Electronic Supplementary Information

Multi-Electron Bipolar-Type Organic Molecules for High-Capacity Dual-Ion

Zinc Batteries

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Section S1. Experimental procedures and calculation methods

1.1 Experimental Section

The Zn batteries (CR2032) are assembled using commercial zinc foil as an anode, glass fiber membrane, and 2 M Zn(OTF)₂ aqueous electrolyte. The preparation steps of the positive electrode material AQ and IDT are as follows: AQ and IDT are used as the active substance, PTFE is used as the binder, and super P conductive agents are selected, and the slurry is prepared by mixing them in an ethanol dispersant in a mass ratio of 6:3:1. Then, the obtained slurry is dried in an 80 °C vacuum oven to remove the solvent. The dried slurry was uniformly loaded on the stainless-steel mesh (the mass loading of active materials in the cathode is ~1.0 mg cm⁻²). Then, we further increased the mass loading to 4, 8, and 10 mg cm⁻² for high mass-loading electrochemical performance tests, respectively.

1.2 Characterization

The sample morphology was observed by field-emission scanning electron microscopy (SEM, Hitachi S-4800) and transmission electron microscopy (TEM, JEM-2100). The elemental mapping characterization was carried out on a JEM-F200 instrument equipped with an energy diffraction system. Fourier-transformed infrared spectrum (FT-IR) was collected through a Thermo Nicolet NEXUS spectrometer. X-ray diffraction test was performed to analyze the material structure using X-ray diffraction (XRD, Bruker D8 advance powder diffractometer with a Cu K α radiation source). X-ray photoelectron spectrometer (XPS, AXIS Ultra DLD) was utilized to study the surface chemistry of the samples. Thermogravimetric (TG) analysis was performed with an STA409 PC thermogravimetric analyzer in a nitrogen atmosphere at a heating speed of 10 °C min⁻¹. Nitrogen adsorption/desorption measurements were performed using a Micromeritics ASAP2020 physisorption analyzer at -196 °C. The specific surface area, pore volume, and pore size distribution were evaluated by using the Brunauer-Emmett-Teller (BET) equation and the nonlocal density functional theory model. The ultraviolet-visible (UV-Vis) spectra were obtained with a JASCO V-750 UV-Vis spectrometer.

The optical energy gaps (E_g , eV) of organic cathodes can be determined by ultraviolet-visible (UV-Vis) spectroscopy, which is expressed as:

$$\alpha \propto (hv - E_g)^{1/2} / hv$$

$$hv = 1240 / \lambda$$

where α denotes the optical absorption coefficient, hv is the photon energy, λ is the wavelength.

Before *ex-situ* characterizations, the electrode surface needs to be fine polishing to remove zinc salts. For *ex-situ* characterizations including XPS, XRD, and SEM, the organic cathodes were collected by disassembling the batteries at specific voltages during (dis)charging. After that, the electrodes were rinsed thoroughly with distilled water for 5 times to guarantee the removal of adhered glass fiber and residual electrolyte. Finally, the electrodes were dried in a vacuum oven at 60 °C for 24 h.

1.3 Electrochemical Tests

The cyclic voltammetry (CV) and electrochemical impedance spectroscopy (EIS) measurements with an amplitude of 0.005 V and a test frequency of $10^{-2} \sim 10^6$ H_Z were characterized on a CHI660E electrochemical workstation. The equivalent circuit of Nyquist plots includes the equivalent series resistance (R_s), charge transfer resistance (R_{ct}), Warburg impedance (Z_w) and constant phase angle element (CPE). Galvanostatic charge/discharge (GCD) measurements were conducted on the CT3001A battery test system in the potential range of 0–1.6 V. The specific capacity (C_m , mAh g^{-1}) was determined from GCD profiles using the following form:

$$Cm = \frac{I \times \Delta t}{m}$$
(Eq. S1)

where I, Δt , m refer to the current density (A g⁻¹), the discharging time (s) and the mass loading (g) of active materials on the cathode, respectively.

The gravimetric energy density (E, Wh kg^{-1}) and power density (P, W kg^{-1}) of ZIHCs were estimated based on the following forms:

$$E = C_{\rm m} \times \Delta V \tag{Eq. S2}$$

$$P = E / 1000 \times \Delta t \tag{Eq. S3}$$

where ΔV is the voltage window (V).

1.4 Density functional theory (DFT) calculation

Density functional theory (DFT)^{S1, S2} was employed to optimize the stabilized structures of AQ

and IDT with Gaussian 09 software package^{S3}. The B3LYP functionalS4, 5 with 6-31G(d, p) basis sets^{S6-8} were selected in all the calculations. On the basis of the optimized structure of AQ/IDT molecule, the electrostatic potential (ESP) analysis on van der Waals surface was done to deduce the possible Zn^{2+} and OTF⁻ ions uptake positions using the Multiwfn 3.7 software package^{S9} and the cubeman utilization in the Gaussian 09 software package. According to the analysis of ESP, the coordination structures of IDT with Zn^{2+} and OTF⁻ ions were optimized.

Considering thermal correction based on frequency analysis, the binding free energies (ΔG) of every system was the difference of electronic energy. According to frequency and optimization analysis results, the ΔG of the five probable discharging progresses were then calculated.



Section S2. Supporting characterization results

Fig. S1. FT-IR spectra of IDT and AQ.



Fig. S2. Solid-state UV-vis spectra of IDT and AQ.



Fig. S3. The calculated electrical conductivity of AQ and IDT.



Fig. S4. SEM images of IDT and AQ.



Fig. S5. TGA curves of AQ and IDT.



Fig. S6. GCD curves of AQ cathode.



Fig. S7. GCD curves of IDT and AQ cathodes at 10 A g^{-1} .



Fig. S8. Cycling stability and corresponding coulombic efficiency of the Zn//AQ battery.



Fig. S9. SEM images of Zn anodes before and after cycles.

Organic cathode	Electrolyte	Voltage	Capacity	Retention	Ref.
		(V)	(mAh g ⁻¹ /A g ⁻¹)	(%) / (cycles)	
cı	1 M Zn(CF ₃ SO ₃) ₂	0.8-1.4	205 / 0.04	70 / 200	S10
ci Ci p-chloranil				at 0.217 A g ⁻¹	
	2 M 7250	0.3-1.4	210.9 / 0.05	83.8 / 23 000	S11
од sдо DTT	2 IVI ZIISO ₄			at 2 A g ⁻¹	
н	2 M ZnSO ₄	0.35-1.25	240 / 0.1	73.7 / 2000	S12
o″ \⊒∕ % NTCDI				at 1 A g ⁻¹	
	2 M ZnSO ₄	0.35-1.25	170 / 0.1	-	S12
		0-1.0	122.9 / 0.2	68.2 / 1000	S13
<i>γ</i> ∠	2 M ZnCl_2			at 8 A g ⁻¹	
+ ⟨ s) ,	3 M	0.2-1.8	203 / 0.02	86 / 50	S14
PBQS	Zn(CF ₃ SO ₃) ₂			at 0.04 A g ⁻¹	
^{HO} →S) "	2 M 7nSO	0.4-1.45	260 / 0.1	79 / 2000	S15
бурн PDBS	2 101 211504			at 2 A g^{-1}	
<u></u> (C), C, C, C, L)	2 M	0.2-1.8	210.2 / 0.05	70.6 / 20, 000	S16
rrpa	$Zn(CF_3SO_3)_2$			at 5 A g ⁻¹	
CL ^A L	1 M ZnSO ₄	0.1-1.6	443 / 0.05	50.2 / 100	S17
ö TAPQ				at 0.05 A g ⁻¹	
NC CTPQ	2 M ZnSO ₄	0.1-1.4	244 / 0.3	50 / 210	S18
				at 0.5 A g ⁻¹	
	2 M	0-1.6	238 / 0.2	88.7 / 3000	This
	Zn(CF ₃ SO ₃) ₂			at 10 A g ⁻¹	work

Table S1. Comparison of rate capacity, energy density and cycling performance of recently

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Fig. S10. Capacitive contribution of the AQ cathode at 20 mV s⁻¹.



Fig. S11. CV curves of IDT and AQ.



Fig. S12. *Ex-situ* XPS spectra of IDT cathodes at various discharged/charged states.



Fig. S13. CV curves of IDT at $ZnSO_4/H_2O$ electrolyte.



Fig. S14. *Ex-situ* XRD patterns.



Fig. S15. GCD curves of IDT cathode at $0.33 \text{ M Zn}(\text{OTF})_2/\text{acetonitrile electrolyte}$.



Fig. S16. GCD curves of IDT cathode at HOTF electrolytes with different pH values.



Fig. S17. ESP plots of IDT and AQ.

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