Supporting information

Fine bubble technology for the green synthesis of fairy chemicals

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Synthetic scheme from ester (18)

At first, we focused on synthesizing the active intermediate AICA from an ester. We have chosen ethyl cyano(hydroxyimino)acetate (18) as a starting material and the reduction reaction was done first to synthesize ethyl 2-amino-2-cyanoacetate (19) by using a spray-type FB generator. Then, the amidation reaction was done using ammonia gas to get 2-amino-2-cyanoacetamide (13) and finally the coupling reaction to get AICA (4).



Scheme S1. Starting material- ethyl 2-cyano-2-(hydroxyimino)acetate (18), reduction to ethyl 2-amino-2-cyanoacetate (19) amidation to 2-amino-2-cyanoacetamide (13), reductive coupling to AICA (4)

Both the reduction and amidation reaction was done by using spray type FB generator with a 78% yield. However low yield was found during the coupling reaction. We found that the previously used ammonia was affecting the coupling reaction, we added excess acetic acid from outside to activate the reaction, but the reactivity did not enhance. The reaction without ammonia and acetic acid is the preferred condition for the coupling reaction. However, it is not easy to remove ammonia from amino nitrile (13) for a plant batch, and it is not a suitable synthesis pathway from the green chemistry viewpoint. Then focused on using ammonia in the final stage by changing the reaction pathway.

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$NC \underbrace{\downarrow}_{NH_2}^{O} NH_2$ 13	H ₂ N ^N NH	AcOH (100 eq)		
	• AcOH 11 (1.0 eq)	EtOH (0.1 M) 1 h	N NH ₂ H 4	
Entry	Solvent	Additives	Temperature (°C)	Yield $(\%)^a$
1	$EtOH^b$	-	80	50
2	EtOH	AcOH	80	n.d. ^c
3	EtOH	-	120	28
4	EtOH	AcOH	120	n.d.
5	EtOH-NH ₃	-	80	20
6	EtOH-NH ₃	AcOH	80	n.d.
7	EtOH-NH ₃	-	120	32
8	EtOH-NH ₃	AcOH	120	n.d.

Table S1. Effect of acid additive for the synthesis of AICA from ethyl ester

^{*a*}Determined by ¹H NMR with dimethyl sulfone as an internal standard. ^{*b*}NH₃ was removed by concentration. ^{*c*}AICA was not detected.

Synthetic scheme by using NH₃ in the final stage



Scheme S2. Starting material ethyl 2-cyano-2-(hydroxyimino)acetate (18), reduction to ethyl 2-amino-2-cyanoacetate (19), coupling reaction to ethyl 5-amino-1*H*-imidazole-4-carboxylate (20), finally amidation reaction to AICA (4)

After reducing oxime (18), a coupling reaction of ethyl 2-amino-2-cyanoacetate (19) and formamidine in batch condition was performed, yielding the ester (20) in 42% yield. Then, the amidation by ammonia which is the final stage was examined. First, the examination of ammonia FB by the spray-type FB generator was tried, but the amidation did not progress at one pass (30 °C, 11 mL/min). In addition, the circulatory system was tested. Still, as it circulated, the solvent absorbed ammonia, and it became difficult to pump the liquid according to the flow rate set by the pump (it is considered that it becomes negative pressure when sucking up the solution, and ammonia in the system becomes gas). Therefore, the amidation of ester 20 was performed at 0.3 MPa and 120 °C conditions in a pressure-resistant container. However, the progress of the reaction was not observed even after 2 hours.

Synthetic scheme using methyl 2-cyano acetate



Scheme S3. Starting material methyl 2-cyano acetate (21), oximation to methyl 2-cyano-2-(hydroxyimino)acetate (22), reduction to methyl 2-amino-2-cyanoacetate (23), coupling reaction to methyl 5-amino-1H-imidazole-4-carboxylate (24) amidation in aqueous ammonia to AICA (4).

Next, we started with methyl ester (21) as the reactivity of methyl ester towards ammonolysis is higher than the ethyl ester.¹ Methyl 2-cyano-2-(hydroxyimino)acetate (22) was prepared using our usual method, yielding compound 24 in 52% yield (21 to 24). Amidation reaction was attempted using the pressureresistant container described above for ethyl ester 20, but the progress of the reaction was not confirmed. Therefore, decided to investigate the uniform liquid-phase reaction using aqueous ammonia, not just the gas-liquid phase reaction. After mixing the ester with aqueous ammonia, the vial was sealed at 100 °C. However, since the progress of the response could hardly be confirmed even after 3 hours had elapsed, it was judged to be difficult to put this scheme into practice.

Synthesis scheme by using 2-cyano acetamide as a starting material

The effect of the reaction using ammonia on the next stage, or the low activity of ammonia has been cited as a problem so far. Therefore, using 2-cyanoacetamide as the starting material, we designed a scheme for AICA synthesis that avoids ammonia.



Scheme S4. Starting material 2-cyano acetamide (9), oximation to 2-amino-N-hydroxy-2-oxoacetimidoyl cyanide (10), reduction to 2-amino-2-cyanoacetamide (13), coupling reaction to AICA (4)

After the synthesis of oxime **10**, the reduction of oxime by using spray type FB generator, the reduction yield was 91%. But there was a possibility of over reduction of **13**, and the stability of **13** was in concern. Again, the coupling reaction yield was 67%. So, we have planned to do a cascade-type one-pot reduction coupling reaction.

Cascade-type one-pot reduction coupling using microporous-FB generator

Micro porous FB generator is supplied by NORITAKE CO., LIMITED, Japan. This system injects pressurized gases through a tubular ceramic membrane with nanopores to create FBs. The reaction setup for a microporous FB method is composed of an HPLC pump, a hydrogen flow controller, a back pressure regulator, an MSE FB generator, a packed bed reactor for catalyst, a column oven (SHIMADZU), an SUS coil reactor, and a thermocouple.



Figure S1. Schematic diagram for the microporous FB reaction



Figure S2. Picture of the reaction set up for microporous FB generator

Set-up explanation: using a glass beaker (1) to make the reaction solution, pump (2) is used to circulate the reaction solution from the glass beaker, microporous FB generator has (5), two connectors, the liquid flow from the up connector and gas flow from side connector. The hydrogen gas passes through a pressure gauge (3) and Mass flow controller (4) to find out the gas pressure and gas flow rate, respectively. Inside the generator, gases are passed through the microporous element and form FB by mixing with liquid. a column oven (8) to heat the reaction solution, a packed bed reactor placed inside the oven filled with catalyst (6) and up flow for the reduction of oxime, and a SUS coil reactor (7) inside the oven for the coupling reaction, another submerged coil reactor (9) to reduce the temperature by cooling, a back pressure regulator (10) to control the flow rate and a thermocouple to check to the temperature of reaction mass.

Temperature dependence on the synthesis of AICA and by-product:

The formation of AICA at different temperatures has been observed by using a microporous type of FB generator. Checked the AICA formation and by-product/AICA area ratio at 60 °C, 80 °C and 120 °C, respectively. other variables like formamidine acetate (1.2 equivalent), methanol (0.1 M), catalyst (3 mol%), and hydrogen gas flow keep constant. The obtained result indicates that the formation of AICA increases with increasing temperature. The ratio of by-product/AICA also increases with increasing temperature; it indicates that by-product formation also increases with increasing temperature.

Microporous type Finebubble



Figure S3. AICA formation at different temperatures



Figure S4. By-product/AICA area ratio at three different temperatures

Cascade-type one-pot reduction coupling using pressurized-depressurized FB generator.

Pressurized-depressurized FB generator was supplied by PMT Inc., Japan, composed of an HPLC pump, a hydrogen flow controller, two back pressure regulators, a mixer, a Packed bed reactor for catalyst, a column oven (SHIMADZU), and a thermocouple.



Figure S5. Schematic diagram for the pressurized-depressurized FB generator



Figure S6. Picture of the reactor set up for pressurized-depressurized FB generator.

Reaction Set-up explanation: using a glass beaker (1) to make the reaction solution, a pressurized depressurized FB generator (2), which is made by combining a pump (3) is used to circulate the reaction solution from the glass beaker, a continuous hydrogen gas flow from a gas cylinder via mass flow controller (4), gas and liquid mix by the back pressure regulator (5) and used to make FB of the gas-liquid mixture, a column oven (6) to heat the reaction solution, a packed bed catalyst column (7) and a SUS coil reactor (8) inside the oven for the coupling reaction, another submerged coil reactor (9) to reduce the temperature after reaction, second back pressure regulator (10) to control the flow rate and a thermocouple to check to the temperature of reaction mass.



Scheme S5. Cascade-type one-pot reduction coupling using pressurized-depressurized FB generator.

Dissolved the oxime, formamidine acetate, and benzimidazole in methanol and placed the spherical Pt/C (5wt%) inside the column.). Placed a coil reactor (6.25 mL) with a catalyst column inside the oven (120 $^{\circ}$ C). Placed a water cooling before the second BPR to decrease the solution temperature. For this generator, the limitation is the flow rate. For this reaction, the liquid flow rate is 4.5 mL/min, and the hydrogen gas flow rate is 1.5 mL/min, applying the pressure of 3 MPa. The reaction was continued for 6 hours, but due to the limited gas supply and limited FB formation the AICA formation is not so high, it is around 34%.

Cascade-type one-pot reduction coupling using spray-type FB generator

Our laboratory developed its spray-type FB generator. Since FB is generated only by attaching a spray nozzle to the reaction tube supplying gas, this device can reduce the cost and experimental space by introducing the conventional FB generator. The reaction set up for the spray FB generator is composed of an HPLC pump, a spray nozzle, a SUS coil reactor, a hydrogen flow controller, a back pressure regulator, a steel reactor, a cylindrical filter, a column oven (SHIMADZU)



Figure S7. The schematic diagram for the spray FB generator

Set-up explanation: using a glass beaker (1) to make the reaction solution, pump (2) is used to circulate the reaction solution from the glass beaker, a continuous hydrogen gas flow from a gas cylinder and measure the gas flow rate by mass flow controller (3) and gas pressure by pressure gauge (4). a column oven (5) to heat the reaction solution, a steel reactor to create the FB (6) which has two connector, liquid flow as spray from upside and gas flow from side connector, FBs formed at the interface between the liquid and liquid spray at the presence of gas, a spray nozzle to convert the liquid into spray, a cylindrical filter to keep the catalyst inside the steel reactor, SUS coil for the coupling reaction (7) a submerged coil reactor (8) to reduce the temperature, a back pressure regulator (9) to control the flow rate and a thermocouple to check to the temperature of reaction mass.



Figure S8. Picture of the reactor set up for spray FB generator



Scheme S6. Cascade-type one-pot reduction coupling using spray-type FB generator.

For this case, we have used a steel reactor and placed the powder Pt/C catalyst inside the reactor in a cylindrical filter paper. The pump flow rate was 10 mL/min, and the gas flow rate was 50-60 mL/min, under a constant pressure of 0.5 MPa. Placed a water bath for cooling after the oven. The reaction was continued for 6 hours at 120 $^{\circ}$ C. The AICA formation after 6 hours is also very low, around 7%.

Cascade-type one-pot reduction coupling using MSE FB generator

MSE FB generator is composed of a two-layer glass reactor, multi-stacked stirrer, mass flow controller, heating ribbons, condenser, and Thermocouple.



Figure S9. Schematic diagram for the MSE FB generator

In this case, the constant gas is supplied through a mass flow controller (1) to the reactor which is made of two separate glass reactors (4 and 5) via the connector (6). A multi-stack element stirrer (8) is connected to the upper glass and stirred by a stirrer (2). A reflux condenser (3) was used to cool down the vapour. The solution was heated by heating ribbons (7)



Scheme S7. Cascade-type one-pot reduction coupling using MSE FB generator.

At first, the gas flow was started (100 mL/min). A 100 mL solution of oxime (**10**, 10 mmol), and formamidine acetate (12 mmol) in methanol was added. the powder Pt/C catalyst (3 mol%) was added to the stirring reactor (carefully added, catalyst gets fire during addition due to the presence of hydrogen gas flow). Stirring speed 500 rpm. The reaction temperature increased by heating the ribbon and the reaction was continued under reflux conditions.



Figure S10. Picture of the reactor set up for MSE FB.



Oxime conversion and AICA formation optimization using MSE FB generator

Figure S11. Reaction conversion and AICA yield% for MSE

Catalyst amount optimization



Figure S12. oxime conversion and AICA formation using different amount of Pt/C

Catalyst optimization



Figure S13. Oxime conversion of different catalyst

Reaction solvent optimization



Figure S14. Oxime conversion and AICA formation using different solvent

Concentration optimization



Figure S15. Oxime conversion and AICA formation using different concentration.

Formamidine acetate equivalent optimization



Figure S16. Oxime conversion and AICA formation using different amounts of formamidine acetate (11).

Different types of formamidine salt



Figure S17. Oxime conversion and AICA formation using different formamidine salt.

Mechanism of FB formation

Pressurized-depressurized FB generator generates FB by applying pressure and depressure respectively in a gas-liquid mixture (Figure A). The microporous FB method contains a microporous body that forms FB by passing the gas through the micropores in the presence of shear liquid force. For spray, first, when the droplet collides with the liquid surface at low speed, a hemispherical gas phase occurs between the droplet and the liquid surface. Next, a perforation is caused on the side of the air phase, and the end is combined as it spreads. Then, bubbles are generated in the form of necklaces. Eventually, they become FB by repeating spontaneous rupture (C, 1-4). For MSE up flow gas is supplied to form milli bubble by mixing with solvent. The FB is formed by high stirring of a multi stack element.



Figure S18. Mechanism for the formation of FB from different FB generator.

FB Concentration measurement

NanoSight LM10 (Malvern Panalytical, UK) was used for UFB measurements, and PartAn SI (MicrotracBEL Corp., Japan) for MB measurements. The basic setup of the measurement equipment followed our previous experimental approach.² The operating times were assumed to be until the FB concentration reached a steady state.

Generation method	Gas flow rate (mL/min)	Liquid flow rate (mL/min)	Total liquid volume (mL)	Operation time (h)
Microporous	20	80	100	4
Pressurized- depressurized ^a	25	25	200	4
MSE^{b}	50	—	450	2
Spray	_	50	200	6

^aBPR was for the maintenance of system pressure (4 MPa). ^bStirring speed was 300 rpm.

Relation between MB and AICA yield

To confirm the yield of AICA synthesised using different FB generators, we measured the concentration and size of the FBs. We used Nanosight (LM10, Malvern Panalytical, UK) and PartAn SI (MicrotracBEL Corp., Japan) to quantify the concentration and size of UFBs and MBs, respectively. The concentration of UFBs obtained using the spray-type FB generator was the highest (165 x 10⁷ particle/mL), followed by that obtained using the microporous- (106 x 10⁷ particle/mL), MSE- (79 x 10⁷ particle/mL), and pressurizeddepressurized (40 x 10⁷ particle/mL) FB generators using Nanosight (Table 2). This finding indicates the reactivity order of the FB generators as spray > microporous > MSE > pressurised-depressurised. In our previous study, we confirmed that higher MB concentrations led to lower catalytic activity because larger MBs were adsorbed on the catalyst surface, reducing the available area for the reaction.² Therefore, we determined the MB concentration using PartAn SI, with the following results: spray (1635 particle/mL) > pressurised-depressurised (763 particle/mL) > microporous (103 particle/mL) > MSE (23 particle/mL). This finding indicates that the order of the FB generators for the catalytic activity is MSE > microporous > pressurised-depressurised > spray. Greater MB concentration reduces the catalytic activity.

FB	generation	UFB concentration	UFB size $(nm)^a$	MB concentration	MB size $(\mu m)^b$
method	1	(×10 ⁷		(particle/mL) ^b	
		particle/mL) ^a			
Spray		165±1.95	114±1	1635±15	34.8±0
Pressur	rised-	39.7±2.0	113±1	763±17	66.7 ± 0.6
depress	surised				
Microp	orous	106±1.5	103±2	429±98	36.9±2.6
MSE		79.3±12.3	91±3	23±0	10.6±0

Table S2. Concentration and size of UFBs and MBs measured using different FB generation methods

^aDetermined by Nanosight. ^bDetermined by PartAn SI

Calibration curve for AICA with internal standard (Benzimidazole)

Hilic column ($250 \times 4.6 \text{ mm}$ l.D. S-5 µm, 12 nm) has been used for the quantification of AICA. Acetonitrile and 50 mM NH₄HCO₂ aqueous solution are used as an eluent with a gradient manner acetonitrile-50 mM NH₄HCO₂ aq with a liner gradient of 95:5 to 40:60 over 15 minutes and then isocratic flow of 40:60 for 5 minutes at a flow rate of 1 mL/min at a detection wavelength of 265 nm. Benzimidazole was used as an internal standard.



Figure S19. Calibration curve for AICA and internal standard (benzimidazole)



HPLC chromatogram for OPRCR

Figure S20. HPLC chromatogram of COPRC

DICA stability determination

DICA stability was determined by ¹H NMR, using a similar amount of DICA (0.017 mmol) and dimethyl sulfone (IS, 0.016 mmol). Here, the data for 0 days and after 22 days were shown. The ratio of the integrated area of DICA/dimethyl sulfone remained the same at 0.16 after 22 days. It indicates that DICA is stable at 4 °C for a long period.



Mass spectra of intramolecular cyclisation reaction



Figure S21. (a) Mass spectrum of PhI(OAc)₂ in water. (b) Mass spectrum of reaction mass



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References

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Compound Data

2-Amino-N-hydroxy-2-oxoacetimidoyl cyanide (10) Chemical Formula: C₃H₃N₃O₂, ¹H NMR (DMSO-d₆, 400 MHz) δ 7. 88 (s, 1H, -NH₂), 7. 80 (s, 1H, -NH₂), 14.4 (-OH) ¹³C NMR (DMSO-d₆ 100 MHz) δ 109.2 (CN), 128.3 (C), 160.0 (CO)





2-Amino-2-cyanoacetamide (13)

Chemical Formula: $C_3H_5N_3O$ ¹H NMR (DMSO-d₆, 400 MHz,) δ 4.43 (s, 1H, -CH-), 7. 60 (br, 2H, -CONH₂) ¹³C NMR (DMSO-d₆ 100 MHz) δ 47.3 (CH), 120.1 (CN), 168.1 (CO)





5-Amino-1H-imidazole-4-carboxamide (AICA, 4)

Chemical Formula: C₄H₆N₄O

¹H-NMR (400 MHz, DMSO-d₆), δ_{H} : 5.48 (2H, br, $-NH_2$), 6.67 (2H, br, $-CONH_2$), 7.10 (1H, s, Ar–H), and 11.48 (br, -NH). ¹³C-NMR (100 MHz, DMSO-d₆), δ_C : 110.5 (C), 129.7 (C), 145.3 (CH), 166.1 (CO).





4-Diazo-4H-imidazole-5-carboxamide (DICA, 5)

Chemical Formula: C₄H₃N₅O,

¹H NMR (DMSO-d₆, 400 MHz) δ 7.61 (s, 1H, -CH-), 7. 82 (s, 1H, -CONH₂), 8.0 (s, 1H, -CONH₂) ¹³C NMR (DMSO-d₆ 100 MHz) δ 102.8 (C-N=N), 150.2 (C-CO), 155.8 (CH), 161.8 (CO)





AHX (6)

Chemical Formula: $C_4H_3N_5O$, ¹H NMR (CD₃OD, 400 MHz) δ 8.41 (s, 1H, -CH-) ¹³C-NMR (100 MHz, CD₃OD), δ_C : 119.7, 143.1, 152.0, 153.0





By-product: 5-Hydroxy-1H-imidazole-4-carbonitrile (15)

Chemical formula: C₄N₃H₄O, ¹H NMR (CD₃OD, 400 MHz): δ 6.933 (s, 1H, -CH-) ¹³C NMR (CD₃OD, 100 MHz) δ 22.6, 85.6, 119.9, 127.2, 163.9, 178.7 DEPT 135(CD₃OD, 100 MHz) δ 22.6, 127.2, DEPT 90 (CD₃OD, 100 MHz) δ 127.2







Ethyl 2-amino-2-cyanoacetate (19)

Chemical Formula: C₅H₈N₂O₂, ¹H NMR (400 MHz, DMSO-d₆) δ 1.23 (t, 3H), 4.20 (q, 2H) ¹³C NMR (DMSO-d₆ 100 MHz) δ 13.8 (CH₃), 46.4 (CH₂), 62.0 (CH), 118.6 (CN), 167.2 (CO)





Ethyl 5-aminoimidazole-4-carboxylate (20)

Chemical Formula: $C_6H_9N_3O_2$, $R_f = 0.50$ (AcOEt : MeOH = 90 : 10) ¹H NMR (DMSO-d₆, 400 MHz) δ 1.26 (t, J = 7.2, 3H, -CH₃), 4.20 (q, J = 7.2, 2H, -CH₂-), 5.54 (br, 2H, -NH₂), 7.32 (s, 1H, Ar-H), 11.97 (br, 1H, -NH-)

¹³C NMR (DMSO-d₆ 100 MHz) δ 161.1, 162.84 (C=O), 153.2 (N=C-N), 135.4 (N-C-N), 101.2 (*C*-CO), 58.6 (-CH₂-), 14.5 (-CH₃)





Methyl 2-cyano-2-(hydroxyimino)acetate (22)

Chemical Formula: $C_4H_4N_2O_3$, ¹H NMR (DMSO-d₆, 400 MHz) δ 3.85 (s, 3H, -CH₃), 15.12 (br, 1H, -OH) ¹³C NMR (DMSO-d₆ 100 MHz) δ 53.4 (CH₃), 108.9 (CN), 125.7 (C), 159.0 (CO)





Methyl 2-amino-2-cyanoacetate (23)

Chemical Formula: $C_4H_6N_2O_2$, ¹H NMR (DMSO-d₆, 400 MHz) δ 3.33 (br, 2H, -NH₂), 3.75 (s, 3H, -OMe), 4.83 (s, 1H, -CH-) ¹³C NMR (DMSO-d₆ 100 MHz) δ 46.4 (CH3), 53.1 (CH), 118.6 (CN), 167.8 (CO)





Methyl 5-amino-1H-imidazole-4-carboxylate (24)

Chemical Formula: $C_5H_7N_3O_2$, $R_f = 0.50$ (AcOEt : Methanol = 90 : 10)

¹H NMR (DMSO-d₆, 400 MHz) δ 3.71 (s, 3H, -OCH₃), 5.57 (br, 2H, -NH₂), 7.34 (s, 1H, Ar-H), 12.10 (br, 1H, -NH-)

¹³C NMR (DMSO-d₆ 100 MHz,) δ 50.2 (CH₃), 99.5 (C), 136.7 (C), 154.7 (CH), 161.1 (CO)



