Supporting Information

Surfacial Enriched Ru onto Octahedral CeO₂ with Strong Electronic Interactions as Efficient Electrocatalyst for Hydrogen Generation in Alkaline Freshwater/seawater

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1. Experimental Section

1.1 Chemicals and Materials

Cerium nitrate hexahydrate (Ce(NO₃)₃·6H₂O), sodium phosphate (Na₃PO₄), ruthenium (III) chloride anhydrous (RuCl₃), hydrogen peroxide aqueous solution (30 % H₂O₂), potassium hydroxide (KOH), sulfuric acid (H₂SO₄), commercial Pt/C (20 *wt* % platinum on carbon black) and ruthenium dioxide (RuO₂).

1.2 Synthesis of CeO₂

 $0.87 \text{ g Ce}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$ and $0.0076 \text{ g Na}_3\text{PO}_4$ were added into a beaker containing 80 mL of deionized water and stirred for 30 minutes at room temperature. Then, the above solution was added to the Teflon-lined autoclave and placed in an oven at 170 °C for 600 min. After cooling to room temperature, the solution was centrifuged with deionized water and ethanol several times and put it into the oven for drying. The dried powder was oxidized in a tune furnace at 350 °C for 3 hours to obtain white CeO₂ powder.¹

1.3 Synthesis of Ru/CeO₂-H₂O₂

10 mg of anhydrous RuCl₃ and 20 mg CeO₂ were fully ground to obtain the black powder, and then put it into the porcelain boat and added 10 μ L of H₂O₂ reaction for one minute. Then, added 20 mL deionized water and evaporated it at 80 °C with stirring to obtain black Ru/CeO₂-H₂O₂.

1.4 Synthesis of CeO₂-H₂O₂

The synthesis of CeO_2 -H₂O₂ was identical to the Ru/CeO₂-H₂O₂ without the addition of RuCl₃.

2. Physical Characterization

Physical characterizations of the involved catalysts were performed by scanning electron microscope (SEM) (Regulus 8100) and transmission electron microscopy (TEM) (JEM-F200). X-ray diffraction (XRD) (Japan Rigaku Ultima IV) and X-ray photoelectron spectroscopy (XPS) (America Thermo Scientific K-Alpha) were used to determine the crystal structure and chemical composition. Electron paramagnetic resonance (EPR) (BRUKE EMXPLUS) can be used to qualitatively and quantitatively

detect oxygen vacancies in catalysts. Raman spectroscopy (D-MAX 2500/PC) can analyze the structural information of the catalysts. Inductively coupled plasma optical emission spectrometer (ICP-OES) (Hitachi U4150) analyzes the amount of Ru in the catalyst.

3. Electrochemical Measurements

All electrochemical measurements were conducted using a typical three-electrode setup in 1 M KOH and 0.5 M H₂SO₄ with a reversible hydrogen electrode (RHE), glassy carbon electrode and carbon rod as the reference electrode, working electrode, and counter electrode, respectively, at room temperature. In 1 M KOH + seawater, glassy carbon electrode, Ag/AgCl electrodes and graphite rods were used as working electrode, reference electrode, and counter electrode, respectively. All the potentials were transformed to the RHE according to the following equation: $E_{RHE} = E_{Ag/AgCl} +$ 0.0592 pH + 0.197. For ink preparation, 5 mg of catalyst and 1mg of carbon black were added to 1 mL Nafion solution and sonicated for 30 minutes. Then, the 20 µL prepared ink was applied to the glassy carbon electrode for testing. Linear sweep voltammetry (LSV) was collected with scanning rate of 5 mV s⁻¹ with 95% IR compensation. Electrochemical impedance spectroscopy (EIS) measurements were carried out in frequency ranges from 100 kHz to 0.01 Hz with an amplitude of 5 mV. Multi-step chronopotentiometry, multi-step chronoamperometry and chronoamperometry were performed to study the stability of the prepared catalysts.

3.1 Cyclic voltammetry (CV) Measurements

CV was performed with different scan rates (20-120 mV s⁻¹) in the non-Faraday interval.

3.2 Mass activity computation

Mass activity = Current (mA) $/ m_{Ru(Pt)}$

Current is taken from linear sweep voltammetry curves at an overpotential of 100 mV, and $m_{Ru(Pt)}$ is the mass of Ru(Pt) on the working electrode.

3.3 Turnover frequency calculation (TOF)

TOF is a familiar evaluation criterion of catalysts, which is identified as the number of reactants of the electrocatalytic active sites per area to convert to the expected product per time.²

Total hydrogen turnovers

$$= (|\mathbf{j}| \frac{\mathrm{mA}}{\mathrm{cm}^2})(\frac{1}{1000 \mathrm{mA}})(\frac{1 \mathrm{mol} \mathrm{e}^-}{96485.3 \mathrm{C}})(\frac{1 \mathrm{mol}}{2 \mathrm{mol} \mathrm{e}^-})(\frac{6.022 \times 10^{23} \mathrm{molecules} \mathrm{H}_2}{1 \mathrm{mol} \mathrm{H}_2})$$
$$= 3.12 \times 10^{15} \frac{\mathrm{H}_2/\mathrm{s}}{\mathrm{cm}^2} \mathrm{per} \frac{\mathrm{mA}}{\mathrm{cm}^2}$$

 $Ru/CeO_2 - H_2O_2$ (active sites) 10 mV

$$= \left(\frac{\text{catalyst loading per geometric area } \times \left(\frac{g}{\text{cm}^2}\right) \times \text{Ru } wt\%}{\text{Ru } M_W \left(\frac{g}{\text{mol}}\right)} \right) \left(\frac{6.022 \times 10^{23} \text{Ru } \text{atomes}}{1 \text{ mol } \text{Ru }}\right)$$
$$= \left(\frac{0.509 \times \frac{10^{-3} \text{g}}{\text{cm}^2} \times 12.40 \text{ } wt\%}{101.1} \right) \left(\frac{6.022 \times 10^{23} \text{Ru } \text{atomes}}{1 \text{ mol } \text{Ru }}\right)$$
$$= 3.76 \times 10^{17} \text{ Ru sites per cm}^2$$

$$\text{TOF} = \left(\frac{3.12 \times 10^{15}}{3.76 \times 10^{17}} \times |\mathbf{j}|\right) = 8.30 \times 10^{-3} \times |-2.06| = 0.017 \text{ Ru sites per } \text{cm}^2$$

 $Ru/CeO_2 - H_2O_2$ (active sites) 50 mV

$$\text{TOF} = \left(\frac{3.12 \times 10^{15}}{3.76 \times 10^{17}} \times |\mathbf{j}|\right) = 8.30 \times 10^{-3} \times |-15.56| = 0.13 \text{ Ru sites per cm}^2$$

 Ru/CeO_2 - H_2O_2 (active sites) 100 mV

$$\text{TOF} = \left(\frac{3.12 \times 10^{15}}{3.76 \times 10^{17}} \times |\mathbf{j}|\right) = 8.30 \times 10^{-3} \times |-51.92| = 0.43 \text{ Ru sites per cm}^2$$

Pt/C (active sites) 10 mV

$$= (|\mathbf{j}| \frac{\mathrm{mA}}{\mathrm{cm}^2})(\frac{1}{1000 \mathrm{mA}})(\frac{1 \mathrm{mol} \mathrm{e}^-}{96485.3 \mathrm{C}})(\frac{1 \mathrm{mol}}{2 \mathrm{mol} \mathrm{e}^-})(\frac{6.022 \times 10^{23} \mathrm{molecules} \mathrm{H}_2}{1 \mathrm{mol} \mathrm{H}_2})$$
$$= 3.12 \times 10^{15} \frac{\mathrm{H}_2/\mathrm{s}}{\mathrm{cm}^2} \mathrm{per} \frac{\mathrm{mA}}{\mathrm{cm}^2}$$

$$= \left(\frac{\text{catalyst loading per geometric area } \times \left(\frac{g}{\text{cm}^2}\right) \times \text{Pt wt\%}}{\text{Pt } M_W\left(\frac{g}{\text{mol}}\right)} \right) \left(\frac{6.022 \times 10^{23} \text{Pt atomes}}{1 \text{ mol Pt}}\right)$$
$$= \left(\frac{0.509 \times \frac{10^{-3} \text{g}}{\text{cm}^2} \times 20 \text{ wt\%}}{195} \right) \left(\frac{6.022 \times 10^{23} \text{Pt atomes}}{1 \text{ mol Pt}}\right)$$
$$= 3.14 \times 10^{17} \text{ Pt sites per cm}^2$$

$$\text{TOF} = \left(\frac{3.12 \times 10^{15}}{3.15 \times 10^{17}} \times |\mathbf{j}|\right) = 9.90 \times 10^{-3} \times |-0.82| = 0.0082 \text{ Pt sites per cm}^2$$

Pt/C (active sites) 50 mV

$$\text{TOF} = \left(\frac{3.12 \times 10^{15}}{3.15 \times 10^{17}} \times |\mathbf{j}|\right) = 9.90 \times 10^{-3} \times |-7.85| = 0.077 \text{ Pt sites per cm}^2$$

Pt/C (active sites)100 mV

$$\text{TOF} = \left(\frac{3.12 \times 10^{15}}{3.15 \times 10^{17}} \times |\mathbf{j}|\right) = 9.90 \times 10^{-3} \times |-23.99| = 0.24 \text{ Pt sites per cm}^2$$

 $\rm Ru/CeO_2$ - $\rm H_2O_2$ (active sites) 10 $\rm mV = 0.017~Ru~sites~per~cm^2$

Ru/CeO₂ - H_2O_2 (active sites) 50 mV = 0.13 Ru sites per cm²

 $Ru/CeO_2 - H_2O_2$ (active sites) 100 mV = 0.43 Ru sites per cm²

Pt/C (active sites) 10 mV= 0.0082 Pt sites per cm²

Pt/C (active sites) 50 mV = 0.080 Pt sites per cm²

Pt/C (active sites) 100 mV = 0.24 Pt sites per cm²

1 M KOH: When the overpotential is 10 mV, 50 mV, 100 mV, the current density of Ru/CeO₂-H₂O₂ are 2.06 mA cm⁻², 15.56 mA cm⁻², 51.92 mA cm⁻², TOF=0.017 H₂ s⁻¹, 0.13 H₂ s⁻¹, 0.43 H₂ s⁻¹. Similarly, the current density of Pt/C at 10 mV, 50 mV, 100 mV are 0.82 mA cm⁻², 7.85 mA cm⁻², 23.99 mA cm⁻² and TOF = 0.0082 H₂ s⁻¹, 0.080 H₂ s⁻¹ and 0.24 H₂ s⁻¹.

4. DFT Calculations

All density functional theory calculations were performed by Vienna ab initio simulation package (VASP).³ The Perdew-Burke-Ernzerhof (PBE)⁴ functional was employed to treat the exchange-correlation interactions. The plane-wave basis set with a kinetic energy cutoff of 400 eV, the energy convergence criterion of 10^{-4} eV, the force convergence criterion of 0.02 eV Å⁻¹, and a (1×1×1) Monkhorst-Pack k-point sampling was employed for structure relaxation. A sufficiently large vacuum gap (> 12 Å) was employed to prevent the interaction between neighboring periodic structures. H₂ and H₂O were calculated in boxes of 20 Å×20 Å×20 Å with the gamma point only. The free energy diagrams for HER were calculated with reference to the computational hydrogen electrode.⁵ The free energy of gas phase and adsorbed species can be obtained from the following equation:

 $\Delta G = \Delta E_{DFT} + \Delta ZPE - T\Delta S$

where T was set as 298.15 K. Δ ZPE and T Δ S was the change in the zero point energy and entropy.



Figure S1. Schematic of the synthesis procedure for CeO_2 and octahedral Ru/CeO₂-H₂O₂.



Figure S2. SEM images of (a) CeO_2 -H₂O₂ and (b) Ru/CeO₂-H₂O₂. (c) TEM image of Ru/CeO₂-H₂O₂.



Figure S3. The oxygen vacancy content in various catalysts.



Figure S4. The CV plots with different scan rates of (a) Ru/CeO₂-H₂O₂, (b) CeO₂ and (c) CeO₂-H₂O₂ in 1 M KOH.



Figure S5. The electrochemical double-layer capacitance (C_{dl}) of Ru/CeO₂-H₂O₂, CeO₂-H₂O and CeO₂.



Figure S6. (a) Nyquist plots and (b) Bode plots of $Ru/CeO_2-H_2O_2$ at different overpotentials.



Figure S7. (a) Nyquist plots and (b) Bode plots of CeO₂ at different overpotentials.



Figure S8. (a) Nyquist plots and (b) Bode plots of $CeO_2-H_2O_2$ at different overpotentials.



Figure S9. The equivalent circuit for Ru/CeO₂-H₂O, CeO₂ and CeO₂-H₂O₂.



Figure S10. Charge transfer resistance (R_{ct}) at different potentials.



Figure S11. Phase peak angles of Ru/CeO_2 - H_2O_2 , CeO_2 , CeO_2 - H_2O_2 at different potentials.



Figure S12. Polarization curves normalized by mass contents of Ru or Pt in Ru/CeO₂- H_2O_2 and Pt/C.



Figure S13. Multiple-step chronopotentiometric measurement in 1 M KOH.



Figure S14. XPS spectra of (a) Ce 3d, (b) O 1s and (c) Ru 3p in Ru/CeO_2 -H₂O₂ after stability.



Figure S15. The computed work function values for the CeO_2 (111), Ru (001), Ru/CeO₂-H₂O₂.



Figure S16. H adsorbed at the (a) Ce site, (b) O site, (c) Ru (001) site and (d) interface of Ru/CeO_2 (111)-Ov.



Figure S17. The CV plots with different scan rates of (a) Ru/CeO₂-H₂O₂, (b) CeO₂ and (c) CeO₂-H₂O₂ in 1 M KOH + seawater.



Figure S18. The C_{dl} of Ru/CeO_2 - H_2O_2 , CeO_2 - H_2O and CeO_2 in 1 M KOH + seawater.



Figure S19. HER performance of Ru/CeO₂-H₂O₂ in 0.5 M H₂SO₄. Polarization curves of Pt/C, Ru/CeO₂-H₂O₂, CeO₂-H₂O₂ and CeO₂ at (a) low and (b) high current densities. (c) Comparison of overpotentials of Ru/CeO₂-H₂O₂ and Pt/C at different current densities. (d) Corresponding Tafel slopes. (e) Multiple-step chronopotentiometric measurement. (f) Chronoamperometric measurement of Ru/CeO₂-H₂O₂ in 0.5 M H₂SO₄.



Figure S20. The CV plots with different scan rates of Ru/CeO_2 - H_2O_2 , CeO_2 and CeO_2 - H_2O_2 in 0.5 M H₂SO₄.



Figure S21. The C_{dl} of Ru/CeO_2 - H_2O_2 , CeO_2 - H_2O and CeO_2 in 0.5 M H_2SO_4 .



Figure S22. Multi-step chronopotentiometric measurement for overall water splitting (OWS).



Figure S23. (a) Multi-step chronopotentiometric measurement and (b) long-term stability test for overall seawater splitting.



Figure S24. (a) Optical photograph of $RuO_2 ||Ru/CeO_2-H_2O_2$ two-electrode device for OWS. (b) Optical photograph of drainage method collecting gas system. (c) Faradic efficiencies of $RuO_2 ||Ru/CeO_2-H_2O_2$ electrolyzer under 100 mAcm⁻² in 1 M KOH solution.

 Table S1. The ICP-OES (Ru) of Ru/CeO2-H2O2.

ICP-OES (Ru)	wt %
Ru/CeO ₂ -H ₂ O ₂	12.40

Overpotential (mV)@ Tafel slope (mV dec⁻¹) Catalysts References 10 mA cm^{-2} $Ru/CeO_2\text{-}H_2O_2$ 37 36.7 This work Ru-H₂O/CC 44 91 6 7 Ru-NiCoP/NF 44 45.4 Ru/OG 48 32.4 8 Ru/Co_4N - CoF_2 9 53 144.1 Ru SAs-Ni₂P 57 75 10 N-Ru-1/C 67 125 11 $N-Ru/Sb_2S_3$ 72 193 12 RuCu NPs/C 111 73.1 13

Table S2. Comparison of the HER activity of the $Ru/CeO_2-H_2O_2$ with other previously reported electrocatalysts in 1 M KOH.

Table S3. Comparison of the HER activity of the Ru/CeO_2 - H_2O_2 with other previouslyreported electrocatalysts under 1 M KOH + seawater.

Catalysts	Overpotential (mV)@ 10mA cm ⁻²	References
Ru/CeO ₂ -H ₂ O ₂	47	This work
Mo-Ru/CNTs	45	14
BPed-Ru-Gr	51	15
Ru ₂₂ NiMoP/NF	52	16
Ru _{1+NPs} /N-C	58	17
Co@RuCO-3	59	18
Ru/NC	72	19
Ru-Gr	82	15
Ru/BC	97	19
Ru/CNT	107	20

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