

## **Elaborated Built-In Electric Field in Mn/C<sub>60</sub> heterojunction Promotes Electrocatalytic Nitrogen Reduction to Ammonia**

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## **SI. Experimental section**

### **1. Materials**

Buckminsterfullerene [ $C_{60}$ , 99.9%], manganese carbonyl [ $Mn_2(CO)_{10}$ , 98%], di-sodium hydrogen phosphate dihydrate [ $Na_2HPO_4 \cdot 2H_2O$ , 99%], acetone [ $CH_3COCH_3$ , 99.9%], salicylic acid [ $C_7H_6O_3$ ,  $\geq 99.0\%$ ], sodium citrate [ $C_6H_5Na_3O_7$ , 98%], sodium hypochlorite (NaClO), sodium nitroferricyanide dihydrate [ $C_5FeN_6Na_2O \cdot 2H_2O$ , 99.0%], sodium hydroxide [NaOH, 98-100.5%], ammonium chloride [ $NH_4Cl$ , 99.5%] and Nafion membrane 211 were purchased from Sigma-Aldrich Chemical Reagent Co., Ltd. Ethanol (99.5%) were purchased from Beijing Chemical Crop. The water was purified by a Millipore system. All these reagents were used without any further purification.

### **2. Preparation of Mn/ $C_{60}$**

$Mn_2(CO)_{10}$  (20 mg) and  $C_{60}$  (80 mg) were put into the agate mortar and ground for 30 minutes, followed by heating to 300 °C at a heating rate of 5 °C min<sup>-1</sup> under argon atmosphere. After annealing at 300 °C for 1 h, the Mn/ $C_{60}$  sample was obtained through natural cooling to room temperature.

### **3. Preparation of Mn**

Mn NPs were synthesized to demonstrate the critical role of  $C_{60}$  in the electrocatalytic process.  $Mn_2(CO)_{10}$  (40 mg) was mingled evenly and put into porcelain boat for heating treatment. Subsequently, after the same annealing and post-treatment process as in the synthesis of Mn/ $C_{60}$ , the metal Mn nanoparticles were successfully synthesized.

### **4. Preparation of $C_{60}$**

The synthetic procedures for C<sub>60</sub> is similar to those for Mn, C<sub>60</sub> (40 mg) was mingled evenly and put into porcelain boat for heating treatment. Subsequently, proceeding the same annealing and post-treatment process as in the synthesis of Mn/C<sub>60</sub>.

## **5. Characterization**

X-ray diffraction (XRD, X'PERT PRO MPD diffractometer, Cu K $\alpha$  radiation,  $\lambda=0.15418$  nm, scanned range of 2-90°) was used to identify the crystal structure of all prepared catalysts. Scanning electron microscopy (SEM, JSM-7800F Prime) and transmission electron microscopy (TEM, JEM-2100F) were utilized to investigate the morphology of all samples. X-ray photoelectron spectroscopy (XPS) data were collected by using Krato, AXIS-HS monochromatized Al K $\alpha$  cathode source of 75-150 W under ultrahigh vacuum. Moreover, the UV-visible adsorption spectra were recorded on a spectrophotometer (UV-2550). <sup>1</sup>H NMR spectra were collected on a superconducting-magnet NMR spectrometer (Bruker AVANCE III HD 700 MHz). Besides, dimethyl sulphoxide was utilized as an internal standard to calibrate the chemical shifts in the spectra.

## **6. Electrochemical measurements**

In order to eliminate any ammonia and other contaminants, all components of the electrochemical cell were firstly soaked in 0.05 M H<sub>2</sub>SO<sub>4</sub> solution for 24 h and then washed copiously with fresh ultrapure water before NRR tests. Besides, all labware (needles, vials, pipet tips, containers, etc.) utilized in this work were also treated by 0.1 M H<sub>2</sub>SO<sub>4</sub> solution and water. All electrochemical characterizations were performed using a CHI 660E workstation coupled with a three-electrode system in a single-

chamber electrolytic cell. Carbon cloth utilized in this work was purchased from CeTech (W1S1009 type) and treated with the mixture of H<sub>2</sub>SO<sub>4</sub>:H<sub>2</sub>O<sub>2</sub> (1:3 vol.) for 12 h to remove surface impurities. To avoid excessive oxidation by oxygen and contamination with ambient ammonia or other nitrogen-containing species in air, electrodes were used either immediately after preparation or kept in vacuum before being used in electrochemical experiments. The prepared catalyst loaded on a piece of pretreated carbon cloth (1×1 cm<sup>2</sup>) was used as the working electrode, a graphite rod and Ag/AgCl (saturated KCl electrolyte) were employed as counter electrode and reference electrode, respectively. Potential without iR-compensated were converted to RHE scale via the following equation:  $E \text{ (vs. RHE)} = E \text{ (vs. Ag/AgCl)} + 0.7736$ . The catalyst ink for working electrode was prepared by dispersing 2 mg of catalyst in a mixed solution of 15 μL Nafion (0.5 wt%), 250 μL acetone and 235 μL water followed by sonication for 30 minutes. Mass loading of 0.3 mg cm<sup>-2</sup> was used for electrochemical study. All experiments were carried out at room temperature (25°C). To remove the impurities in the inlet gas, such as NH<sub>3</sub> and NO<sub>x</sub>, the prepurification of high-purity N<sub>2</sub> (purity 99.999%) and Ar (purity 99.99%) by passing through a saturator filled with 0.05 M NaOH and a saturator filled with 0.05 M H<sub>2</sub>SO<sub>4</sub> solution to remove any possible contaminants. Before carrying out all the electrochemical characterizations, the 0.08 M Na<sub>2</sub>HPO<sub>4</sub> electrolyte solution was purged with N<sub>2</sub> for 30 minutes. Cyclic voltammetry (CV) test was carried out on at a scan rate of 50 mV s<sup>-1</sup> ranging from -1.2264-0.7736 V (vs. RHE). Linear sweep voltammetry (LSV) was also conducted at a scan rate of 10 mV s<sup>-1</sup>. Chronoamperometric test were then conducted at different potentials and pure

N<sub>2</sub> was continuously fed into the cathodic cell during the experiments.

## 7. Calculation of Faradaic efficiency (FE) and NH<sub>3</sub> formation rate

The FE for NRR was defined as the amount of electric charge used for producing NH<sub>3</sub> divided the total charge passed through the electrodes during the electrolysis. Assuming three electrons were needed to produce one NH<sub>3</sub> molecule, the FE was calculated according to the following equation:

$$FE = 3 \times 0.318 \times F \times C_{\text{NH}_4\text{Cl}} \times V / (17 \times Q)$$

The rate of formation of NH<sub>3</sub> was calculated using the following equation:

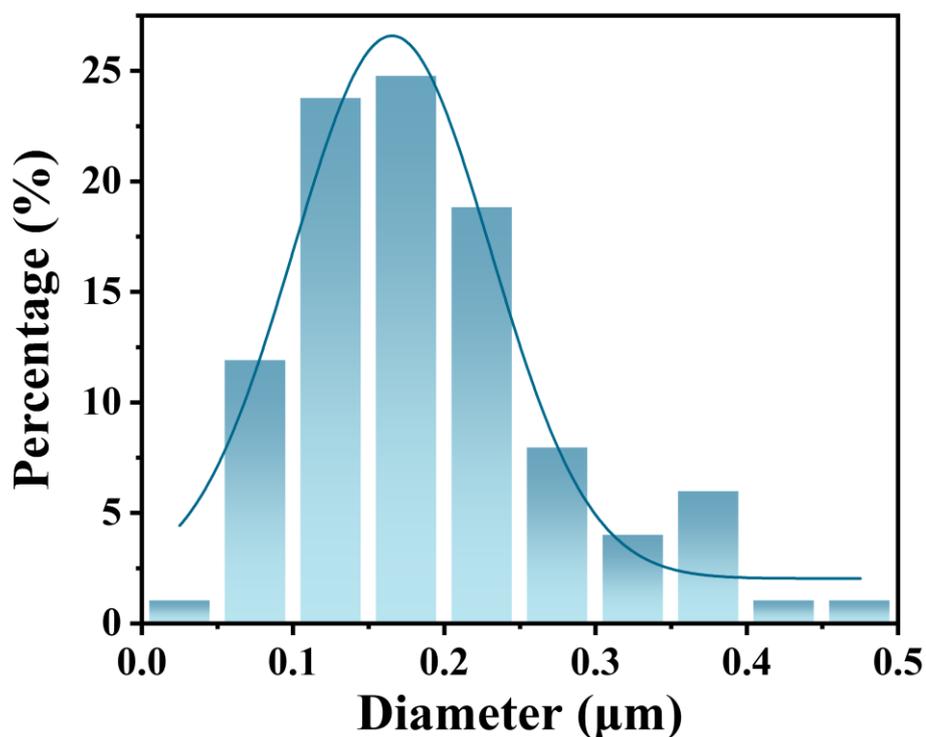
$$\text{NH}_3 \text{ yield rate} = 0.318 \times C_{\text{NH}_4\text{Cl}} \times V / (m_{\text{cat}} \times t)$$

Where F is Faraday constant (96485 C mol<sup>-1</sup>), C<sub>NH<sub>4</sub>Cl</sub> is the measured mass concentration of NH<sub>4</sub>Cl; V is the volume of the cathodic reaction electrolyte; Q is the quantity of applied charge/electricity; t is the time for which the potential was applied; m<sub>cat</sub> is the mass of catalyst loaded at the carbon cloth.

## 8. DFT calculations

The first-principles spin-polarized calculations were carried out using the Vienna Ab initio Simulation Package (VASP).<sup>1,2</sup> The exchange-correlation energy was modeled with the Perdew-Burke-Ernzerhof (PBE) functional within the generalized gradient approximation (GGA).<sup>3,4</sup> The interactions between ions and electrons were accurately described using the projector augmented wave (PAW) method.<sup>5</sup> A plane-wave basis set with a cutoff energy of 500 eV was employed throughout the calculations. Convergence criteria for energy and force were set to 10<sup>-5</sup> eV and 0.01 eV/Å, respectively. For structural relaxation, the Brillouin zone was sampled using a 3 × 3 × 1 grid based on the Monkhorst-Pack scheme. Long-range van der Waals (vdW) interactions were accounted for with Grimme's DFT-D3 dispersion correction method. A vacuum slab of over 15 Å was applied along the z-direction. The change in free

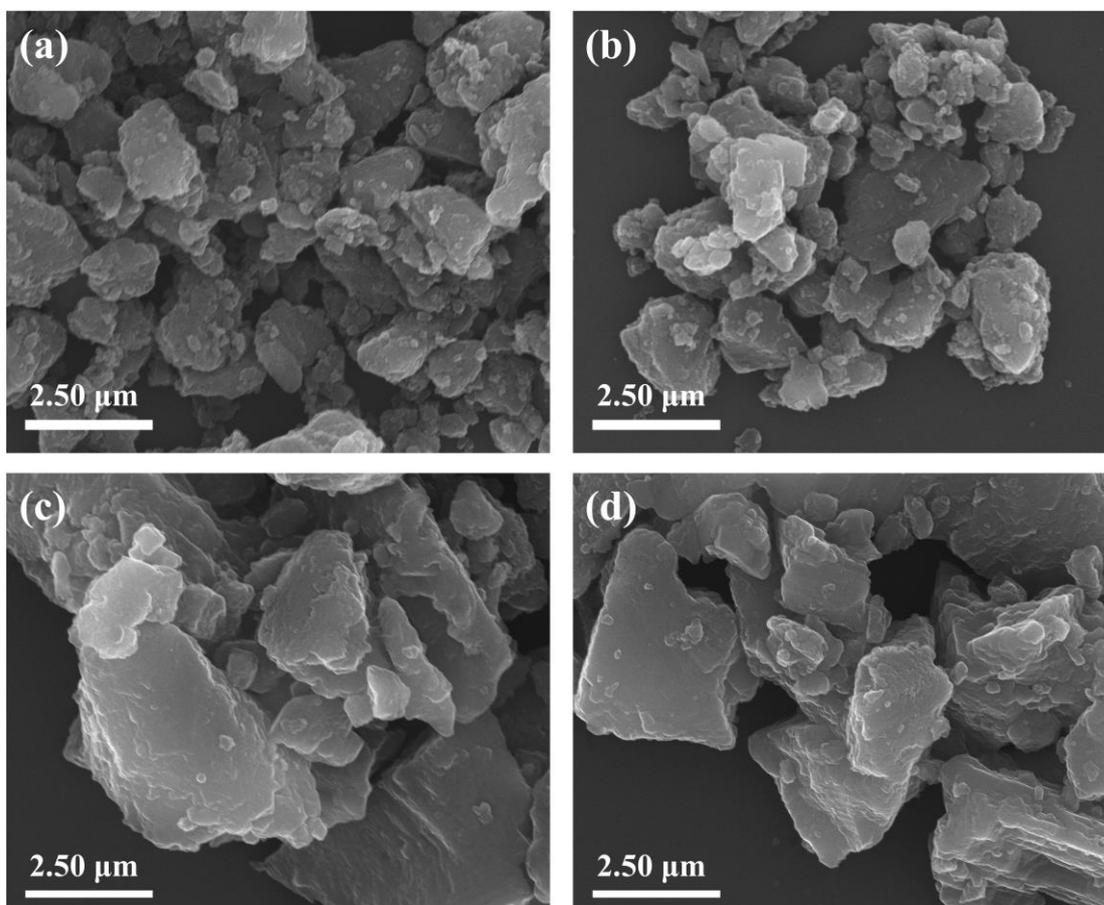
energy ( $\Delta G$ ) for each hydrogenation step was computed using the computational hydrogen electrode (CHE) model,<sup>7</sup> where  $\Delta G$  for each surface was defined by the equation:  $\Delta G = \Delta E + \Delta E_{\text{ZPE}} - T\Delta S + \Delta G_{\text{U}} + \Delta G_{\text{pH}}$ . Here,  $\Delta E$  was derived from DFT calculations,  $\Delta E_{\text{ZPE}}$  represents the zero-point energy (ZPE) corrections, and  $\Delta S$  accounts for entropy corrections. The temperature ( $T$ ) was set to 298.15 K, and the pressure was set to 0.1 MPa.  $\Delta G_{\text{U}}$  represents the contribution of the applied potential, with  $U$  being the applied electrode potential.  $\Delta G_{\text{pH}}$  is the free energy correction for the  $\text{H}^+$  concentration, defined as  $\Delta G_{\text{pH}} = k_{\text{B}}T \times \ln 10 \times \text{pH}$ , where  $k_{\text{B}}$  is the Boltzmann constant and the pH value is zero. The limiting potential ( $U_{\text{L}}$ ) for the overall elementary step was calculated by determining the potential-determining step (PDS), which exhibits the most positive Gibbs free energy change ( $\Delta G_{\text{max}}$ ), using the formula:  $U_{\text{L}} = -\Delta G_{\text{max}}/e$ .



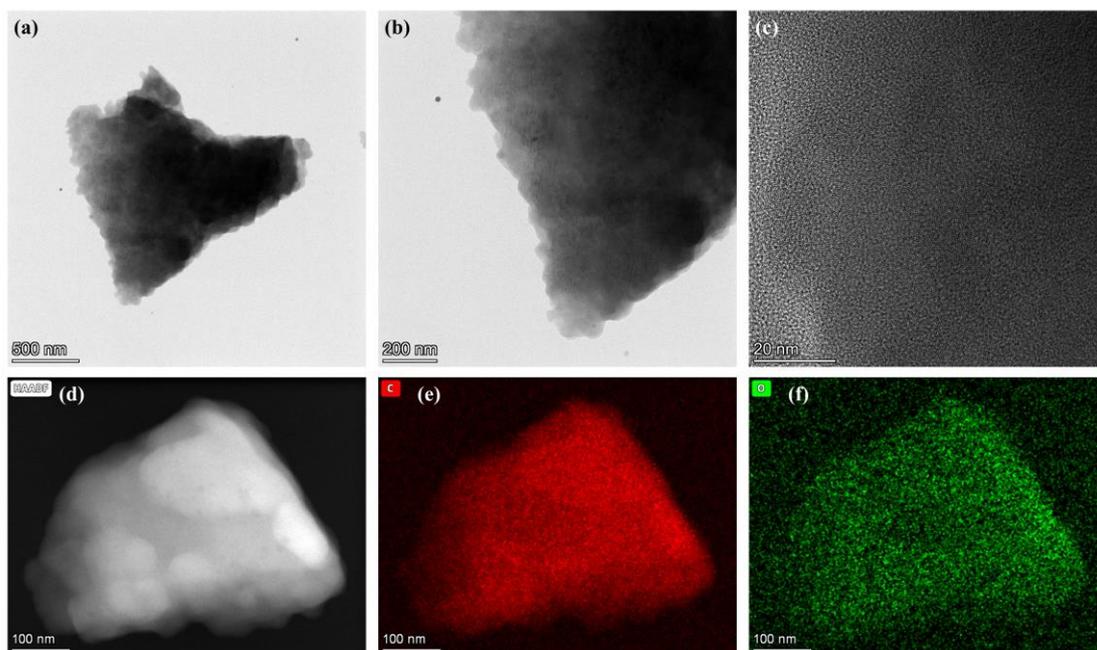
**Figure S1.** Average size distribution measured in SEM for 101 particles utilizing *Nano Measurer 1.2* software.

**Table S1.** Work function of Mn (101), C<sub>60</sub> and C<sub>60</sub>/Mn (101).

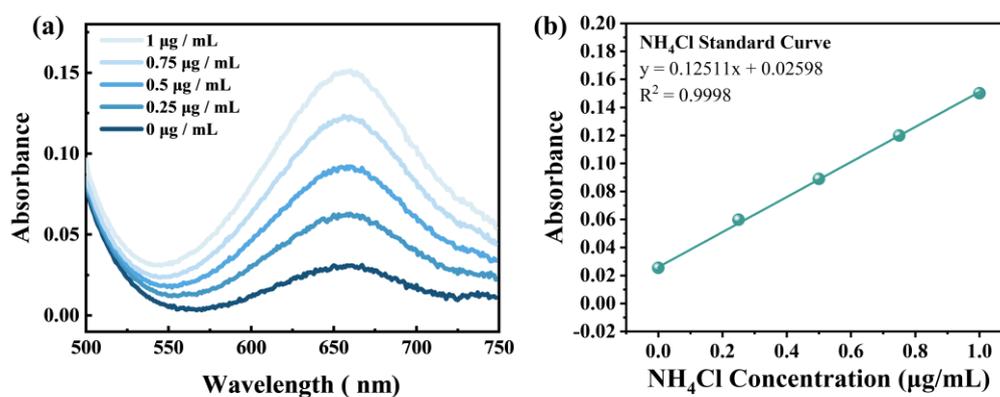
Slab	Work function (eV)
C <sub>60</sub>	5.52
Mn(101)	3.75
C <sub>60</sub> /Mn(101)	3.23



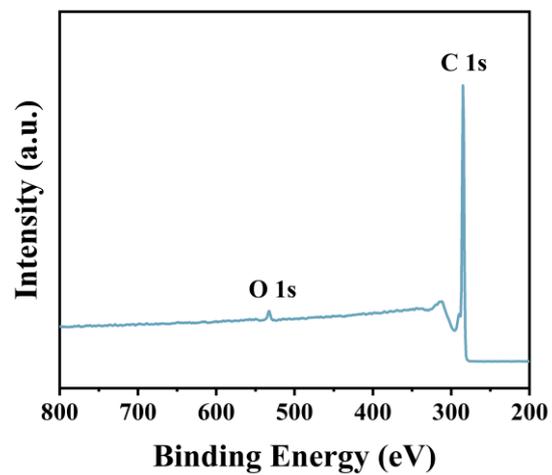
**Figure S2.** SEM image of synthesised (a-b) Mn/C<sub>60</sub> and (c-d) C<sub>60</sub>.



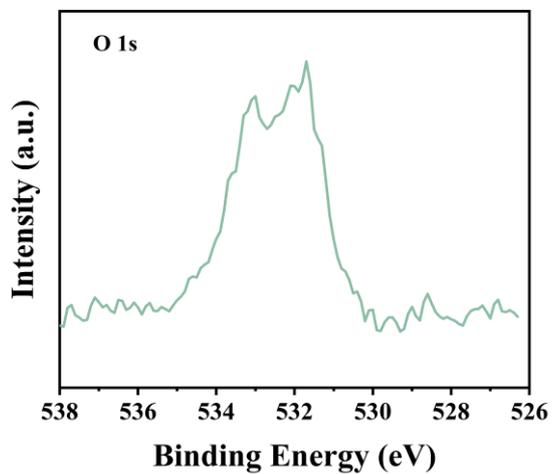
**Figure S3.** (a-c)The high resolution transmission electron microscopy (HRTEM) image of synthesised C<sub>60</sub> and (d-f) corresponding EDS mapping images of C<sub>60</sub>.



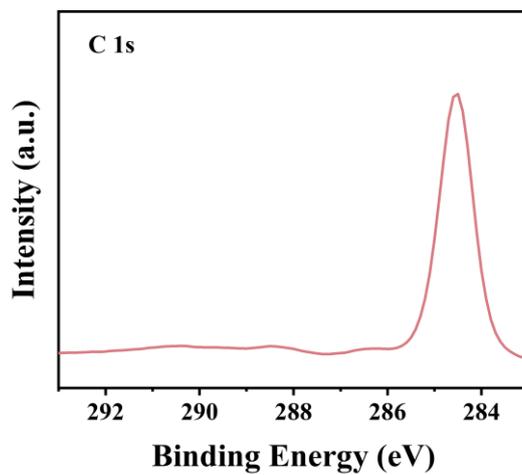
**Figure S4.** (a) UV-vis curves and (b) concentration-absorbance of NH<sub>4</sub>Cl solution with a series of standard concentration (0-1 µg mL<sup>-1</sup>) in 0.08 M Na<sub>2</sub>HPO<sub>4</sub>. The absorbance at 655 nm was measured by UV-vis spectrophotometer. The standard curve showed good linear relation of absorbance with NH<sub>4</sub>Cl concentration ( $y=0.12511x+0.02598$ ,  $R^2=0.9998$ ).



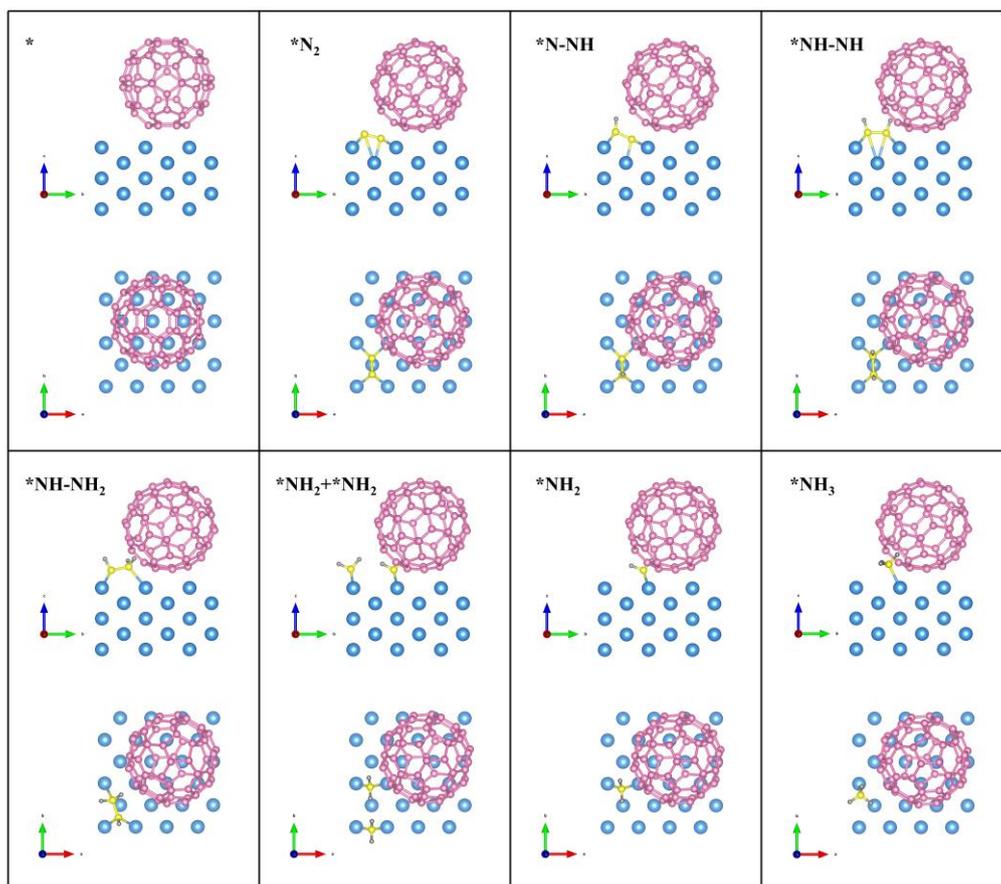
**Figure S5.** XPS survey spectrum of C<sub>60</sub>.



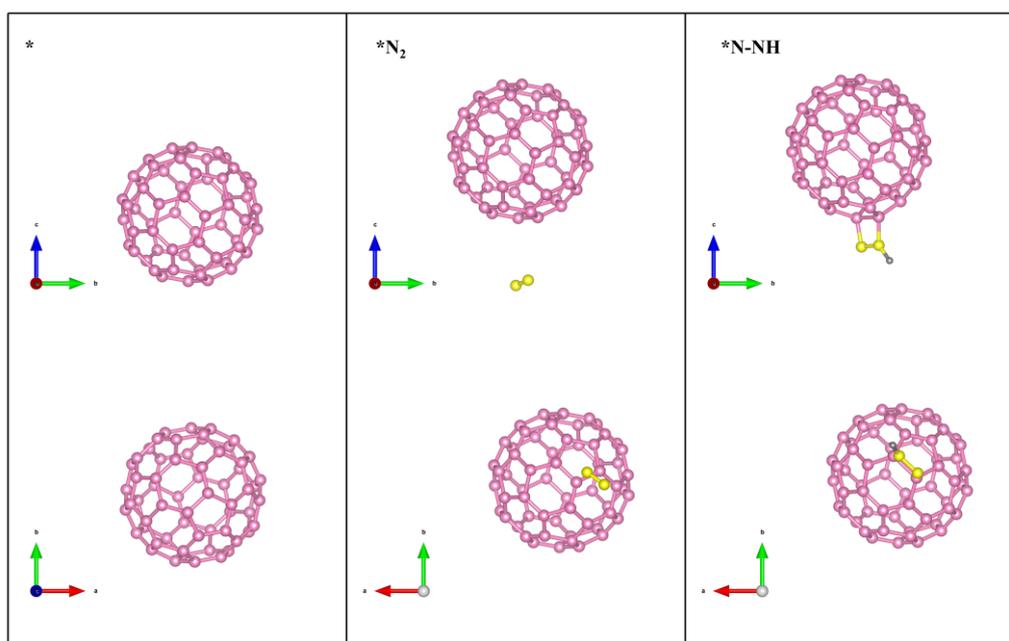
**Figure S6.** High-resolution XPS spectra of O 1s for C<sub>60</sub>.



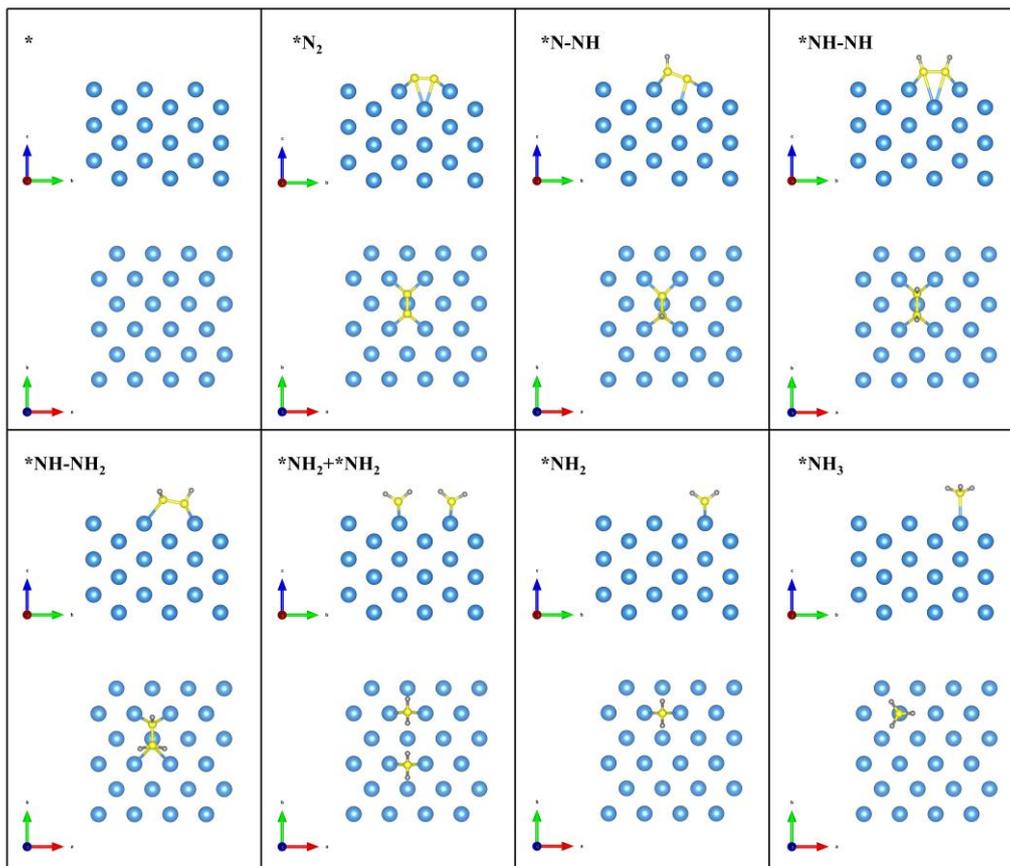
**Figure S7.** High-resolution XPS spectra of C 1s for C<sub>60</sub>.



**Figure S8.** Adsorption configurations of different species during the NRR on Mn/C<sub>60</sub>.



**Figure S9.** Adsorption configurations of different species during N<sub>2</sub> → \*N<sub>2</sub>H on C<sub>60</sub>.



**Figure S10.** Adsorption configurations of different species during the NRR on Mn.

**Table S2.** Calculated zero-point energy ( $E_{ZPE}$ ) and  $TS$  of different adsorption species, where \* denotes the adsorption site, and 298.15 K.

Adsorption species	$E_{ZPE}$ (eV)	$TS$ (eV)
*N≡*N	0.19	0.14
*N≡N	0.21	0.13
*N-*NH	0.47	0.19
*NH-*NH	0.82	0.19
*NH <sub>2</sub> -*N	0.83	0.12
*NH-*NH <sub>2</sub>	1.14	0.18
*NH <sub>2</sub> +*NH <sub>2</sub>	1.25	0.25
*NH <sub>2</sub>	0.63	0.14
*NH <sub>3</sub>	1.02	0.16
*H	0.15	0.01

**Table S3.** Energies of N<sub>2</sub>, H<sub>2</sub>, NH<sub>3</sub> adopted in this work where  $E_{\text{DFT}}$  stands for the energy obtained from DFT calculations. For the gas molecules, their  $E_{\text{ZPE}}$  and  $S$  values (gas phase H<sub>2</sub>, N<sub>2</sub>, NH<sub>3</sub> at T = 298.15 K, P = 1 bar) are from the NIST database. (<https://doi.org/10.18434/T4D303>)

Species	$E_{\text{DFT}}$ (eV)	$E_{\text{ZPE}}$ (eV)	$TS$ (eV)	$G$ (eV)
H <sub>2</sub>	-6.77	0.27	0.40	-6.90
N <sub>2</sub>	-16.63	0.15	0.60	-17.08
NH <sub>3</sub>	-19.54	0.91	0.60	-19.23

**Table S4.** Comparison of the electrocatalytic activity of Mn/C<sub>60</sub> to produce NH<sub>3</sub> through NRR with previously reported NRR electrocatalysts.

Catalyst	NH <sub>3</sub> yield rate ( $\mu\text{g h}^{-1} \text{mg}^{-1}$ ) <sub>1)</sub>	Faradaic efficiency (%)	Reference
Mn/C <sub>60</sub>	14.52	42.18	This work
Pd/C	4.5	8.2	8
V <sub>2</sub> O <sub>3</sub> /C	12.3	7.28	9
C-TiO <sub>2</sub>	16.22	1.84	10
Mn <sub>3</sub> O <sub>4</sub> Nanocube	11.6	3	11
F-SnO <sub>2</sub> /CC	19.3	8.6	12
SnO <sub>2</sub> /CC	4.03	2.17	13
NPC	27.2	1.42	14
Nb <sub>2</sub> O <sub>5</sub> nanofiber	43.6	9.26	15
Au-Bi <sub>2</sub> Te <sub>3</sub> Nanosheets	32.73	20.39	16
WO <sub>x</sub> /NPC	46.8	10.2	17
PC/Sb/SbPO <sub>4</sub>	23	34	18

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