## **Supporting Information**

# Synthesis of 2-Imidazolidinone from Ethylenediamine using CO<sub>2</sub> as a C1 building block over the SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> catalyst

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#### Contents.

- 1. Experimental section
- 2. Characterization techniques.
- 3. Computational Details.
- 4. Figure S1. PXRD pattern of 10 SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> catalyst.
- 5. **Figure S2**. FT-IR spectrum of  $SnO_2$ ,  $g-C_3N_4$  and 5, 10, and 15  $SnO_2$ /  $g-C_3N_4$  catalyst.
- 6. **Fig. S3** (a, b) TEM, (c) HRTEM, and (d) SAED pattern of the  $10 \text{ SnO}_2/\text{g-C}_3\text{N}_4$  catalyst.
- 7. Figure S4 EDS spectra of  $10 SnO_2/g-C_3N_4$  catalyst.
- 8. **Figure S5** Elemental mapping image (a-f) of 10 SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> catalyst.
- 9. **Figure S6** XPS spectra of synthesized SnO<sub>2</sub>, and 10 SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> catalyst: (a,b) survey spectrum, (c,d) Sn 3d, and (e,f) O 1s spectrum.
- 10. Table S1. XPS result of SnO<sub>2</sub> and 10 SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> catalyst.
- 11. TGA analysis.
- 12. Figure S7 TGA curve of pure  $SnO_2$ ,  $g-C_3N_4$ , and  $10 SnO_2/g-C_3N_4$  materials.
- 13. Figure S8 N<sub>2</sub>-physisorption isotherm and pore size distribution curve of 10 SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> composite.
- 14. Catalytic activity test.
- 15. Figure S9 GC-MS chromatogram of the reaction mixture after 2 h.
- 16. Figure S10 Mass spectra of 2-imidazolidinone confirmed by GC-MS analysis.
- 17. Table S2: Reaction of different substrate a
- 18. Figure S11 Effect of different reaction parameters on the conversion of ethylenediamine to 2-imidazolidinone over  $10 \text{ SnO}_2/\text{g-C}_3\text{N}_4$ .
- 19. Reusability test.
- 20. Figure S12 The reusability test of the 10 SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> catalyst.
- 21. Figure \$13 PXRD patterns of the 10 SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> before and after 4<sup>th</sup> cycle.
- 22. Figure S14 TEM, HRTEM and SAED pattern of 10 SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> fresh and spent catalyst after 4<sup>th</sup> cycle.
- 23. Figure S 15 XPS spectra of the 10 SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> fresh and spent catalyst after 4<sup>th</sup> cycle.
- 24. Figure S16 FTIR spectra of the  $10 \text{ SnO}_2/\text{g-C}_3\text{N}_4$  fresh and spent catalyst after  $4^{th}$  cycle.
- 25. **Figure S17** (a) Charges on atoms in the topmost surface layer and (b) charge density difference on the  $SnO_2/g$ - $C_2N_4$  surface.
- 26. **Table S3** Comparison results of synthesis of ethylene urea (EU) from ethylenediamine (EDA) and ethylenediamine carbamate (EDA-CA).
- 27. References.

#### **Experimental section**

#### Chemicals

Stannic Chloride Anhydrous (SRL chemicals India), Methanol (Finar), Ammonia Solution (Qualigens), Melamine (Alfa Aesar), ethylenediamine (Alfa Aesar), ethanolamine (Loba Chemie Pvt. Ltd.), tridecane (TCI).

#### Synthesis of SnO<sub>2</sub> nanoparticles

Nanocrystalline tin oxide  $SnO_2$  has been prepared by the conventional precipitation method.<sup>1</sup> 2.602 g (10 mmol) of anhydrous stannic chloride is dissolved in 100 ml of methanol and continued the stirring for 15 minute to dissolve it completely. It was followed by dropwise addition of ammonia solution  $NH_3.H_2O$  to alc. solution of tin chloride at room temperature. Then we adjust the pH of the mixed solution to 8 and obtained a white precipitate of tin oxide. The solution was remained still for 1 hour with continuous stirring. The obtained product was taken for centrifugation and washed with methanol and deionised water several times to remove chloride ions coming from stannic chloride. The resulting product was dried at 100 °C for 24 h in drying oven and calcined in muffle furnace at 400°C temperature for 4 h.

#### Synthesis of g-C<sub>3</sub>N<sub>4</sub>

The g-C<sub>3</sub>N<sub>4</sub> was obtained by directly heating the melamine (nitrogen-rich organic compound). Melamine (6 g) was placed in porcelain crucible and calcined it at 550°C in muffle furnace for 4 h with the heating rate of 5°C/min. The calcined product was then grinded in mortar and pestle, a pale-yellow colour powdered g-C<sub>3</sub>N<sub>4</sub> obtained.<sup>2</sup>

#### Synthesis of SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> nanocomposites

Different weight percent of  $SnO_2$  used for synthesizing the catalyst, like 5 wt. %, 10 wt. %, 15 wt. % of  $SnO_2$ , and impregnated it with  $g-C_3N_4$  in distilled water. A 10 wt. %  $SnO_2/g-C_3N_4$  catalyst have been prepared by taking 0.1 g  $SnO_2$  powder and impregnating it with 1 g of  $g-C_3N_4$ , both dissolved in 25 ml of distilled water in a 100 ml beaker. A resulting mixture was stirred and heating simultaneously at 100 °C till the water gets evaporated completely. Then the beaker was kept inside the hot oven at 100 °C for a day, so that the catalyst is completely moisture free. The obtained powder was grinded properly to fine powder form.

#### Synthesis of in-situ SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> Composite

In a 100 mL beaker, 0.219 g of anhydrous stannic chloride was dissolved in 10 mL of methanol under continuous stirring. Separately, 0.9 g of as-prepared g- $C_3N_4$  was dispersed in 25 mL of deionized water and stirred for 30 min. The stannic chloride solution was then added dropwise to the g- $C_3N_4$  dispersion, followed by a further 30 min of stirring. Subsequently, ammonia solution ( $NH_3$ - $H_2O$ ) was added dropwise to adjust the pH to 8, and the mixture was stirred for an additional 2 h to facilitate precipitation. The resulting solid was collected by centrifugation, thoroughly washed with deionized water and methanol, and dried overnight at 100 °C. Finally, the product was calcined at 400 °C for 2 h to obtain the  $SNO_2/g$ - $C_3N_4$  composite catalyst.

### Characterization techniques:

The crystalline structure of the samples was analyzed using X-ray diffraction (XRD) on a Rigaku SmartLab high-resolution diffractometer (HRXRD) equipped with Cu Kα radiation. The measurements were carried out in the 2θ range of 10°–80°, with a scanning rate of 6° min<sup>-1</sup> and a step size of 0.02°. Fourier transform infrared (FTIR) spectra of all samples and reaction products were obtained using a PerkinElmer GX spectrometer (USA) within the wavenumber range of 4000–400 cm<sup>-1</sup>, employing KBr pellet techniques. High-resolution transmission electron microscopy (HRTEM) was conducted on a Talos F200X G2 instrument (Thermo Scientific, USA) operated at 200 kV to study the crystallite size, exposed crystal facets, and morphology. For TEM analysis, the metal oxide powders were dispersed in ethanol and drop-cast onto copper grids, followed by drying. X-ray photoelectron spectroscopy (XPS) measurements were performed using a PHI 5000 Versa Probe III spectrometer (USA) with Al Kα (1486.6 eV) radiation as the excitation source, and the binding energies were calibrated against the C 1s peak at 284.6 eV.³ Nitrogen adsorption—desorption experiments were conducted using a Micromeritics ASAP 2020 analyzer to determine the surface area, pore volume, and pore size distribution of the samples. Prior to measurements, all samples were degassed under high vacuum at 200 °C for 3 h to eliminate adsorbed gases and moisture. The Brunauer–Emmett–Teller (BET) method was used to calculate the specific surface area (S<sub>BET</sub>) of the materials. The acid–base characteristics of the samples were analyzed using temperature-programmed desorption of ammonia (NH<sub>3</sub>-TPD) and carbon dioxide (CO<sub>2</sub>-TPD), conducted on an Altamira AMI-300 Lite instrument. Before the adsorption analysis, the samples were

pretreated under an argon flow (40 mL min<sup>-1</sup>) at 150 °C for 1 h. After cooling to room temperature, the gas flow was switched to NH<sub>3</sub> or CO<sub>2</sub> (40 mL min<sup>-1</sup>) for 1 h to allow adsorption. Subsequently, any physisorbed NH<sub>3</sub> or CO<sub>2</sub> was removed by purging with argon at room temperature for 1 h. The desorption step was then carried out in argon (40 mL min<sup>-1</sup>), heating from room temperature to 600 °C at a rate of 10 °C min<sup>-1</sup>. Thermogravimetric analysis (TGA) was performed using a PerkinElmer STA 6000 instrument in the temperature range of 25–800 °C under a continuous flow of nitrogen gas. Electron paramagnetic resonance (EPR) analysis was conducted using a JEOL JES-X310 spectrometer at both room temperature and 77 K.

#### **Computational Details:**

The surface model was generated by positioning a SnO $_2$ (101) slab on top of a g-C $_3$ N $_4$  sheet, maintaining an interlayer distance of about 3.4 Å. The final supercell consists of 164 atoms and maintains a lattice mismatch below 5%. This combined configuration, hereafter referred to as surface(\*)-was fully relaxed, along with all associated reaction intermediates, using the Quantum ESPRESSO package. Exchange—correlation energy correction has been done using the Perdew—Burke—Ernzerhof (PBE) functional within the Generalized Gradient Approximation (GGA). Electronic and ionic convergence thresholds were set to  $7.35 \times 10^{-7}$  Ry ( $\approx 10^{-5}$  eV) and  $1 \times 10^{-4}$  Ry ( $\approx 0.001$  eV), respectively, and a force tolerance of  $7.78 \times 10^{-4}$  Ry/Bohr (0.02 eV/Å) was applied in all structural optimizations. Brillouin-zone integration was performed using a 3 × 3 × 1 Monkhorst—Pack k-point mesh. Gaussian smearing with a width of 0.01 Ry was used, and long-range dispersion forces were included via the DFT-D3 van der Waals correction with damping. A vacuum layer of 16 Å was added along the z-direction to avoid spurious interactions between periodic images.

The Gibbs free energy change ( $\Delta G$ ) for each reaction step was calculated according to:

where  $\Delta E$  is the DFT-derived energy difference between the adsorbed intermediate and the pristine surface,  $\Delta ZPE$  denotes the zero-point energy correction, and  $\Delta S$  represents the entropy change of both gas-phase and adsorbed species at 298.15 K. $^{11,12}$ 

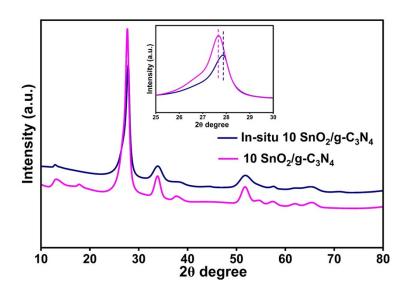


Figure S1. PXRD pattern of 10 SnO₂/g-C₃N₄ catalyst.

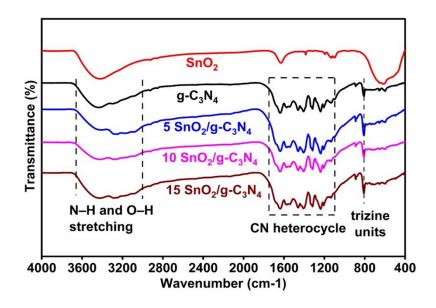


Figure S2. FT-IR spectrum of SnO $_2$ , g-C $_3$ N $_4$  and 5, 10, and 15 SnO $_2$ / g-C $_3$ N $_4$  catalyst.

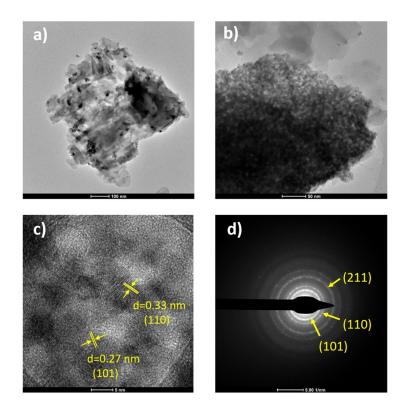


Fig. S3 (a, b) TEM, (c) HRTEM, and (d) SAED pattern of the 10  $SnO_2/g-C_3N_4$  catalyst.

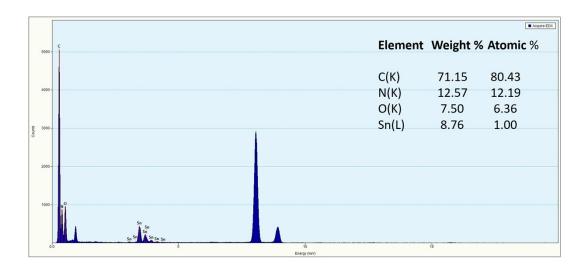


Figure S4 EDS spectra of 10 SnO<sub>2</sub>/g-C<sub>3</sub>N<sub>4</sub> catalyst.

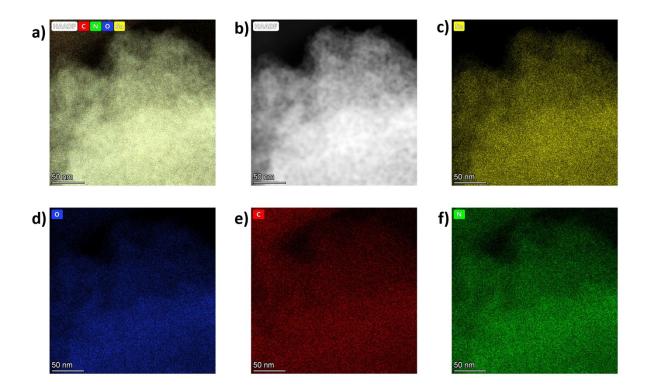


Figure S5 Elemental mapping image (a-f) of 10  $SnO_2/g$ - $C_3N_4$  catalyst.

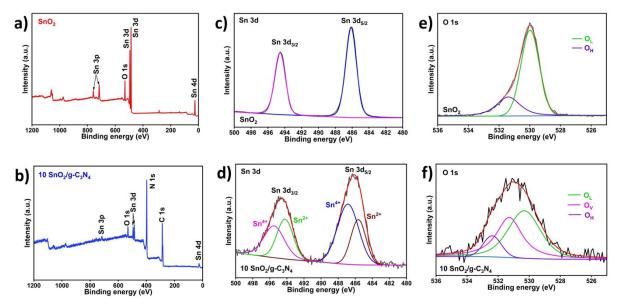


Figure S6 XPS spectra of synthesized  $SnO_2$ , and 10  $SnO_2/g$ - $C_3N_4$  catalyst: (a,b) survey spectrum, (c,d) Sn 3d, and (e,f) O 1s spectrum.

Table S1. XPS result of  $SnO_2$  and 10  $SnO_2/g$ - $C_3N_4$  catalyst.

Catalyst	Element orbital	Peak No.	Binding energy	Assignment
			(eV)	
SnO <sub>2</sub>	Sn 3d	1	486.1	Sn <sup>4+</sup> (3d <sub>5/2</sub> )
		2	494.5	Sn <sup>4+</sup> (3d <sub>3/2</sub> )
	O 1s	1	529.9	$O_L$
		2	531.4	$O_H$
SnO <sub>2</sub> /g-C <sub>3</sub> N <sub>4</sub>	Sn 3d	1	485.6	Sn <sup>2+</sup> (3d <sub>5/2</sub> )
		2	486.8	Sn <sup>4+</sup> (3d <sub>5/2</sub> )
		3	494.2	Sn <sup>2+</sup> (3d <sub>3/2</sub> )
		4	495.5	Sn <sup>4+</sup> (3d <sub>3/2</sub> )
	O 1s	1	530.3	$O_L$
		2	531.2	$O_V$
		3	532.4	$O_H$
	SnO <sub>2</sub>	$SnO_2$ $Sn 3d$ $O 1s$ $SnO_2/g-C_3N_4$ $Sn 3d$	$\begin{array}{cccccccccccccccccccccccccccccccccccc$	SnO <sub>2</sub> Sn 3d 1 486.1 2 494.5 O 1s 1 529.9 2 531.4 SnO <sub>2</sub> /g-C <sub>3</sub> N <sub>4</sub> Sn 3d 1 485.6 2 486.8 3 494.2 4 495.5 O 1s 1 530.3 2 531.2

#### TGA analysis

The thermal stability of  $SnO_2$ ,  $g-C_3N_4$ , and the  $10 SnO_2/g-C_3N_4$  composite was examined in the 25-800 °C temperature range at a heating rate of 10 °C/min under  $N_2$  atmosphere,  $^{13}$  and the corresponding TGA profiles are displayed in (**Figure S7**). For  $g-C_3N_4$ , no significant mass loss was noticed until about 505 °C. A minor weight decrease was then observed between 520 and 631 °C, which can be ascribed to the initial stages of  $g-C_3N_4$  decomposition. This was followed by a sharp decline in mass from 631 to 760 °C, reflecting the intrinsic thermal instability of  $g-C_3N_4$  in this region. At this stage, the pronounced weight reduction was mainly due to the conversion of  $g-C_3N_4$  into volatile carbon- and nitrogen-based species.  $^{13}$  Pure  $SnO_2$ , in contrast, exhibited almost no weight change throughout the heating cycle, confirming its excellent thermal stability. For the  $10 SnO_2/g-C_3N_4$  hybrid, weight loss commenced around 502-635 °C, after which a rapid decrease was recorded between 635 and 745 °C. This indicates that the composite is thermally less stable than its individual components, most likely because of  $SnO_2$  crystallization interfering with the layered framework of  $g-C_3N_4$  or the catalytic action of  $SnO_2$  in accelerating  $g-C_3N_4$  decomposition. A similar trend has been reported for  $ZnO/g-C_3N_4$  composites.  $^{14}$  By approximately 755 °C, the  $10SnO_2/g-C_3N_4$  material was nearly fully decomposed, evidencing its reduced thermal resistance. Overall, the TGA data (Figure S7) suggest that the composite maintains stability only up to around 500 °C.

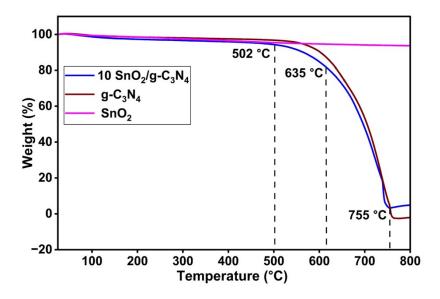


Figure S7 TGA curve of pure  $SnO_2$ ,  $g-C_3N_4$ , and  $10 SnO_2/g-C_3N_4$  materials.

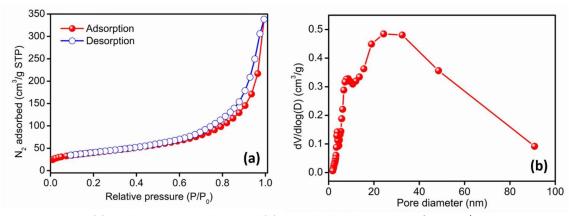


Figure S8 (a)  $N_2$ -physisorption isotherm, and (b) pore size distribution curve of  $10 \, \text{SnO}_2/\text{g-C}_3 N_4$  composite.

#### **Catalytic activity test**

All the reactions executed the in high pressure autoclave reactor with its inner volume of 250 ml. The synthesis of cyclic urea from  $CO_2$  and diamine was as follows: catalyst (250 mg), ethylenediamine (0.1 mol), solvent methanol (80 ml) and internal standard (IS) tridecane (0.1 ml) were together put into autoclave vessel, and then the purging of  $CO_2$  was done (3-4 times). The reactor was then filled with  $CO_2$  to the targeted pressure (2.5 MPa), then we closed the gas line and heated to the desired temperature of the reaction, and constantly stirred at 600 rpm for a fixed time. After the reaction is over, reactor was cooled down to room temperature. The reaction mixture was withdrawn from the vessel, centrifuged, and analyzed using a TRACE 1310 gas chromatograph coupled with an ISQ 7000 single quadrupole mass spectrometer (Thermo Scientific, USA). The conversion of ethylenediamine and selectivity of products were calculated by using tridecane as an internal standard (IS) from eqn. 1 and 2, respectively. 15

Conversion (%) = 
$$\{(C_0 - C_f)/C_0\} \times 100$$
 (1)

Selectivity (%) = 
$$\{C_p/(C_0 - C_f)\}$$
 x 100 (2)

(where,  $C_0$  is initial concentration of ethylenediamine,  $C_f$  and  $C_p$  are concentration of ethylenediamine and the product after the reaction, respectively).

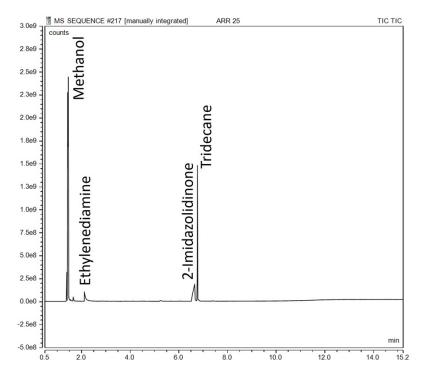
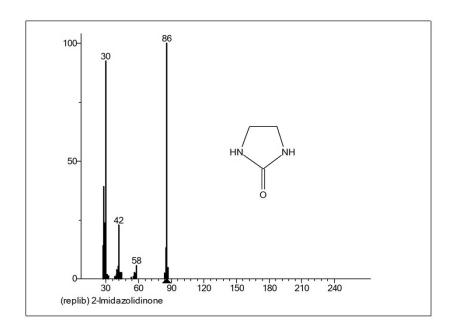


Figure S9 GC-MS chromatogram of the reaction mixture after 2 h.



 $\textbf{Figure S10} \ \text{Mass spectra of 2-imidazolidinone confirmed by GC-MS analysis}.$ 

Table S2: Reaction of different substrate <sup>a</sup>

Entry	Catalyst	Reactant	Solvent	Conv.b (%)	Product	Sel. <sup>c</sup>	Yield
						(%)	
1	10 SnO <sub>2</sub> /g-C <sub>3</sub> N <sub>4</sub>	H <sub>2</sub> N NH <sub>2</sub>	Methanol	95	HN_NH	99	94
2	10 SnO <sub>2</sub> /g-C <sub>3</sub> N <sub>4</sub>	H <sub>2</sub> N OH	Methanol	16	0	96	15
			Propan-2-ol	83	HN	96	80

<sup>&</sup>lt;sup>a</sup>Reaction condition: reactant, (0.1 mol); catalyst, (0.2 g); solvent, (80 ml); temperature, (160° C); time, (2 h); CO<sub>2</sub>, (2.5 MPa).

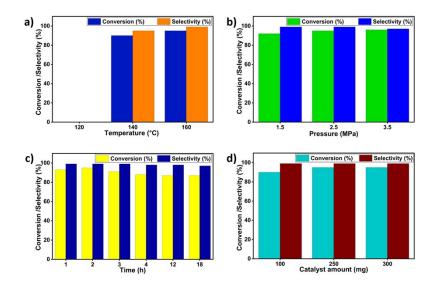
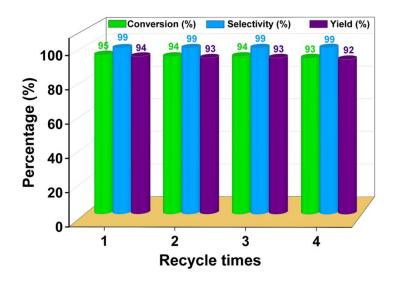


Figure S11 Effect of different reaction parameters on the conversion of ethylenediamine to 2-imidazolidinone over 10  $SnO_2/g-C_3N_4$ : (a) reaction temperature, (b)  $CO_2$  pressure, (c) time, and (d) catalyst amount. Optimized conditions: EDA, 0.1 mol; catalyst, 250 mg; Methanol, 80 ml; tridecane (IS), 0.1 mL; temperature, 160 °C;  $CO_2$  pressure, 2.5 MPa; reaction time, 2 h. During each study, only the parameter of interest was varied while the others were kept constant.

#### **Reusability test**

To evaluate the reusability of the catalyst, the spent  $10 \text{ SnO}_2/\text{g-C}_3\text{N}_4$  was recovered after each reaction cycle by centrifugation, thoroughly washed with distilled water to remove residual organics, and dried at  $120 \,^{\circ}\text{C}$  for  $24 \, \text{h}$ . The recovered catalyst was then reused directly in subsequent reactions without any further treatment. As shown in (**Figure S12**), the catalyst consistently maintained high catalytic activity and yield even after four consecutive cycles. No significant change in conversion or yield was observed, confirming its excellent stability and reusability in the synthesis of cyclic urea. These results highlight the catalyst's robust performance and potential for sustainable catalytic applications.



**Figure S12** The reusability test of the  $10 \text{ SnO}_2/\text{g-C}_3\text{N}_4$  catalyst. Reaction conditions: EDA, 0.1 mol; catalyst, 250 mg; tridecane (IS), 0.1 mL; 160 °C; CO<sub>2</sub> pressure, 2.5 MPa; reaction time, 2 h.

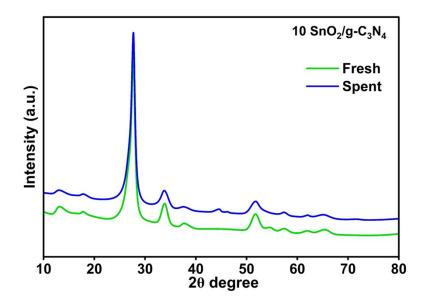
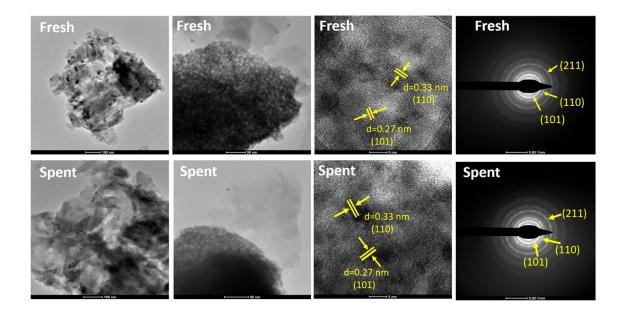


Figure S13 PXRD patterns of the 10 SnO $_2$ /g-C $_3$ N $_4$  before and after 4 $^{th}$  cycle.



 $\textbf{Figure S14} \ \text{TEM, HRTEM and SAED pattern of } 10 \ \text{SnO}_2/\text{g-C}_3\text{N}_4 \ \text{fresh and spent catalyst after } 4^{\text{th}} \ \text{cycle.}$ 

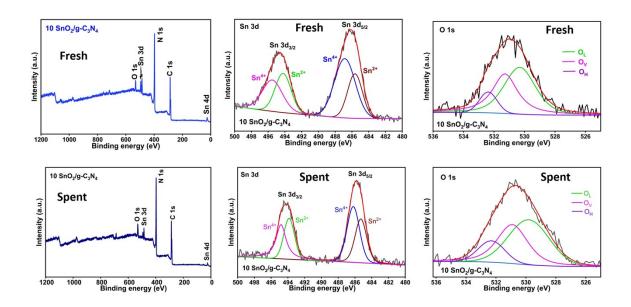


Figure S15 XPS spectra of the  $10 \text{ SnO}_2/\text{g-C}_3\text{N}_4$  fresh and spent catalyst after  $4^{\text{th}}$  cycle.

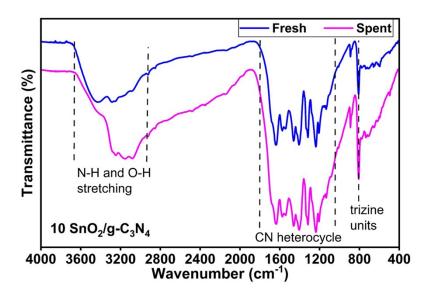


Figure S16 FTIR spectra of the  $10\ SnO_2/g$ - $C_3N_4$  fresh and spent catalyst after  $4^{th}$  cycle.

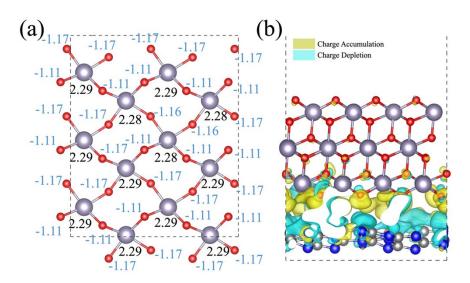


Figure S17 (a) Charges on atoms in the topmost surface layer and (b) charge density difference on the  $SnO_2/g$ - $C_3N_4$  surface.

**Table S3** Comparison results of synthesis of ethylene urea (EU) from ethylenediamine (EDA) and ethylenediamine carbamate (EDA-CA).

Entr y	Catalyst	Condition	Surfac e Area (m²/g)	Acid ity (mm ol/g)	Basi city (mm ol/g)	React or type	Temp (°C)	Time (h)	CO <sub>2</sub> (MP a)	Con v. (%)	Yield (%)	Ref.
1	None	EDA: 1.0 mmol mL <sup>-1</sup> , Catalyst free. Solvent free.	-	-	-	Batch	180	24	10	97	97	16
2	CeO <sub>2</sub>	EDA: 2 mmol, Catalyst: 75 mg, Ethanol: 35 mmol	-	-	-	Batch	160	8	0.7	-	37	17
3	CeO <sub>2</sub>	EDA: (10 mmol), Catalyst: 0.34 g, 2- Propanol: 200 mmol.	78	-	-	Batch	160	12	0.5	97	96	18
4	2.40ZnO/0. 49KF/Al <sub>2</sub> O <sub>3</sub>	20 mmol of amine, 10 Catalyst: wt.% w.r.t amine, Methanol: 3.2 g	113.4	230	130	Batch	180	4	1	96	86	19
5	MOF- derived CeO <sub>2</sub>	EDA: 10 mmol, Catalyst: 200 mg, Isopropanol: 200 mmol	147	24.9 4	88.9 6	Batch	160	12	0.5	95	94	20
6	CeO <sub>2</sub>	EDA-CA: 2.08 g, Catalyst: 0.34 g, 2- propanol: 15 mL	60	-	-	Batch	140	24	-	83	83	21
7	Silica- supported IL	EDA: 5.0 mmol, Catalyst: 20 mg, Solvent free	254	-	-	Batch	100	12	2.5	98	94	22
8	CeO <sub>2</sub>	$F_{EDA-CA} = 0.57 \text{ mmol h}^{-1},$ $F_{Sol} = 0.42 \text{ mL h}^{-1}, CeO_2$ $2.0 \text{ g, W}_{Cat}/F_{EDA-CA} = 3.48 \text{ g h mmol}^{-1}.$	86	94	52	Flow	90	72	-	99	93	23
9	Zr-doped CeO <sub>2</sub>	EDA: 0.6 g, Catalyst 0.2 g, Isopropanol: 19.6 g.	119	-	439 0	Batch	160	3	0.6	91.5	91.5	24
10	10 SnO <sub>2</sub> /g- C <sub>3</sub> N <sub>4</sub>	EDA: 0.1 mol, Catalyst: 250 mg, methanol: 80 ml.	142	295	480	Batch	160	2	2.5	95	94	This wor k

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