

**High Voltage Driven MnO<sub>2</sub>/CuO for Efficient Oxidation of  
5-Hydroxymethylfurfural**

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## **Experimental**

### **Chemicals**

All chemicals and reagents are purchased from Shanghai Macklin Biochemical Technology Co., Ltd.

### **Synthesis of MnO<sub>2</sub>**

0.51 g Mn(NO<sub>3</sub>)<sub>2</sub>·4H<sub>2</sub>O and 1.30 g dimethylimidazole are added to 40 mL deionized water, respectively. The two solutions are mixed and stirred at room temperature for 10 min. Ni foam (1×2 cm<sup>2</sup>) is vertically immersed into the above solution for 0.5 h to obtain Mn<sub>3</sub>O<sub>4</sub>. Finally, the MnO<sub>2</sub> are obtained after activation by cyclic voltammetry (CV).

### **Synthesis of CuO and MnO<sub>2</sub>/CuO**

In a three-electrode system (Ag/AgCl as the reference electrode, Pt wire as the counter electrode, Ni foam or MnO<sub>2</sub> as the working electrode), precursor is prepared by deposition at a constant voltage (-1.2 V vs Ag/AgCl) for 200 s using 0.05 mol/L Cu(NO<sub>3</sub>)<sub>2</sub> as the electrolyte. The samples are activated by CV operation in 1.0 M KOH (-0.7 to 1.8 V<sub>RHE</sub>), CuO and MnO<sub>2</sub>/CuO are then obtained.

### **Physical characterization**

In this experiment, the crystal structure of samples is determined by X-ray diffractometer (XRD, SmartLab). Surface morphology and phases of samples are investigated by scanning electron microscopy (SEM, Apreo S HiVac) and high resolution transmission electron microscopy (HRTEM, JEM-2100). The chemical bonding is studied by Raman spectroscopy (Raman, DXR). The chemical composition is determined by X-ray photoelectron spectroscopy (XPS, ESCALAB QXi).

### **Electrochemical experiments**

All electrochemical performances are studied on CHI 1440D electrochemical

workstation. Electrochemical experiments are carried out in a three-electrode system, with Hg/HgO electrode as the reference electrode, Pt wire as the counter electrode, samples as the working electrode and 1.0 M KOH as the electrolyte.

### **Quantitative analysis of products**

20 uL reaction solution is taken out and then diluted to 2 mL. The diluted reaction solution is detected by high performance liquid chromatography (HPLC). Mobile phase A is 5 mM ammonium formate solution, and mobile phase B is 10% methanol solution. The ratio of mobile phase A to B is 8:2 (flow rate 0.6 mL/min, elution time 14 min). Finally, the reactants and products are quantitatively analyzed by the external standard method. HMF conversion, FDCA yield and Faraday efficiency (FE) are calculated according to the following equations:

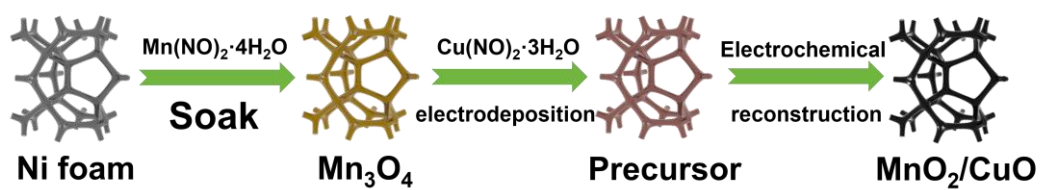
$$\text{HMF conversion (\%)} = \frac{\text{mole of consumed HMF}}{\text{mole of initial HMF}} \times 100\%$$

$$\text{FDCA yield (\%)} = \frac{\text{mole of FDCA formed}}{\text{mole of initial HMF}} \times 100\%$$

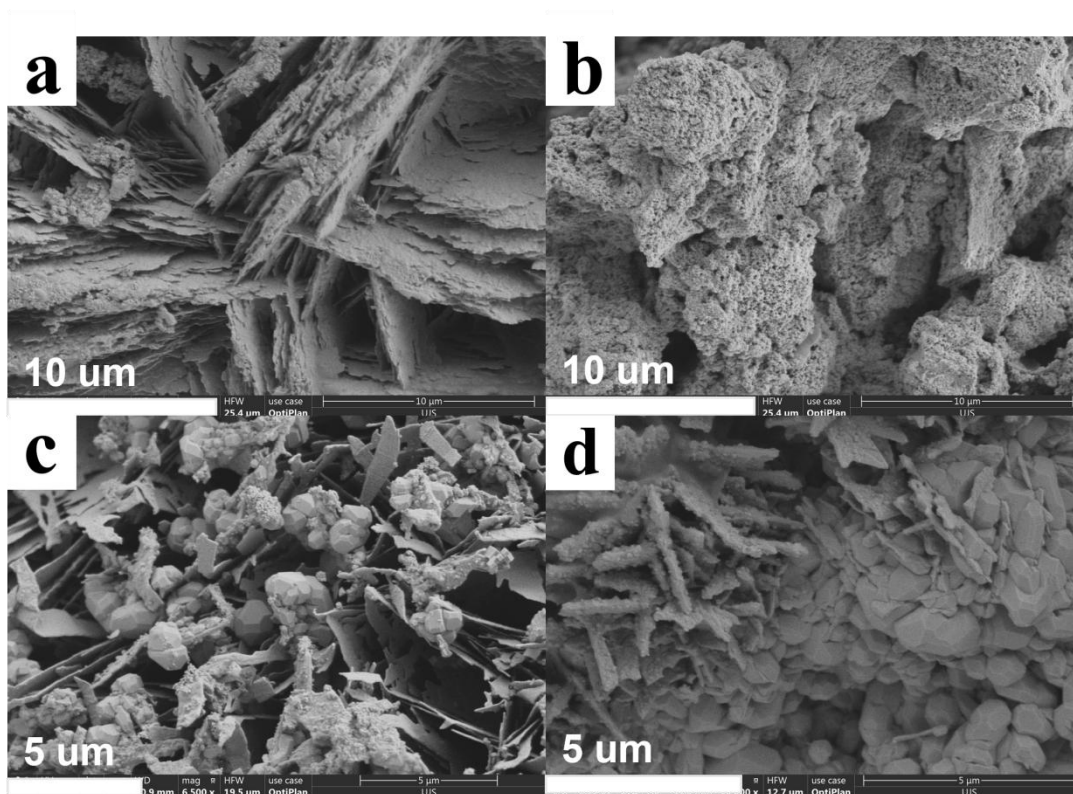
$$\text{FE of FDCA (\%)} = \frac{\text{mole of FDCA formed}}{\text{total charge passed}/(6 \times F)} \times 100\%$$

### **Measurement in continuous flow electrolytic cell**

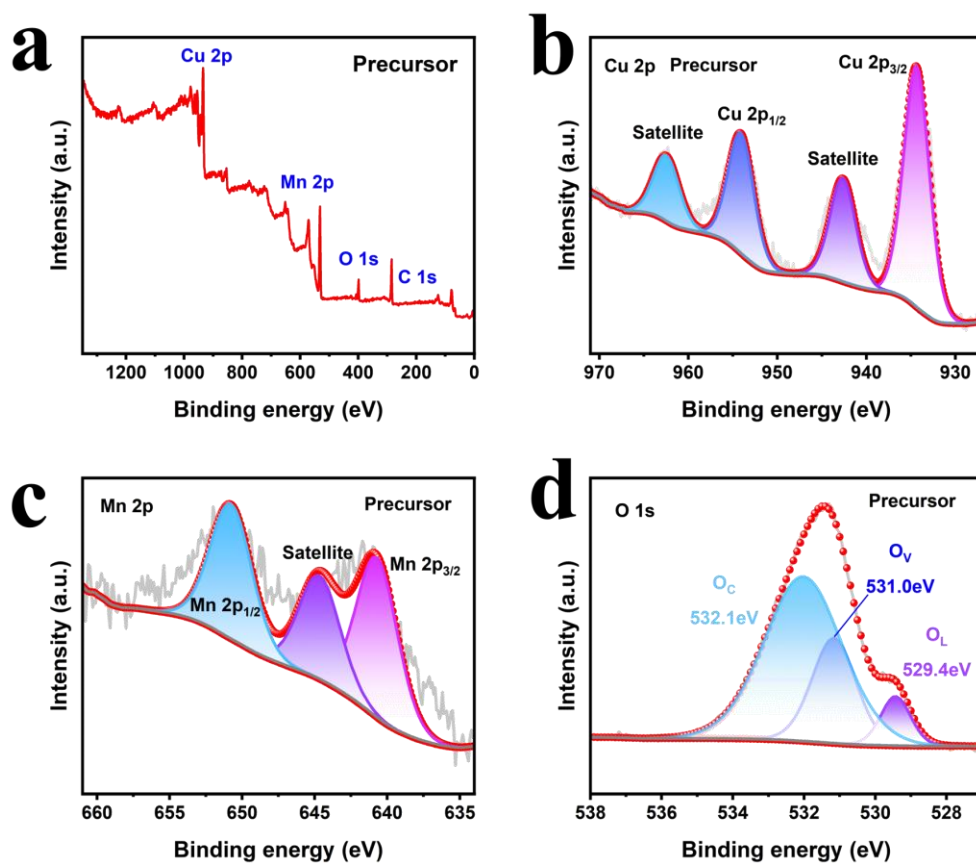
Compared with H-type electrolytic cell, the continuous flow electrolytic cell can realize the continuous supply of reactants and product of FDCA, which effectively prevents the polarization of solution concentration and improves the mass transfer efficiency of substances. Two separate electrolytic cells are connected using peristaltic pumps. The MnO<sub>2</sub>/CuO with an area of 1 cm<sup>2</sup> are prepared and mounted on the anode of the continuous flow electrolytic cell, and proton exchange membrane is installed between the anode and the cathode.



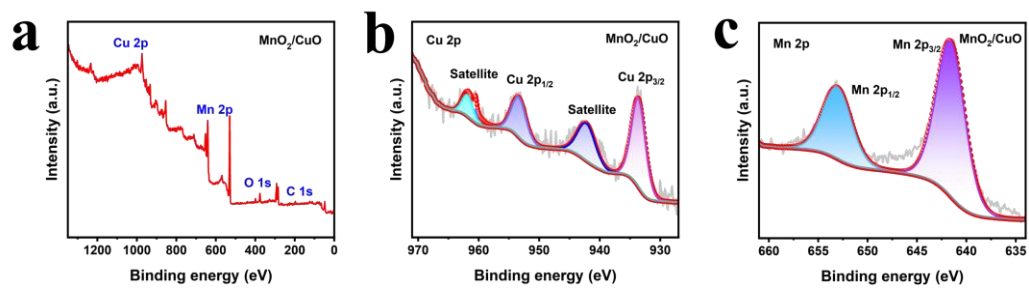
**Fig. S1.** Schematic diagram of the synthesis process of MnO<sub>2</sub>/CuO.



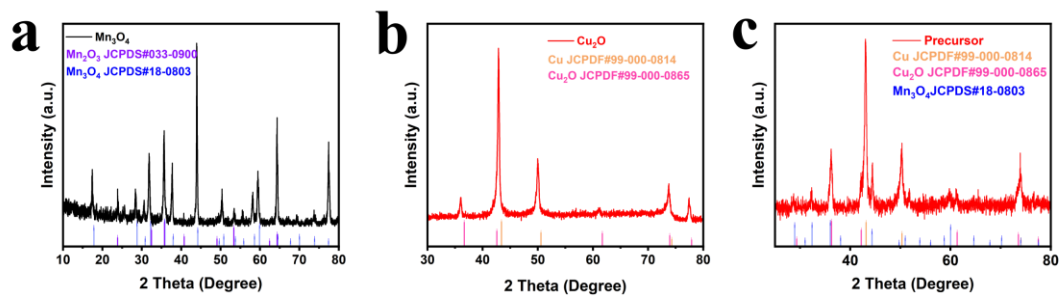
**Fig. S2.** SEM images of (a)  $\text{Cu}_2\text{O}$ , (b)  $\text{Mn}_3\text{O}_4$ , (c) Precursor, and (d)  $\text{MnO}_2/\text{CuO}$  (low magnification).



**Fig. S3.** (a) Full-scan XPS spectra of precursor. XPS survey spectra of (b) Cu 2p, (c) Mn 2p, and (d) O 1s.

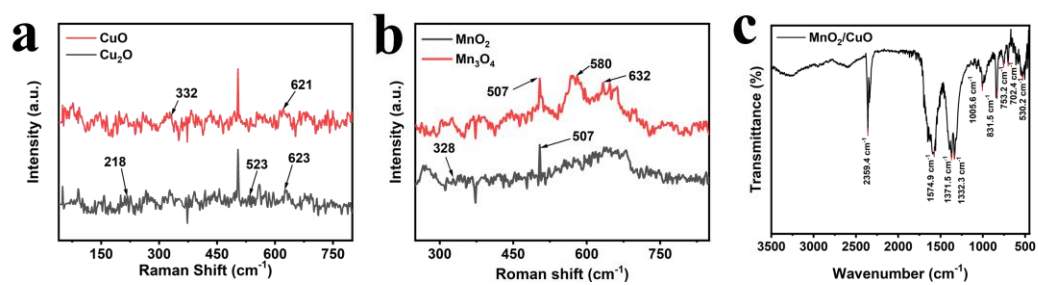


**Fig. S4.** (a) Full-scan XPS spectra of  $\text{MnO}_2/\text{CuO}$ . XPS survey spectra of (b) Cu 2p, and (c) Mn 2p.

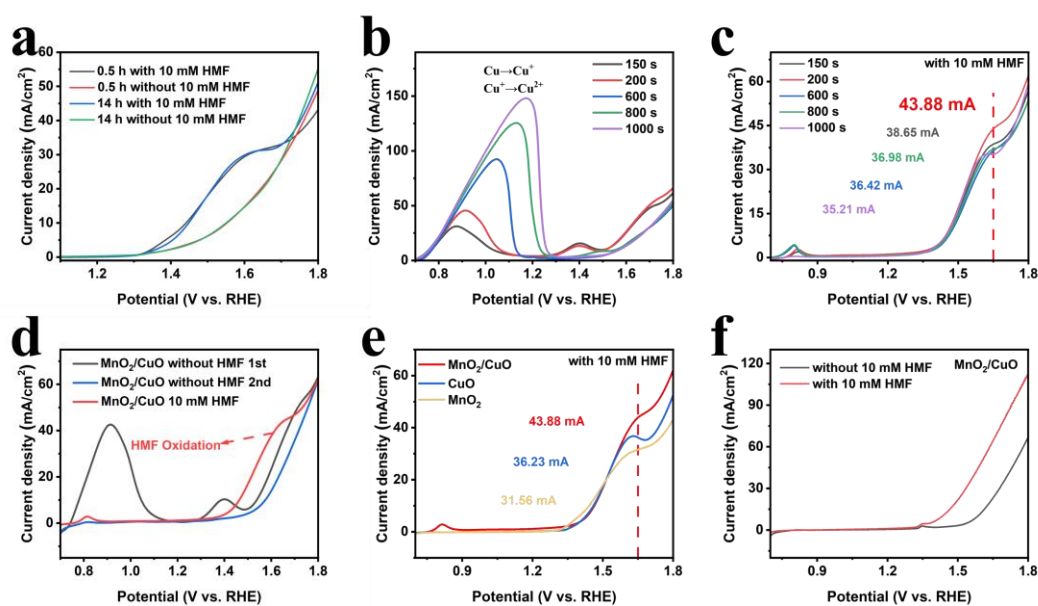


**Fig. S5.** XRD patterns of (a)  $\text{Mn}_3\text{O}_4$ , (b)  $\text{Cu}_2\text{O}$ , and (c) Precursor.

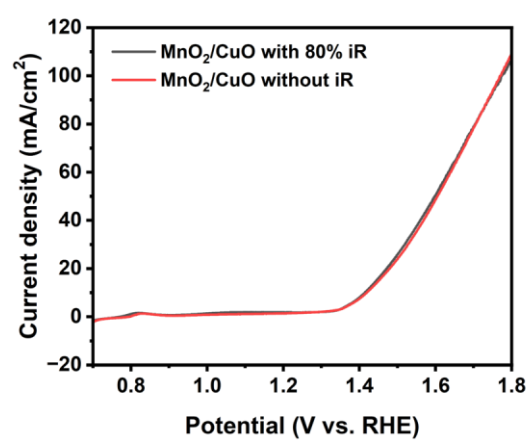




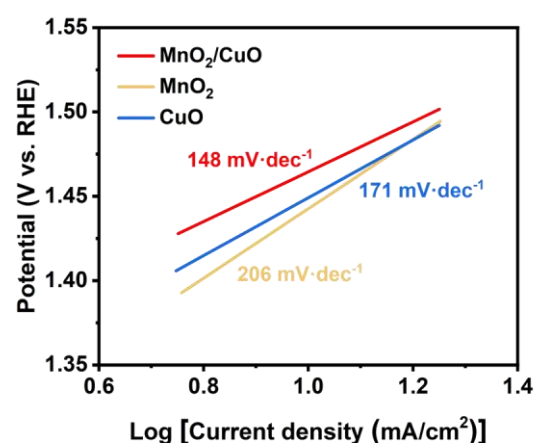
**Fig. S6.** Raman spectra of (a) CuO, and (b) MnO<sub>2</sub>. (c) FT-IR spectrum of MnO<sub>2</sub>/CuO.



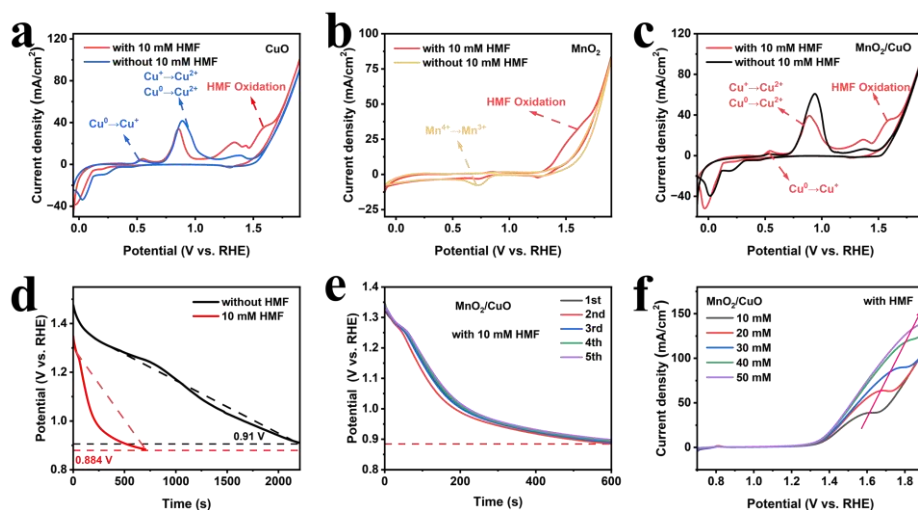
**Fig. S7.** (a) LSV curves of MnO<sub>2</sub> with different soaking times (with and without 10 mM HMF). (b) LSV curves of CuO with different electrodeposition times in 1.0 M KOH. (c) LSV curves of MnO<sub>2</sub>/CuO with different electrodeposition times at 10 mM HMF. (d) LSV curves of MnO<sub>2</sub>/CuO with and without 10 mM HMF. (e) LSV curves with 10 mM HMF. (f) LSV curves of MnO<sub>2</sub>/CuO with and without 10 mM HMF (stirring conditions).



**Fig. S8.** LSV curves of MnO<sub>2</sub>/CuO with and without iR (10 mM HMF).

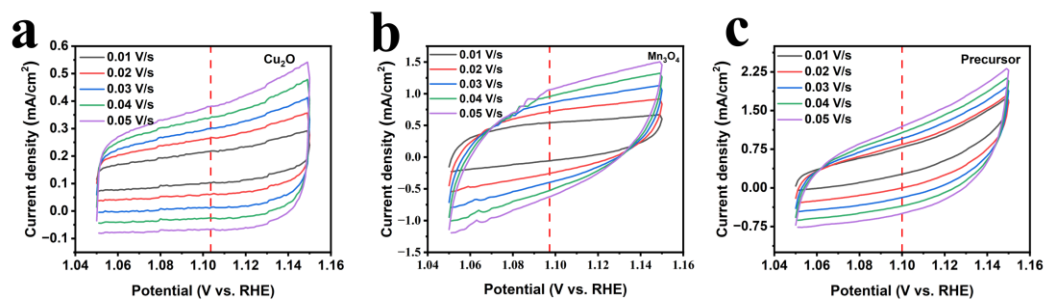


**Fig. S9.** Tafel slopes.

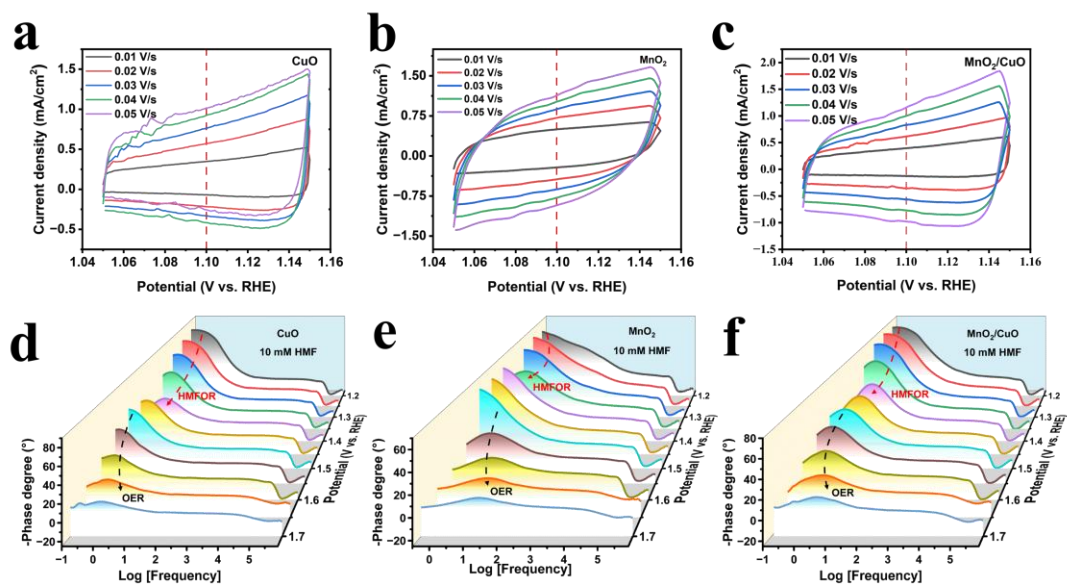


**Fig. S10.** CV curve of (a) CuO, (b) MnO<sub>2</sub>, (c) MnO<sub>2</sub>/CuO with and without 10 mM HMF. (d) Open circuit voltage vs. time. (e) Five cycles of regeneration between Cu<sup>2+</sup>→Cu<sup>1+</sup>. (f) LSV curves of MnO<sub>2</sub>/CuO at different concentrations (10-50 mM HMF).

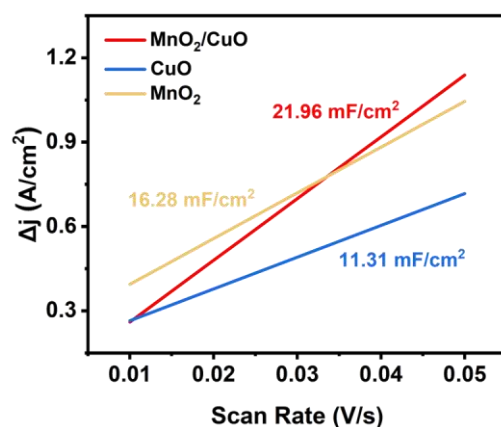
In 1.0 M KOH, the initial OCP voltage is about 1.35 V<sub>RHE</sub>, which is related to the oxidation voltage of Cu<sup>2+</sup>. The OCP voltage decreased to 0.91 V<sub>RHE</sub> for about 2000 s. However, after the addition of 10 mM HMF, the OCP voltage quickly decreased to 0.884 V<sub>RHE</sub> for only 700 s, which corresponds to the formation of Cu<sub>2</sub>O species. The shorter decay time indirectly confirms that CuO is the main active site for HMFOR. Fig. S10e shows the regeneration experiments for five cycles of Cu<sup>2+</sup>→Cu<sup>+</sup>. The initial and equilibrium voltages of the five cycles are basically the same, indicating that the CuO active species underwent the spontaneous and reversible transformation on the surface of catalyst. Furthermore, the LSV experiments (10-50 mM HMF) show a linear correlation between the current density and HMF concentration (Fig. S10f), suggesting that HMFOR over MnO<sub>2</sub>/CuO belongs to the surface-adsorption controlled process.



**Fig. S11.** CV curve of (a)  $\text{Cu}_2\text{O}$ , (b)  $\text{Mn}_3\text{O}_4$ , and (c) precursor with 10 mM HMF.



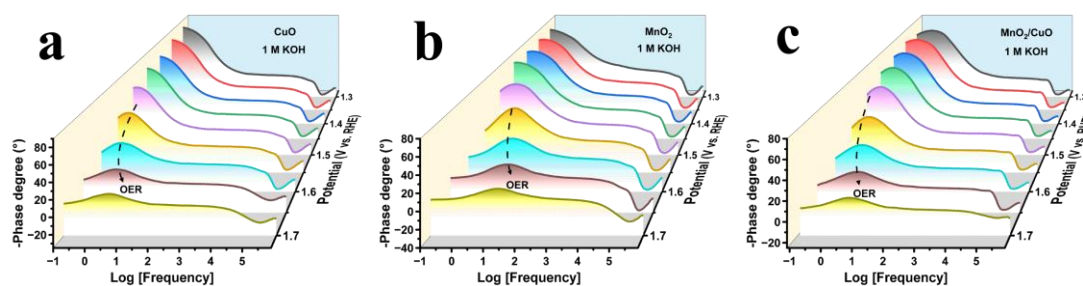
**Fig. S12.** CV curve of (a) CuO, (b) MnO<sub>2</sub>, (c) MnO<sub>2</sub>/CuO with 10 mM HMF. EIS spectra of (d) CuO, (e) MnO<sub>2</sub>, (f) MnO<sub>2</sub>/CuO with 10 mM HMF.



**Fig. S13.** Cdl of CuO, MnO<sub>2</sub> and MnO<sub>2</sub>/CuO.

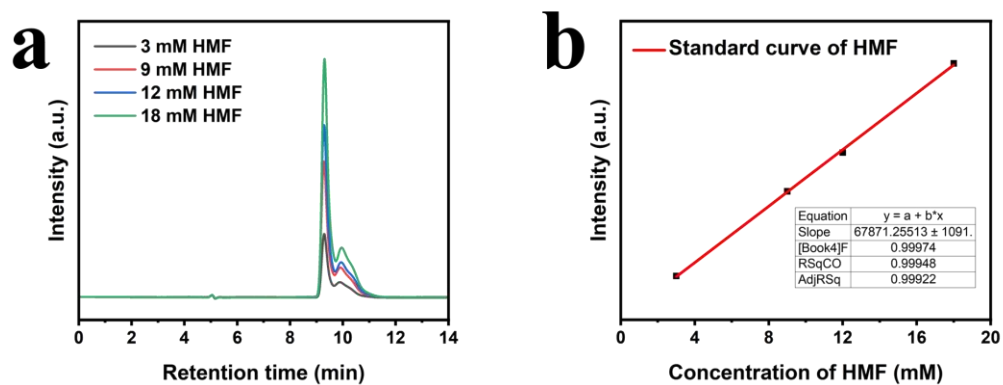
The inherent electrocatalytic performances are estimated by the electrochemically surface area (ECSA) of CuO, MnO<sub>2</sub> and MnO<sub>2</sub>/CuO (Fig. S11, Fig. S12a-c). The double-layer capacitance (Cdl) has a linear relationship with ECSA, which could be measured by CV curves at different scan rates. As shown in Fig. S13, the Cdl in 10 mM HMF is 11.31, 16.28 and 21.96 mF·cm<sup>-2</sup> for CuO, MnO<sub>2</sub> and MnO<sub>2</sub>/CuO, respectively. The larger ECSA of MnO<sub>2</sub>/CuO indicates that MnO<sub>2</sub>/CuO have better electrocatalytic ability than the bare CuO and MnO<sub>2</sub>.



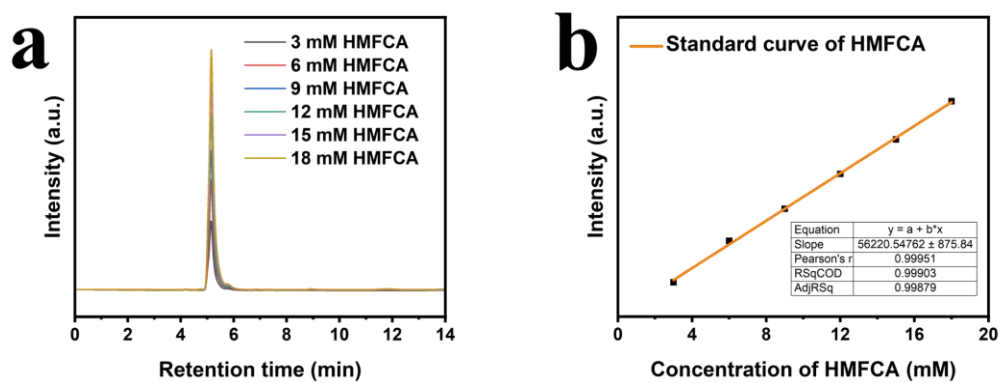


**Fig. S14.** EIS spectrum of (a) CuO, (b) MnO<sub>2</sub>, and (c) MnO<sub>2</sub>/CuO with 1.0 M KOH.

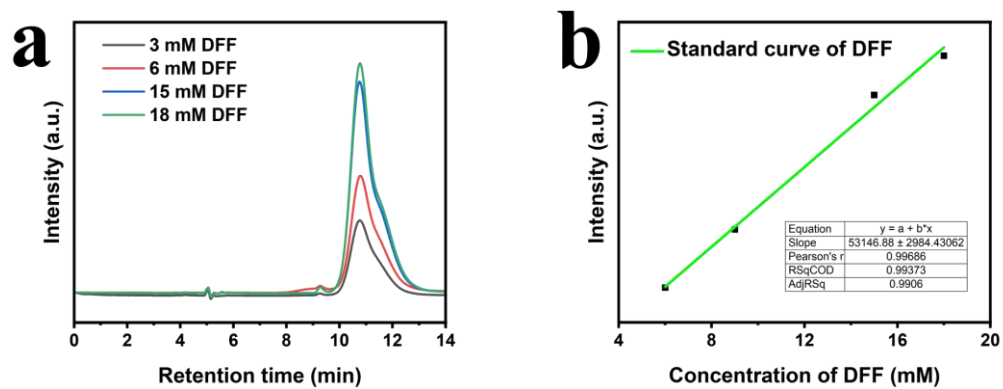
The difference in reaction kinetics between OER and HMFOR is further investigated by the electrochemical impedance spectroscopy (EIS) to account for the interfacial electrochemical behavior during HMFOR. EIS tests are performed on CuO, MnO<sub>2</sub> and MnO<sub>2</sub>/CuO in 1.0 M KOH and 10 mM HMF solutions, respectively. As shown in Fig. S14a-c, OER begin to appear in the low frequency region (0.1-10 Hz) since 1.5 V<sub>RHE</sub>, which reveals the slow kinetics of water oxidation. In the intermediate frequency region (10-102 Hz), a new peak responding to HMFOR appeared from 1.35 V<sub>RHE</sub>, which is also consistent with LSV results.



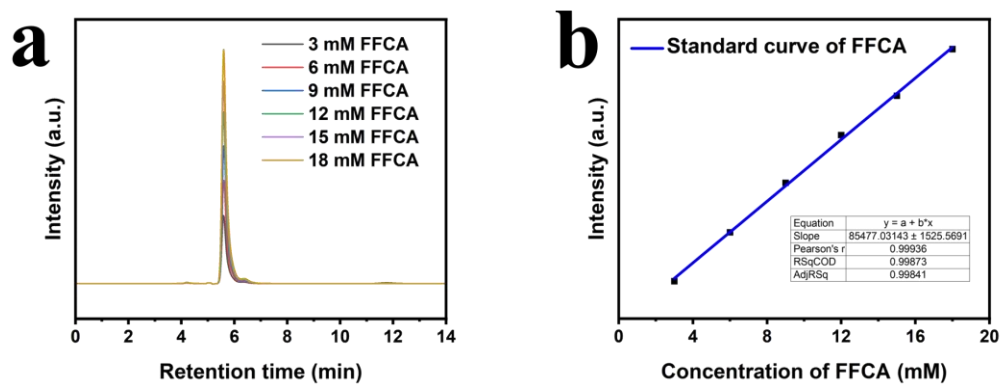
**Fig. S15.** (a) HPLC measurements of pure HMF. (b) Calibration of HPLC for HMF.



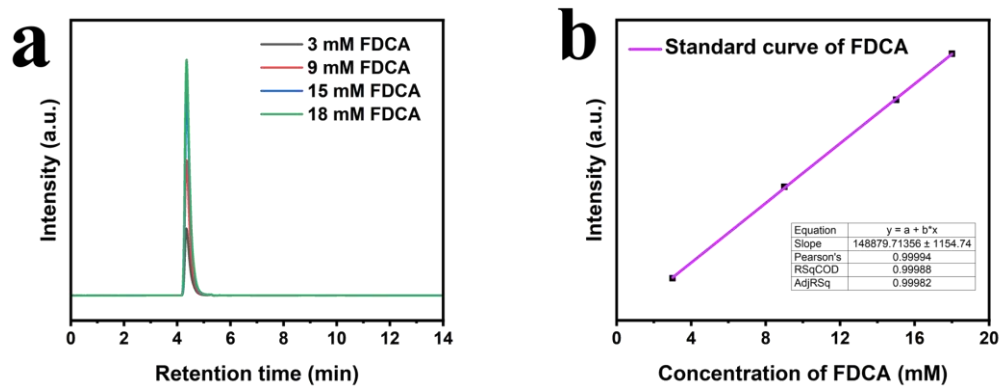
**Fig. S16.** (a) HPLC measurements of pure HMFCA. (b) Calibration of HPLC for HMFCA.



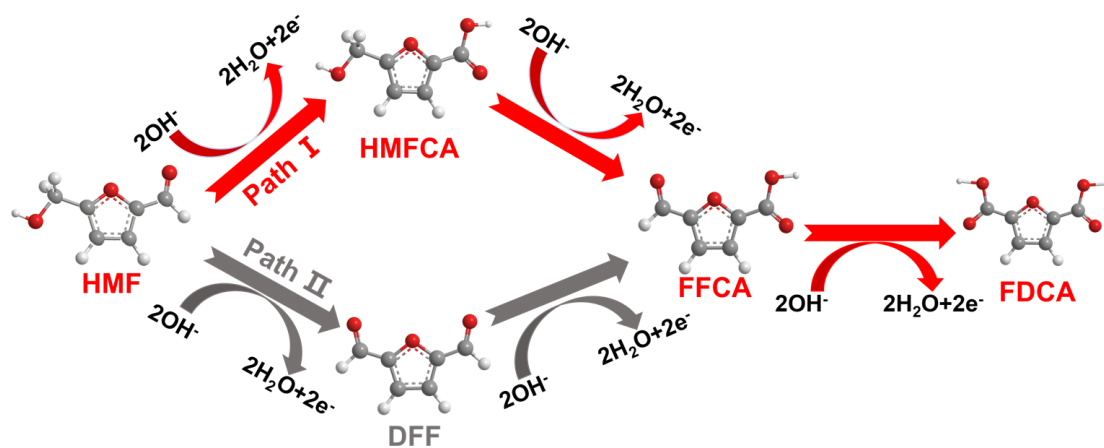
**Fig. S17.** (a) HPLC measurements of pure DFF. (b) Calibration of HPLC for DFF.



**Fig. S18.** (a) HPLC measurements of pure FFCA. (b) Calibration of HPLC for FFCA.

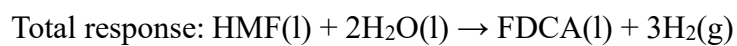
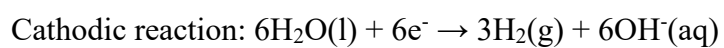
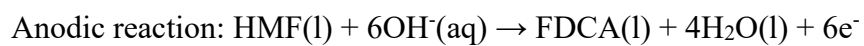


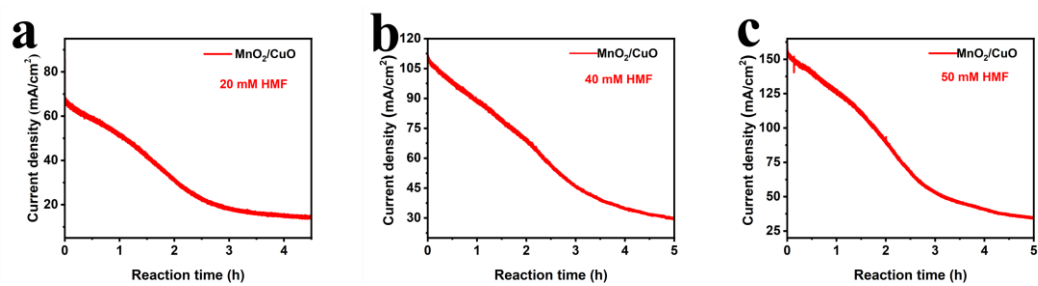
**Fig. S19.** (a) HPLC measurements of pure FDCA. (b) Calibration of HPLC for FDCA.



**Fig. S20.** Two alternative pathways for HMFOR.

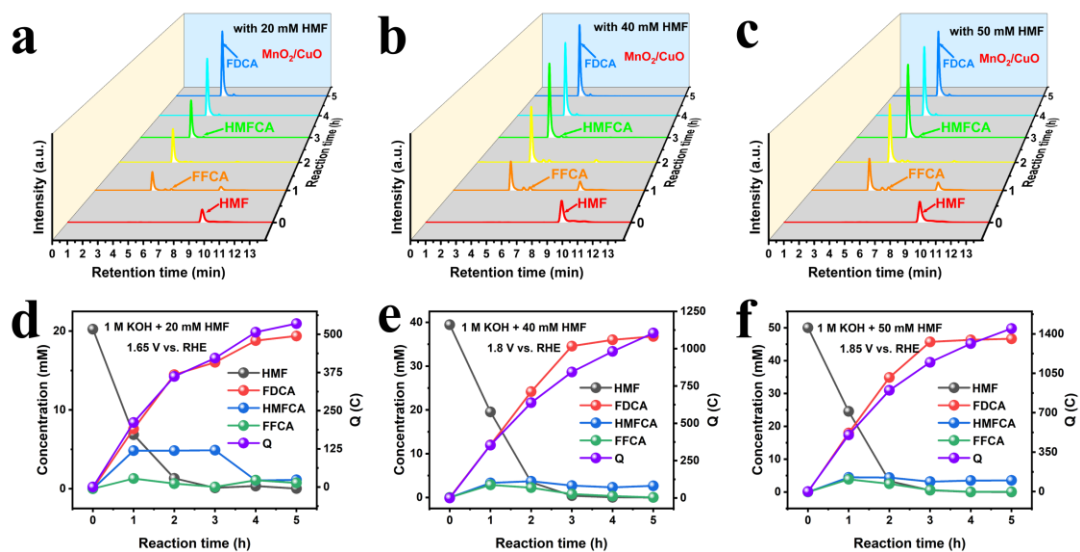
The following reactions are performed at the anode and cathode of the cell:



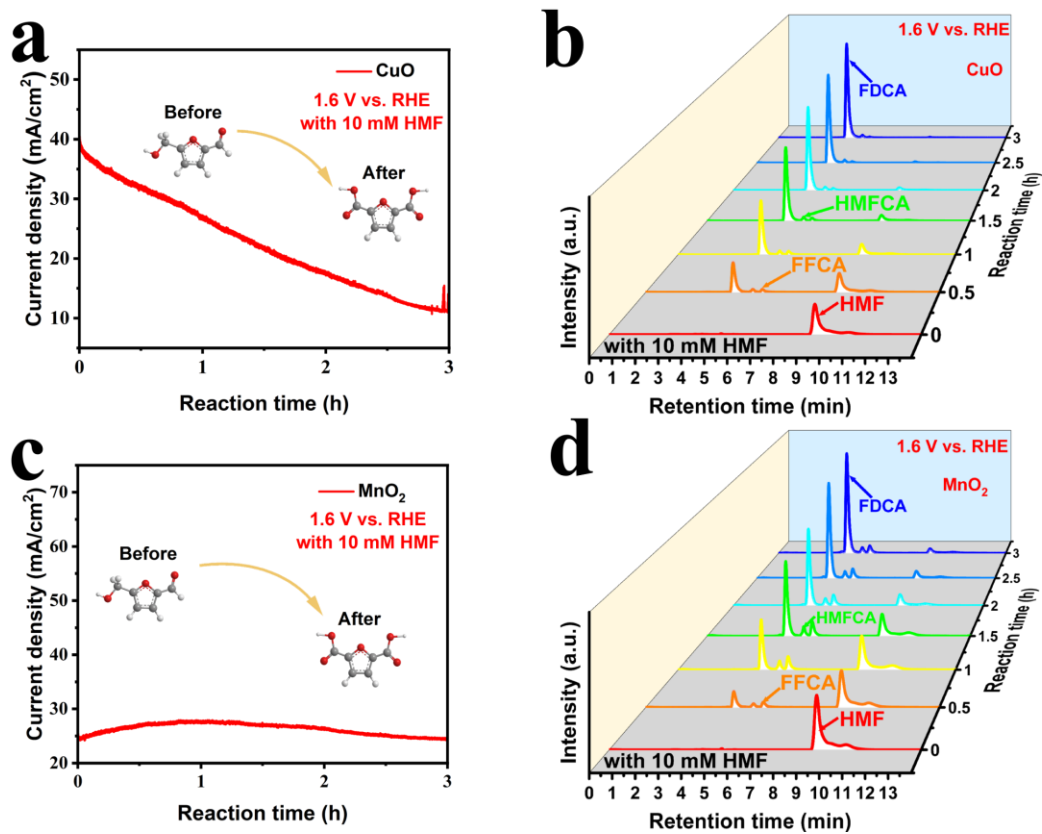


**Fig. S21.** The curve of current density vs time over the MnO<sub>2</sub>/CuO (1.0 M KOH) (a) 20 mM HMF. (b) 40 mM HMF. (c) 50 mM HMF.

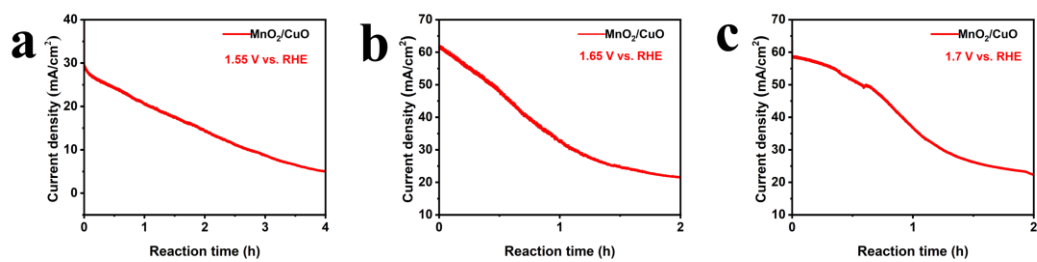




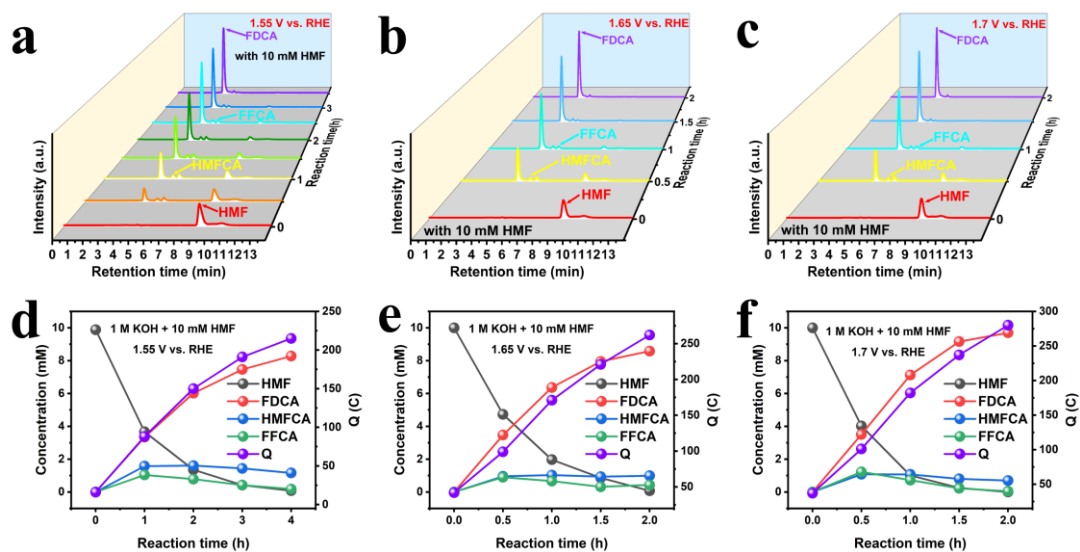
**Fig. S22.** HPLC chromatogram of  $\text{MnO}_2/\text{CuO}$  at (a) 20 mM, (b) 40 mM and (c) 50 mM HMF concentrations. Concentration of HMF, FDCA, HMFCa, FFCA and total charge vs time over the  $\text{MnO}_2/\text{CuO}$  (d) 20 mM, (e) 40 mM and (f) 50 mM HMF concentrations.



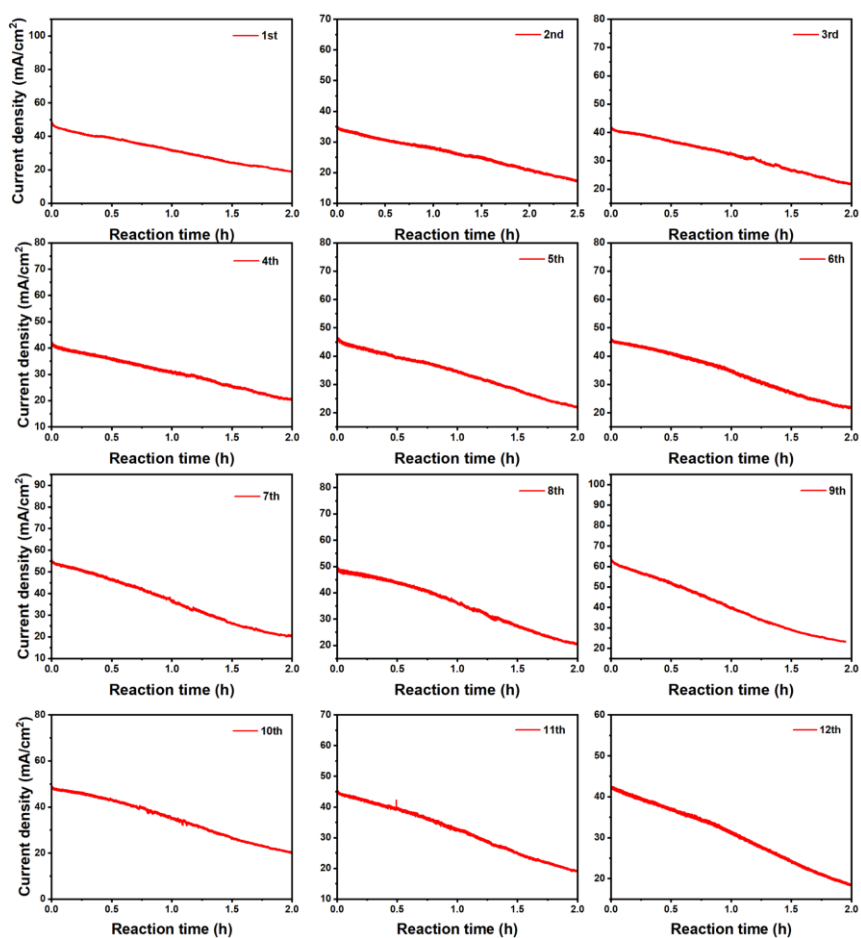
**Fig. S23.** The curve of current density vs time over (a) CuO, and (c) MnO<sub>2</sub>. HPLC chromatogram of the (b) CuO, and (d) MnO<sub>2</sub>.



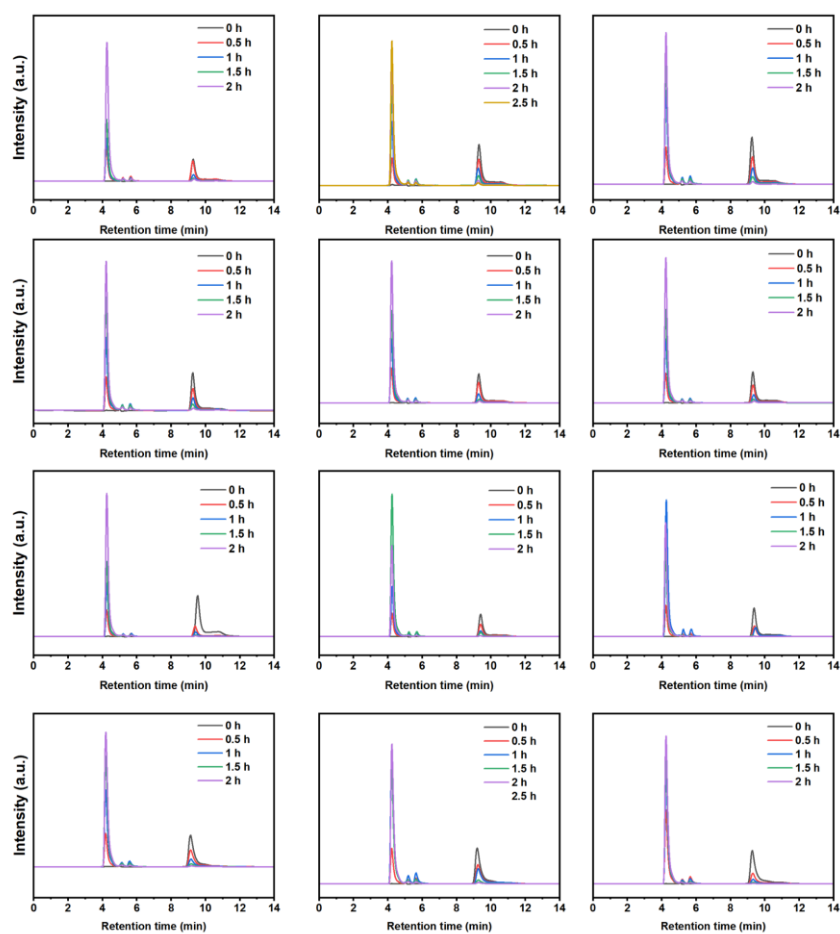
**Fig. S24.** The curve of current density vs time over the MnO<sub>2</sub>/CuO at (a) 1.55 V<sub>RHE</sub>, (b) 1.65 V<sub>RHE</sub>, and (c) 1.7 V<sub>RHE</sub> (10 mM HMF, 1 M KOH). HPLC chromatogram of the MnO<sub>2</sub>/CuO at (d) 1.55 V<sub>RHE</sub>, (e) 1.65 V<sub>RHE</sub>, and (f) 1.7 V<sub>RHE</sub> (10 mM HMF, 1.0 M KOH).



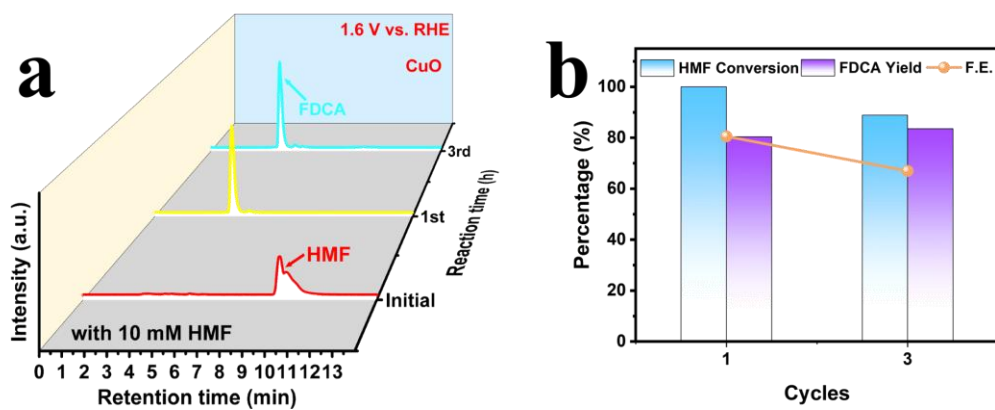
**Fig. S25.** HPLC chromatogram of the MnO<sub>2</sub>/CuO at (a) 1.55 V<sub>RHE</sub>, (b) 1.65 V<sub>RHE</sub>, and (c) 1.7 V<sub>RHE</sub> (10 mM HMF, 1.0 M KOH). Concentration of HMF, FDCA, HMFCFA, FFCA and total charge vs time over the MnO<sub>2</sub>/CuO at (d) 1.55 V<sub>RHE</sub>, (e) 1.65 V<sub>RHE</sub>, and (f) 1.7 V<sub>RHE</sub> (10 mM HMF, 1.0 M KOH).



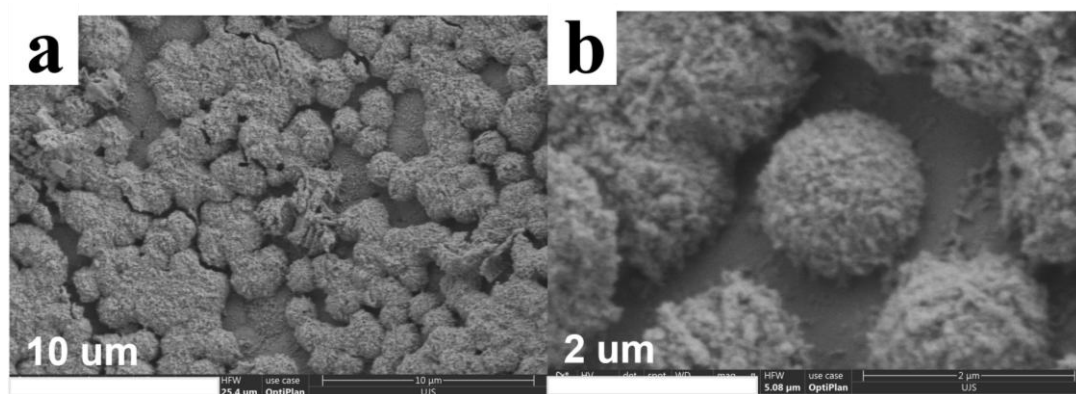
**Fig. S26.** The curve of current density vs time over the MnO<sub>2</sub>/CuO (1.0 M KOH, twelve consecutive cycles)



**Fig. S27.** HPLC chromatogram of twelve consecutive cycles of MnO<sub>2</sub>/CuO.

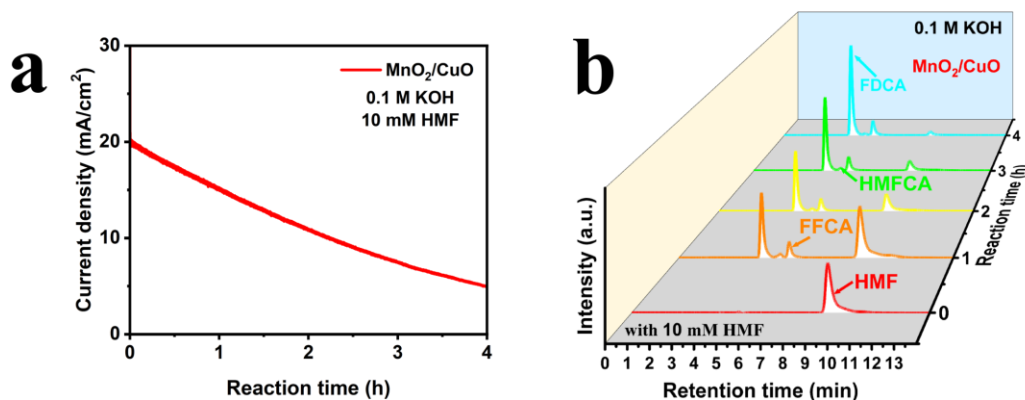


**Fig. S28.** (a) HPLC chromatogram of the CuO (three cycles). (b) HMF conversion, FDCA yield and FE over CuO during three successive of HMF oxidations ( $1.6 V_{\text{RHE}}$ , 10 mM HMF, 1.0 M KOH).



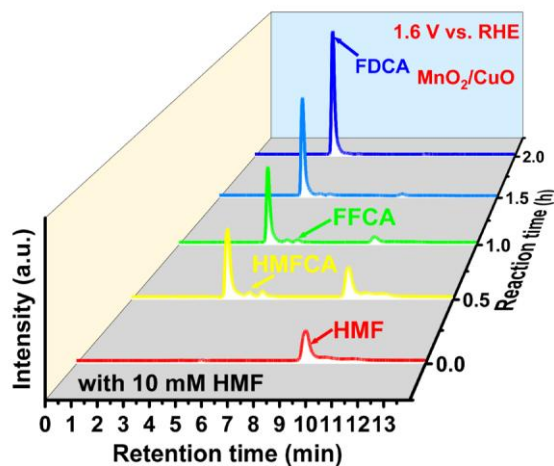
**Fig. S29.** SEM images of MnO<sub>2</sub>/CuO after twelve consecutive cycles(low magnification).





**Fig. S30.** (a) The curve of current density vs time over the MnO<sub>2</sub>/CuO (10 mM HMF, 0.1 M KOH). (b) HPLC chromatogram of the MnO<sub>2</sub>/CuO (10 mM HMF, 0.1 M KOH).

The effect of low OH<sup>-</sup> concentration (0.1 M KOH) on the selectivity during HMFOR is also investigated. Compared with 1 M KOH, the HMF conversion and FDCA yield of the reaction decreased. Interestingly, DFF is not found in the intermediate during the reaction. Therefore, it further confirms that reaction pathway I takes the dominant position. The concentration of intermediate FFCA is noticeably higher than that of HMFCFA in 0.1 M KOH. However, in 1 M KOH, the concentration of HMFCFA is distinctly higher than that of FFCA. The concentration of the intermediate FFCA is significantly higher than that of HMFCFA in 0.1 M KOH, which is different from the results in 1.0 M KOH. Therefore, it is speculated that the oxidation of FFCA to FDCA is the rate-determining step (RDS) of HMFOR in 0.1 M KOH. Whereas, in 1.0 M KOH solution, the conversion of HMFCFA to FFCA is the RDS of the HMFOR reaction.



**Fig. S31.** HPLC chromatogram of the  $\text{MnO}_2/\text{CuO}$  in flow electrolytic cell (10 mM HMF, 1.0 M KOH).

Compared with H-type electrolytic cell, the continuous flow electrolytic cell can realize the continuous supply of reactants and product of FDCA, which effectively prevents the polarization of solution concentration and improves the mass transfer efficiency of substances. The  $\text{MnO}_2/\text{CuO}$  with an area of 1  $\text{cm}^2$  are prepared and mounted on the anode of the continuous flow electrolytic cell, and proton exchange membrane is installed between the anode and the cathode. Experiments in a continuous flow electrolytic cell can better simulate the actual industrial production and provide strong evidence for the practical application value of the catalyst.

**Table S1.** Comparison of HMFOR performance for MnO<sub>2</sub>/CuO and other reported catalysts

Entry	Catalyst	Potential (V vs.RHE)	HMF concentration (mM)	Electrolyte	FDCA Yield (%)	FE (%)	Ref
1	Cu NPS with Fe <sup>3+</sup>	1.57	10	1.0 M KOH	70.3	70.3	[1]
2	Co <sub>1</sub> Cu <sub>1</sub> -CH	1.57	10	1.0 M KOH	90.0	70.0	[2]
3	Ni <sub>x</sub> Co <sub>3-x</sub> O <sub>4</sub>	1.60	10	1.0 M KOH	-	78.0	[3]
4	CuO/Co <sub>3</sub> O <sub>4</sub>	1.60	10	1.0 M KOH	-	79.8	[4]
5	N-MoO <sub>2</sub> /Ni <sub>3</sub> S <sub>2</sub>	1.57	10	1.0 M KOH	90.0	90.0	[5]
6	Ni MOF/Ag	1.623	10	1.0 M KOH	98.6-	98.6-	[6]
7	NF@Co <sub>3</sub> O <sub>4</sub> /CeO <sub>2</sub>	1.60	10	1.0 M KOH	30.2	55.2	[7]
8	Co <sub>3</sub> O <sub>4</sub> -NiO-500	1.45	10	0.1 M KOH	83.33	89.47	[8]
9	CuO-PdO	-	50	1.0 M KOH	96.2	93.7	[9]
10	CF-CuO/CeO <sub>2</sub>	1.61	10	1.0 M KOH	99.7	97.9	[10]
11	Cu <sub>2</sub> P <sub>7</sub> -CoP (1 : 5)	1.43	10	1.0 M KOH	98.8	98	[11]
12	14%Ce-Ni(OH) <sub>2</sub>	1.56	10	1.0 M KOH	97.8	86.6	[12]
13	P-Co <sub>3</sub> O <sub>4</sub> -NBA@N F	1.636	10	1.0 M NaOH	96.9	97.0	[13]
14	NiS <sub>x</sub> /Ni <sub>2</sub> P	1.46	10	1.0 M KOH	98.5	95.1	[14]
15	NiO/CeO <sub>2</sub> @NF	1.575	10	1.0 M KOH	90.0	83.0	[15]
16	MnO <sub>2</sub> /CuO	1.60	10	1.0 M KOH	98.0	98.2	<b>This work</b>

## References

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spectroscopy coupled with an Fe<sup>3+</sup> probe. *Applied Catalysis B: Environmental* **2022**, *317*, 121776.

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