

Supplementary Information

Acid-Functionalized PVA Composite Membranes for Pervaporation-Assisted Esterification

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1. Technical Data Sheet of commercial pervaporation membranes

Table S1 Technical Data Sheet of pervaporation membranes,
provided by DeltaMem AG

Membrane type	PERVAP™ 4100
Typical application	Standard membrane, developed for most dehydration of volatile organic mixtures
Feed temperature	Max. short term operating temperature – 105 °C
Feed pressure	Above the feed vapor pressure, typically up to 4 bar
Melting point	Typical operating pH range: 5-8, operation outside these pH values – acceptable in some cases
Compatibility with chemicals	Fully compatible with: alcohols, ether (including cyclic ethers), acetates / esters, ketones, hydrocarbons, acetonitrile Conditionally compatible with: aldehydes and derivatives <30ppm (as acetaldehyde), organic acids <0.1 % w/w, acetals / ketals, special solvents (DMF, DMSO, NMP, DMAc <0.1 % w/w Not compatible with amines (e.g. MMA) <500 ppm, mineral acids and peroxides

2. General procedure for the batch-wise synthesis of ionic liquids

Both ionic liquids were synthesized based on the procedure described by Liu et. al.¹

- (1) Liu, L. K.; Deng, J. H.; Guo, Y. M. Synthesis of Coumarin Derivatives in a Microfluidic Flow System Employing the Pechmann Condensation: A Case Study. *J. Chinese Chem. Soc.* **2020**, *67* (12), 2208–2215.
<https://doi.org/10.1002/jccs.202000371>.

Synthesis procedure for 3-(4-sulfonyl)-1-vinyl-imidazolium hydrogen sulfate (IL1) and of 3-(4-sulfonyl)-1-vinyl-imidazolium bromide (IL2)

1-vinylimidazole (0.12 mol) and 1, 4-butanedisulfone (0.12 mol) were mixed in a 250 mL round bottom flask and dissolved in 60 mL of acetonitrile. The mixture was stirred at 42-45°C for 16 h. The solvent was removed, and white solid zwitterion was washed repeatedly with ether to remove non-ionic residues, filtrated through a Buchner funnel and dried in vacuum for 4h. A stoichiometric amount (0.12 mol) of HSO₄ (for IL1 synthesis) or HBr (for IL2 synthesis) was added dropwise, the mixture was stirred for 6h at 80°C. The viscous liquid was washed three times with ether and dried in vacuum to form IL-1.

3. Calculations of membrane pervaporation performance

To evaluate the membrane separation performance, the two main parameters were considered: membrane flux J , partial flux of component i and separation factor α_i . They can be described with Equations (S1-S3):

$$J = \frac{m}{A \cdot t} \quad (S1)$$

Where
e J is
mem
brane
flux

[g·m⁻²·h⁻¹], m stands for the mass of collected permeate [g], t is pervaporation time [h] and A stands for the effective area of a membrane (0.006793 m²). For component i , partial flux J_i is described by the following equation:

$$J_i = J \times \omega_i^P \quad (S2)$$

where ω_i^P is the weight fraction of component i in permeate.

Separation factor α_i for a given compound i can be defined as:

$$\alpha_i = \frac{\omega_i^P / (1 - \omega_i^P)}{\omega_i^F / (1 - \omega_i^F)} \quad (S3)$$

Where ω_i^P stands for weight fraction of the component i in permeate and ω_i^F is weight fraction of the compound i in feed.

The enrichment factor β_i , calculated from Equation (S4) indicates the degree to which component i (of greater permeability), is enriched.

$$\beta_i = \frac{\omega_i^P}{\omega_i^F} \quad (S4)$$

4. F

ull ¹H NMR spectra of IL1, IL2 and neat PVA

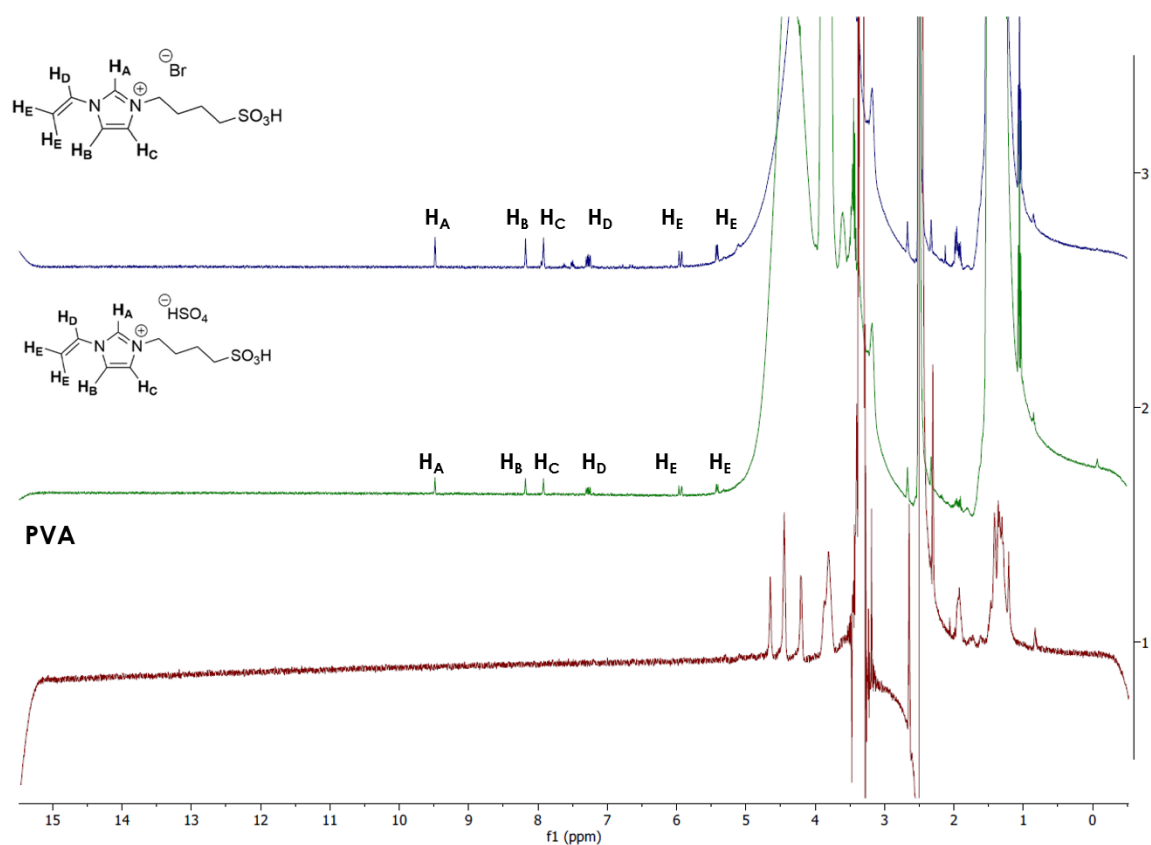


Fig. S1 Full ^1H NMR spectra of PVA/IL1(top),
PVA/IL2 (middle) and neat PVA (bottom)

The assignment of signals characteristic for ILs, according to the markers in Fig. S1 is as follows: 9.49 (1H, s, H_A), 8.19 (1H, s, H_B), 7.93 (1H, s, H_C), 7.31 (1H, m, H_D), 5.93 (1H, m, H_E), 4.63 (1H, m, H_E).

5. FT-IR spectra of coated membranes before and after pervaporation test

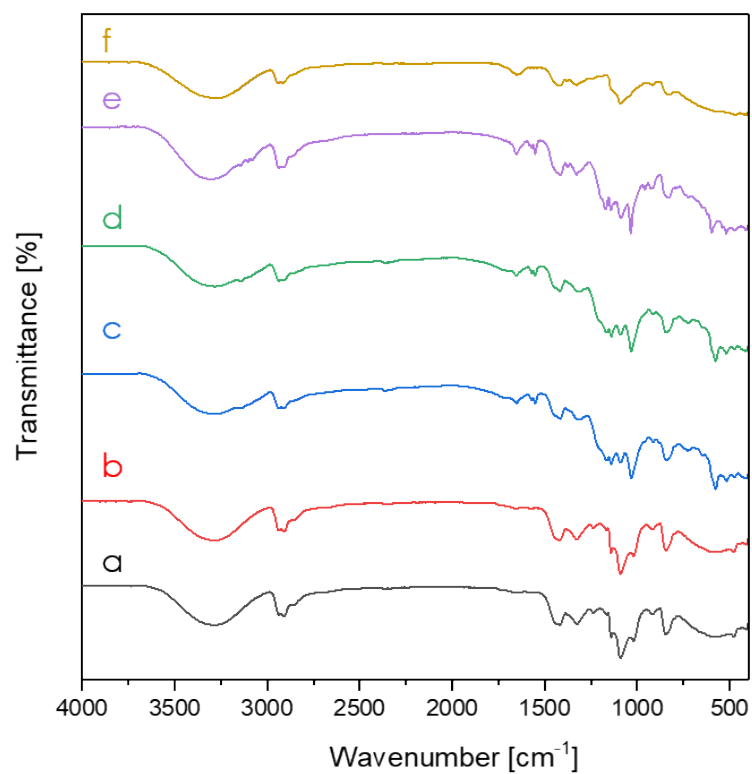


Fig. S2 FT-IR spectra of composite membranes, coated with PVA (a,b), PVA/IL1 (c,d), PVA/IL2 (e,f) before (a,c,e) and after (b,d,f) pervaporation test.

6. ^1H NMR spectra of the supernatant after catalyst leaching tests

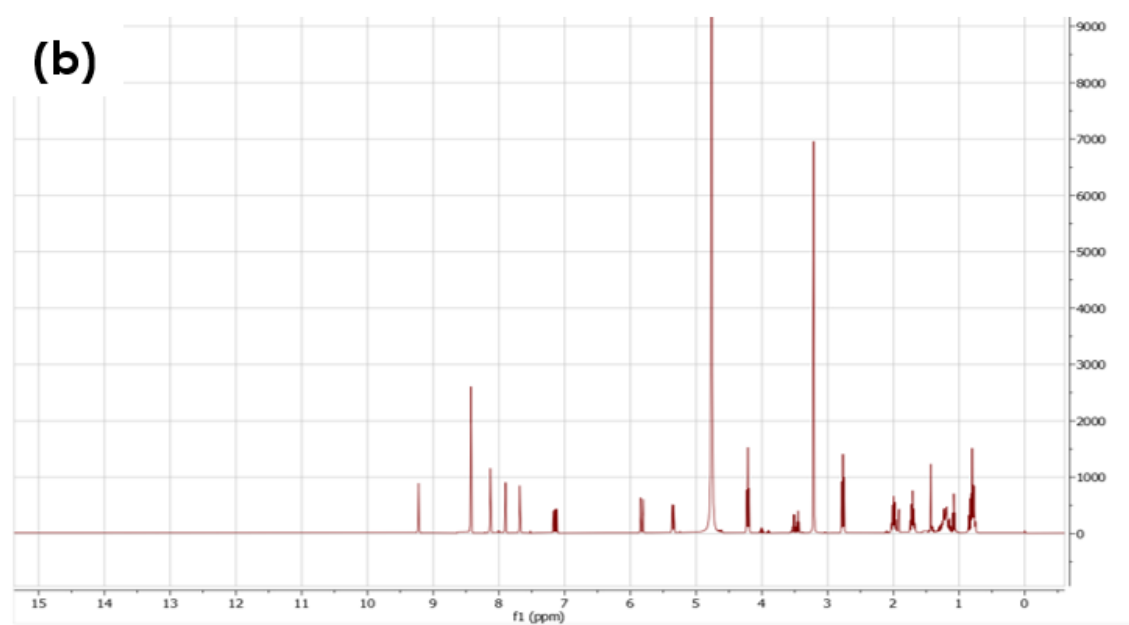
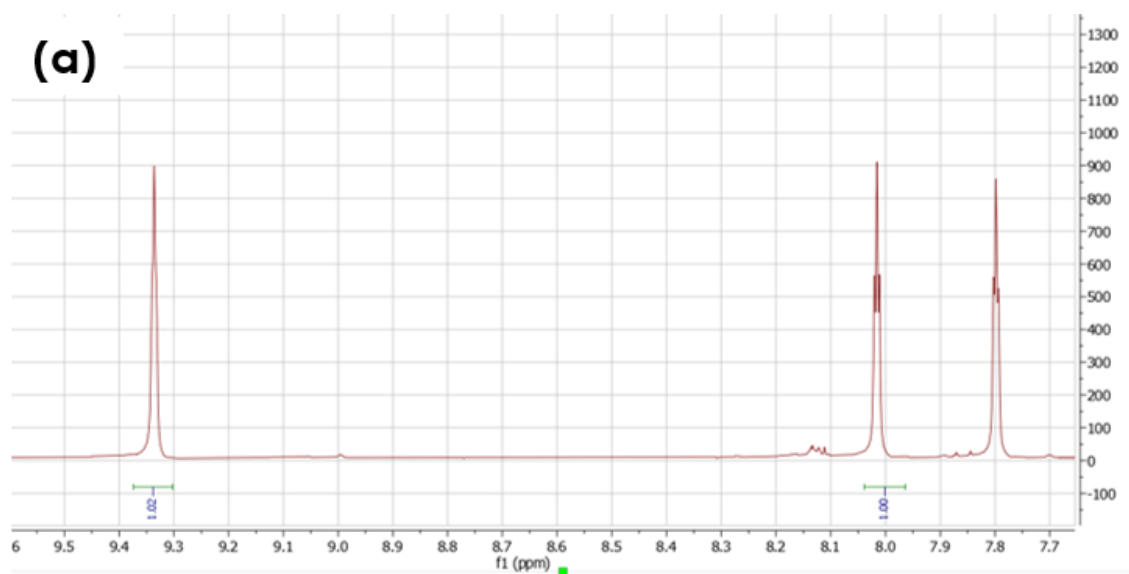


Fig. S3 ^1H NMR spectra of supernatant after the leaching tests with PVA/IL1-coated (a) and PVA/IL2-coated (b) membranes.