

Electronic Supplementary Information

**Redox regulation of Ni hydroxides with controllable phase composition towards biomass-derived polyol electro-refinery**

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## Experimental Section

### Chemicals

Ni foam (NF, 1.5 mm thickness, 70 pores per inch) was purchased from Suzhou Taili Material Co., Ltd. Nickel sulfate hexahydrate ( $\text{NiSO}_4 \cdot 6\text{H}_2\text{O}$ , 98.5%), sodium sulfate ( $\text{Na}_2\text{SO}_4$ , 99.0%), potassium hydroxide (KOH, 85.0%), formic acid (FA, 98.0%), glycolic acid (GA, 98.0%), acetic acid (AA, 99.5%), ethylene glycol (EG, 99.0%) and mannitol (MAN, 98.0%) were acquired from Sinopharm Chemical Reagent Co., Ltd. Glycerol (GLY, 99.0%), glyceric acid (GLA, 20 wt% in water) and 1,3-propylene glycol (1,3-PG, 98.0%) were obtained from Aladdin. Tartronic acid (TA, 98.0%), 1,2-propylene glycol (1,2-PG, 99.0%), malonic acid (MA, 99.0%) and Xylitol (XYL, 99.0%) were purchased from Adamas-beta. 3-hydroxypropionic acid (3-HPA, ~30 wt% in water), erythritol (ERY, 97.0%) were obtained from Bidepharm Co., Ltd.

### Preparation of catalysts

$\text{Ni}(\text{OH})_2@\text{NFs-}E$  were prepared by a facile and simple electrodeposition method with a three-electrode configuration (' $E$ ' represents the cathodic potential applied during the electrodeposition).  $1.5 \times 1.0 \text{ cm}^2$  Ni foam was ultrasonicated for 60 min in anhydrous ethanol and rinsed by deionized water in advance, which was used as the working electrode subsequently. Pt foil and Ag/AgCl (saturated KCl) were applied as the counter and reference electrode, respectively. The electrodeposition was carried out under constant potential (vs. Ag/AgCl) for 600 s in the electrolyte containing 1 M  $\text{Na}_2\text{SO}_4$  and 0.1 M  $\text{NiSO}_4$ . The as-prepared  $\text{Ni}(\text{OH})_2@\text{NFs-}E$  were cleaned by deionized water before further characterization and electrochemical measurement.

## **Physical Characterization**

Scanning electron microscopy (SEM) images were obtained by a Zeiss Gemini 300 with a 3.0 kV accelerating voltage. Transmission electron microscopy (TEM) and high-resolution TEM patterns were acquired by a Tecnai G2 F30 FEI. X-ray diffraction (XRD) was carried out on a Bruker D2 with Cu-K $\alpha$  radiation at 10 kV and 30 mA with a  $2\theta$  scanning range of  $10^\circ$  to  $100^\circ$ . Attenuated total reflectance-Fourier transform infrared spectroscopy (ATR-FTIR) experiments were conducted by a Spectrum Two Spectrometer (PerkinElmer) using a diamond ATR detector. X-ray photoelectron spectroscopy (XPS) data were recorded on a Thermo Scientific K-Alpha equipped with Al K $\alpha$  radiation. H<sub>2</sub> temperature programmed reduction (H<sub>2</sub>-TPR) experiments were performed on a Micromeritics AutoChem II 2920 at the heating rate of 5 K/min from 313 to 873 K under the flow of 5% H<sub>2</sub>/Ar. Inductively coupled plasma-atomic emission spectrometry (ICP-AES) was carried out on a PE-8000 instrument to evaluate the metal species in the electrolyte after GOR.

## **Electrochemical measurement**

All of the electrochemical measurements were conducted on a typical three-electrode setup with a CHI760E electrochemical workstation, which was divided by proton exchange membrane (Nafion 117). The as-prepared Ni(OH)<sub>2</sub>@NFs-*E* with geometric area of 1.0 $\times$ 1.0 cm<sup>2</sup> were used as the working electrode, while Pt foil and Ag/AgCl (saturated KCl) presented to be the counter and reference electrode respectively. Cathode chamber was filled with 6 mL of 1 M KOH and anode chamber was filled with 6 mL of 1 M KOH with or without certain concentration of substrate. Specifically, LSV

and CV measurements were performed at the scan rate of 5 mV/s and 2 mV/s. It should be noticed that LSV curves in this report were not compensated with any  $iR$ -correction at the aim of presenting a holistic characterization without manipulation. GOR performance of the catalysts was evaluated by chronoamperometry (CA) method in the reactor mentioned above under vigorous stirring. The potentials measured throughout this work ( $E_{\text{Ag/AgCl}}$ ) could be converted to the RHE scale ( $E_{\text{RHE}}$ ) according to the Nernst equation:<sup>1</sup>

$$E_{\text{RHE}} = E_{\text{Ag/AgCl}} + 0.059 \times \text{pH} + 0.198$$

Calculation of turnover frequency (TOF) values for  $\text{Ni(OH)}_2@\text{NFs-E}$  in GOR were based on the following equation:<sup>2-4</sup>

$$\text{TOF} = (j \times N_{\text{A}}) / (n \times F \times \Gamma)$$

Where  $j$  represents the current density ( $\text{A}/\text{cm}^2$ ) measured by LSV,  $N_{\text{A}}$  is the Avogadro constant,  $n$  stands for the transferred electron number for GOR to produce FA ( $8 e^-$ ),  $F$  is the Faradaic constant ( $96485 \text{ C}/\text{mol}$ ).  $\Gamma$  is the number of participating active sites for the catalysts, which considers all loaded  $\text{Ni(OH)}_2$  over NF (measured by  $\text{H}_2$ -TPR) in this work. Electrochemically active surface areas (ECSA) of  $\text{Ni(OH)}_2@\text{NFs-E}$  were evaluated by measuring the double-layer capacitance ( $C_{\text{dl}}$ ) at various CV scan rates in the non-faradaic region. *In-situ* Raman spectroscopy was performed on a typical Raman micro-spectrometer (Horiba HR-800) combined with a three-electrode setup and a CHI760E electrochemical workstation. The corresponding Raman spectra were recorded during the CA tests at various potentials and constant time.

### **Product analysis**

The liquid products within the anolyte were separated and analyzed by high performance liquid chromatography (HPLC) equipped with a Bio-Rad Aminex HPX-87H column at 35°C using 8.0 mM H<sub>2</sub>SO<sub>4</sub> aqueous solution as mobile phase under the flow of 0.6 mL/min and detected by a refractive index detector (RID). Calibration curves of standard samples with certain concentrations were established in order to conduct the quantitative analysis of reaction substrates and corresponding oxidation products. The conversion of various substrates, yield and selectivity of formic acid as well as faradaic efficiency were determined by the following equations:

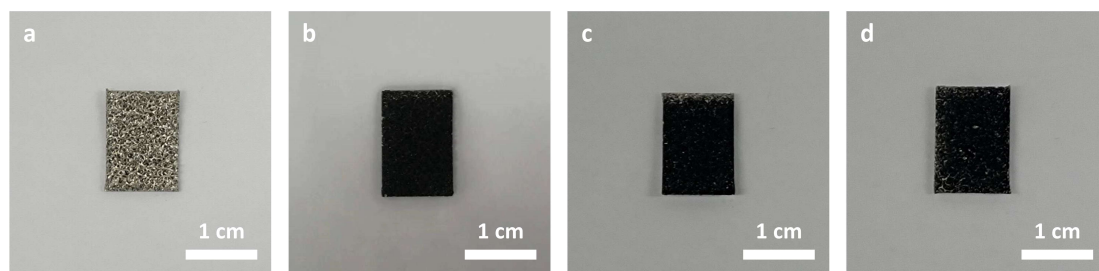
$$\text{Conversion (\%)} = \frac{N(\text{Glycerol Consumed})}{N(\text{Initial Glycerol})} \times 100\%$$

$$\text{Yield (\%)} = \frac{N(\text{Formic Acid Formation})}{3 \times N(\text{Initial Glycerol})} \times 100\%$$

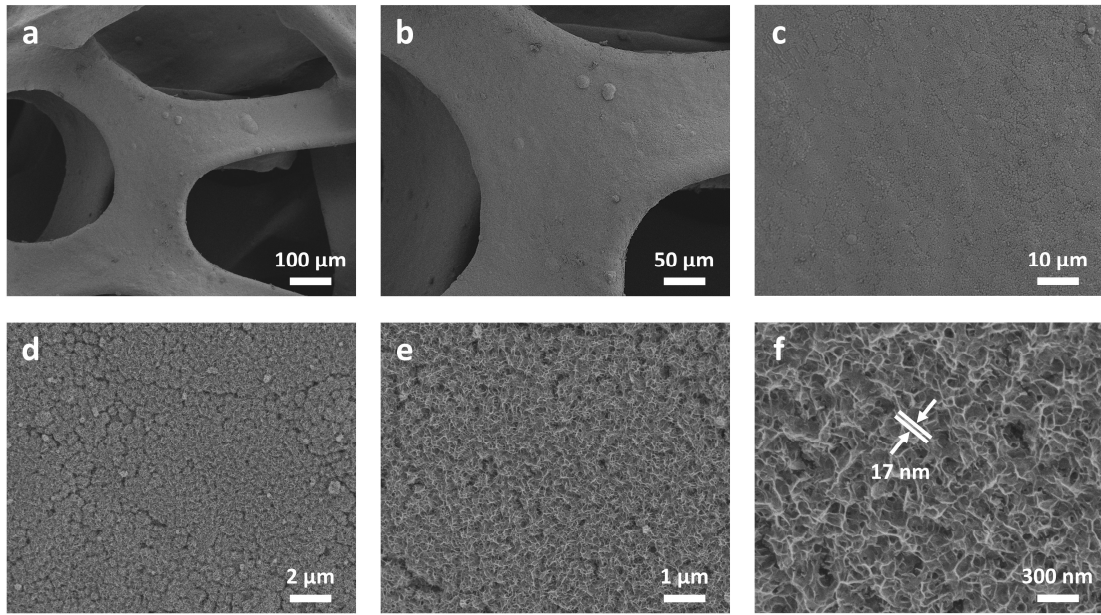
$$\text{Selectivity (\%)} = \frac{N(\text{Formic Acid Formation})}{3 \times N(\text{Glycerol Consumed})} \times 100\%$$

$$\text{Faradaic Efficiency (\%)} = \frac{N(\text{Formic Acid Formation})}{Q_{\text{total}} / (Z \times F)} \times 100\%$$

Where 'Z' represents the number of electrons transferred to produce per mole of formic acid (Z = 8/3 for glycerol, Z = 3 for ethylene glycol, Z = 5/2 for erythritol, Z = 12/5 for xylitol and Z = 7/3 for mannitol).

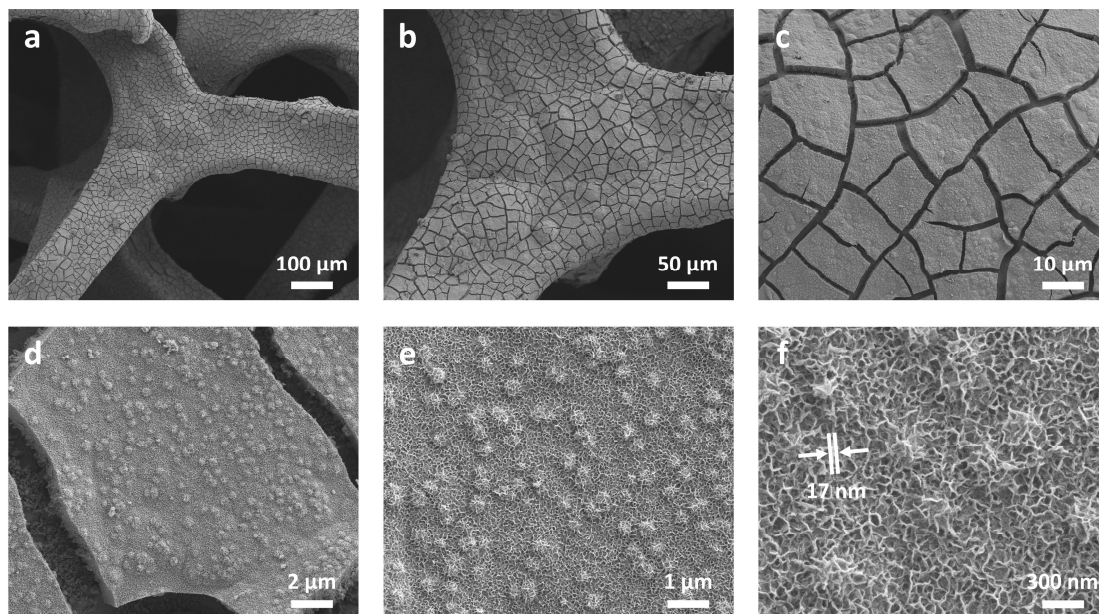


**Figure S1.** Digital graphs of the as-synthesized catalysts. a) Bare NF, b) Ni(OH)<sub>2</sub>@NF-0.9, c) Ni(OH)<sub>2</sub>@NF-1.0 and d) Ni(OH)<sub>2</sub>@NF-1.2.

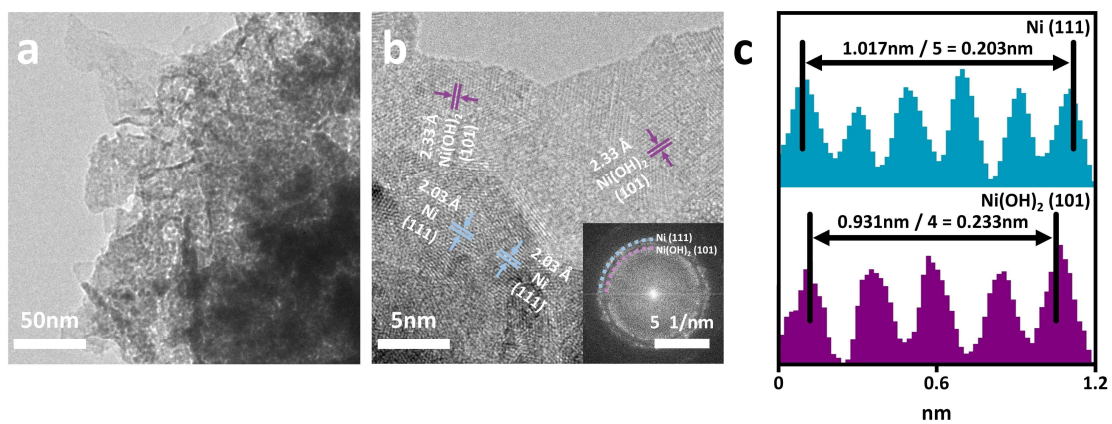


**Figure S2.** SEM images of Ni(OH)<sub>2</sub>@NF-0.9.

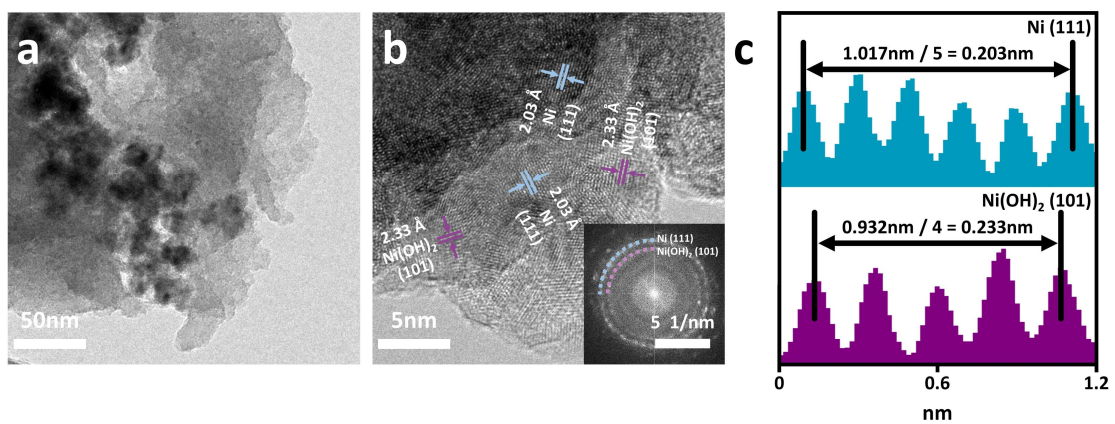




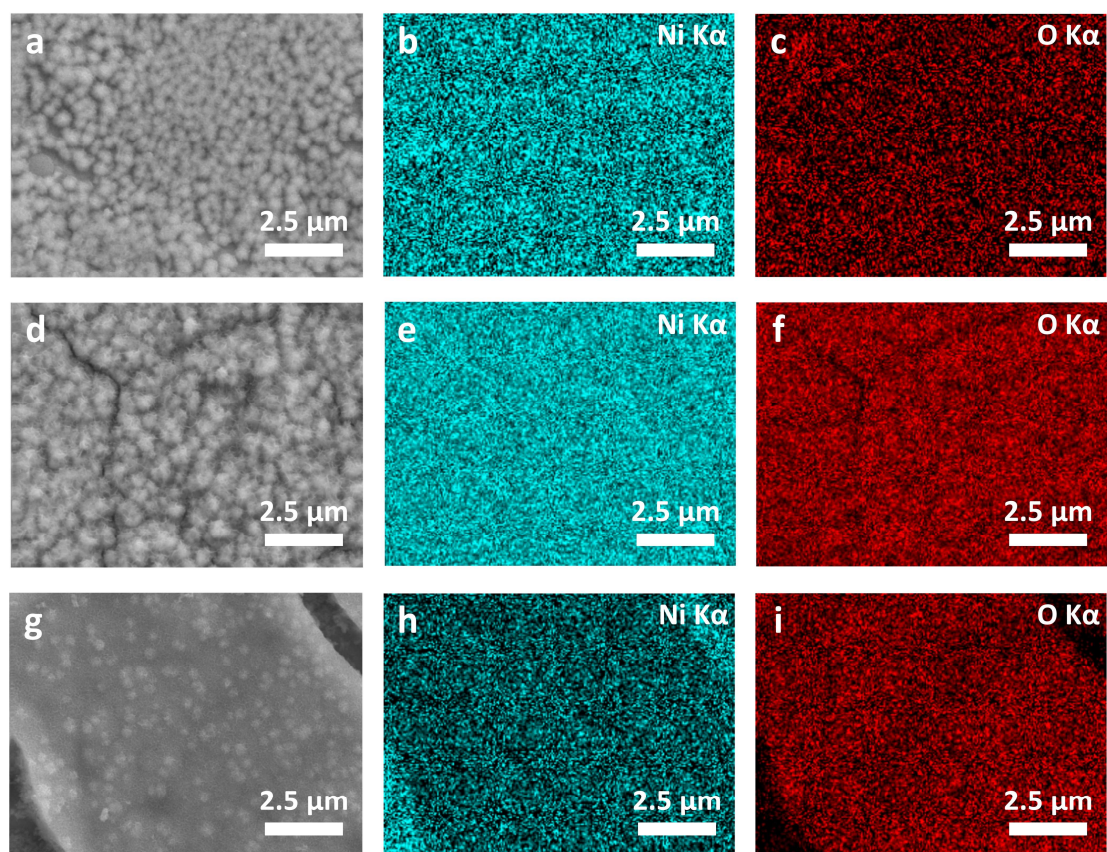
**Figure S3.** SEM images of Ni(OH)<sub>2</sub>@NF-1.2.



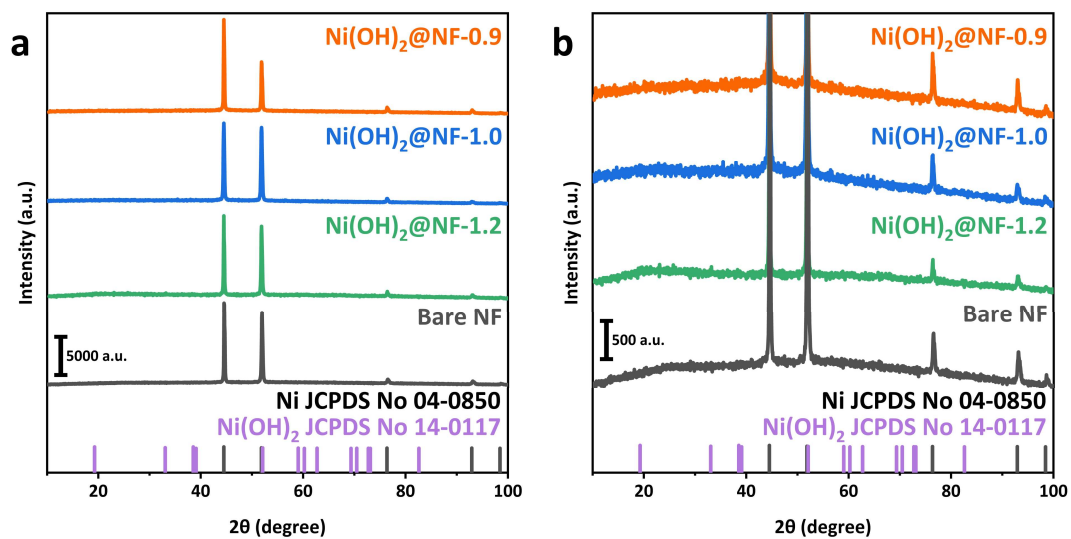
**Figure S4.** a-b) TEM images of Ni(OH)<sub>2</sub>@NF-0.9 (inset: Reduced FFT images of HR-TEM). c) Line scan measurements of HR-TEM images.



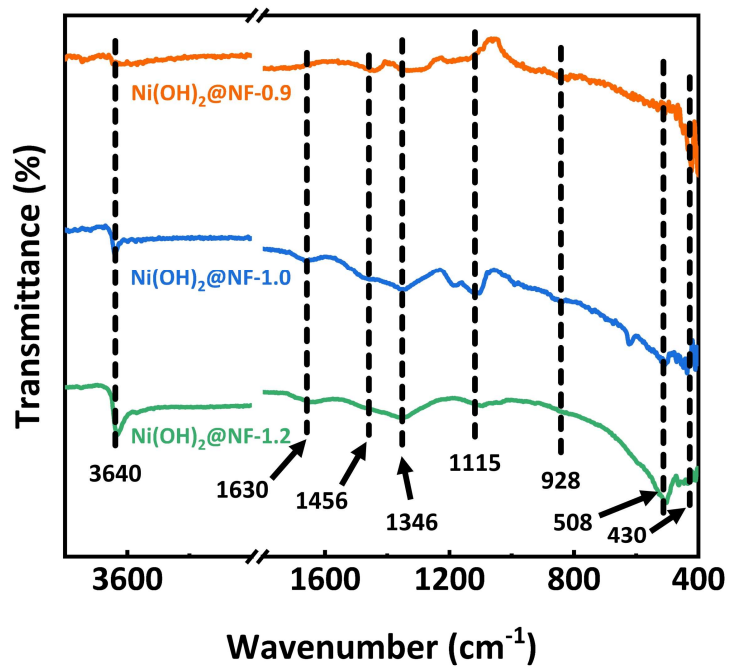
**Figure S5.** a-b) TEM images of Ni(OH)<sub>2</sub>@NF-1.2 (inset: Reduced FFT images of HR-TEM). c) Line scan measurements of HR-TEM images.



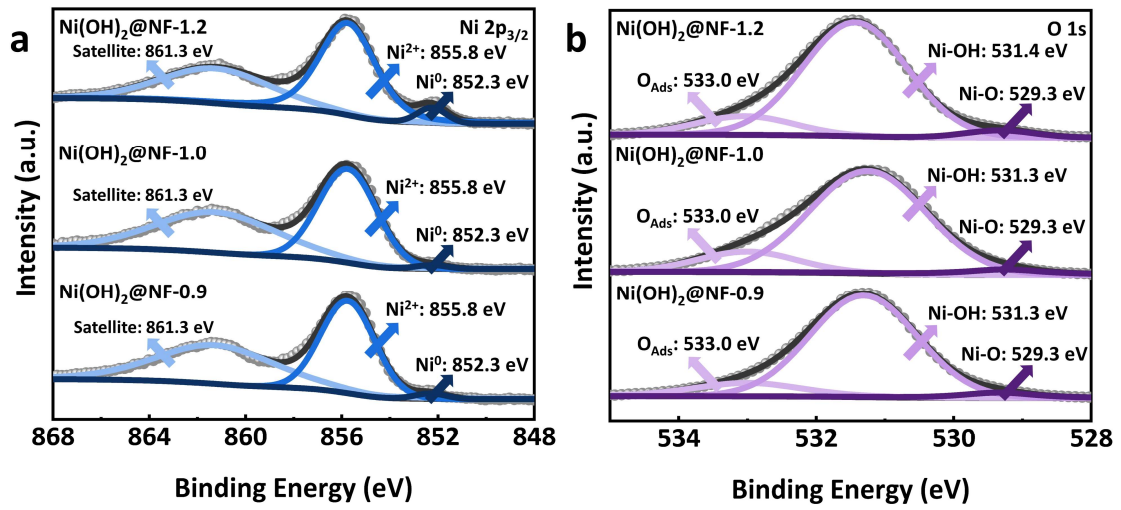
**Figure S6.** SEM-EDS mapping of a-c) Ni(OH)<sub>2</sub>@NF-0.9. d-f) Ni(OH)<sub>2</sub>@NF-1.0. g-i) Ni(OH)<sub>2</sub>@NF-1.2.



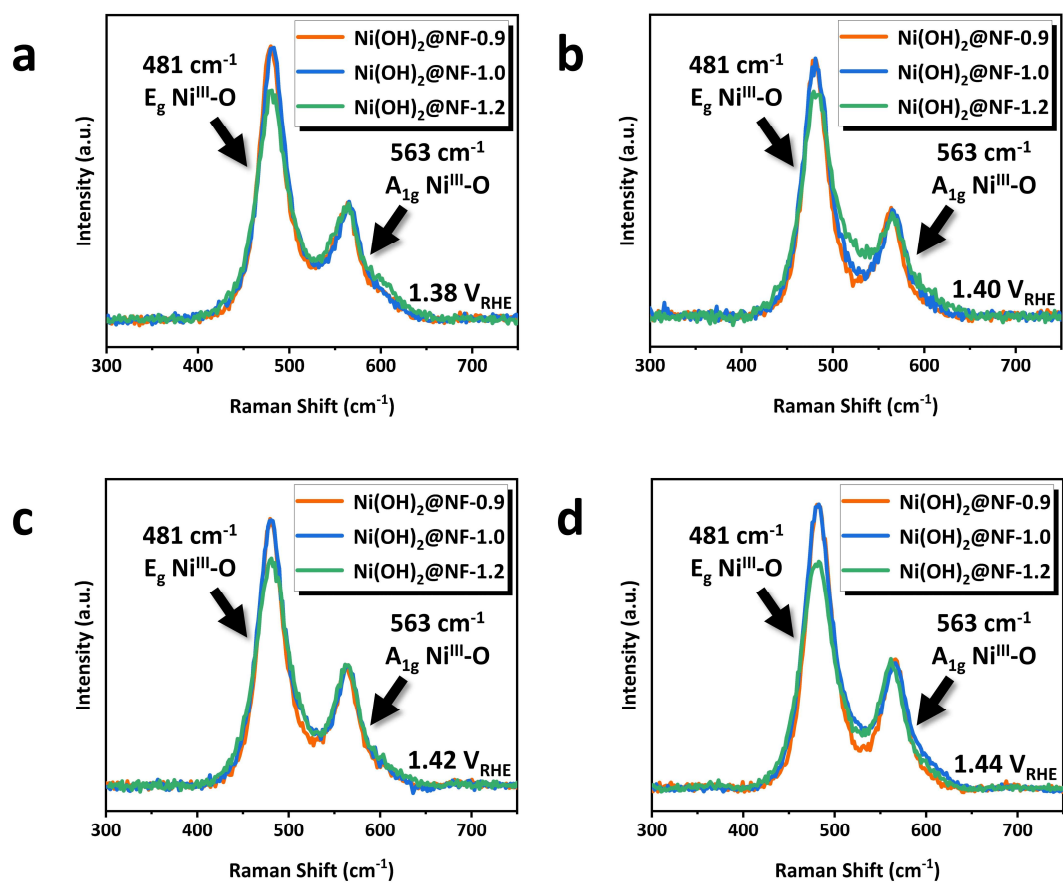
**Figure S7.** a) XRD patterns of Bare NF and Ni(OH)<sub>2</sub>@NFs-E. b) Enlarged XRD patterns of Bare NF and Ni(OH)<sub>2</sub>@NFs-E.



**Figure S8.** ATR-FTIR spectra of Ni(OH)<sub>2</sub>@NFs-*E*.

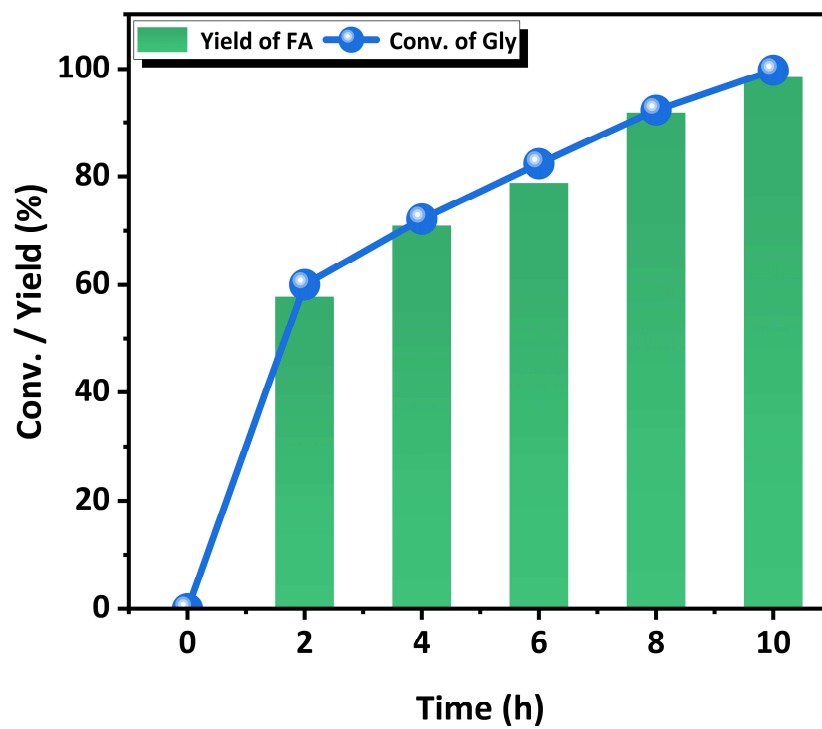


**Figure S9.** a) Ni 2p<sub>3/2</sub> and b) O 1s XPS spectra of Ni(OH)<sub>2</sub>@NFs-*E*.

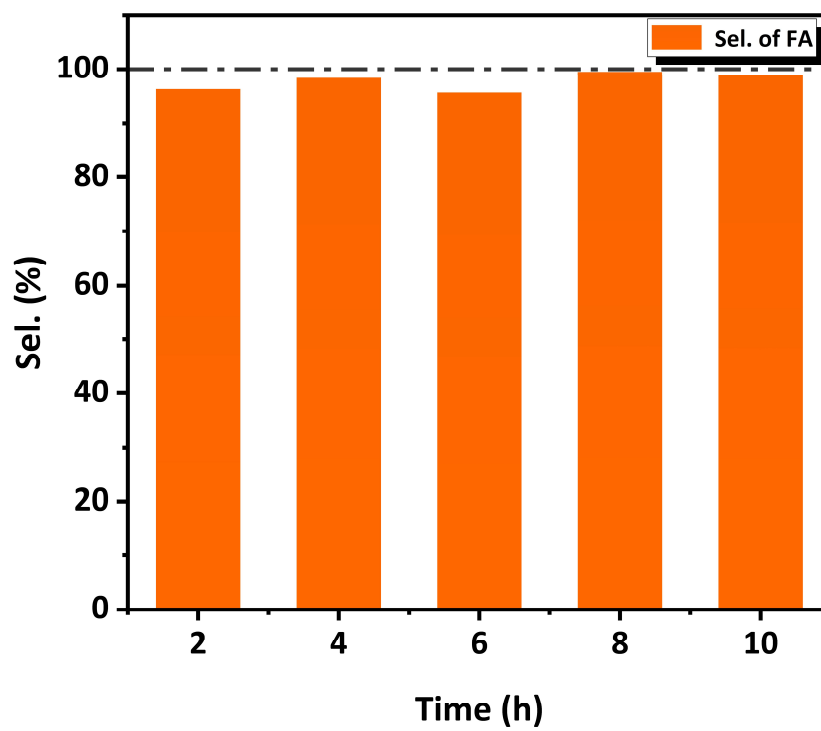


**Figure S10.** Detailed comparison of the intensity ratio of Ni<sup>III</sup>-O bands centered at 481 and 563 cm<sup>-1</sup> from *in-situ* Raman spectra at various potentials for Ni(OH)<sub>2</sub>@NFs-*E*.

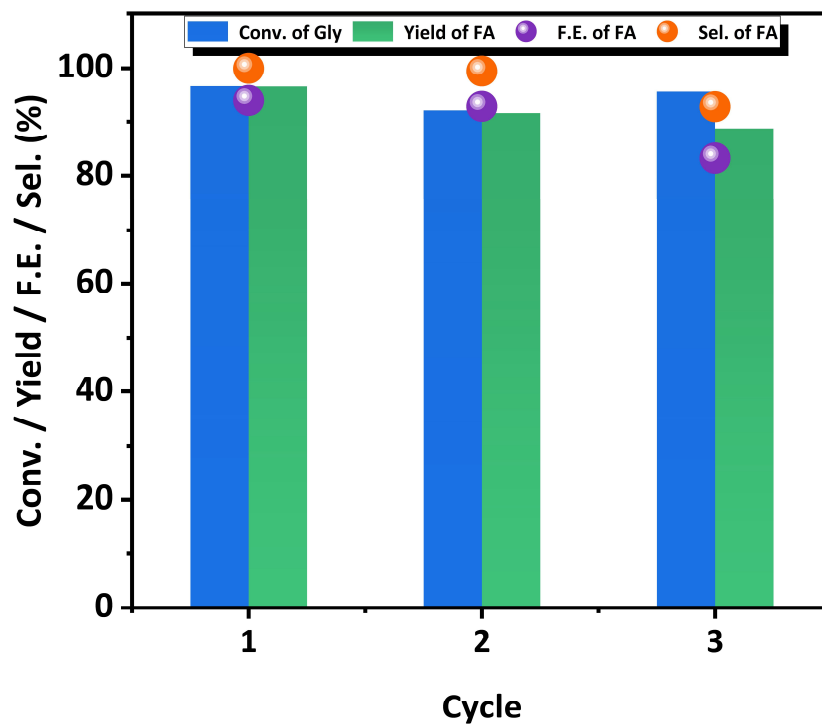




**Figure S11.** The evolution of GLY conversion and FA yield over Ni(OH)<sub>2</sub>@NF-1.0 as a function of time.

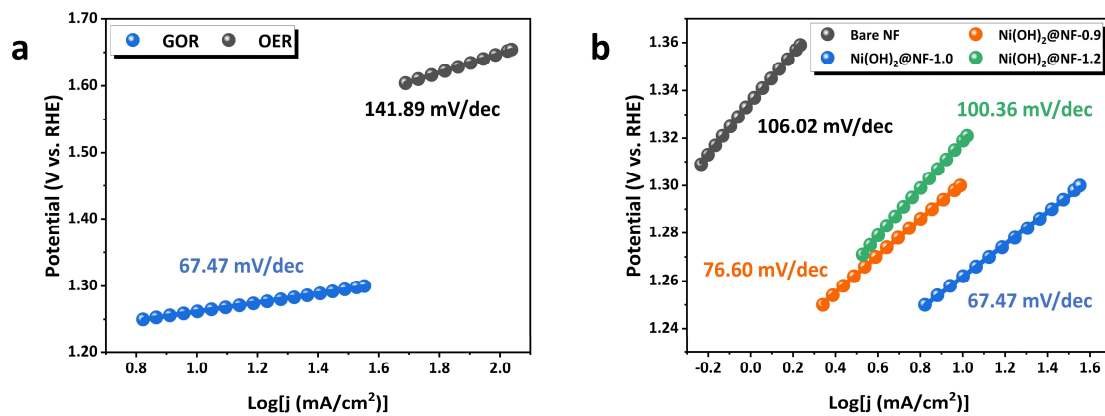


**Figure S12.** FA selectivity during GOR process over Ni(OH)<sub>2</sub>@NF-1.0.

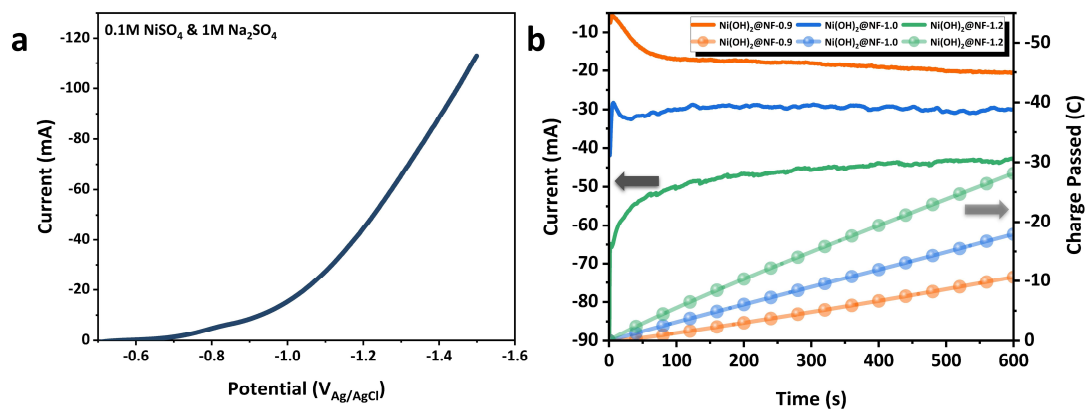


**Figure S13.** Three successive long-term electrolysis (30 h in total) over Ni(OH)<sub>2</sub>@NF-

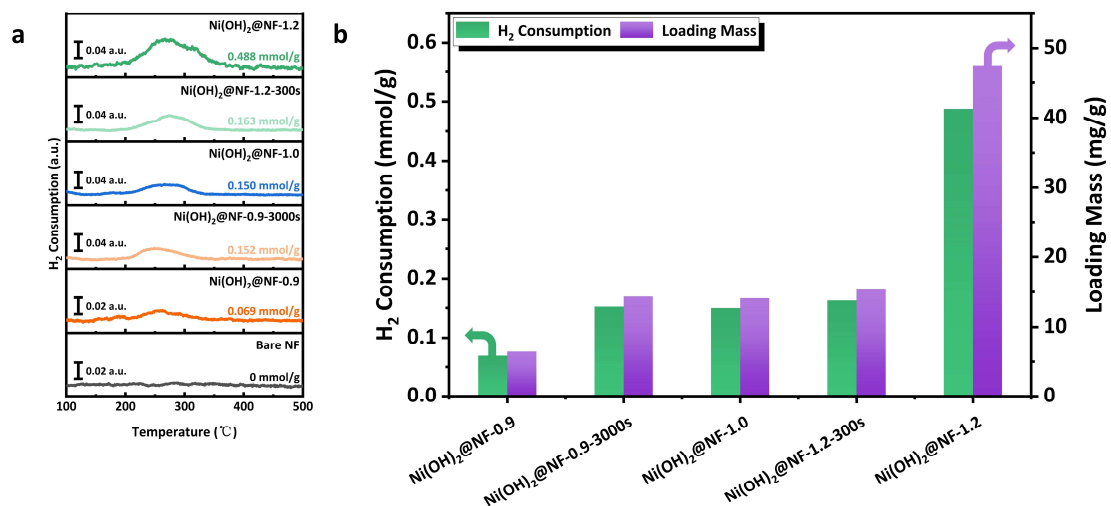
1.0.



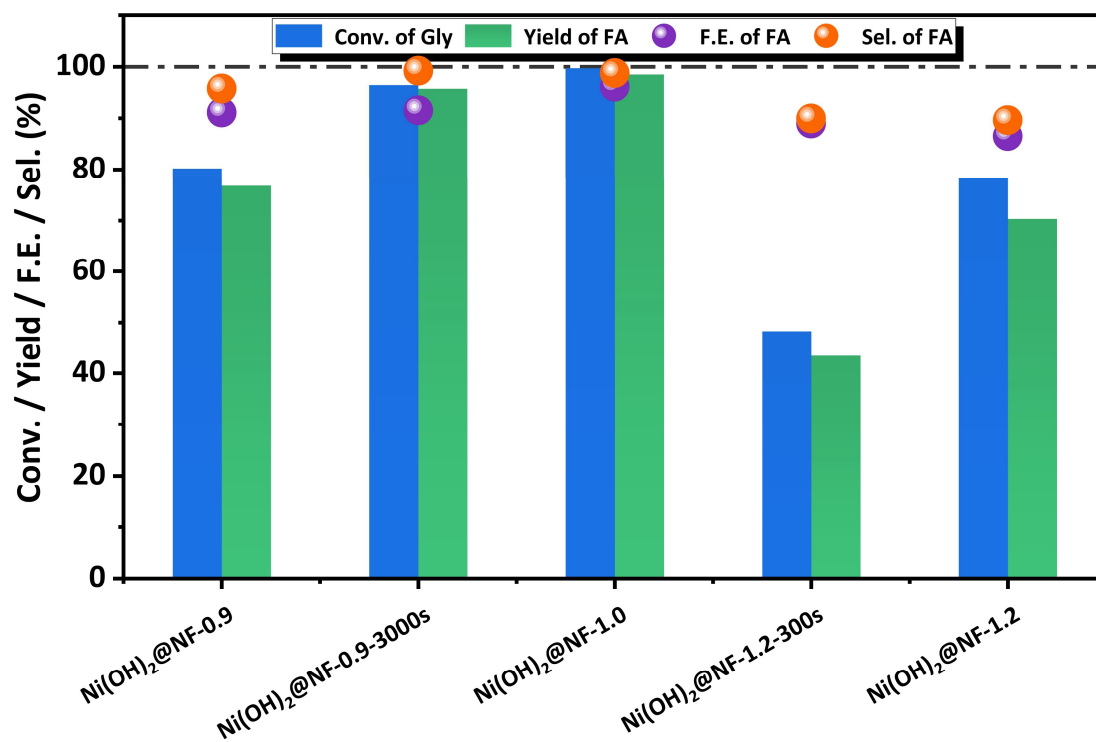
**Figure S14.** a) Tafel plots derived from LSV curves of  $\text{Ni}(\text{OH})_2@\text{NF}-1.0$  in 1 M KOH with or without the addition of 100 mM GLY. b) Tafel plots derived from LSV curves of  $\text{Ni}(\text{OH})_2@\text{NFs}-E$  in 1 M KOH with the addition of 100 mM GLY.



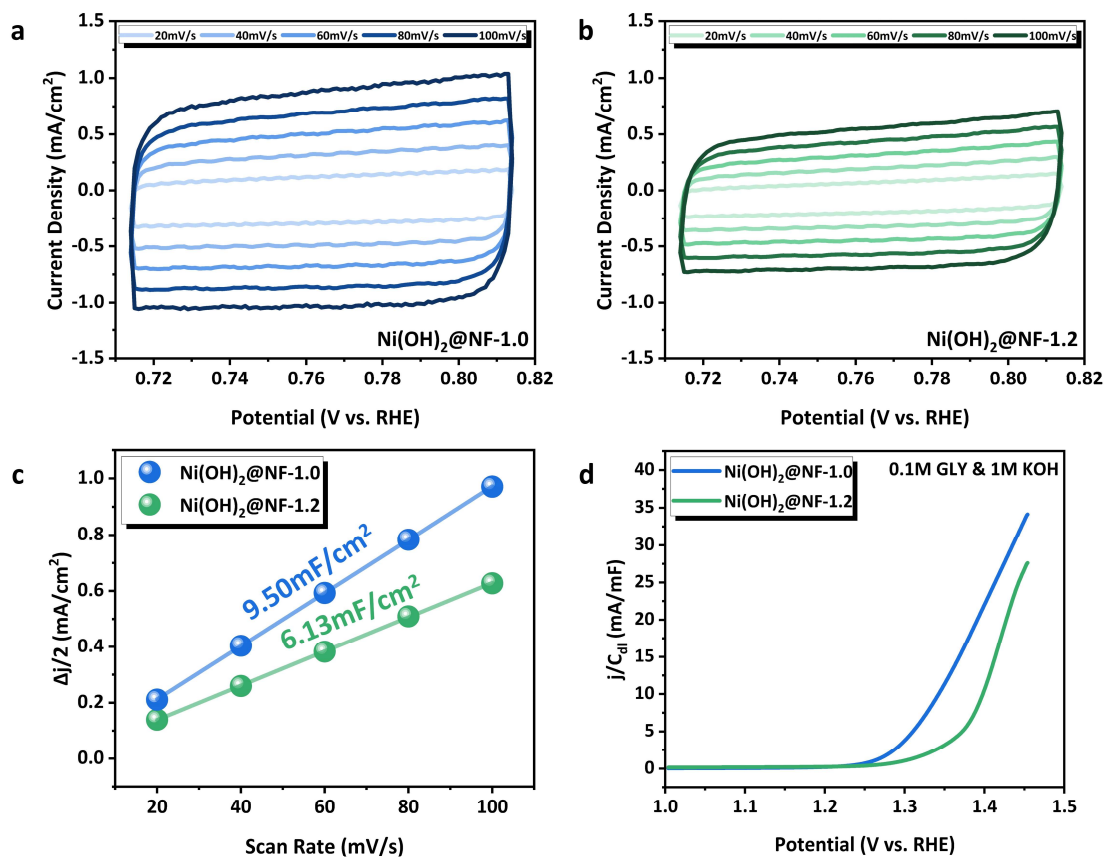
**Figure S15.** a) LSV curves recorded at the condition of catalysts synthesis. b) Deposition current and charge passed during the synthesis process.



**Figure S16.** a) H<sub>2</sub>-TPR curves for Ni(OH)<sub>2</sub>@NFs-*E* with different deposition time. b) Calculated H<sub>2</sub> consumption and loading mass of Ni(OH)<sub>2</sub>@NFs-*E* with controlled deposition time.

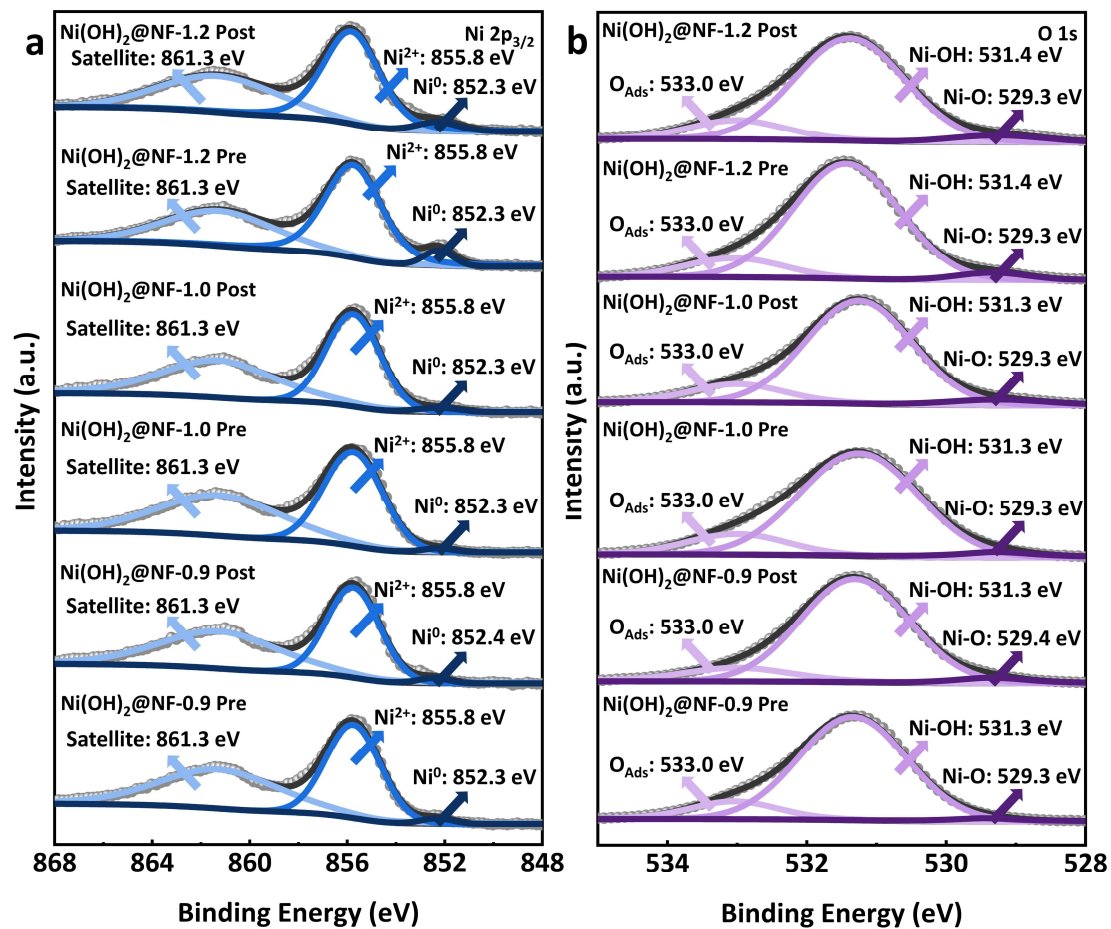


**Figure S17.** GOR performance (in 1 M KOH & 100 mM GLY at 1.36  $V_{\text{RHE}}$  after 10 h) of Ni(OH)<sub>2</sub>@NFs-*E* with different deposition time.

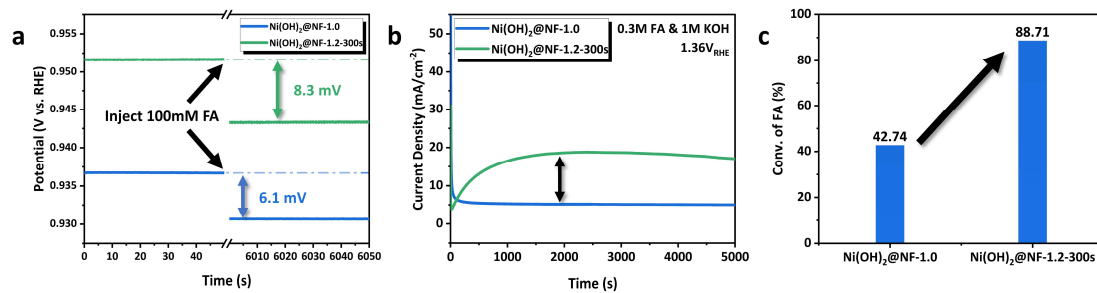


**Figure S18.** a-b) CV curves of  $\text{Ni(OH)}_2\text{@NF-1.0}$  and  $\text{Ni(OH)}_2\text{@NF-1.2}$  at different scan rates in the non-faradaic region. c) Double-layer capacitances of  $\text{Ni(OH)}_2\text{@NF-1.0}$  and  $\text{Ni(OH)}_2\text{@NF-1.2}$ . d) Normalized LSV curves of GOR for  $\text{Ni(OH)}_2\text{@NF-1.0}$  and  $\text{Ni(OH)}_2\text{@NF-1.2}$ .

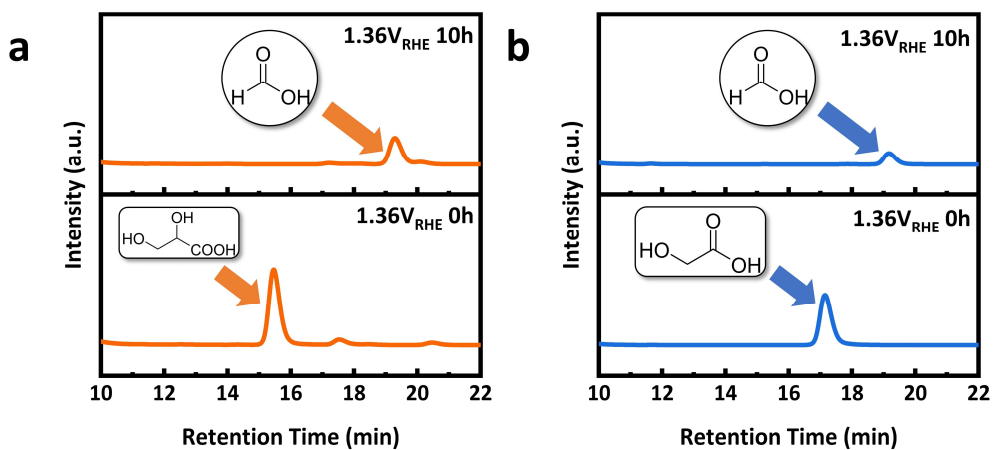




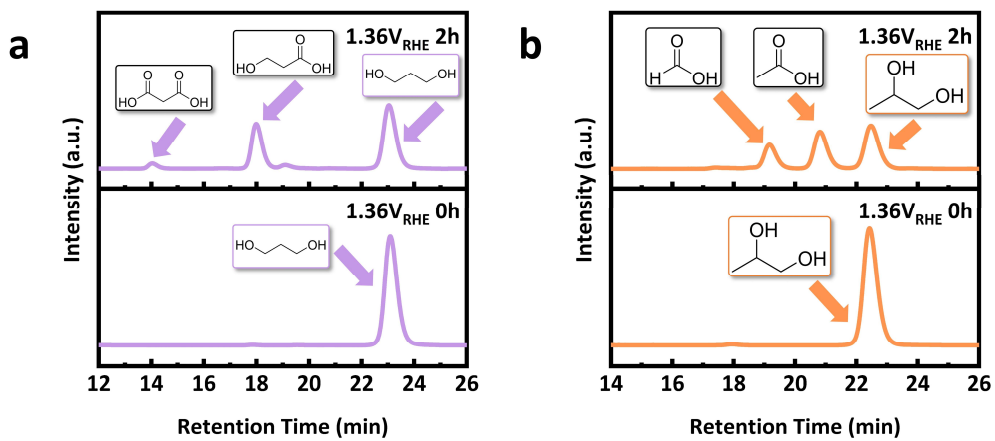
**Figure S19.** a) Ni 2p<sub>3/2</sub> XPS spectra and b) O 1s XPS spectra of Ni(OH)<sub>2</sub>@NFs-E before and after GOR.



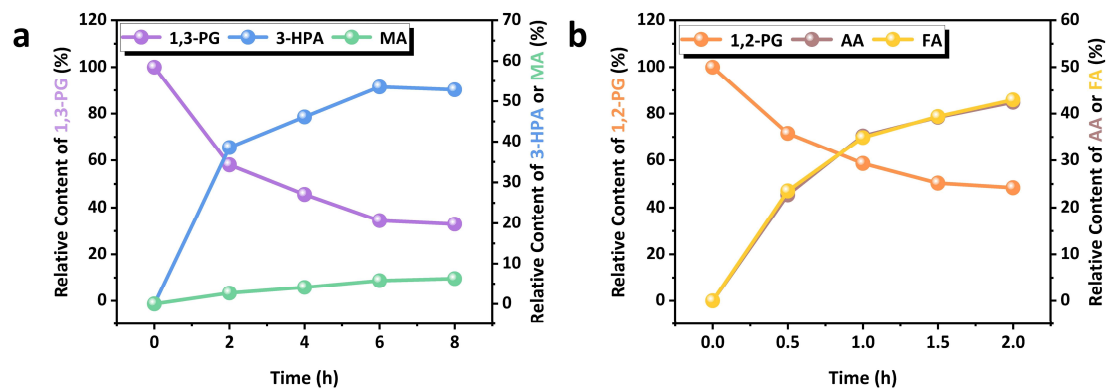
**Figure S20.** a) The variation of OCP as the function of time with the injection of 100 mM FA for Ni(OH)<sub>2</sub>@NF-1.0 and Ni(OH)<sub>2</sub>@NF-1.2-300s. b) I-t curves of FAOR conducted at 1.36 V<sub>RHE</sub> in 1 M KOH. c) Conversion of FA after 10 h FAOR.



**Figure S21.** HPLC elution curves of the electrolyte from the electrooxidation of intermediates over Ni(OH)<sub>2</sub>@NF-1.0 using a) GLA and b) GA as substrates.



**Figure S22.** HPLC elution curves of the electrolyte from the electrooxidation of probe molecules over Ni(OH)<sub>2</sub>@NF-1.0 using a) 1,3-PG and b) 1,2-PG as substrates.



**Figure S23.** Results of probe reactions over Ni(OH)<sub>2</sub>@NF-1.0 using a) 1,3-PG and b) 1,2-PG as substrates.

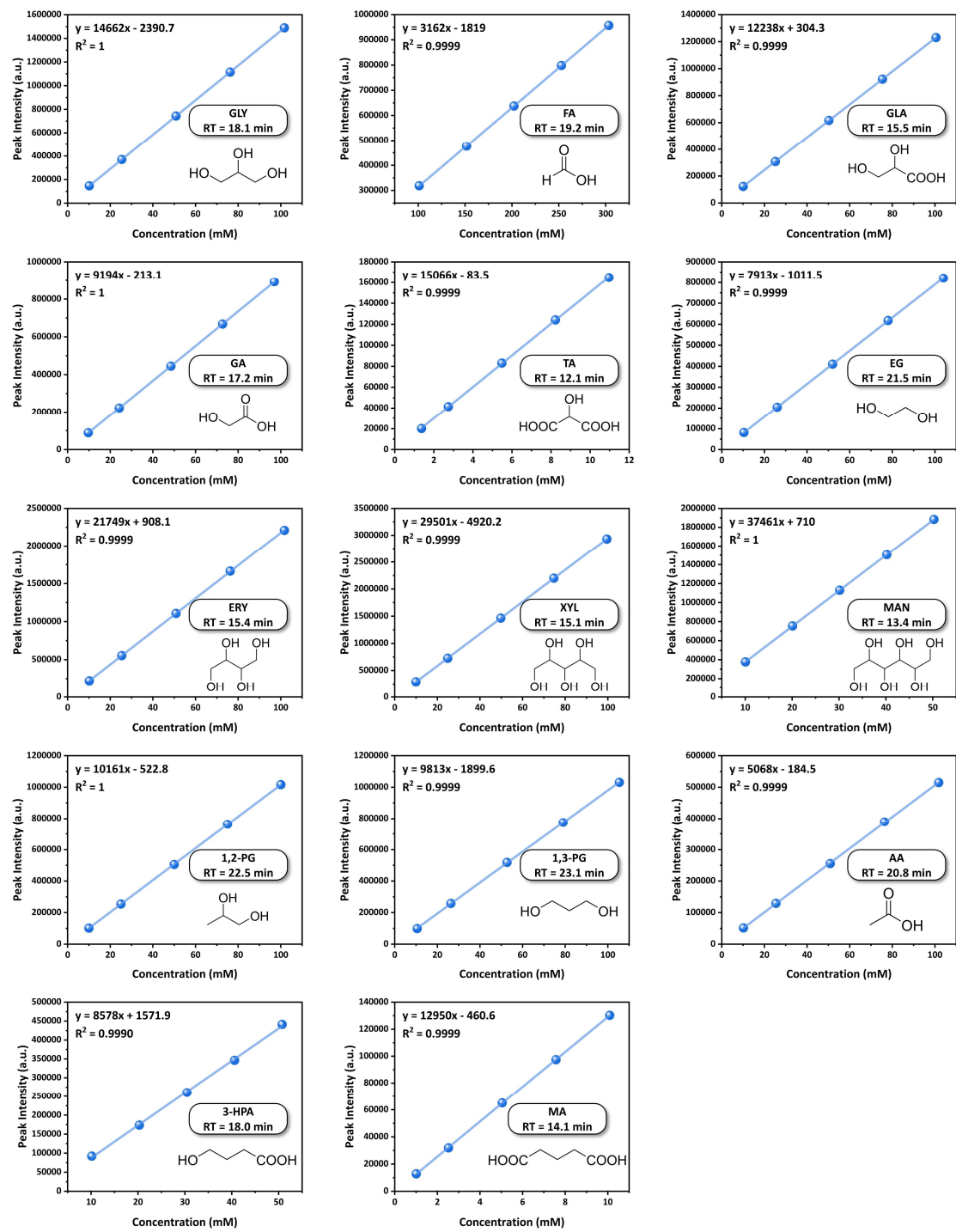
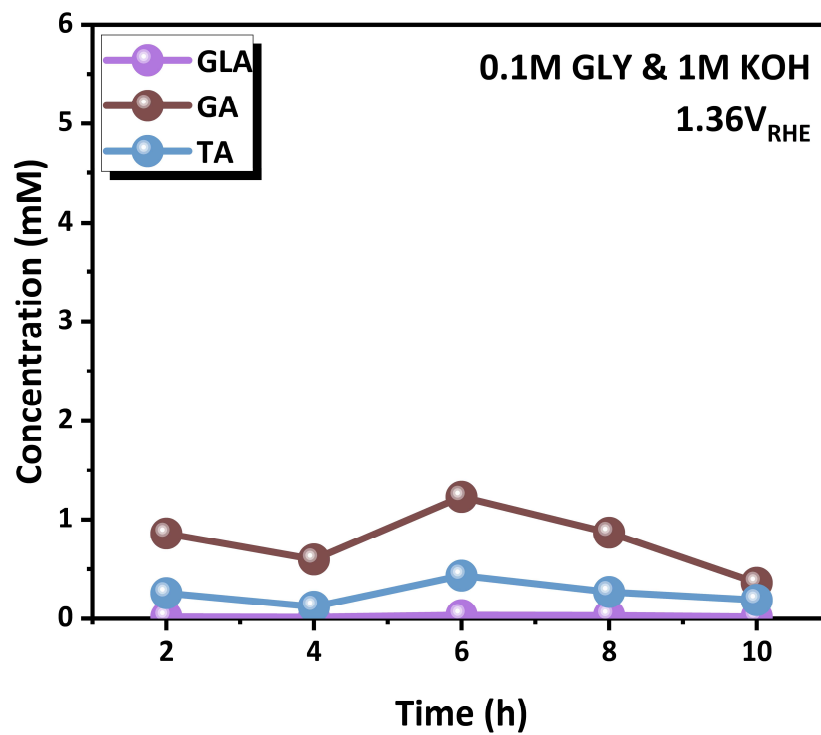


Figure S24. HPLC calibration curves of compounds related to this work.



**Figure S25.** Variation of intermediates concentration during GOR measured by HPLC.

**Table S1.** Ni content in the anolyte after GOR detected by ICP-AES.

<b>Catalyst</b>	<b>Ni content (ppm)</b>
<b>Ni(OH)<sub>2</sub>@NF-0.9</b>	Below detection limit (< 0.2 ppm)
<b>Ni(OH)<sub>2</sub>@NF-1.0</b>	Below detection limit (< 0.2 ppm)
<b>Ni(OH)<sub>2</sub>@NF-1.2</b>	Below detection limit (< 0.2 ppm)

Reaction Condition: 100 mM GLY; 1.36 V<sub>RHE</sub>; 10 h.



**Table S2.** The comparison of ‘GOR to FA’ performance between Ni(OH)<sub>2</sub>@NF-1.0 and the state-of-the-art catalysts.

Catalysts	Tafel Slope (mV/dec)	Conditions	Conv. (%)	FA Sel. (%)	F. E. of FA (%)	Ref.
<b>Ni(OH)<sub>2</sub>@NF-1.0</b>	67.5	1.36 V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	~100	98.8	96.1	This work.
NiCo <sub>2</sub> O <sub>4</sub> /NF	73.0	1.40 V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	~20	93.7	89.9	5
S-CuO/CF	108	1.35 V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	~30	95.1	95.7	6
Ni(OH) <sub>2</sub> /NF	/	1.50 V <sub>RHE</sub> ; 0.1 M GLY; 2 M LiOH.	/	/	81.3	7
NiVRu-LDHs/NF	102.7	1.40 V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	/	/	~97	8
SA-Bi/Co <sub>3</sub> O <sub>4</sub>	76.5	1.35 V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	~20	97	97	9
NiCo Hydroxide	68.8	1.62 V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	~89	84	94.3	10
NiCo(OH) <sub>2</sub> @HOS/NF	35.0	1.35 V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	~90	81.8	~74	11
CoCuMnMoNi High Entropy Alloy	53.5	1.32 V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	/	/	~93	12
Ru-NiP/N-C/NF	86.0	1.45V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	~90	~80	93	13
Cu-CuS/BM	/	1.45V <sub>RHE</sub> ; 0.1 M GLY; 0.1 M KOH.	~40	86.0	90.4	14
Mn-CoSe <sub>2</sub> /CFC	157.1	1.27V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	/	/	~95	15
ZnFe <sub>x</sub> Co <sub>2-x</sub> O <sub>4</sub>	163.0	1.62V <sub>RHE</sub> ; 0.5 M GLY; 1 M KOH.	~36	69.5	~50	16
Ni <sub>x</sub> B	/	1.80V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	73.0	80.0	/	17
CuNi/ACF	/	1.47V <sub>RHE</sub> ; 0.1 M GLY; 0.1 M KOH.	/	97.4	/	18
CuCo <sub>2</sub> O <sub>4</sub> Spinel Oxide	/	1.30V <sub>RHE</sub> ; 0.1 M GLY; 0.1 M KOH.	79.7	80.6	89.1	19
Ni-Pd/C	/	1.55V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	73.1	~98	98	20
Ni-Mo-N/CFC	87.0	1.35V <sub>RHE</sub> ; 0.1 M GLY; 1 M KOH.	~100	92.5	~97	21

**Table S3.** The amount of Ni hydroxides loaded over NF and TOF values of GOR for

Ni(OH)<sub>2</sub>@NFs-*E*.

Catalyst	Catalytic species content (mg/cm <sup>2</sup> ) <sup>a</sup>	TOF (×10 <sup>-3</sup> s <sup>-1</sup> )
Ni(OH) <sub>2</sub> @NF-0.9	0.88	7.02
Ni(OH) <sub>2</sub> @NF-1.0	1.93	7.86
Ni(OH) <sub>2</sub> @NF-1.2	6.48	0.44

<sup>a</sup>The calculated TOF values were based on the total Ni(OH)<sub>2</sub> loaded over NF at a geometric area of 1.0 cm<sup>2</sup> measured by H<sub>2</sub>-TPR and the current density tested by LSV.

**Table S4.** Surface content of Ni species over Ni(OH)<sub>2</sub>@NFs-*E* before and after GOR measured by XPS.

<b>Catalyst</b>	<b>Content (%)</b>	
	Ni <sup>2+</sup>	Ni <sup>0</sup>
<b>Ni(OH)<sub>2</sub>@NF-0.9-Pre</b>	96.8	3.2
<b>Ni(OH)<sub>2</sub>@NF-0.9-Post</b>	96.8	3.2
<b>Ni(OH)<sub>2</sub>@NF-1.0-Pre</b>	97.8	2.2
<b>Ni(OH)<sub>2</sub>@NF-1.0-Post</b>	96.6	3.4
<b>Ni(OH)<sub>2</sub>@NF-1.2-Pre</b>	93.2	6.8
<b>Ni(OH)<sub>2</sub>@NF-1.2-Post</b>	93.3	6.7

## Supplementary References

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