

## **Supplementary Information**

### **Conversion of recovered carbon black from waste tire to activated carbon via chemical/microwave methods for efficient removal of heavy metal ions from wastewater**

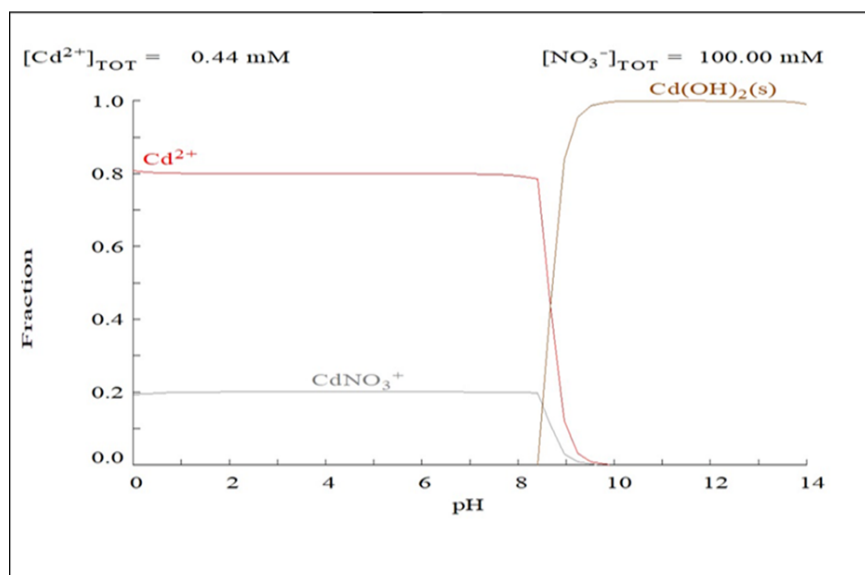
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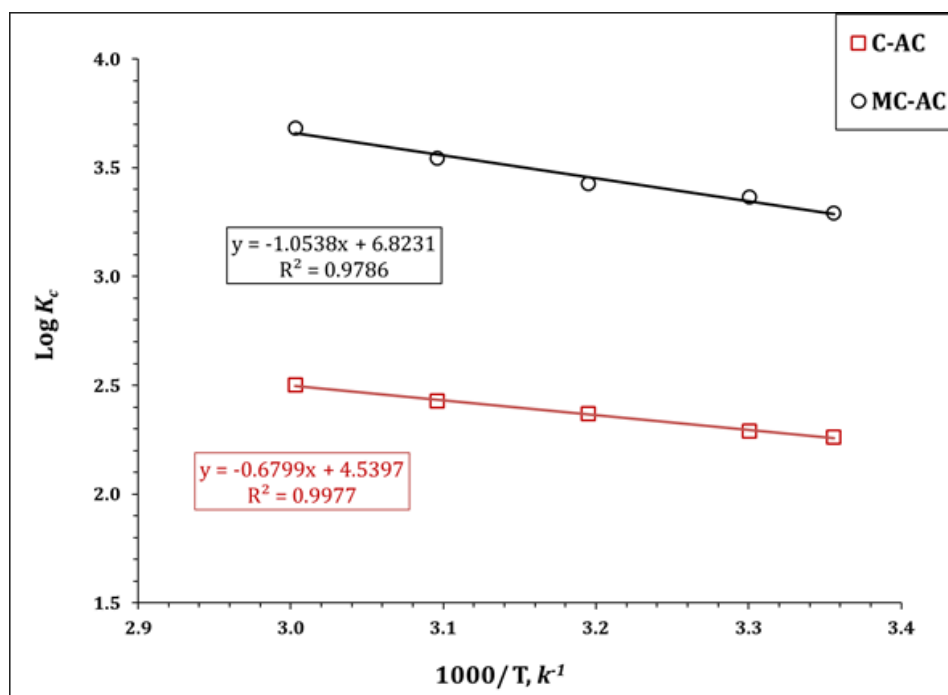
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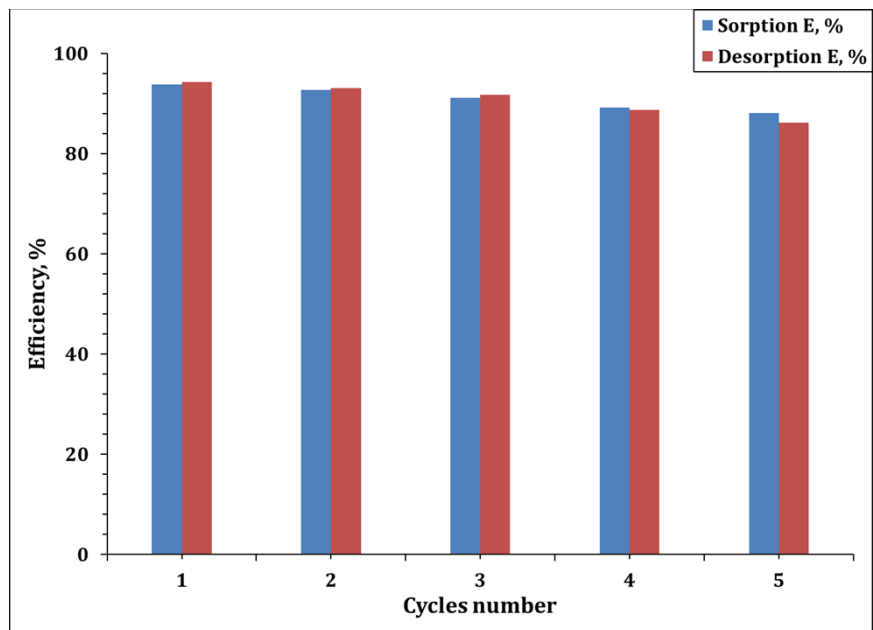
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**Figure S1:** Expected aqueous speciation of Cd(II) concentration (50 mg L<sup>-1</sup>) as a function of pH in 0.1 M HNO<sub>3</sub> using Medusa/Hydra program.



**Figure S2:** Van't Hoff plot for Cd(II) sorption onto C-AC and MC-AC sorbents.



**Figure S3:** Recycling investigation for Cd(II) uptake using MC-AC sorbent.

**Table S1: Kinetics, isotherm, and thermodynamics equations for Cd(II) ions adsorption of [1-5]**

Kinetics	Equations
Pseudo-first-order	$\text{Log} (q_e - q_t) = \text{Log} q_e - \frac{K_1}{2.303} t$
Pseudo-second-order	$\left(\frac{t}{q_t}\right) = \frac{1}{K_2 q_e^2} + \frac{1}{q_e} t$
Intra-particle diffusion model (IPD)	$q_t = K_{id} t^{0.5} + C_i$
Isotherms	Equations
Langmuir model	$C_e/q_e = (1/K_L q_{max}) + [C_e/q_m]$
Freundlich model	$\ln q_e = \ln K_F + \left[\frac{1}{n}\right] \ln C_e$
Temkin model	$q_e = \frac{RT}{b_T} \ln K_T C_e$
Thermodynamics	Equations
	$\log K_C = -\frac{\Delta H^o}{2.303 R} X \frac{1}{T} + C$
	$-\Delta G^o = 2.303 RT \log K_C$
	$\Delta G^o = \Delta H^o - T \Delta S^o$

$q_e$  (mg g<sup>-1</sup>) is the equilibrium concentration of Cd(II) ions, and  $q_t$  (mg g<sup>-1</sup>) is the adsorbed amount of Cd(II) ions after time  $t$  (min),  $k_1$  (min<sup>-1</sup>) and  $k_2$  (min<sup>-1</sup>) are the rate constants for the pseudo first and second order, respectively.  $K_{id}$  (mg/g. min<sup>0.5</sup>) is a rate constant, and  $C$  is the thickness of the boundary layer.  $C_e$  (mg L<sup>-1</sup>) is equilibrium concentration of Cd(II) ions,  $q_{max}$  (mg g<sup>-1</sup>) is the theoretical adsorption capacity,  $K_L$  is Langmuir constant,  $K_F$  and  $n$  are Freundlich constants.  $b_T$  is Temkin constant that refers to the adsorption heat, and  $K_T$  (L min<sup>-1</sup>) is the equilibrium binding constant.  $K_C$  is a non-dimensional equilibrium constant and it equals  $K_d \times 1000 \times \rho$  [1];  $T$  is the temperature (K),  $R$  is the universal gas constant (8.314 J mol<sup>-1</sup>. K<sup>-1</sup>),  $\rho$  is solution density g/L, and  $C$  is a constant.

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**Table S2:** *Cd(II)* recovery from loaded MC-AC sorbent using different solutions (5.0 g/L, room temperature; 240 min).

<b>Desorption investigation</b>		
<b>Eluent Type</b>	<b>Concentration, M</b>	<b>%</b>
Hydrochloric acid	0.5	93.5
Sulfuric acid	0.5	74.4
Nitric acid	0.5	56.2