## **Supplementary Information**

## Robust metal–organic framework monoliths for long-cycling lithium metal batteries

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## Supplementary note 1 Experimental details on the liquid adsorption test

The porosity of the membrane was calculated by the following formula:

$$\frac{\frac{W_s - W_m}{\rho_b}}{\frac{W_s - W_m}{\rho_b} + \frac{W_m}{\rho_m}}$$
Porosity =  $\frac{W_s - W_m}{\rho_b} + \frac{W_m}{\rho_m} \times 100\%$ 

where  $w_{\rm m}$  and  $w_{\rm s}$  are weights of the dry membrane and the membrane soaked in 2-propanol for 1h, respectively.  $\rho_{\rm b}$  and  $\rho_{\rm m}$  are the density of 2-propanol and dry membrane, respectively. Similarly, electrolyte uptakes of membranes were calculated by the following formula:

$$\frac{(w_e - w_m)}{w_e - w_m}$$

Electrolyte uptake =  $W_m \times 100\%$ 

where  $w_e$  is weight of the membrane soaked in the liquid electrolyte for 2 h.



Fig. S1 Geometries of LMBs for the electrochemical simulations.

Parameter	PP	c-MOF/PP	m-MOF/PP
$i_1 ({ m mA \ cm^{-2}})$	3	3	3
$\sigma_{ m l}~({ m S~cm^{-1}})$	1×10 <sup>-3</sup>	1×10 <sup>-3</sup> (bulk), 1×10 <sup>-7</sup> (binder)	1×10 <sup>-3</sup>
$Li^+$ transference number ( $t_{Li^+}$ )	0.25	0.25	0.25
$c_1 \pmod{\mathrm{L}^{-1}}$	1	1	1
$i_{0,\rm ref} ({\rm A} \; {\rm m}^{-2})$	100	100	100
$lpha_{ m a}$	0.5	0.5	0.5

 Table S1 Parameters used for 2D electrochemical modeling.



**Fig. S2** SEM images of the m-MOF/PP after nucleation, confirming that the rhombic dodecahedral structure of ZIF-8 is not formed.



**Fig. S3** SEM images of the m-MOF/PP synthesized under different conditions, such as types and concentrations of precursors and the temperature for the growth process. The precursors are (a) zinc acetate dihydrate, 2-methyl imidazole, and (b) zinc nitrate hexahydrate, 2-methyl imidazole. The concentration of precursors is shown in each image, as follows (Zn metal precursor, 2-methylimidazole). When using the zinc acetate dihydrate as Zn source, small welldefined cubic crystals of MOF are formed due to a high nucleation rate for zinc acetate precursor.<sup>S1</sup> A high concentration of precursors leads to equilibria shifting toward enhanced metal-ligand complexation thereby stopping crystal growth, resulting in small particles.<sup>S1</sup> The decrease in temperature of synthesis process induces the particles exhibiting higher purity and perfection.<sup>S2</sup>



Fig. S4 XRD patterns of the m-MOF/PP, c-MOF/PP, MOF particle and PP.



**Fig. S5** (a) Topology and (b) distribution of *E* value of MOF particle on Si wafer, (c) FD curve of MOF particle at point 1, acquired using AFM.



**Fig. S6** (a, c, e) N<sub>2</sub> adsorption–desorption isotherm and (b, d, f) pore size distribution of (a, b) the m-MOF/PP, (c, d) the c-MOF/PP, and (e, f) PP.



Fig. S7 FE-SEM images of m-MOF/PP membrane after electrolyte impregnation.

Separator	m-MOF/PP	c-MOF/PP	РР
SSIP (%)	34	40	89
CIP (%)	67	60	11

 Table S2 Relative amounts of the SSIP and CIP in various membranes.



**Fig. S8** AC-impedance spectra of electrolyte-impregnated PP at temperatures ranging from 10 to 60 °C.



Fig. S9 DC polarization curve and AC-impedance spectra of electrolyte-impregnated PP.



Fig. S10 Electrochemical modeling results for Li<sup>+</sup> flux and local current densities through PP.



Fig. S11 SEM images of Cu substrate after Li deposition with a capacity of 10 mAh cm<sup>-2</sup> at 1 mA cm<sup>-2</sup> using [Li || Cu] cell with the PP.



**Fig. S12** SEM images of Cu substrate after Li deposition with a capacity of 10 mAh cm<sup>-2</sup> at 1 mAh cm<sup>-2</sup> using [Li || Cu] cell with the c-MOF/PP, showing the MOF particles exfoliated from the c-MOF/PP (inside the yellow dotted line).



Fig. S13 Voltage profiles of [Li  $\parallel$  Cu] cell with the PP measured during Li plating–stripping at 0.5 mA cm<sup>-2</sup>.



**Fig. S14** Top view SEM images of Li anodes after 50 cycles using the [Li || Li] cells with the (a) PP, (b) c-MOF/PP and (c) m-MOF/PP.



Fig. S15 Charge–discharge profiles of full cells with PP measured at 0.5C.

Membrane	Fabrication method	Test condition			
		Electrolyte	C-rate	<ul> <li>Capacity retention</li> </ul>	Ref.
PI-ZIF8	Slurry-casting	1 M LiPF <sub>6</sub> in EC/DMC/DEC /PEGDA/BMA	1C	75.2% after 300 cycles	[S3]
Hollow ZIF-8 membrane	Slurry-casting	1 M LiPF <sub>6</sub> in EC:DEC = 1:1 vol%	0.1C	85.1% after 100 cycles	[S4]
UIO-66/PAN/PVDF	Electrospinning	1 M LiPF <sub>6</sub> solution	1C	94.9% after 100 cycles	[S5]
3D-UIO-66/PAN	Electrospinning	LiTFSI-PEO ([EO]:LiTFSI = 18:1)	0.2C	86% after 300 cycles	[S6]
m-MOF/PP	Direct growth	1 M LiTFSI in DOL:DME = 1:1 with 1wt% LiNO <sub>3</sub>	0.5C	96.6% after 300 cycles	This work

Table S3 Comparison of the electrochemical performances of the [Li  $\parallel$  LFP] full cell using MOF-based membranes.



Fig. S16 Voltage profiles of the [Li  $\parallel$  LFP] full cells using (a) PP, (b) c-MOF/PP, and (c) m-MOF/PP membrane operated at 0.1–1C. (d) Rate performances of the full cells using various membranes at 30 °C.

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