

5-hydroxymethylfurfural (HMF) synthesis in a deep eutectic solvent-based biphasic system: closing the loop of solvent reuse, product isolation and green metrics

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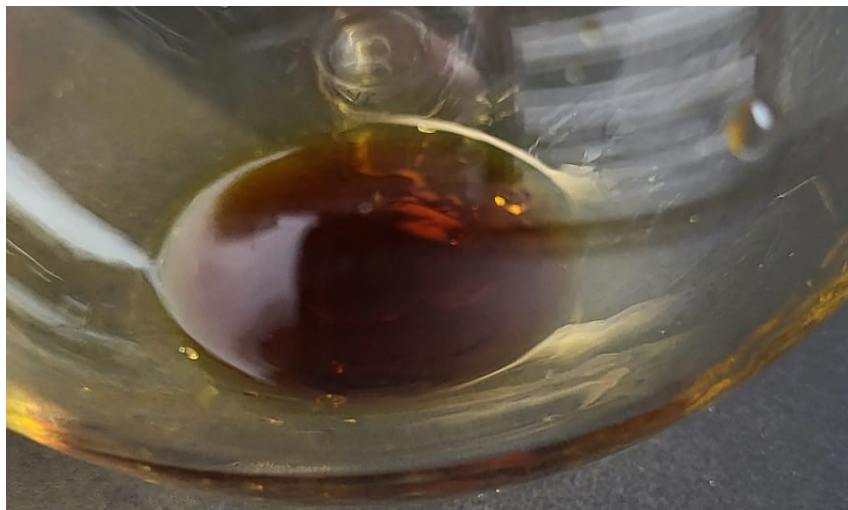


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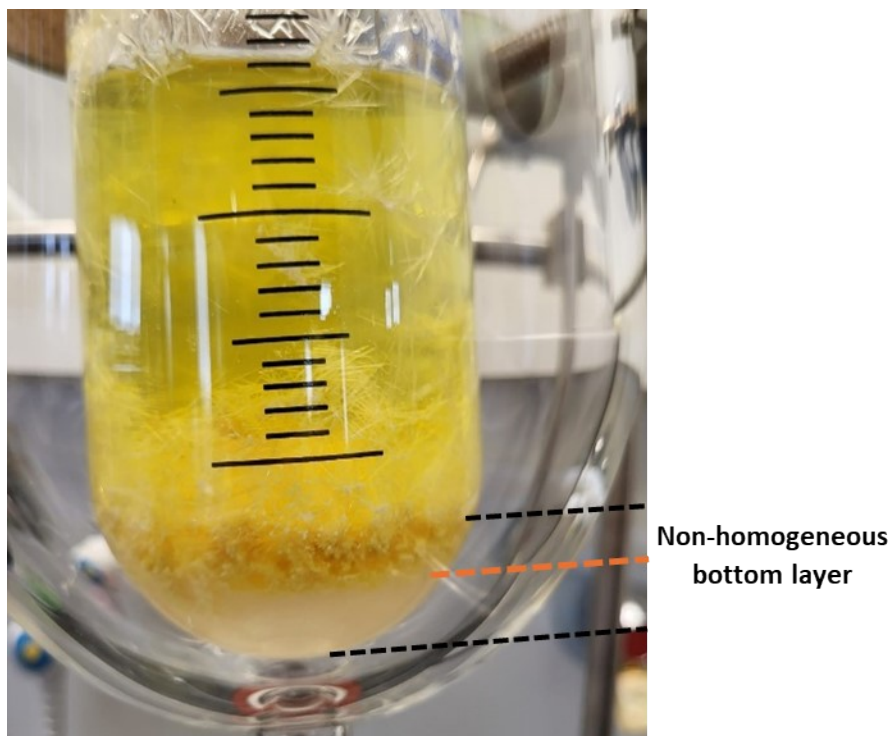


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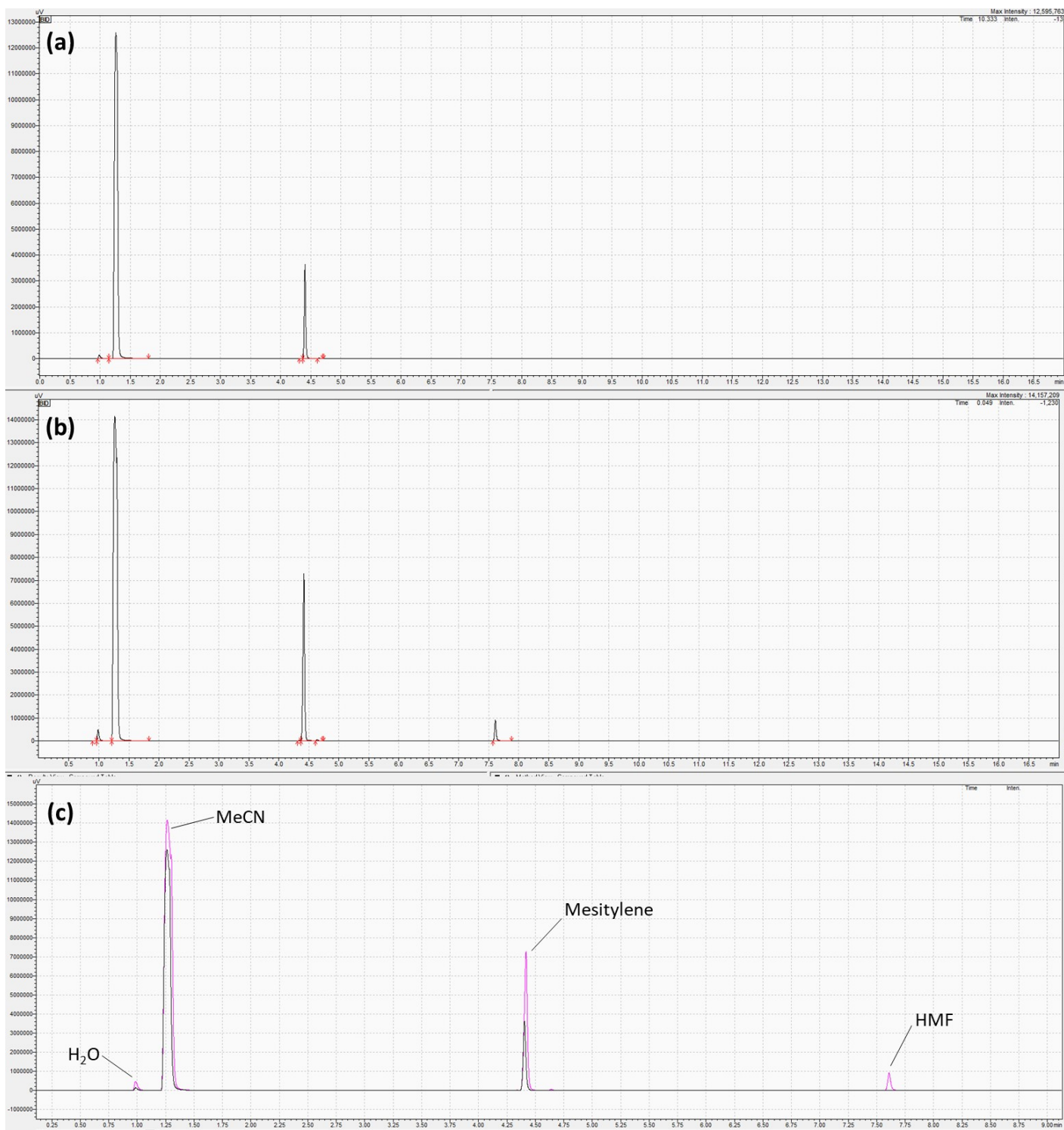


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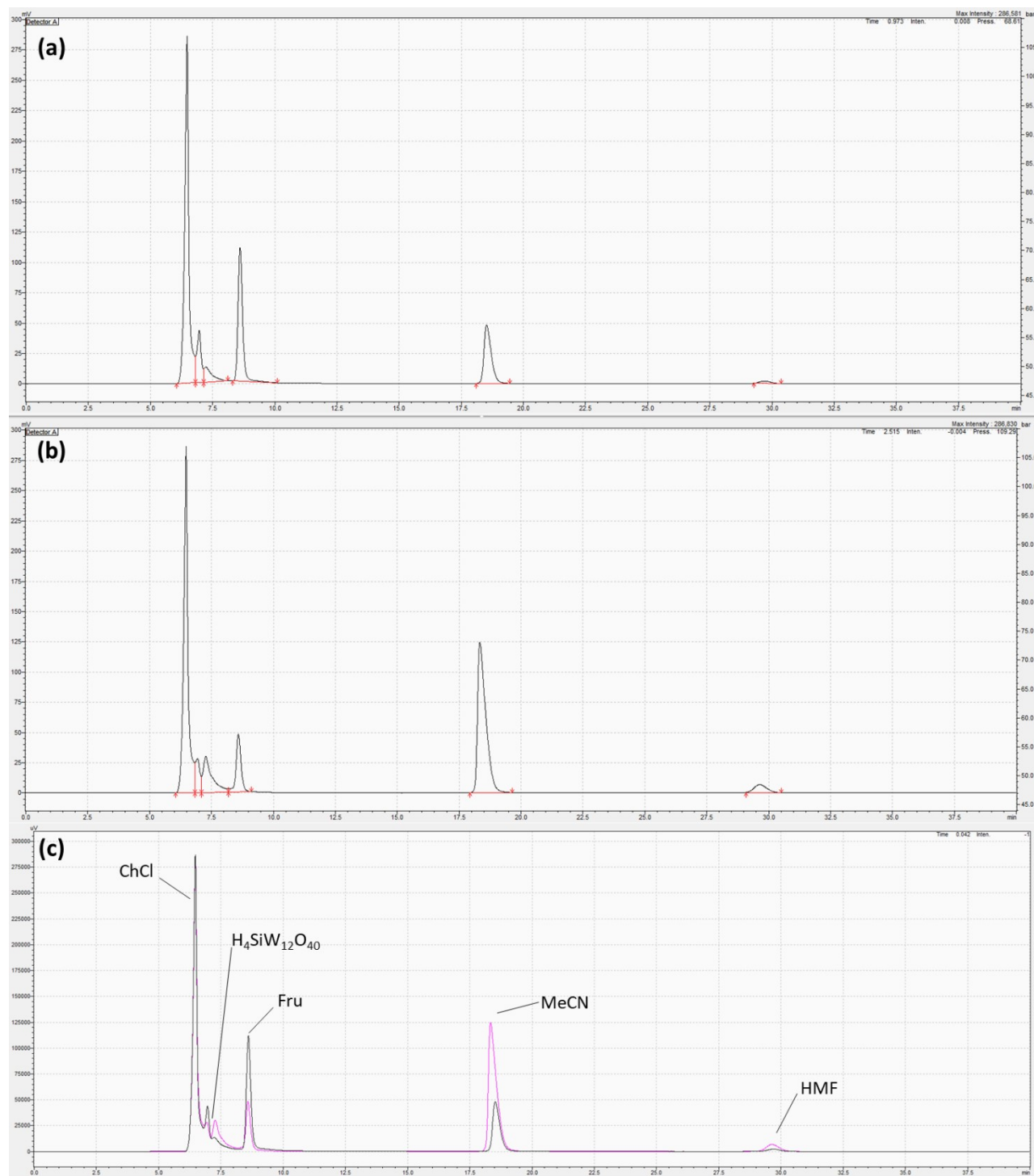


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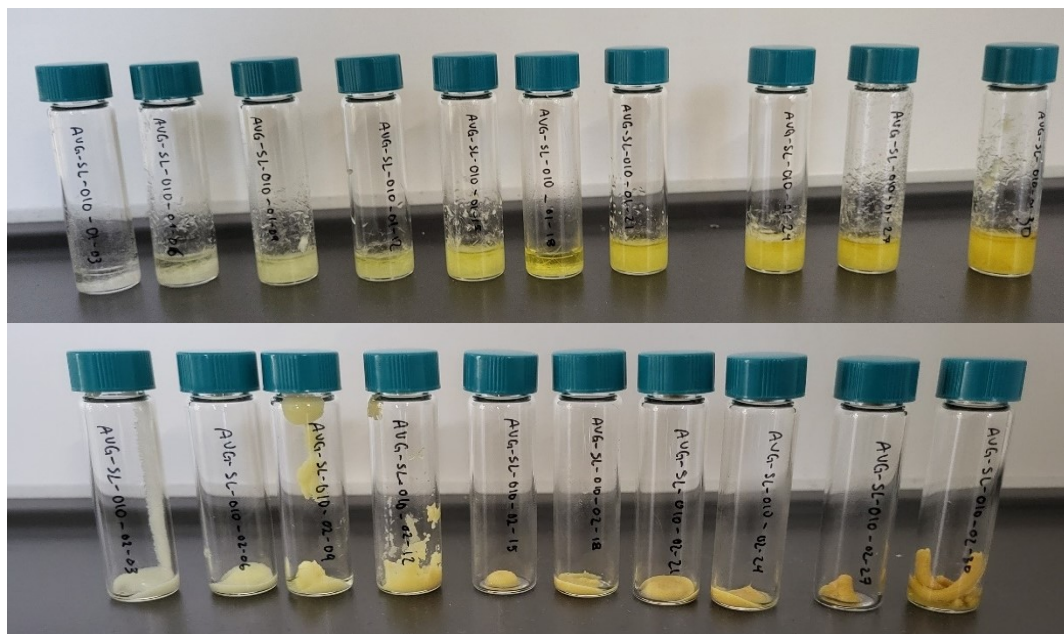


Figure S5. Samples of the extraction phase (top) and reaction phase (bottom) after: 3, 6, 9, 12, 15, 18, 21, 24, 27, 30 min. Reaction Conditions: 18 g ChCl, 4,5 g Fru, ChCl:Fru (5:1), $V_{\text{solvent}} = 150 \text{ mL}$, $T = 80^\circ\text{C}$, $t = 15 \text{ min}$, $\omega = 400 \text{ rpm}$, $c_{\text{H}_4\text{SiW}_{12}\text{O}_{40}} = 0.87 \text{ mol}\%_{\text{Fru}}$

Table S1. Formulae and definitions for the calculations of green metrics

E-factor:	$E = \frac{\text{Total mass of waste}}{\text{Mass of product}}$	(S1)
Process mass intensity:	$PMI = \frac{\text{Total mass in process (incl. H}_2\text{O)}}{\text{Mass of product}}$	(S2)
Solvent intensity:	$SI = \frac{\text{Mass of solvents}}{\text{Mass of product}}$	(S3)
Reaction mass efficiency:	$RME\% = \frac{\text{Mass of product}}{\text{Total mass of reactants}} \cdot 100$	(S4)
Mass Productivity:	$MP\% = \frac{\text{Mass of product}}{\text{Total mass of reactants (incl. solvents)}} \cdot 100$	(S5)

Table S2. Values used to calculate the green metrics in Table 1

Case	RP	EP	Σm (RP) [g]	Σm (EP) [g]	Σm (Fru) [g]	Catalyst	Σm Catalyst [g]	Σ Yield HMF [g]	Ref
1.1	[Bmim][Cl] WCl ₆	THF	0.50	177.80	0.5	WCl ₆	0.0110	0.2660	40
1.2	[Bmim][Cl] WCl ₆	THF	100.00	4445.00	70	WCl ₆	2.2000	26.700	40
2	TEAC : fructose (1 : 0.92) ^{a d}	THF	2.00	71.10	5	NaHSO ₄ •H ₂ O	0.0766	1.7709	41
3	ChCl : fructose (1 : 0.2) ^a	MeCN	3.60	141.48	5.4	HCl	0.0354	3.2318	15
4	ChCl : citric acid (1 : 2.33) ^a	EtOAc	2.00	20	0.02	Citric Acid	0.7400	0.0129	42
5	ChCl : fructose (5 : 1) ^{a b}	MeCN	18.00	117.9	4.5	H ₄ SiW ₁₂ O ₄₀	0.6230	2.4000	
6	ChCl : fructose (5 : 1) ^{a b c}	MeCN	18.00	117.9	22.5	H ₄ SiW ₁₂ O ₄₀	0.6230	8.2000	

^a for DESs. the ratio in brackets corresponds to the molar ratio of HBA : HBD.

^b this work

^c this work with recycled extraction phase according to Figure 6 (only considering HMF in the extraction Phase)

^d 5 g H-Y Zeolite were added at the beginning of the reaction.

Table S3. Recovered volume of extraction phase from the reactor and volume of MeCN after the distillation step.

Recycling Run	V before distillation [mL]	V after distillation [mL]	loss [%]
0	139	135	2.9%
1	140	136	2.9%
2	138	133	3.6%
3	139	134	3.6%
4	140	137	2.1%
5	138	136	1.4%

