition  $\Pi(\psi_{B1}) = \Pi(\psi_{B2})$  is satisfied.

## S2 Lubrication approximation

We here summarize the simplification of Stokes equation by using the lubrication approximation.<sup>2,3</sup> The Stokes equation represents the balance of the forces arising from the gradient of hydrostatic pressure  $p$  and the forces due to the mechanical stress  $\sigma$ ,

$$-\nabla p(\mathbf{r}) + \nabla \cdot \sigma(\mathbf{r}) = 0. \quad (\text{S9})$$

The gradient  $\nabla$  is represented as

$$\nabla = \mathbf{e}_r \frac{\partial}{\partial r} + \mathbf{e}_\phi \frac{1}{r} \frac{\partial}{\partial \phi} + \mathbf{e}_z \frac{\partial}{\partial z} \quad (\text{S10})$$

in the cylindrical coordinate system, where  $\mathbf{e}_r$  is the unit vector to the radial direction,  $\mathbf{e}_\phi$  is the unit vector the azimuthal direction, and  $\mathbf{e}_z$  is the unit vector to the  $z$ -direction, see Fig. 4 in the main article.

The mechanical stress is represented by the components in the cylindrical coordinate system,

$$\begin{aligned}\sigma &= \sigma_{rr}\mathbf{e}_r\mathbf{e}_r + \sigma_{r\phi}\mathbf{e}_r\mathbf{e}_\phi + \sigma_{rz}\mathbf{e}_r\mathbf{e}_z \\ &\quad + \sigma_{\phi r}\mathbf{e}_\phi\mathbf{e}_r + \sigma_{\phi\phi}\mathbf{e}_\phi\mathbf{e}_\phi + \sigma_{\phi z}\mathbf{e}_\phi\mathbf{e}_z \\ &\quad + \sigma_{zr}\mathbf{e}_z\mathbf{e}_r + \sigma_{z\phi}\mathbf{e}_z\mathbf{e}_\phi + \sigma_{zz}\mathbf{e}_z\mathbf{e}_z\end{aligned}\tag{S11}$$

The force  $\mathbf{f}$  applied by mechanical stress  $\sigma$

$$\mathbf{f} = \nabla \cdot \sigma.\tag{S12}$$

have the form

$$\mathbf{f} = f_r\mathbf{e}_r + f_\phi\mathbf{e}_\phi + f_z\mathbf{e}_z\tag{S13}$$

with

$$f_r = \frac{1}{r}\frac{\partial}{\partial r}(r\sigma_{rr}) - \frac{\sigma_{\phi\phi}}{r} + \frac{\partial\sigma_{rz}}{\partial z} + \frac{1}{r}\frac{\partial\sigma_{r\phi}}{\partial\phi}\tag{S14}$$

$$f_\phi = \frac{1}{r}\frac{\partial}{\partial r}(r\sigma_{\phi r}) + \frac{1}{r}\frac{\partial\sigma_{\phi\phi}}{\partial\phi} + \frac{\sigma_{r\phi}}{r} + \frac{\partial\sigma_{\phi z}}{\partial z}\tag{S15}$$

$$f_z = \frac{1}{r}\frac{\partial}{\partial r}(r\sigma_{zr}) + \frac{1}{r}\frac{\partial\sigma_{z\phi}}{\partial\phi} + \frac{\partial\sigma_{zz}}{\partial z}.\tag{S16}$$

Because of the cylindrical symmetry,  $\frac{\partial}{\partial\phi} = 0$  and  $\sigma_{r\phi} = \sigma_{\phi r} = \sigma_{z\phi} = \sigma_{\phi z} = 0$ , Eqs. S14 - S16

are reduced to

$$f_r = \frac{1}{r} \frac{\partial}{\partial r} (r \sigma_{rr}) - \frac{\sigma_{\phi\phi}}{r} + \frac{\partial \sigma_{rz}}{\partial z} \quad (\text{S17})$$

$$f_\phi = 0 \quad (\text{S18})$$

$$f_z = \frac{1}{r} \frac{\partial}{\partial r} (r \sigma_{zr}) + \frac{\partial \sigma_{zz}}{\partial z}. \quad (\text{S19})$$

Now we treat the dynamics of a fluid between cylindrical surfaces of radius  $r_0$ , see Fig. 4 in the main article. The cylindrical surfaces are rigid bodies and their radius is fixed, while the thickness  $h(t)$  of the fluid depends on time. The first and second terms of Eq. S17 are in the order of  $\sigma_{rr}/r_0$  and  $\sigma_{\phi\phi}/r_0$ , while the third term of Eq. S17 is in the order of  $\sigma_{rz}/h(t)$  by using the estimate  $\frac{\partial}{\partial r} \approx \frac{1}{r_0}$  and  $\frac{\partial}{\partial z} \approx \frac{1}{h(t)}$ . In the limit of  $h(t) \ll r_0$ , the third term of Eq. S17 dominates the first and second terms of this equation. Similarly, the first term of Eq. S19 is in the order of  $\sigma_{zr}/r_0$ , while the second term of Eq. S19 is in the order of  $\sigma_{zz}/h(t)$ . In the limit of  $h(t) \ll r_0$ , the second term of Eq. S19 dominates the first term of this equation. This order of magnitude argument leads to the approximate forms of Eqs. S17 - S19,

$$f_r = \frac{\partial \sigma_{rz}}{\partial z} \quad (\text{S20})$$

$$f_\phi = 0 \quad (\text{S21})$$

$$f_z = \frac{\partial \sigma_{zz}}{\partial z}. \quad (\text{S22})$$

Eq. S9 is decomposed to components

$$-\frac{\partial}{\partial r} p(r) + \frac{\partial \sigma_{rz}}{\partial z} = 0 \quad (\text{S23})$$

$$-\frac{\partial}{\partial z} p(r) + \frac{\partial \sigma_{zz}}{\partial z} = 0. \quad (\text{S24})$$

Eq. S23 is equal to Eq. 8 in the main article. Integrating Eq. S24 with respect to  $z$  leads to

$$-p(r) + \sigma_{zz}(r) = -\sigma_\perp(r) \quad (\text{S25})$$

Eq. S25 represents the fact that the applied normal stress  $\sigma_{zz}(r)$  is balanced with hydrostatic pressure  $p(r)$ .

In the above argument, one might wonder the dependence of the stress components,  $\sigma_{rr}$ ,  $\sigma_{\phi\phi}$ ,  $\sigma_{zz}$ , and  $\sigma_{rz}$ , on the radius  $r_0$  and the thickness  $h(t)$ . We here estimate the order of these stress components for viscous fluids. The viscous stress has the form

$$\sigma = 2\eta\dot{\epsilon}, \quad (\text{S26})$$

where  $\dot{\epsilon}$  is the strain rate tensor. The strain rate tensor has the form

$$\dot{\epsilon} = \frac{1}{2}((\nabla \mathbf{v}) + {}^T(\nabla \mathbf{v})), \quad (\text{S27})$$

where  $\mathbf{v} = v_r \mathbf{e}_r + v_\phi \mathbf{e}_\phi + v_z \mathbf{e}_z$  is the velocity field in the fluid and  ${}^T$  is the transpose. This tensor is represented with the components of the cylindrical coordinate system

$$\begin{aligned} \dot{\epsilon} = & \dot{\epsilon}_{rr} \mathbf{e}_r \mathbf{e}_r + \dot{\epsilon}_{r\phi} \mathbf{e}_r \mathbf{e}_\phi + \dot{\epsilon}_{rz} \mathbf{e}_r \mathbf{e}_z \\ & + \dot{\epsilon}_{\phi r} \mathbf{e}_\phi \mathbf{e}_r + \dot{\epsilon}_{\phi\phi} \mathbf{e}_\phi \mathbf{e}_\phi + \dot{\epsilon}_{\phi z} \mathbf{e}_\phi \mathbf{e}_z \\ & + \dot{\epsilon}_{zr} \mathbf{e}_z \mathbf{e}_r + \dot{\epsilon}_{z\phi} \mathbf{e}_z \mathbf{e}_\phi + \dot{\epsilon}_{zz} \mathbf{e}_z \mathbf{e}_z \end{aligned} \quad (\text{S28})$$

with

$$\dot{\epsilon}_{rr} = \frac{\partial v_r}{\partial r} \quad (\text{S29})$$

$$\dot{\epsilon}_{\phi\phi} = \frac{1}{r} \frac{\partial v_\phi}{\partial \phi} + \frac{v_r}{r} \quad (\text{S30})$$

$$\dot{\epsilon}_{zz} = \frac{\partial v_z}{\partial z} \quad (\text{S31})$$

$$\dot{\epsilon}_{r\phi} = \dot{\epsilon}_{\phi r} = \frac{1}{2} \left( \frac{\partial v_\phi}{\partial r} + \frac{1}{r} \frac{\partial v_r}{\partial \phi} - \frac{v_\phi}{r} \right) \quad (\text{S32})$$

$$\dot{\epsilon}_{\phi z} = \dot{\epsilon}_{z\phi} = \frac{1}{2} \left( \frac{1}{r} \frac{\partial v_z}{\partial \phi} + \frac{\partial v_\phi}{\partial z} \right) \quad (\text{S33})$$

$$\dot{\epsilon}_{zr} = \dot{\epsilon}_{rz} = \frac{1}{2} \left( \frac{\partial v_z}{\partial r} + \frac{\partial v_r}{\partial z} \right). \quad (\text{S34})$$

Because of the cylindrical symmetry of the system,  $\frac{\partial}{\partial \phi} = 0$  and  $v_\phi = 0$ , the components of the stress tensor has the form

$$\sigma_{rr} = 2\eta \frac{\partial v_r}{\partial r} \quad (\text{S35})$$

$$\sigma_{\phi\phi} = 2\eta \frac{v_r}{r} \quad (\text{S36})$$

$$\sigma_{zz} = 2\eta \frac{\partial v_z}{\partial z} \quad (\text{S37})$$

$$\sigma_{rz} = \sigma_{zr} = \eta \left( \frac{\partial v_r}{\partial z} + \frac{\partial v_z}{\partial r} \right) \quad (\text{S38})$$

and  $\sigma_{r\phi} = \sigma_{\phi r} = \sigma_{\phi z} = \sigma_{z\phi} = 0$ .

Eqs. S35 - S38 suggest that  $\sigma_{rr}$  and  $\sigma_{\phi\phi}$  are in the order of  $\eta v_r / r_0$ , while  $\sigma_{rz}$  is in the order of  $\eta v_r / h(t)$ . This ensures that the third term of Eq. S17 dominates the first and second terms of Eq. S17 in the limit of  $h(t) \ll r_0$ . We note that the first term Eq. S38 dominates the second term of Eq. S38 in this limit. These estimates and Eq. S23 lead to the fact that the hydrostatic pressure  $p$  is in the order of  $\eta r_0 v_r / h(t)$ .  $\sigma_{rz}$  is in the order of  $\eta v_r / h(t)$ , see Eq. S38 and the discussion above, while  $\sigma_{zz}$  is in the order of  $\eta v_z / h(t)$ , see Eq. S37. The first term of Eq. S24 is estimated as  $\eta r_0 v_r / h^2(t)$  by using the above estimate of the hydrostatic pressure and thus dominates the contribution of  $\sigma_{rz}$  to the second term of Eq. S24, where

this contribution is estimated as  $\eta v_r/(r_0 h(t))$ , see the first term of Eq. S19 and the above estimate of  $\sigma_{rz}$ . The first term of Eq. S19 is thus negligible and this treatment leads to Eq. S24.

In Eq. S24, we have tentatively left the contribution of  $\sigma_{zz}$  to the second term of Eq. S24 because  $\sigma_{zz}$  is in the order of  $\eta v_z/h(t)$  and the order estimate  $v_z$  relative to  $v_r$  is not specified. Eq. S24 leads to Eq. S25. We solve Eq. S23 with the incompressibility condition

$$\frac{1}{r} \frac{\partial}{\partial r}(r v_r) + \frac{\partial v_z}{\partial z} = 0. \quad (\text{S39})$$

Eq. S39 implies that  $v_z$  is in the order of  $h(t)v_r/r_0$ .  $\sigma_{zz}$  is thus estimated as  $\eta v_r/r_0$  and is much smaller than the hydrostatic pressure, which is in the order of  $\eta r_0 v_r/h(t)$ , see the above discussion. Therefore, Eq. S25 is further reduced to

$$-p(r) = -\sigma_{\perp}(r). \quad (\text{S40})$$

We note that Eq. S40 is valid only for incompressible fluids; if not, one should use Eq. S25s.

## References

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