Supplementary Information:

Procedure for CO chemisorption:

Chemisorption experiments of carbon monoxide were conducted at 40°C utilising AutoChem 2950 Micromeritics apparatus. A 100 mg catalyst sample was introduced into a reactor and reduced with pure hydrogen for 30 minutes at 750 °C. The sample was subsequently cooled to 40°C in a helium flow.

The adsorption of CO was conducted via the pulse chemisorption method with a 10% CO/He gas mixture. The results were computed based on the assumption that the adsorption stoichiometry of CO/Ni is 1:1.

Catalyst (spent)	Surface Area (m ² g ⁻¹)	Pore volume (cm ³ g ⁻¹)	Pore size (nm)
Ni/SA	247	0.57	5.68
Ba-Ni/SA	221	0.53	5.68
La-Ni/SA	165	0.44	7.12
Ce-Ni/SA	212	0.52	6.22

Table S1: TableS1: Textural properties of spent catalysts

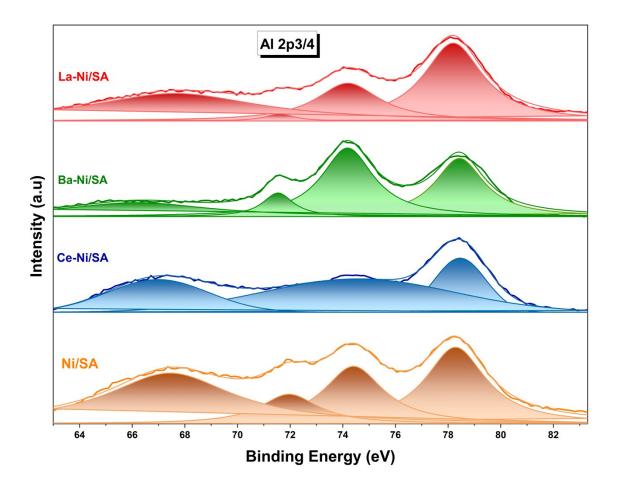


Figure S1: Al 2p XPS spectra of calcined X-Ni/SA catalysts

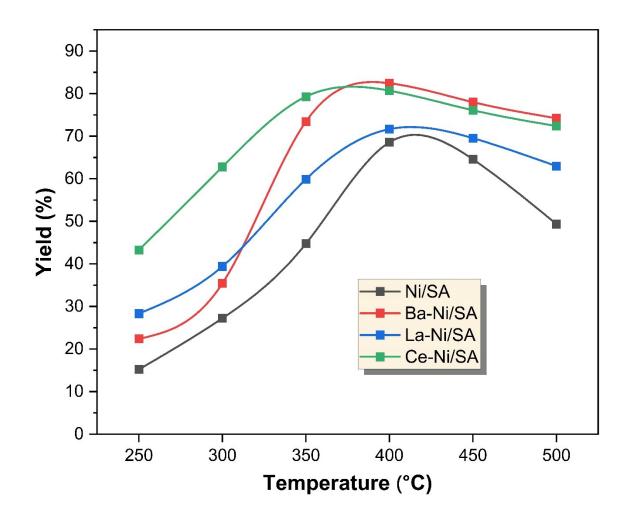


Figure S2: Product yield of X-Ni/SA catalysts; 1 atm, 250-500 °C, 12000 ml/g.h, H₂:CO₂=4/1

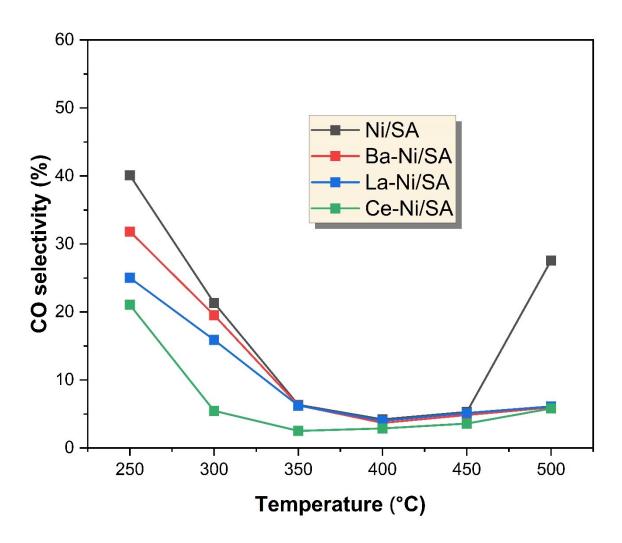
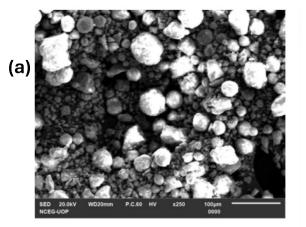
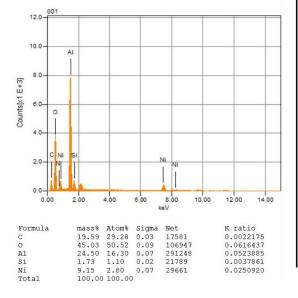


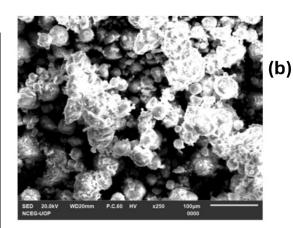
Figure S3: CO selectivity of X-Ni/SA catalysts; 1 atm, 250-500 °C, 12000 ml/g.h, H₂:CO₂=4/1

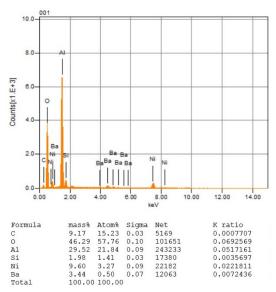
Sample	FWHM
	(rad)
Ni/SA	2.30
Ba-Ni/SA	1.98
La-Ni/SA	2.95
Ce-Ni/SA	2.87

Table S2: FWMH data for calcined sample to calculate crystal size using Scherrer equation









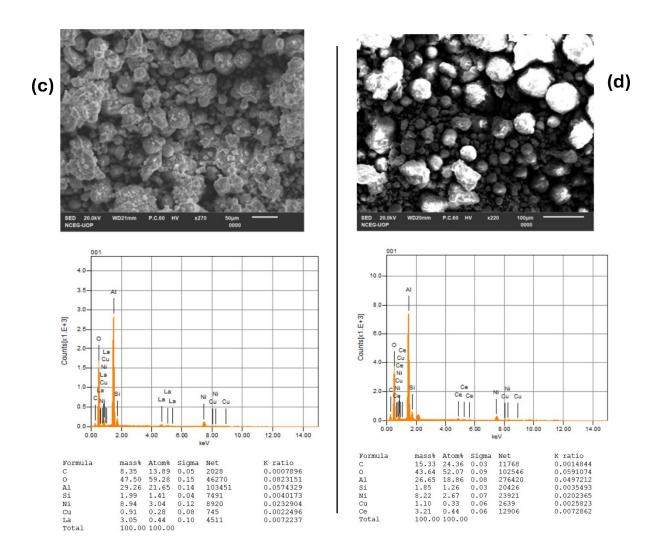
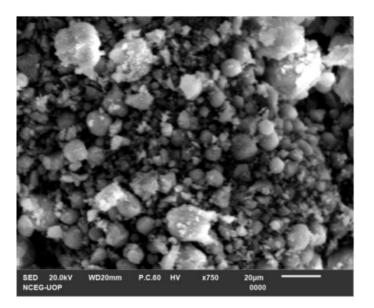


Figure S4: SEM & EDS of calcined samples (a) Ni/SA (b) Ba-Ni/SA (c) La-Ni/SA (d) Ce-Ni/SA



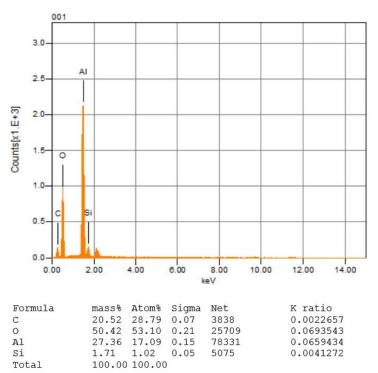


Figure S5: SEM & EDS of puree SA support

Catalyst	Metal particle Size (nm) ^a	Active metal area (m²/g) ª
Ni/SA	5.7	3.55
Ba-Ni/SA	7.3	2.77
La-Ni/SA	5.4	3.74
Ce-Ni/SA	5.1	3.98

^a Calculated from CO chemisorption analysis