

**Supplemental Information
for
Rational design of stable carbon nitride monolayer membranes for
highly controllable CO₂ capture and separation from CH₄ and C₂H₂**

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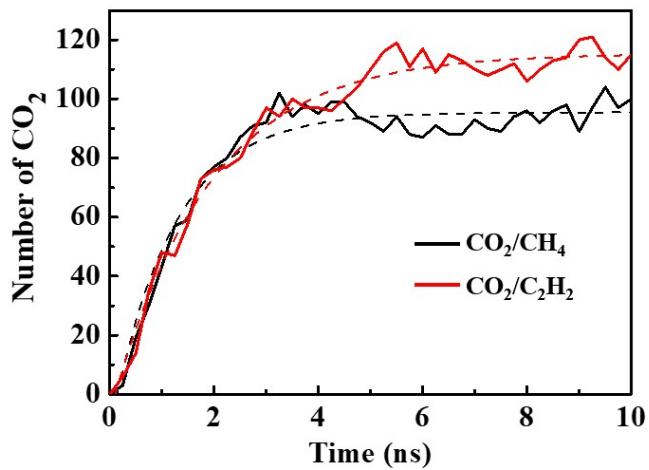


Fig. S1. The number of permeated CO₂ molecules versus the simulation time in the separation of CO₂/CH₄ and CO₂/C₂H₂ at 300 K. The corresponding dotted lines are the fitted lines.

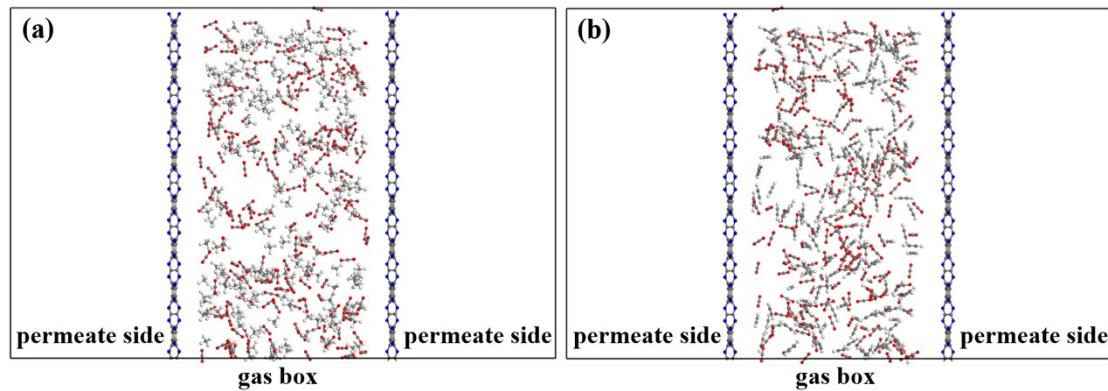


Figure S2. The initial models of (a) CO₂/CH₄ and (b) CO₂/C₂H₂ mixtures through the g-C₁₂N₈ membrane.

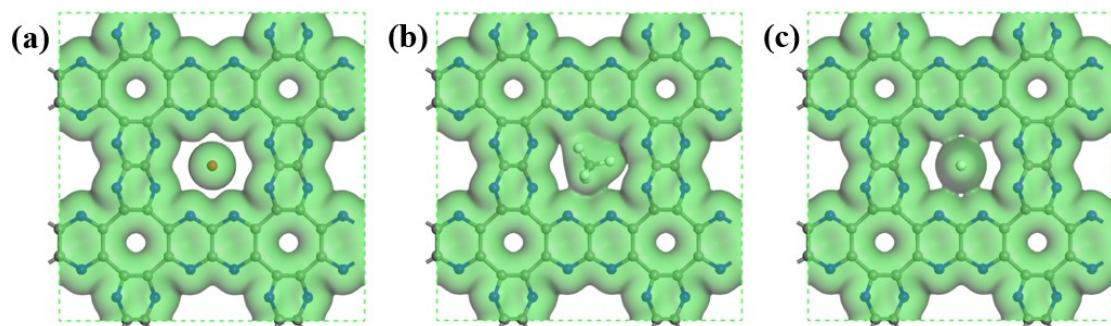


Figure S3. Electron density isosurfaces for (a) CO₂, (b) CH₄, and (c) C₂H₂ molecules permeating through the C₁₂N₈ monolayer (isovalue of 0.08 e·Å⁻³).

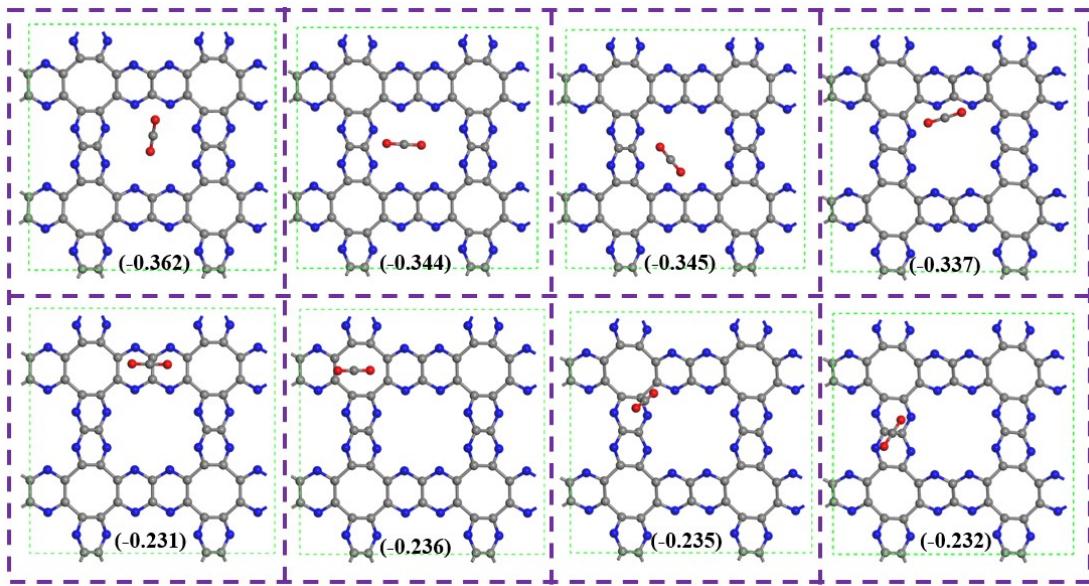


Figure S4. The stable adsorption sites for CO_2 on the $\text{g-C}_{12}\text{N}_8$ membrane. The values in parentheses are the corresponding adsorption energy (in eV).

Table S1 Atomic coordinates for the unit cell of the g-C₁₂N₈ monolayer.

| Lattice Parameters (Å, °) | Atom | Coordinates (fractional) | | |
|------------------------------|------|--------------------------|--------|--------|
| | | x | y | z |
| | N | 0.1429 | 0.6736 | 0.5057 |
| | N | 0.8571 | 0.3264 | 0.4943 |
| | N | 0.8571 | 0.6736 | 0.4943 |
| | N | 0.1429 | 0.3264 | 0.5057 |
| | N | 0.3742 | 0.8551 | 0.5374 |
| | N | 0.6258 | 0.1449 | 0.4626 |
| | N | 0.6258 | 0.8551 | 0.4626 |
| | N | 0.3742 | 0.1449 | 0.5374 |
| a=8.01 | C | 0.2844 | 0.5900 | 0.5119 |
| b=8.01 | C | 0.7156 | 0.4100 | 0.4881 |
| c=25 | C | 0.7156 | 0.5900 | 0.4881 |
| α=β=γ=90 | C | 0.2844 | 0.4100 | 0.5119 |
| | C | 0.4237 | 0.2862 | 0.5151 |
| | C | 0.5763 | 0.7138 | 0.4849 |
| | C | 0.5763 | 0.2862 | 0.4849 |
| | C | 0.4237 | 0.7138 | 0.5151 |
| | C | 0.0000 | 0.4117 | 0.5000 |
| | C | 0.0000 | 0.5883 | 0.5000 |
| | C | 0.4409 | 0.0000 | 0.5214 |
| | C | 0.5591 | 0.0000 | 0.4786 |

Table S2 A summary of the CO₂/CH₄ separation performance of membranes in this work along with reported literature.

| Membranes | Permeance (GPU) | Selectivity | Reference |
|--|---------------------------|-----------------------|-----------|
| g-C ₁₂ N ₈ | 1.21×10 ⁷ | 3.03×10 ³ | This work |
| MMM-0.5wt.% | 154 | 21.4 | [1] |
| 2D-CAP | 4.824 × 10 ⁵ | 32 | [2] |
| GO-PEGDA500 | 175.5 | 69.5 | [3] |
| LDH membrane with 8 nm-thick | 202 | 7 | [4] |
| GDY monolayer(x=10%,y=20%) | 1.29×10 ⁶ | 5.27×10 ³ | [5] |
| ZSM-58 zeolite membranes(0.2MPa) | 510 | 290 | [6] |
| MMM 15% | 2.74 | 13.30 | [7] |
| PES CNTs | 35.18 | 4.97 | [8] |
| Charged NPG | 5.65×10 ⁶ | 42.8 | [9] |
| Strain-controlled graphenylene | 3.52×10 ⁶ | 1.8 × 10 ⁵ | [10] |
| CHA (t < 500 nm) | 3.82×10 ⁴ | 198 | [11] |
| Amino-functionalized SAPO-34 | 1.5×10 ³ | 245 | [12] |
| g-C ₃ N ₄ -MXene-X/Pebax | about 1.2×10 ³ | 47.76 | [13] |

Table S3 A summary of the CO₂/C₂H₂ separation performance of membranes in this work along with reported literature.

| Membranes | Permeance (GPU) | Selectivity | Reference |
|------------------------------------|----------------------|-------------|-----------|
| g-C ₁₂ N ₈ | 1.39×10 ⁷ | 310 | This work |
| Strain-controlled C ₂ N | 5.05×10 ³ | 6 | [14] |
| Strain-controlled C ₂ O | 1.44×10 ⁶ | 6 | [14] |
| Porous graphene | 585 | 17 | [15] |
| High-silica CHA zeolite | 3.28×10 ³ | 55 | [16] |
| ZIF-8 M-60 | 319.1 | 1.8 | [17] |

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