

Supporting Information

Fabrication of monodisperse micron-sized and aldehyde-functionalized microspheres coating with covalent organic framework for efficient and rapid removal of copper ions from wastewater

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67 1. Experiment details

68 1.1 Preparation of seed

69 Monodisperse polystyrene seeds were synthesized via dispersion polymerization. First,
70 2 g of polyvinylpyrrolidone (PVP), 10 mL of styrene (St), and 0.2 g of AIBN were added
71 in sequence to dissolve them in ethanol (40 mL), and the mixture was mechanically stirred
72 at 70 °C at 200 rpm for 24 h. After the reaction was over, the product was alternately
73 washed with water and ethanol. The product was stored in 0.2% SDS (w/w).

74 1.2 PAD@COF for degradation and recovery

75 PAD@COF was added in of HCl and H₂SO₄ solutions (0.5 mol L⁻¹ and 1 mol L⁻¹),
76 respectively, and reacted at room temperature for 48 h. After drying, a reusable PAD was
77 obtained.

78 1.3 Adsorption of copper ion

79 The adsorption capacity of PAD@COF for copper ions was evaluated through both
80 isothermal and kinetic adsorption experiments. In the isothermal adsorption experiment,
81 150 mL of different concentrations (2.5, 3.5, 5, 10, 20, 30, 40, 50 and 60 mg L⁻¹) of copper
82 ion solutions were taken into the conical bottle, and PAD@COF (8 mg) was added to carry
83 out isothermal adsorption experiments, respectively. After the conical bottle was oscillated
84 at constant temperature under the condition of 170 rpm for 6 h, the suspension was
85 centrifuged and then passed through a 0.22 μm filter membrane to obtain the adsorbed
86 copper ions solution. The isothermal adsorption experiment was carried out by UV-VIS
87 spectrophotometer 3 times to obtain the average value, and the adsorption amount was
88 calculated according to the following:

$$89 \quad Q_e = (C_0 - C_e)V/m \quad (1)$$

90 where Q_e (mg g⁻¹) is the equilibrium adsorption capacity, C_0 and C_e (mg L⁻¹) are the
91 initial and equilibrium concentration of copper ion solutions, V (mL) is the volume of
92 copper ion solutions, and m (mg) is the mass of the material. The isothermal adsorption
93 data were further analyzed by Langmuir and Freundlich isothermal models, whose
94 formulas are as follows:

$$95 \quad C_e/Q_e = C_e/Q_{\max} + 1/K_L Q_{\max} \quad (2)$$

$$96 \quad \lg Q_e = \lg C_e/n + \lg K_F \quad (3)$$

97 where $Q_{\max}$ (mg g⁻¹) is the maximum adsorption capacity, C_e (mg g⁻¹) is the

equilibrium concentration, $1/n$ is the Freundlich empirical coefficient, K_L (mL mg⁻¹) and K_F (mg g⁻¹) are Langmuir and Freundlich constants respectively.

In the kinetic adsorption experiment, 150 mL of copper ion solutions with a concentration of 30 mg L⁻¹ were placed in the conical bottle to monitor the change in equilibrium concentration over time. After dispersing the material of 8 mg into the copper ion solution and oscillating at different times (5, 10, 30, 45, 60, 90, 120, 180 and 240 min) at constant temperature under the condition of 170 rpm, the suspension was centrifuged and then passed the adsorbed solution through the filter membrane of 0.22 μm. The kinetic adsorption property is the key factor to measure whether the material can quickly remove the target substance. The absorbance was measured 3 times in the UV-VIS spectrophotometer, and the average value was obtained. The dynamic adsorption data were further analyzed by the pseudo-first-order and pseudo-second-order kinetic models, whose formulas are as follows:

$$\ln(Q_e - Q_t) = \ln Q_e - K_1 t \quad (4)$$

$$t/Q_t = t/Q_e + 1/K_2 Q_e^2 \quad (5)$$

where K_1 and K_2 are the reaction rate constants of pseudo-first-order and pseudo-second-order kinetic model, respectively, and Q_t (mg g⁻¹) is the adsorption capacity at a particular time.

1.4 Instrument and Characterization Analysis

The morphology and size of materials were obtained by scanning electron microscope (SEM) (Carl Zeiss Jena, Sigma 500, GER). The surface functional groups of the adsorbent were determined by Fourier-transform infrared spectroscopy (FT-IR, Thermo Nicolet iS50 spectrometer, USA). The nitrogen adsorption/desorption experiment was implemented on an ASAP 2460 physisorption analyzer (Micromeritics, USA). The specific surface area was calculated via the Brunner-Emmet-Teller model (BET, Quantachrome Nova 2000e, USA). X-ray photoelectron spectroscopy (XPS) data were obtained on the ESCALAB 250XI XPS spectrometer (Thermo Scientific, USA). The residual concentration was analyzed with an ultraviolet-visible spectrophotometer (UV, TU-1950, China). The dissolution and polymerization reactions were accomplished in a constant temperature oscillator (Jintan Liangyou Instrument, Changzhou, China).

1.5 Mechanical stability of PAD@COF

The mechanical stability of the material was tested by treating the polymer with high

130 speed oscillation and grinding. As shown in Fig. S8, it can be seen that the polymer
131 structure was complete, indicating that the material has good mechanical stability.

132 **1.6 Surface area of the material before and after adsorption**

133 The pore structure and specific surface area pore structure of the adsorbed material
134 after 10 cycles was exhibited in **Table S3**. It can be seen that the specific surface area of
135 the material is significantly reduced after 10 cycles of adsorption, because copper ions
136 occupied part of the pore of the material.

137 **1.7 PXRD patterns of COF and PAD@COF**

138 The crystal properties of the materials were evaluated by PXRD. COF and
139 PAD@COF have two prominent peaks at 28.34° (2θ) and 19.78° (2θ), respectively,
140 indicating stacking between the COF layers.

141 **2. Material Characterization Supplement**

142 **2.1 Specific surface area analysis details**

143 The specific surface area was processed at 110°C and 1.33 Pa for about 6 h for
144 determination, and then air adsorption/desorption experiments were performed at liquid
145 nitrogen temperature.

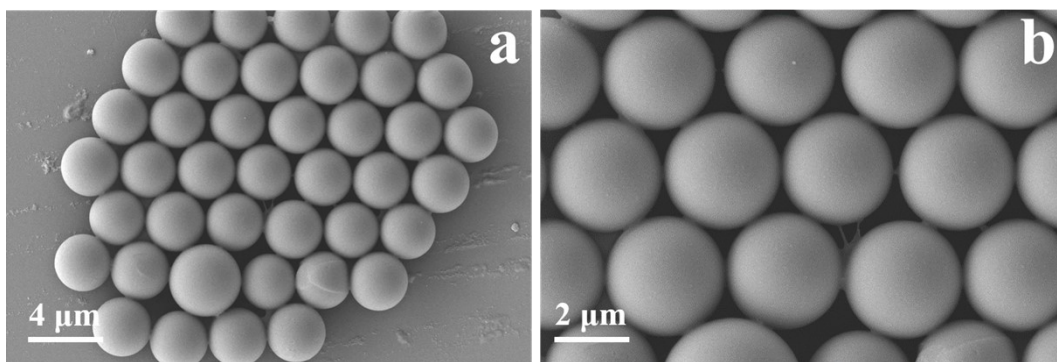


Fig. S1 SEM images of polystyrene seed.

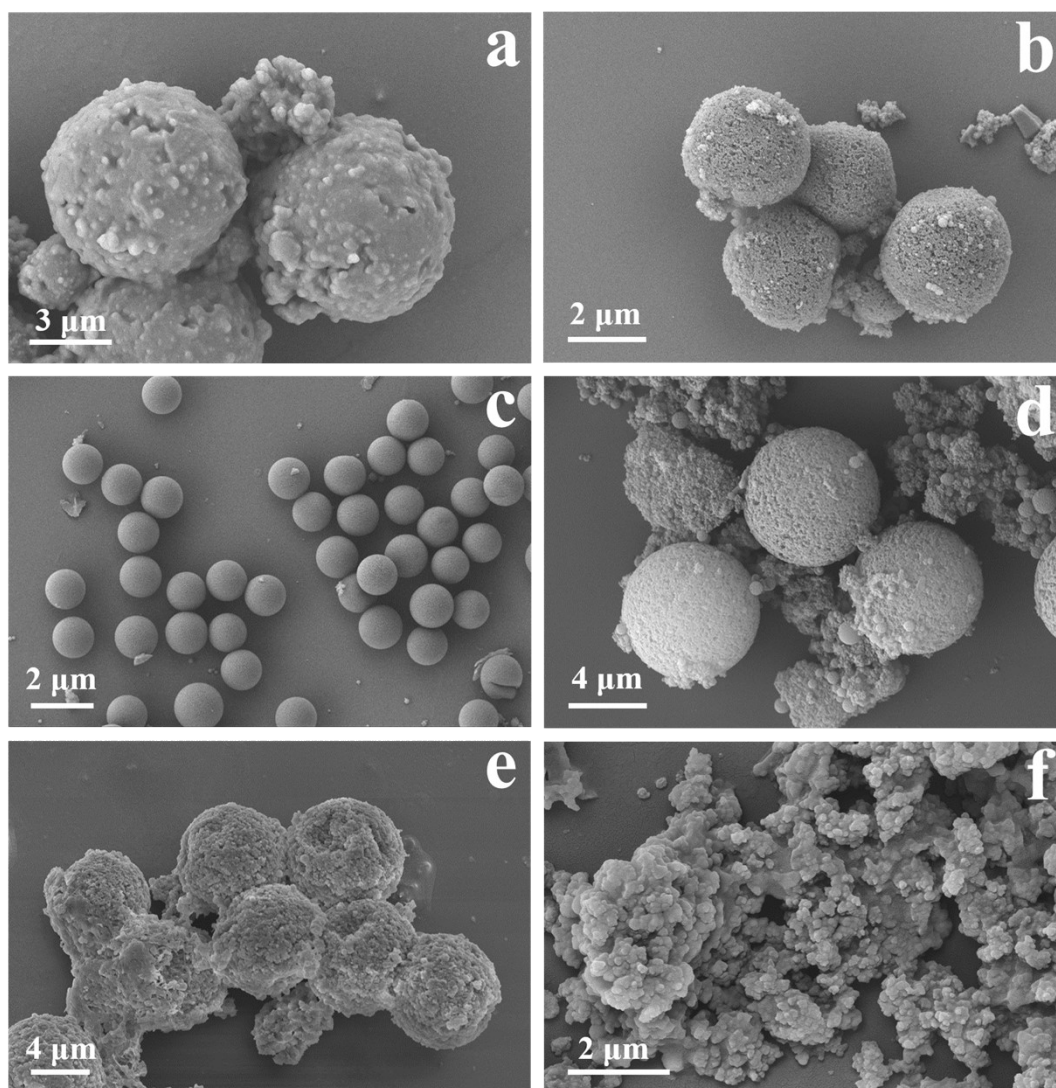


Fig. S2 SEM images of **(a)** PAD-2, **(b)** PAD-3, **(c)** PAD-4, **(d)** PAD-5, **(e)** PAD-7 and **(f)** PAD-8 fabricated with DBP and toluene as porogenic agents.

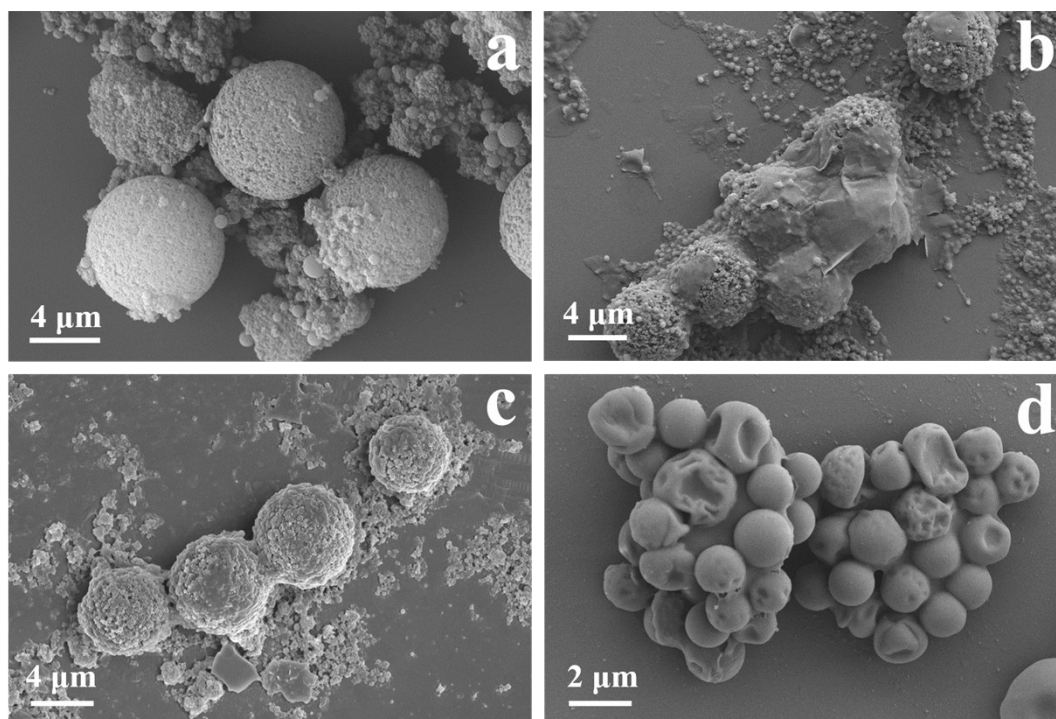


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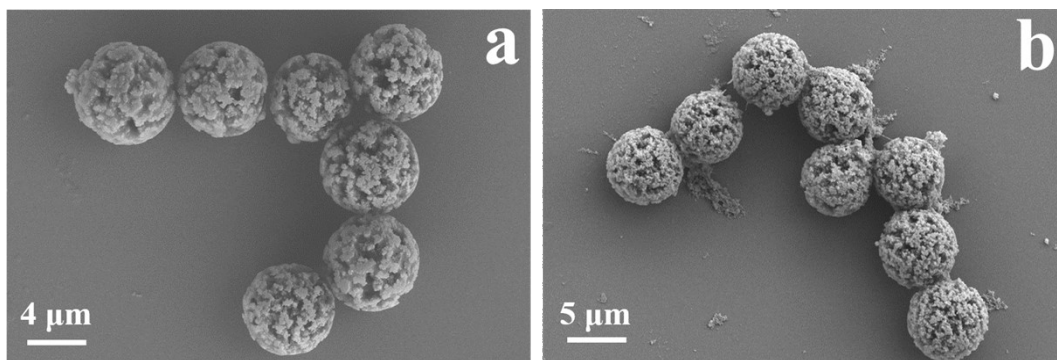


Fig. S4 SEM images of **(a)** PAD-15 and **(b)** PAD-16 with DBP and cyclohexanol as porogenic agents.

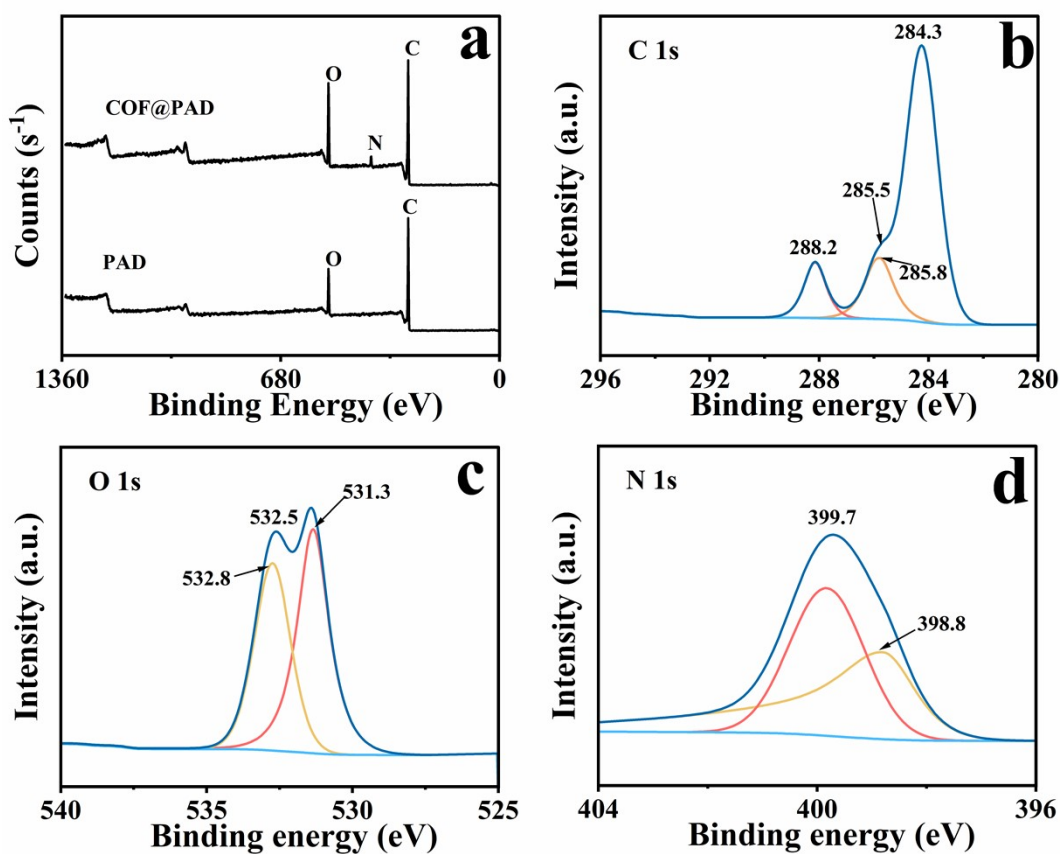


Fig. S5 (a) XPS spectra for PAD and PAD@COF. (b-d) C1s, O1s and N1s XPS spectra of PAD@COF.

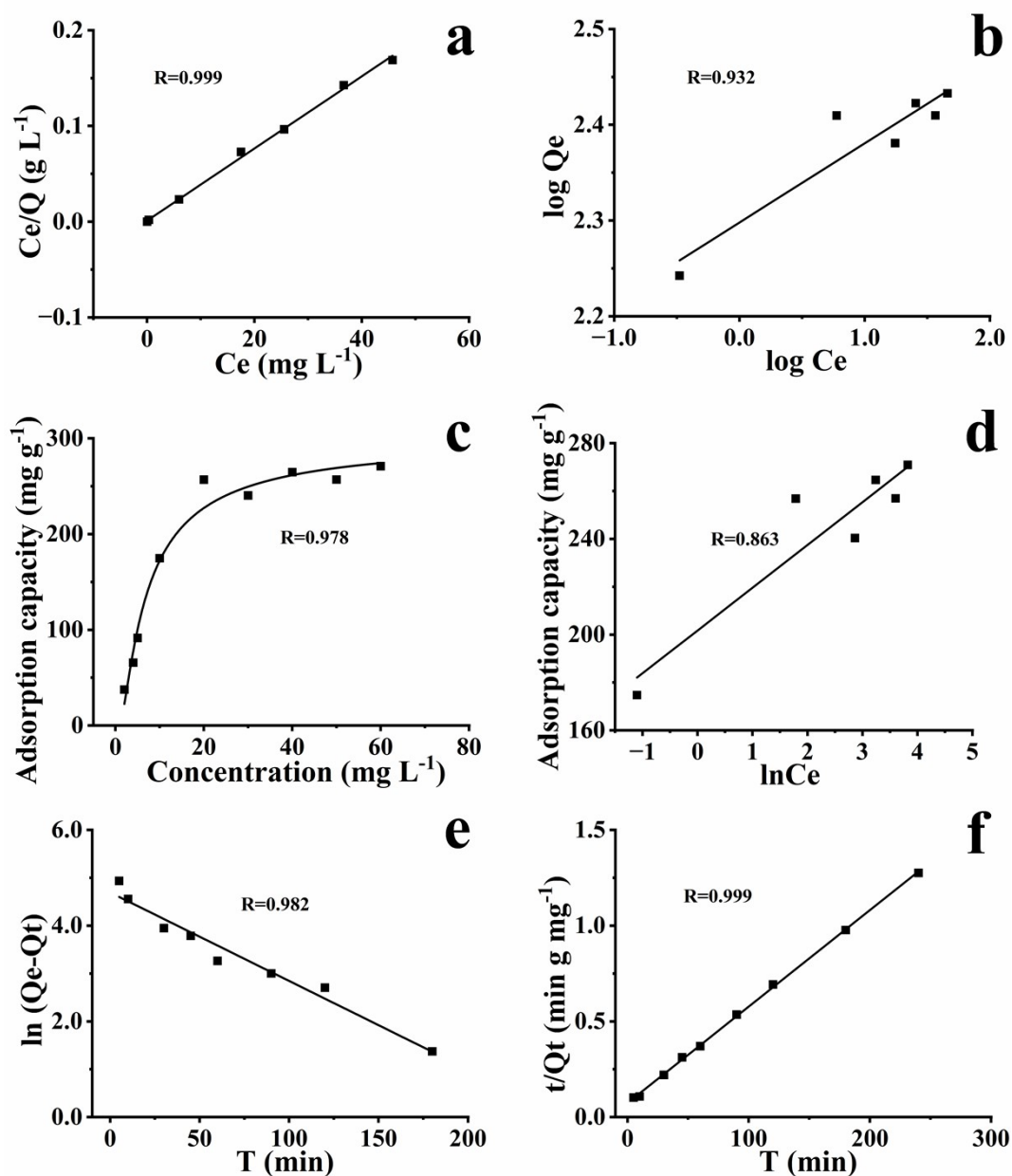


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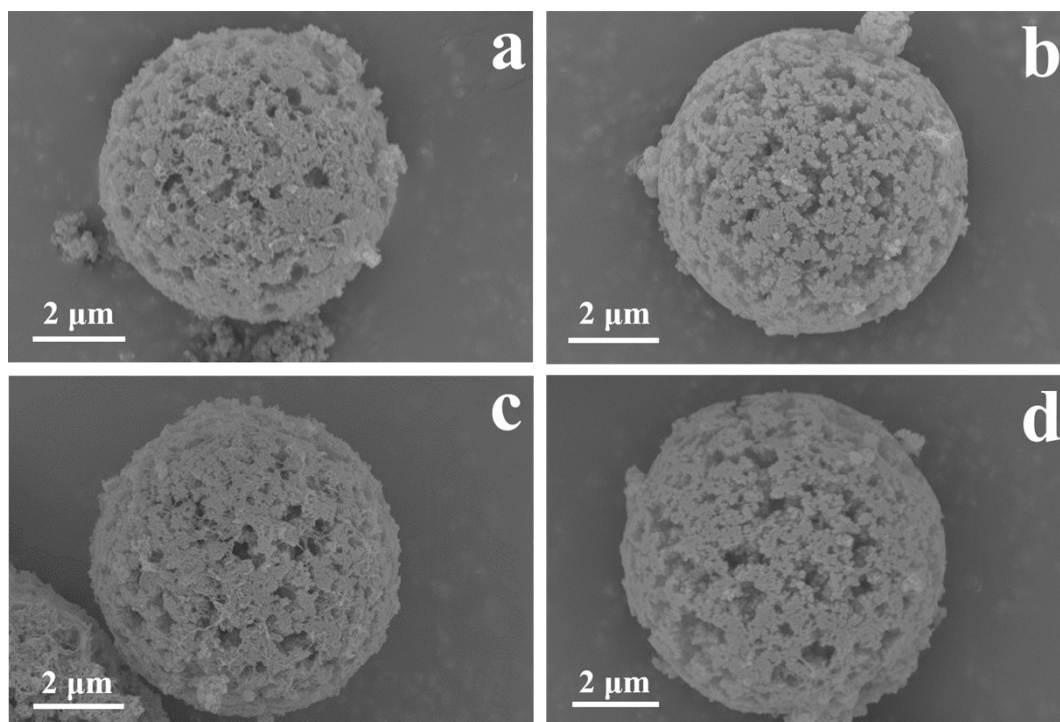


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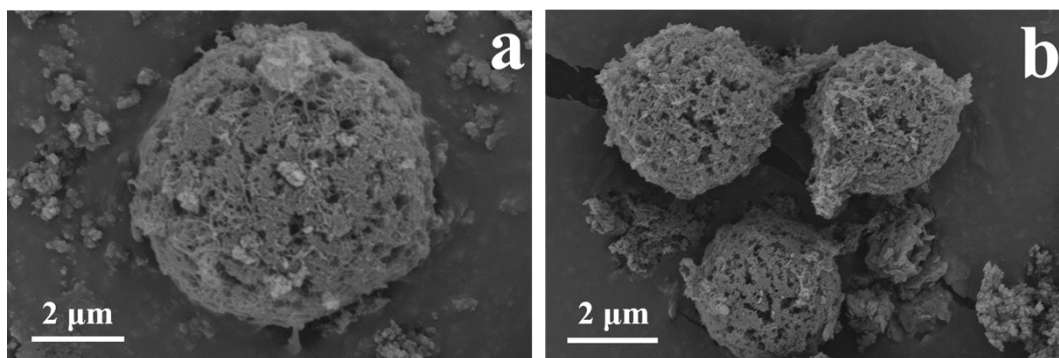


Fig. S8 SEM images of PAD@COF after grinding and high speed oscillation.

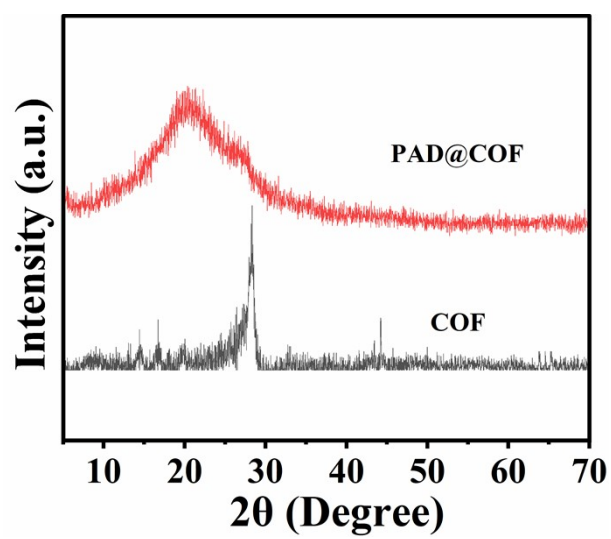


Fig. S9 PXRD patterns of COF and PAD@COF.

Table S1 The results of elemental analysis of materials

Sampled	C%	O%	N%
PAD	84.99	15.01	0
PAD@COF	75.64	20.72	3.65

Table S2 Adsorption isotherm models of Cu²⁺

Materials	Q _e (mg g ⁻¹)	Langmuir	Freundlich	Sips	Temkin
		R _L	R _F	R _S	R _T
PAD@COF	270.9	0.999	0.932	0.978	0.863

185 **Table S3** Kinetic parameters in pseudo-first-order and pseudo-second-order models of
 186 Cu^{2+}

Sample	Pseudo-first-order			Pseudo-second-order		
	k_1 (min^{-1})	$Q_{1\text{cal}}$ (mg g^{-1})	R	k_2 ($\text{g mg}^{-1} \text{min}^{-1}$)	$Q_{2\text{cal}}$ (mg g^{-1})	R
PAD@COF	0.0185	109.4	0.982	0.000345	198.4	0.999

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189 **Table S4** Specific surface area, pore size, and pore volume of PAD@COF and
 190 PAD@COF(10 cycles)

Materials	Specific surface area (m ² g ⁻¹)	Pore volume (cm ³ g ⁻¹)	Average pore diameter (nm)
PAD@COF	163.8	0.40	9.7
PAD@COF(10 cycles)	120.5	0.41	13.6

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