A Direct Approach to Zn²⁺ Pre-Intercalated V₂O₅ Cathodes with Superior Electrochemical Performance for Aqueous Zinc-Ion Batteries

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List of Content

- 1. Chemicals
- 2. Physicochemical Characterization
- 3. Electrochemical measurements
- 4. Assembly of coin cell
- 5. Computational Details
- 1) Figure S1. XRD pattern of VOPO₄.2H₂O.
- 2) Figure. S2. XRD pattern of synthesized pure (a) ZnO and (b) Zn_xV₂O₅.nH₂O
- 3) **Figure S3.** FTIR pattern of V_2O_5 and $Zn_xV_2O_5 \cdot nH_2O$
- 4) **Figure S4.** XPS high-resolution spectrum of (a) V 2p, (b) O 1s (c) Zn 2p, and (d) C 1s of Zn_xV₂O₅·nH₂O.
- 5) **Figure S5.** FESEM of VOPO₄.2H₂O
- 6) **Figure S6.** Contributions of surface and diffusion-controlled processes to the overall CV profile of Zn_xV₂O₅·nH₂O at 5 mVs-1 and 50 mVs⁻¹.
- 7) **Figure S7.** CV and GCD profile of Zn_xV₂O₅·nH₂O with Nafion as separator.
- 8) FigureS8. GCD profile of Zn_xV₂O₅·nH₂O synthesized used Zn alloy strip
- 9) **FigureS9.** EIS spectra of V_2O_5 and $Zn_xV_2O_5 \cdot nH_2O$.
- 10) **Figure S10 (a, b,c)** FESEM, EDX, and elemental mapping of Zn_xV₂O₅·nH₂O after cycling.
- 11) Figure S11. XRD spectra of Zn_xV₂O₅·nH₂O at various charging and discharging step.
- 12) **Figure S12 (a, b)** PDOS of V_2O_5 and $Zn_xV_2O_5 \cdot nH_2O$.
- 13) **Table S1** Comparison Table of reported pre-intercalated Zn²⁺ in V₂O₅

1. Chemicals

Vanadium Pentoxide (V_2O_5)-99%, Phosphoric Acid (H_3PO_2 were purchased from SRL Chemical. Zinc Strip was purchased from BATSOL India. Throughout the synthesis, deionized water (Millipore DI water, 18.2 M Ω cm-1) was used.

- **2. Physiochemical Characterization:** Powder X-ray diffraction (PXRD) was performed on a Bruker AXA D8 Advance diffractometer using monochromatic Cu K α radiation (λ = 1.54 Å) over a 2 θ range of 5–80° with a step size of 0.02° min⁻¹. Morphological and elemental analyses were conducted via field-emission scanning electron microscopy (FE-SEM, JEOL 7610F Plus) equipped with energy-dispersive X-ray spectroscopy (EDS). Fourier-transform infrared (FTIR) spectra were recorded on a Bruker Tensor 27 spectrometer in the 400–4000 cm⁻¹ range. X-ray photoelectron spectroscopy (XPS) was carried out using a Shimadzu spectrometer with an Al K α source (1486.7 eV).
- **3. Electrochemical measurements:** The electrochemical properties of the electrodes were tested using Autolab 204 potentiostat and NEWARE battery test system to carry out the electrochemical performance of the electrode.
- **4. Assembly of coin cell:** Coin cells were assembled to evaluate the electrochemical performance of both pristine V₂O₅ and Zn-intercalated V₂O₅·nH₂O (Zn_xV₂O₅·nH₂O) cathodes. The cathode slurry was prepared by mixing the active material (either V₂O₅ or Zn_xV₂O₅·nH₂O), ¹polyvinylidene fluoride (PVDF), and Super P carbon in a weight ratio of 8:1:1 using N-methyl-2-pyrrolidone (NMP) as the solvent. The resulting slurry was uniformly coated onto stainless steel foil and dried to form the cathode electrode. For both cell types, zinc foil was used as the anode, and 3 M Zn(CF₃SO₃)₂ served as the electrolyte. The cells were assembled in a CR2032 coin cell configuration with a standard separator under ambient conditions. The fabrication process was identical for both V₂O₅//Zn and Zn_xV₂O₅·nH₂O//Zn cells, differing only in the choice of active cathode material.
- **5.** Computational Details: First-principles density functional theory (DFT) calculations were performed using the Vienna *ab initio* Simulation Package (VASP). 1,2 The generalized gradient approximation (GGA) with projector-augmented wave (PAW) potentials was employed for both electronic and structural optimizations. A plane-wave cutoff energy of 450 eV and an energy convergence criterion of 10^{-4} eV were applied. Geometry optimizations were carried out with a force convergence threshold of 0.03 eV Å⁻¹ using a $4 \times 4 \times 1$ Monkhorst–Pack K-point grid. For electronic structure calculations, the K-point mesh was refined to $10 \times 10 \times 1$.

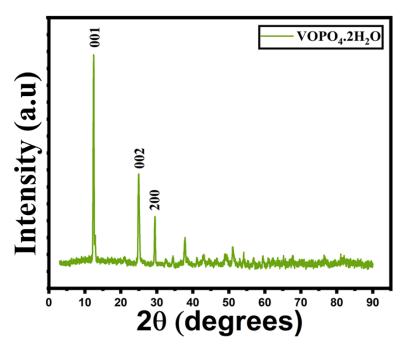


Fig. S1 XRD pattern of VOPO₄.2H₂O

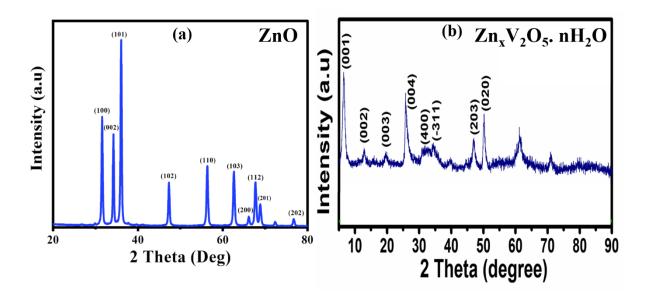


Fig. S2. XRD pattern of synthesized pure (a) ZnO and (b) Zn_xV₂O₅.nH₂O.

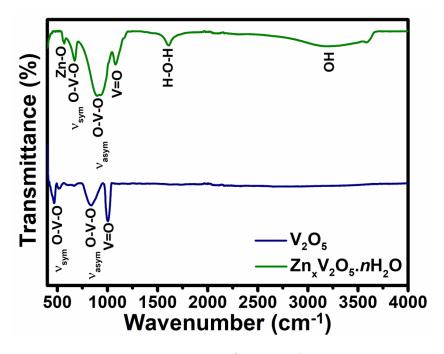


Fig. S3 FTIR spectra of V_2O_5 and $Zn_xV_2O_5 \cdot nH_2O$

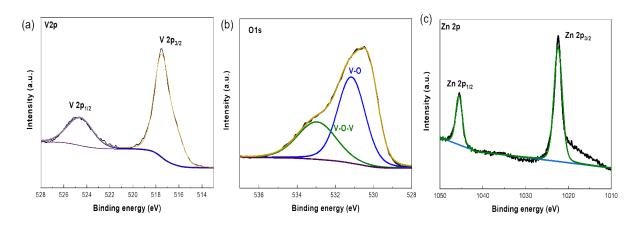


Fig. S4 XPS high-resolution spectra of (a) V 2p, (b) O 1s, and (c) Zn 2p of Zn_xV₂O₅·nH₂O

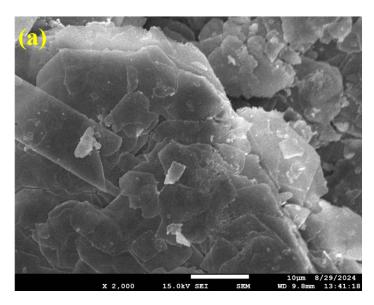


Fig. S5 FESEM of VOPO₄.2H₂O

Dunn's Analysis: To quantify the contributions of surface-controlled and diffusion-controlled processes to the overall capacitance, Dunn's method was employed. This approach expresses the cyclic voltammetric (CV) current response at a given potential as a function of the scan rate (v), considering both capacitive and diffusion-controlled mechanisms, as described by the equation: $\mathbf{i}(\mathbf{v}) = \mathbf{k}_1 \mathbf{v} + \mathbf{k}_2 \mathbf{v}^{1/2} \tag{1}$

where i(v) is the current at a fixed potential and k_1 and k_2 are constant values for the surface-controlled and diffusion-controlled processes, respectively.

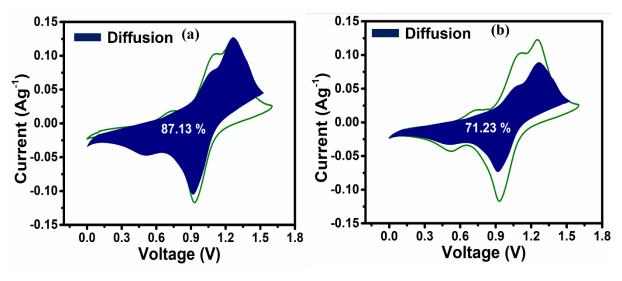


Fig. S6 Contributions of surface and diffusion-controlled processes to the overall CV profile of $Zn_xV_2O_5 \cdot nH_2O$ at 5 mVs⁻¹ and 50 mVs⁻¹.

Evaluation of contribution of H⁺ intercalation in charge storage: The electrochemical behavior of Zn²⁺ intercalation in V₂O₅ must be considered in the context of potential H⁺ cointercalation, particularly given the aqueous electrolyte environment and the inherent proton conductivity of hydrated vanadium oxides (V₂O₅·nH₂O). The smaller ionic radius and higher mobility of H⁺ ions facilitate their preferential insertion into interlayer galleries, especially during initial discharge stages, where they participate in charge compensation during the V⁵⁺/V⁴⁺ redox process. This hypothesis is supported by both the observed 0.3 pH unit decrease in 3 M Zn(CF₃SO₃)₂ electrolyte after 20 cycles. Further, control experiments using Nafion proton-exchange membrane separator exhibited dramatically reduced Cyclic voltammetry area and maximum current with reduced capacity (34.6 mAh/g), confirming that H⁺ transport contribution is minimal.⁸

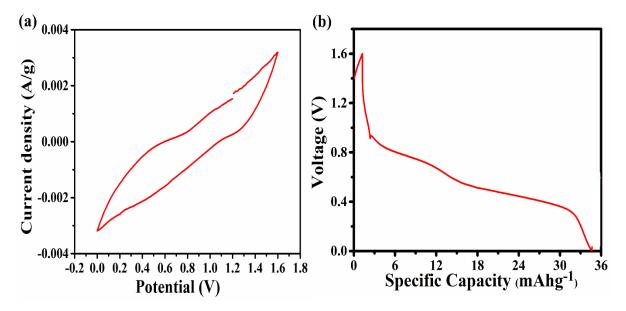


Fig. S7 Electrochemical characterization of Zn_xV₂O₅·nH₂O using Nafion proton-exchange membrane separator. (a) Cyclic voltammetry curves (10 mV/s) show complete suppression of redox peaks compared to standard separator (b) Galvanostatic charge-discharge profiles (0.1 A/g) exhibit severely limited capacity (34.6 mAh/g). These control experiments suggest that the contribution of H⁺ intercalation in charge storage is very low compared to the total charge, and Zn²⁺ intercalation is the primary charge storage mechanism.

Performance sensitivity towards type of Zn strip used during hydrothermal process: The quality of zinc sources significantly impacts both Zn²⁺ intercalation efficiency and the reproducibility of hydrothermal synthesis, as metallic zinc serves dual roles as both reducing agent and Zn²⁺ source. Surface oxides (e.g., ZnO/Zn(OH)₂) and metallic impurities (Fe, Pb, Cu) were found to alter dissolution kinetics and vanadium redox states, with control experiments demonstrating a capacity reduction (280 vs. 324 mAh g⁻¹) when using commercial zinc alloy versus high-purity foil (99.99%). These results, underscore the necessity of employing rigorously cleaned (acid-etched/polished), high-purity zinc to ensure consistent intercalation behaviour and optimal electrochemical performance.

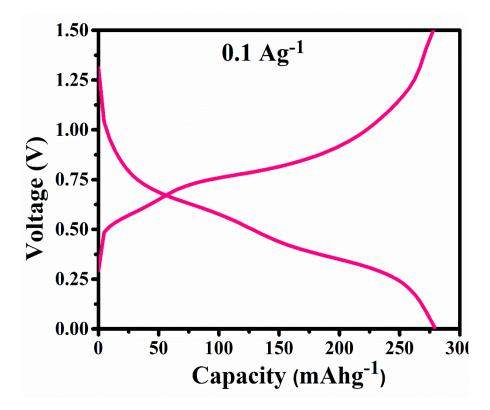
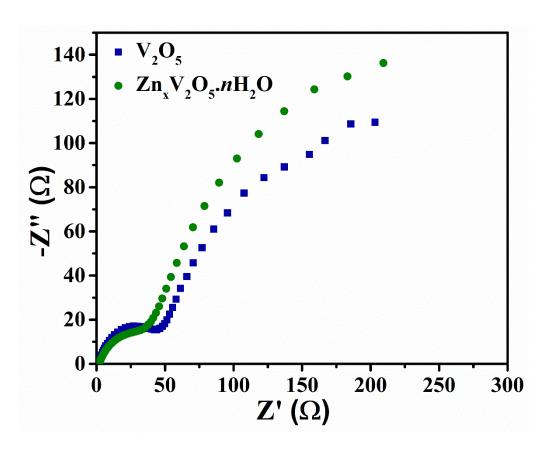


Fig. S8 Galvanostatic charge-discharge (GCD) profiles of Zn_xV₂O₅·nH₂O synthesized using a commercial zinc alloy strip (3 M Zn(CF₃SO₃)₂ electrolyte, 50 mA g⁻¹ current density). The reduced specific capacity (280 mAh g¹ vs. 324 mAh g¹ for high-purity Zn foil) highlights the detrimental effects of alloy-derived impurities on Zn²⁺ intercalation kinetics and redox stability.



 $\textbf{Fig. S9} \ EIS \ spectra \ of \ V_2O_5 \ and \ \ Zn_xV_2O_5 \cdot nH_2O.$

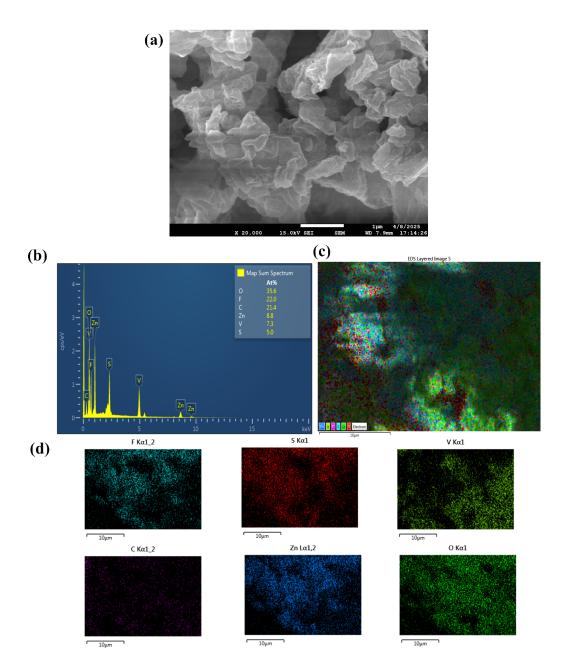


Fig. S10 (a,b,c,d) FESEM, EDX and elemental mapping of $Zn_xV_2O_5\cdot nH_2O$ after cycling.

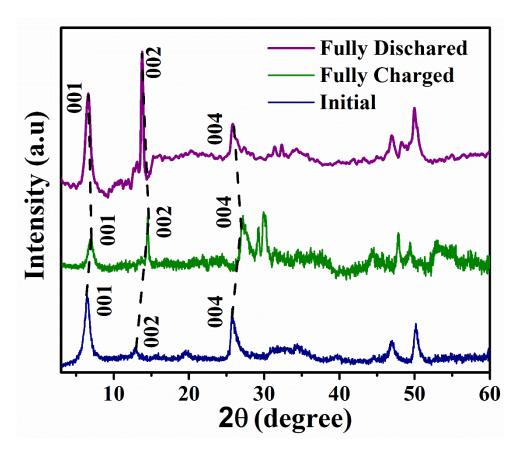


Fig. S11 XRD spectra of Zn_xV₂O₅·nH₂O at various charging and discharging steps.

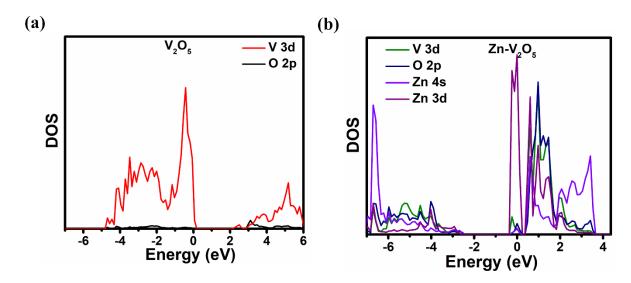


Fig. S12 (a, b) PDOS of V₂O₅ and Zn_xV₂O₅·nH₂O.(Zn_xV₂O₅·nH₂O featuring significant enhanced Zinc 3d contribution near Fermi level).

Table S1. Comparison Table of reported pre-intercalated Zn^{2+} in V_2O_5

S. No	Cathode	Method	Specific Capacity	Retention/Cycle	Energy Density (0.1 Ag ⁻¹)	Capacity Retention (%) (0.1 Ag ⁻¹ - 5 Ag ⁻¹)	Ref
1	$Zn_{0.25}V_2O_5 \cdot nH_2O$	Microwave Hydrothermal method	300 mAh g ⁻¹	80%/1000	450Wh ⁻¹		3
2	Zn _x V ₂ O ₅ ·nH ₂ O	Hydrothermal method	295 mAh g ⁻¹	48%/100		80% (0.1 Ag ⁻¹ - 2Ag ⁻¹)	4
3	Zn _{0.3} V ₂ O ₅ ·1.5H ₂ O	Hydrothermal method	426.3 mAh g ⁻¹	96%/20000	274 Wh kg ⁻¹	78.4 % (0.1 Ag ⁻¹ - 5 Ag ⁻¹)	5
4	ZVO	Microwave Hydrothermal method	355 mAh g ⁻¹	84%/500		50% (0.1 Ag ⁻¹ - 2Ag ⁻¹)	6
5	Zn-V ₂ O ₅ ·nH ₂ O	Sol-gel/Freez Drying	140 mAh g ⁻¹	137%/100		64% (0.1 Ag ⁻¹ - 1Ag ⁻¹)	7
6	Zn _x V ₂ O ₅ · nH ₂ O	Zinc Strip in Hydrothermal method	324 mAh g ⁻¹	97.3%/5000	231 Wh kg ⁻¹	85 % (0.1 Ag ⁻¹ - 5Ag ⁻¹)	This Work

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