

## SUPPLEMENTARY INFORMATION

# Reactions of Fluid and Lattice Oxygen Mediated by Interstitial Atoms at the TiO<sub>2</sub> (110)-Water Interface

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### 1. Method for determination of profile metrics

The metrics  $W$  and  $C_{\min}$  associated with fractionation could be determined by straightforward visual inspection of the profiles. However, the decay constants  $\lambda_1$  and  $\lambda_2$ , along with the net injection flux  $F_{18}$  of <sup>18</sup>O, required more sophisticated methods because  $\lambda_2$  was usually much larger than the depth to which SIMS measurements extended.

Determination of the decay constants exploited the fact that decay of the <sup>18</sup>O concentration beyond the peak obeyed a bi-exponential functional form having two widely separated decay constants, with  $\lambda_1 \ll \lambda_2$ . A practical consequence was that  $\lambda_1$  dominated the change in <sup>18</sup>O concentration near the peak, and  $\lambda_2$  dominated at depths several times  $\lambda_1$  from the peak. In other words, the profile decayed according to  $\lambda_1$  down to an approximate plateau, followed by a much slower decay according to  $\lambda_2$ . The plateau was typically 3-10% higher than the <sup>18</sup>O natural abundance concentration  $C_0$  of  $1.276 \times 10^{20} \text{ cm}^{-3}$ , with larger values occurring at higher temperatures. In each profile, the concentration characterizing this plateau was normalized with respect to  $C_0$  to yield a dimensionless scaling factor  $Z$ , which typically varied from 1.03 to 1.1. Thus, a functional form derived previously<sup>1</sup> for <sup>18</sup>O injection from a surface was adapted to phenomenologically describe the  $\lambda_1$  region according to:

$$C(x) = C_o \left[ \frac{C_{OT}-C_o}{C_o} e^{-\frac{x}{\lambda_1}+b_1} + Z \right] \quad (S1),$$

where  $C$  denotes the concentration of  $^{18}\text{O}$  at depth  $x$  from the surface,  $C_{OT}$  is the total concentration of O atoms in the lattice ( $6.38 \times 10^{22} \text{ cm}^{-3}$ ), and  $b_1$  is a phenomenological amplitude factor. In the  $\lambda_2$  region,  $C$  continued to decay to the natural abundance baseline ( $Z=1$ ) according to a similar adaptation:

$$C(x) = C_o \left[ \frac{C_{OT}-C_o}{C_o} e^{-\frac{x}{\lambda_2}+b_2} + 1 \right] \quad (S2),$$

where  $b_2$  is a second phenomenological amplitude factor.

Eq. (S1) was fitted to the  $\lambda_1$  region of the profile using a nonlinear least squares algorithm to determine  $\lambda_1$ ,  $b_2$  and  $Z$ . The range of depths contributing to the fit lay between  $x=\alpha$ , which is near the peak (determined as described below), and the lesser of either  $\alpha+4\lambda_1$  or the maximum depth to which the SIMS profile extended. For a profile that extended very deep, the fitting process was iterated to ensure self-consistency between the value of  $\lambda_1$  and the depth  $\alpha+4\lambda_1$  used as a boundary of the fitting region. When referenced to  $C_o$ ,  $C$  declines at  $\alpha+4\lambda_1$  to only about 2% of its maximum near the peak. Thus, the value of  $\lambda_1$  exhibits little sensitivity to the exact choice of the deeper boundary. Rarely were more than two iterations needed to achieve self-consistency. When SIMS measurements did not reach all the way to  $x = \alpha+4\lambda_1$ , they usually extended to at least  $\alpha+2.5\lambda_1$ , which proved adequate for nonlinear fitting to extract  $\lambda_1$ ,  $b_1$  and  $Z$ .

The shallow boundary  $\alpha$  of the  $\lambda_1$  region was determined as follows. The contour of the  $^{18}\text{O}$  concentration immediately after the peak grades smoothly into the  $\lambda_1$  region. To delineate a specific boundary in reproducible way, a curvature parameter  $\kappa$  was computed. The parameter quantifies how sharply a function  $y$  bends,<sup>2-4</sup> and is conventionally defined as

$$\kappa = \frac{|y''|}{(1+y'^2)^{\frac{3}{2}}} \quad (S3),$$

where  $y'$  and  $y''$  respectively denote the first and second derivatives of  $y$ . Normally  $\kappa$  is constructed to lie in the range  $0 < \kappa < 10$ . As  $\kappa$  is dimensionless, reaching this range implies that  $y$  and  $x$  should be nondimensionalized to have comparable magnitudes. Concentrations  $C$  were normalized by the natural abundance level of  $^{18}\text{O}$

$$y = \frac{C}{C_o} \quad (S4),$$

and depths  $x$  were normalized by the spacing  $\Delta x$  between SIMS concentration measurements

$$X = \frac{x}{\Delta x} \quad (\text{S5}).$$

These derivatives were calculated using seven-point central difference formulae according to:

$$y' = \frac{y_{i+3} - y_{i-3}}{6\Delta X} \quad (\text{S6})$$

$$y'' = \frac{y_{i+3} - 2y_i + y_{i-3}}{9\Delta X^2} \quad (\text{S7})$$

where  $i$  corresponds to a particular data point with nearest neighbors  $i \pm 1$  and third nearest neighbors  $i \pm 3$ . With these definitions, we found empirically that requiring  $\kappa < 0.02$  reliably identified a value of  $\alpha$  suitable for setting the shallow end of the  $\lambda_1$  region.

As mentioned earlier, SIMS measurements usually terminated at depths much shallower than  $\lambda_2$ . However, with  $\alpha$ ,  $\lambda_1$ ,  $b_1$ , and  $Z$  known,  $\lambda_2$  and  $b_2$  could be determined mathematically by requiring continuity at the boundary between the  $\lambda_1$  and  $\lambda_2$  regions of both the profile itself and its first derivative. We consistently set this boundary at a depth equal to  $\alpha + 4\lambda_1$ , where the spillover contribution attributable to residual  $\lambda_1$  decay is at most about 8% of the contribution attributable to  $\lambda_2$  decay. Requiring continuity of the profile itself at  $\alpha + 4\lambda_1$  means setting Eq. (S1) equal to Eq. (S2) at  $x = \alpha + 4\lambda_1$  to yield

$$\ln \left[ e^{\frac{-\alpha - 4\lambda_1}{\lambda_1} + b_1} + \frac{C_O(Z-1)}{(C_{OT} - C_O)} \right] = \frac{-\alpha - 4\lambda_1}{\lambda_2} + b_2 \quad (\text{S8}).$$

Requiring continuity of the first derivative yields

$$\frac{1}{\lambda_1} e^{\frac{-x}{\lambda_1} + b_1} = \frac{1}{\lambda_2} e^{\frac{-x}{\lambda_2} + b_2} \quad (\text{S9}).$$

Simultaneous solution of Eqs. (S8) and (S9) yields

$$\lambda_2 = \lambda_1 \left[ 1 + \frac{C_O(Z-1)}{(C_{OT} - C_O)} e^{\frac{\alpha}{\lambda_1} + 4 - b_1} \right] \quad (\text{S10}).$$

Substitution of this value of  $\lambda_2$  back into either Eq. (S8) or (S9) yields  $b_2$ .

The net flux  $F_{18}$  was computed as

$$F_{18} = N_{18}/t \quad (\text{S11}),$$

where  $N_{18}$  denotes the number of injected  $^{18}\text{O}$  atoms.  $N_{18}$  was computed as the integral of  $(C - C_O)$  throughout the entire solid. This integral was performed piecewise. The number  $N_{VP}$  of injected  $^{18}\text{O}$  atoms appearing in the valley-peak region between  $x = 0$  and  $\alpha$  was obtained by numerical trapezoidal-rule integration of  $(C - C_O)$ . For  $x > \alpha$ , contributions to the integral from the  $\lambda_1$  and  $\lambda_2$  regions of the profile were computed analytically using Eq. (S1) and (S2) for  $C$  together with the

parameters  $\lambda_1$ ,  $\lambda_2$ ,  $Z$ ,  $b_1$  and  $b_2$  determined as described above. The number of atoms in the  $\lambda_1$  region,  $N_{\lambda 1}$ , is

$$N_{\lambda 1} = \int_{\alpha}^{\alpha+4\lambda_1} \left[ C_o \left[ \frac{C_{OT}-C_o}{C_o} \left( e^{-\frac{x}{\lambda_1}+b_1} \right) + Z \right] - C_o \right] dx \quad (S12),$$

while the corresponding number  $N_{\lambda 2}$  in the  $\lambda_2$  region is

$$N_{\lambda 2} = \int_{\alpha+4\lambda_1}^{\infty} \left[ C_o \left[ \frac{C_{OT}-C_o}{C_o} \left( e^{-\frac{x}{\lambda_2}+b_2} \right) + 1 \right] - C_o \right] dx \quad (S13).$$

Performing the analytical integration and adding all the piecewise components together yields:

$$N_{18} = N_{VP} + N_{\lambda 1} + N_{\lambda 2} = N_{VP} + \left( (C_{OT} - C_o) \left\{ \left[ \lambda_1 e^{\frac{-\alpha}{\lambda_1}+b_1} (1 - e^{-4}) \right] + \left[ \lambda_2 e^{\frac{-\alpha-4\lambda_1}{\lambda_2}+b_2} \right] \right\} \right) + 4\lambda_1 C_o (Z - 1) \quad (S14).$$

## 2. Statistical Analysis Example Calculation

The t-test calculations can be illustrated by comparing the flux ( $F_{18}$ ) for Cases I and II, whose fluxes are closest together. The values of  $s_{\Delta}$  (pooled variance), the t-statistic  $t$ , and the degrees of freedom ( $df$ ) are:

$$s_{\Delta} = \sqrt{\frac{\sigma_{III}^2}{n_{III}} + \frac{\sigma_{IV}^2}{n_{IV}}} = 3.15 \times 10^{10} \text{ cm}^{-2} \text{ s}^{-1} \quad (S15)$$

$$t = \frac{\overline{F_{III}} - \overline{F_{IV}}}{s_{\Delta}} = 1.35 \quad (S16)$$

$$df = \frac{\left( \frac{\sigma_{III}^2}{n_{III}} + \frac{\sigma_{IV}^2}{n_{IV}} \right)^2}{\frac{(s_{III}^2/n_{III})^2}{n_{III}-1} + \frac{(s_{IV}^2/n_{IV})^2}{n_{IV}-1}} = 20.5 \quad (S17)$$

Use of statistical software or a t-table yields  $p = 0.19$ . Mann-Whitney U-tests tests were performed using the MATLAB function ranksum.

### 3. Adsorption Models

#### **Definitions:**

$x$  = fraction of O originating from H<sub>2</sub>O (includes both isotopes)

$(1-x)$  = fraction of O originating from O<sub>2</sub> (includes both isotopes)

$F_{18}$  ( $F_{16}$ ) = time-averaged net injection flux of <sup>18</sup>O (<sup>16</sup>O)

$F_W$  = time-averaged net injection flux of O if only water supplies O (linear proportion model)

$k_{inj}$  = 1<sup>st</sup> order rate constant for O injection

$\theta_{OH,18}$  ( $\theta_{OH,16}$ ) = surface coverage of OH labeled with <sup>18</sup>O (<sup>16</sup>O)

$\theta_{OH}$  = total surface coverage of adsorbed OH

$k_{AW}$  = adsorption rate constant for dissociative adsorption of water on TiO<sub>2</sub>

$k_{AO_2}$  = adsorption rate constant for dissociative adsorption of O<sub>2</sub> on TiO<sub>2</sub>

$Y_{18,W}$  ( $Y_{16,W}$ ) = isotopic mole fraction of <sup>18</sup>O (<sup>16</sup>O) in the water

$Y_{18,O_2}$  ( $Y_{16,O_2}$ ) = isotopic mole fraction of <sup>18</sup>O (<sup>16</sup>O) in the O<sub>2</sub>

$C_{W,18}$  ( $C_{W,16}$ ) = concentration (mol/l) of water labeled with <sup>18</sup>O (<sup>16</sup>O) in the liquid phase

$C_W$  = total concentration (mol/l) of water (all isotopes) in the liquid phase

$C_{O_2,18}$  ( $C_{O_2,16}$ ) = concentration of dissolved <sup>18</sup>O<sub>2</sub> (<sup>16</sup>O<sub>2</sub>) in the liquid phase (mol/l)

$X_{O_2}$  = chemical mole fraction of O<sub>2</sub> (all isotopes) in the gas phase

$C_{O_2}$  = total concentration (mol/l) of dissolved O<sub>2</sub> (all isotopes) in the liquid phase

$C_{O_2,atm}$  = concentration of dissolved O<sub>2</sub> (all isotopes) at atmospheric pressure (mol/l)

$R_{ads}$  = generic adsorption rate from the liquid phase to create OH on the surface

$R_{des}$  = generic desorption rate into the liquid phase to remove OH from the surface

#### **3.1 Linear Proportion Model**

This model assumes that H<sub>2</sub>O and O<sub>2</sub> contribute O and isotopic labels in linear proportion to their respective concentrations. A fraction  $x$  of O originates from H<sub>2</sub>O, and a fraction  $(1-x)$  originates from O<sub>2</sub>. A mass balance on <sup>18</sup>O then yields:

$$F_{18} = Y_{18,W}x F_W + Y_{18,O_2}X_{O_2}(1-x)F_W \quad (S18).$$

Equation (S18) assumes constant flux, neglecting the modest increase in surface annihilation (decrease in flux) that occurs with increasing time, and assumes the validity of Henry's law, where

the O<sub>2</sub> solubility is proportional to its partial pressure. Equation (S18) also implicitly assumes that <sup>18</sup>O injection and diffusion into TiO<sub>2</sub> occurs by two independent pathways (H<sub>2</sub>O, O<sub>2</sub>) with no chemical interactions. Linear regression on the four equations (F<sub>18,I</sub> - F<sub>18,IV</sub>) and two unknowns ( $x$ ,  $F_W$ ) yields  $F_W = 2.5 \times 10^{12} \text{ cm}^{-2}\text{s}^{-1}$  and  $x = 0.78$ , with a total residual variance of  $1.9 \times 10^{22} \text{ cm}^{-4}\text{s}^{-2}$ .

### **3.2 Dual Pathway Model**

This model assumes that both H<sub>2</sub>O and O<sub>2</sub> react through the same OH<sub>ads</sub> intermediate species atop rutile TiO<sub>2</sub>(110). Langmuir kinetics, constant flux, and the validity of Henry's law are all assumed. A mass balance on the rates of species exchange between the solid surface and fluid yields  $\theta_{OH}$ . The calculation begins with the following rates:

$$R_{ads} = (k_{AW}C_W + k_{AO_2}C_{O_2})(1 - \theta_{OH}) \quad (\text{S19})$$

$$R_{des} = (k_{dW} + k_{dO_2})\theta_{OH} \quad (\text{S20}).$$

With the assumption of steady state, the mass balance is  $R_{ads} = R_{des}$ , or:

$$(k_{AW}C_W + k_{AO_2}C_{O_2})(1 - \theta_{OH}) = (k_{dW} + k_{dO_2})\theta_{OH} \quad (\text{S21}).$$

Rearrangement yields  $\theta_{OH}$ :

$$\theta_{OH} = \left[ \frac{(k_{AW}C_W + k_{AO_2}C_{O_2})}{(k_{AW}C_W + k_{AO_2}C_{O_2} + k_{dW} + k_{dO_2})} \right] \quad (\text{S22}).$$

Separation into two isotopic components and  $\theta_{OH,18}$  and  $\theta_{OH,16}$  begins with the substitutions  $C_W = C_{W,16} + C_{W,18}$  and  $C_{O_2} = C_{O_2,16} + C_{O_2,18}$ :

$$\theta_{OH} = \left[ \frac{k_{AW}(C_{W,16} + C_{W,18}) + k_{AO_2}(C_{O_2,16} + C_{O_2,18})}{(k_{AW}C_W + k_{AO_2}C_{O_2} + k_{dW} + k_{dO_2})} \right] \quad (\text{S23})$$

$$= \left[ \frac{(k_{AW}C_{W,18} + k_{AO_2}C_{O_2,18})}{(k_{AW}C_W + k_{AO_2}C_{O_2} + k_{dW} + k_{dO_2})} \right] + \left[ \frac{(k_{AW}C_{W,16} + k_{AO_2}C_{O_2,16})}{(k_{AW}C_W + k_{AO_2}C_{O_2} + k_{dW} + k_{dO_2})} \right] \quad (\text{S24}).$$

Substitution of the mole fractions  $C_{W,18} = Y_{18,W}C_W$ ,  $C_{W,16} = Y_{16,W}C_W$ ,  $C_{O_2,18} = Y_{18,O_2}C_W$ , and  $C_{O_2,16} = Y_{16,O_2}C_W$  yields:

$$\theta_{OH} = \left[ \frac{(Y_{18,W}k_{AW}C_W + Y_{18,O_2}k_{AO_2}C_{O_2})}{(k_{AW}C_W + k_{AO_2}C_{O_2} + k_{dW} + k_{dO_2})} \right] + \left[ \frac{(Y_{16,W}k_{AW}C_W + Y_{16,O_2}k_{AO_2}C_{O_2})}{(k_{AW}C_W + k_{AO_2}C_{O_2} + k_{dW} + k_{dO_2})} \right] \quad (\text{S25}).$$

The first set of terms in brackets corresponds to  $\theta_{OH,18}$  and the second set to  $\theta_{OH,16}$ , so:

$$\theta_{OH,18} = \left[ \frac{(Y_{18,W}k_{AW}C_W + Y_{18,O_2}k_{AO_2}C_{O_2})}{(k_{AW}C_W + k_{AO_2}C_{O_2} + k_{dW} + k_{dO_2})} \right] \quad (S26a)$$

$$\theta_{OH,16} = \left[ \frac{(Y_{16,W}k_{AW}C_W + Y_{16,O_2}k_{AO_2}C_{O_2})}{(k_{AW}C_W + k_{AO_2}C_{O_2} + k_{dW} + k_{dO_2})} \right] \quad (S26b).$$

Note that  $\theta_{OH,18} + \theta_{OH,16} = \theta_{OH}$ . Under water, one can assume  $\theta_{OH} \approx 1$ . Under such conditions, Eq. (S23) suggests  $k_{dW} + k_{dO_2} \ll k_{AW}C_W + k_{AO_2}C_{O_2}$ , which implies that:

$$\theta_{OH,18} = \left[ \frac{(Y_{18,W}k_{AW}C_W + Y_{18,O_2}k_{AO_2}C_{O_2})}{(k_{AW}C_W + k_{AO_2}C_{O_2})} \right] \quad (S27).$$

Use of  $C_{O_2} = X_{O_2}C_{O_2,atm}$  yields:

$$\theta_{OH,18} = \left[ \frac{(Y_{18,W}k_{AW}C_W + Y_{18,O_2}X_{O_2}k_{AO_2}C_{O_2,atm})}{(k_{AW}C_W + X_{O_2}k_{AO_2}C_{O_2,atm})} \right] \quad (S28).$$

The rate of  $^{18}O$  injection is therefore:

$$F_{18} = k_{inj}\theta_{OH,18} = k_{inj} \left[ \frac{(Y_{18,W}k_{AW}C_W + Y_{18,O_2}X_{O_2}k_{AO_2}C_{O_2,atm})}{(k_{AW}C_W + X_{O_2}k_{AO_2}C_{O_2,atm})} \right] \quad (S29).$$

A fraction  $x$  originates from the  $H_2O$  phase, and the remaining fraction  $(1-x)$  from the gas phase:

$$x = \frac{k_{AW}C_W}{k_{AW}C_W + k_{AO_2}C_{O_2,atm}} \quad (S30a)$$

$$1 - x = \frac{k_{AO_2}C_{O_2,atm}}{k_{AW}C_W + k_{AO_2}C_{O_2,atm}} \quad (S30b).$$

Substitution of Eqs. (S30a) into Eq (S28) and rearranging yields:

$$\theta_{OH,18} = \frac{Y_{18,W}x + X_{O_2}Y_{18,O_2}(1-x)}{x + X_{O_2}(1-x)} \quad (S31a).$$

A similar set of steps for  $\theta_{OH,16}$  yields:

$$\theta_{OH,16} = \frac{Y_{16,W}x + X_{O_2}Y_{16,O_2}(1-x)}{x + X_{O_2}(1-x)} \quad (S31b),$$

although it is also true that  $\theta_{OH,16} = 1 - \theta_{OH,18}$  with the assumption of  $\theta_{OH} \approx 1$  employed above.

The injected fluxes are therefore:

$$F_{18} = k_{inj}\theta_{OH,18} = k_{inj} \left[ \frac{Y_{18,W}x + X_{O_2}Y_{18,O_2}(1-x)}{x + X_{O_2}(1-x)} \right] \quad (S32a)$$

$$F_{16} = k_{inj}\theta_{OH,16} = k_{inj} \left[ \frac{Y_{16,W}x + X_{O_2}Y_{16,O_2}(1-x)}{x + X_{O_2}(1-x)} \right] \quad (S32b).$$

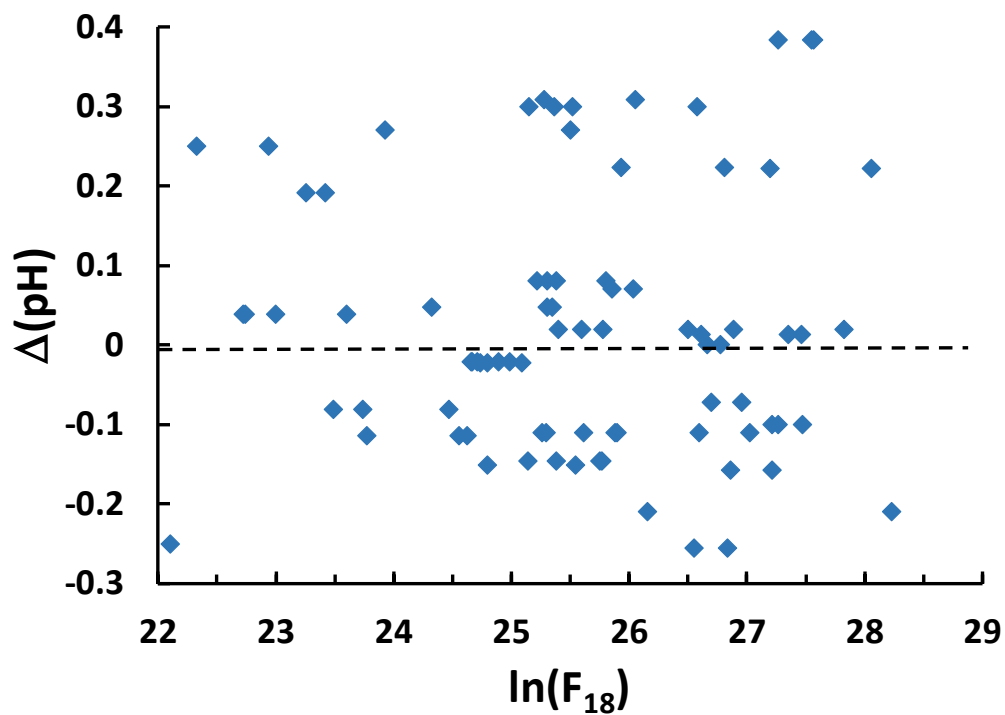
In the asymptotic limit of  $x \rightarrow 1$ , Eq. (S18) from the linear proportion model represents a limiting case of Eq. (S32a) from the dual pathway model, with  $F_w = k_{inj}$ . Formally, the condition of  $x = 0$  and  $X_{O_2} = 1$  leads to the same equivalence but makes no physical sense because experimentally,  $H_2O$  is always present to contribute some of the injected O.

Nonlinear regression for four cases ( $F_{18,I} - F_{18,IV}$ ) yields  $x = 0.76$  and  $k_{inj} = 2.2 \times 10^{12} \text{ cm}^{-2}\text{s}^{-1}$ . From the best-fit value for  $k_{inj}$ , we can estimate  $\theta_{OH,18}$  and  $\theta_{OH,16}$  in one of two ways. One method divides individual values of  $F_{18}$  and  $F_{16}$  by the fitted value of  $k_{inj}$  to obtain corresponding “fitted” values of  $\theta_{OH,18}$  and  $\theta_{OH,16}$  according to the first equalities in Eqs. (S32a) and (S32b). The other method uses the chosen isotopic mole fractions in gas and liquid, the gas mole fraction of  $O_2$ , and the best-fit value of  $x$  to obtain theoretical “ideal” values of  $\theta_{OH,18}$  and  $\theta_{OH,16}$  according to Eqs. (S31a) and (S31b). Table S1 shows the corresponding values for the present experiments.

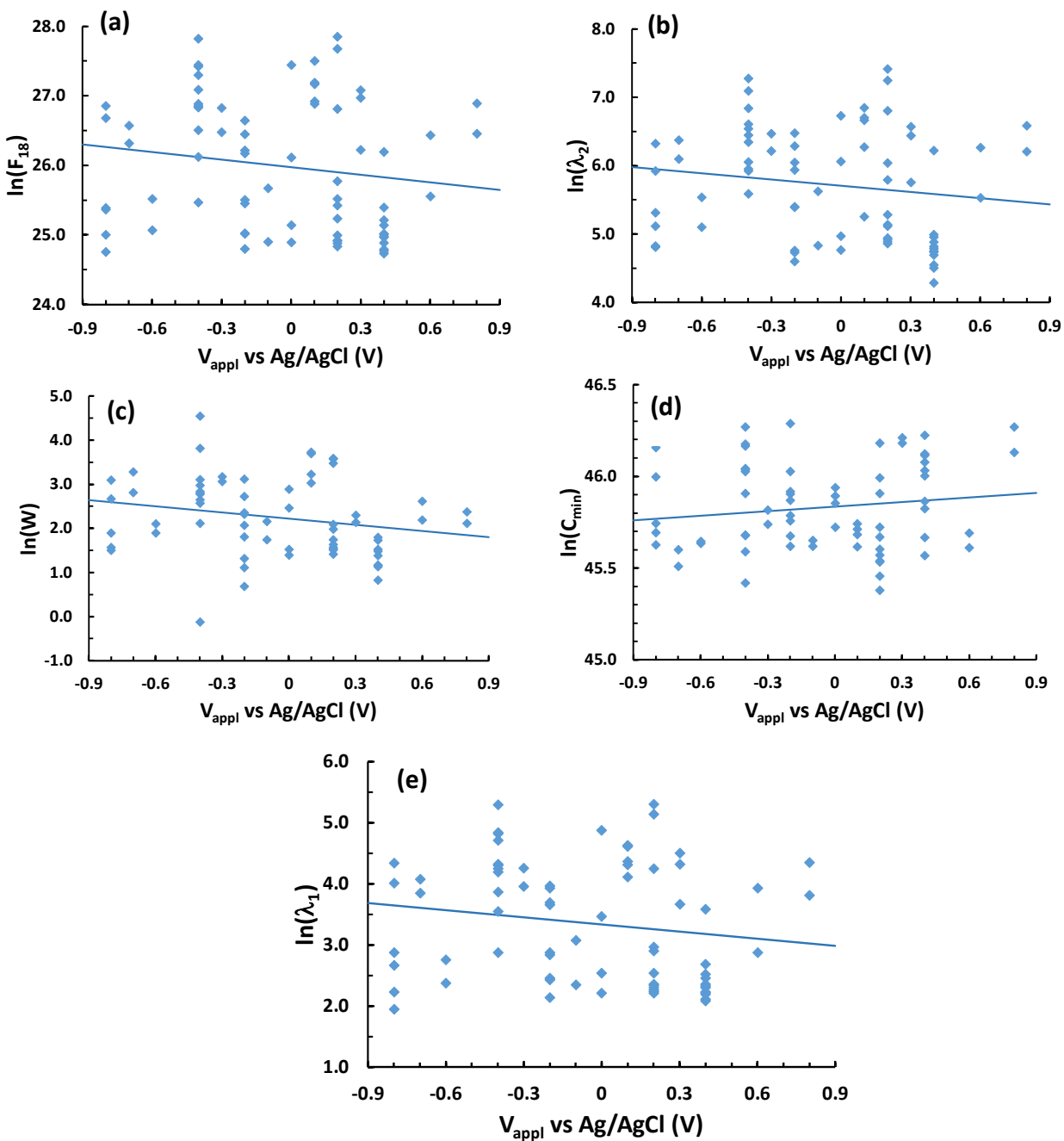
**Table S1.** Surface coverages of  $^{18}O$  and  $^{16}O$

	Case I	Case II	Case III	Case IV
$\theta_{OH,18}$ (fitted)	0.073	0.055	0.14	0.23
$\theta_{OH,18}$ (ideal)	0.10	0.076	0.094	0.23
$\theta_{OH,16}$ (fitted)	0.93	0.94	0.86	0.77
$\theta_{OH,16}$ (ideal)	0.90	0.92	0.91	0.77





**Figure S1.** Change in solution pH measured at the start and end of the diffusion experiment as a function of the flux ( $F_{18}$ ) of injected  $^{18}\text{O}$ . The pH of the solution does not correlate with  $F_{18}$ . Whenever more than one profile was measured for a given specimen resulting in multiple values for  $F_{18}$ , the same pH change is plotted for all the values of  $F_{18}$ . This resulted in obvious discretization that is apparent for some values of  $\Delta\text{pH}$ .

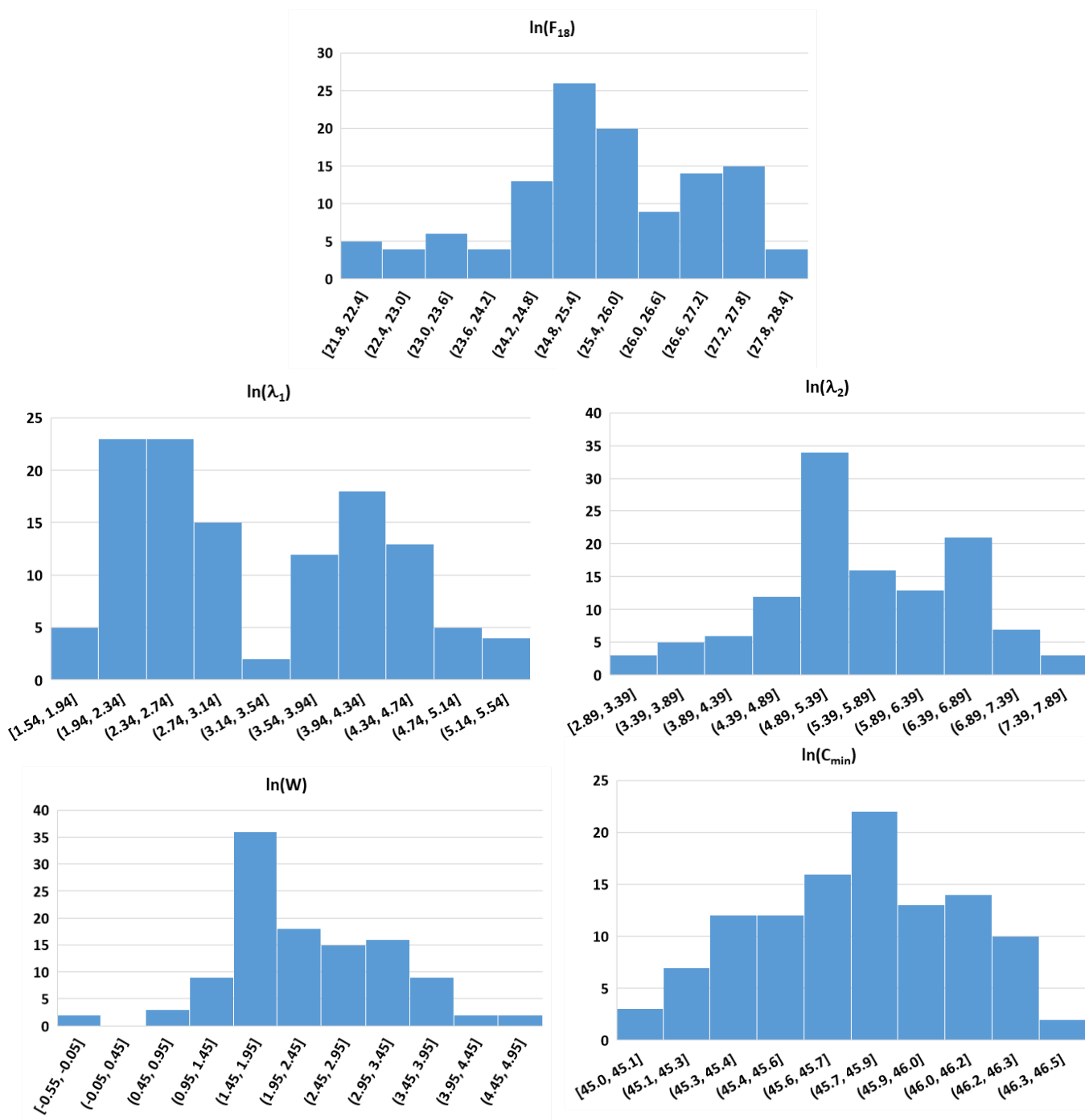


**Figure S2.** Profile metrics vs applied potential bias  $V_{\text{appl}}$  including (a)  $F_{18}$ , (b)  $\lambda_2$ , (c)  $W$ , (d)  $C_{\min}$  and (e)  $\lambda_1$  at 70°C. Lines represent linear least squares fits. For all data here, the water (10 at %  $^{18}\text{O}$ ) contained no electrolyte. The plots have nonzero slopes. Table S2 below reports the results of F-tests to determine whether the nonzero slopes represent statistical departures from zero (the null hypothesis). For all but  $W$ , the likelihood of the null hypothesis (p-value) is 0.15-0.25, which is generally considered too large for the slopes to be accounted statistically significant. For  $W$ , the p-value of 0.08 is noticeably smaller. Although F-tests are rather robust to deviations from normality,<sup>5,6</sup> we do not claim statistical significance, especially because the liquid and solid  $\text{TiO}_2$  are both insulating and provide no mechanism for  $V_{\text{appl}}$  to exert an effect.

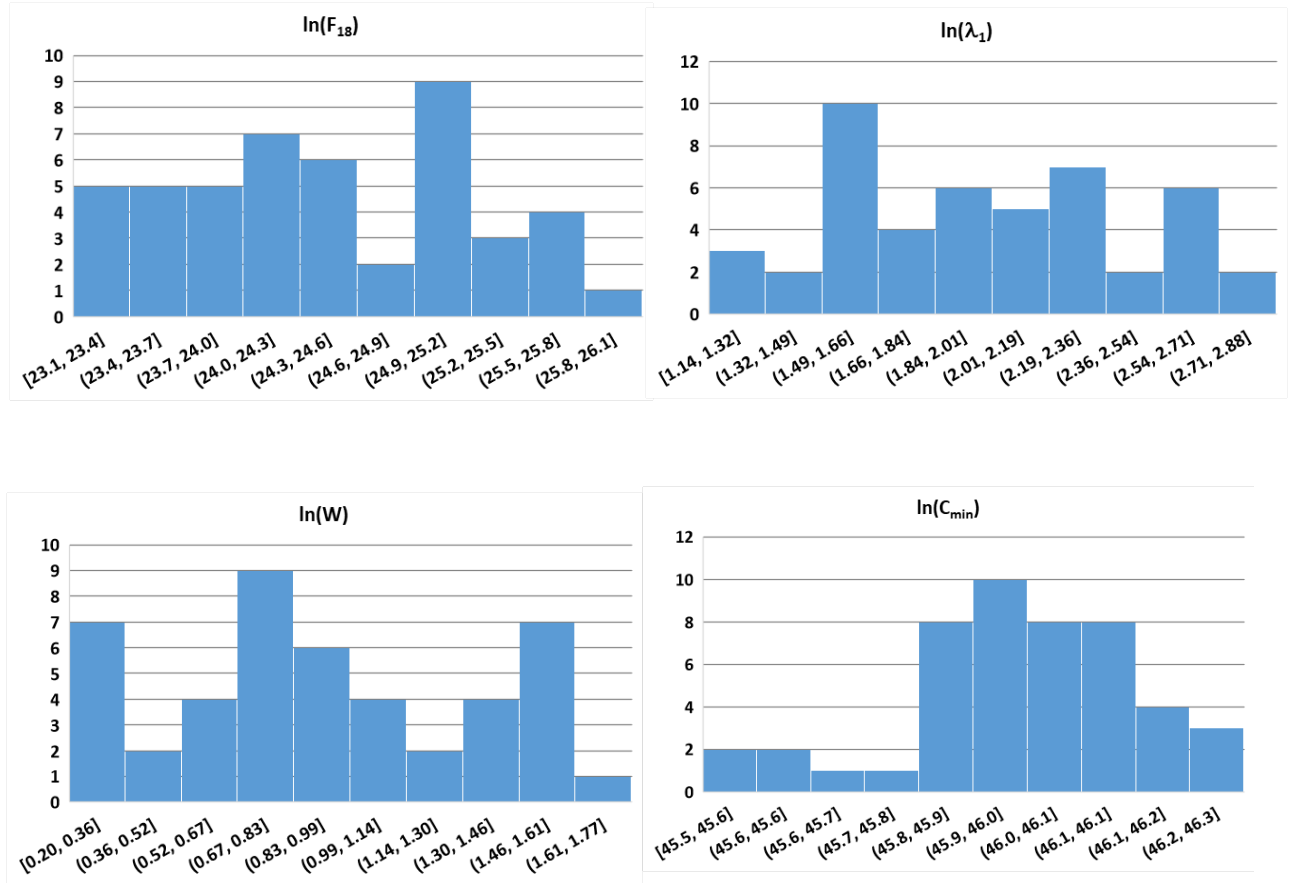
**Table S2.** Slopes of profile metrics vs  $V_{\text{appl}}$ : F-tests for null hypothesis\*

<b>Metric</b>	<b>Slope</b>	<b>Degrees of Freedom</b>	<b>F</b>	<b>p</b>
$F_{18}$	$-0.36 \pm 0.26$	72	1.83	0.18
W	$-0.47 \pm 0.25$	66	3.24	0.08
$C_{\text{min}}$	$0.08 \pm 0.07$	66	1.33	0.25
$\lambda_1$	$-0.39 \pm 0.27$	72	2.01	0.16
$\lambda_2$	$-0.30 \pm 0.23$	72	1.77	0.19

\*Statistical tests were performed on metrics after transformation to a natural logarithmic scale.

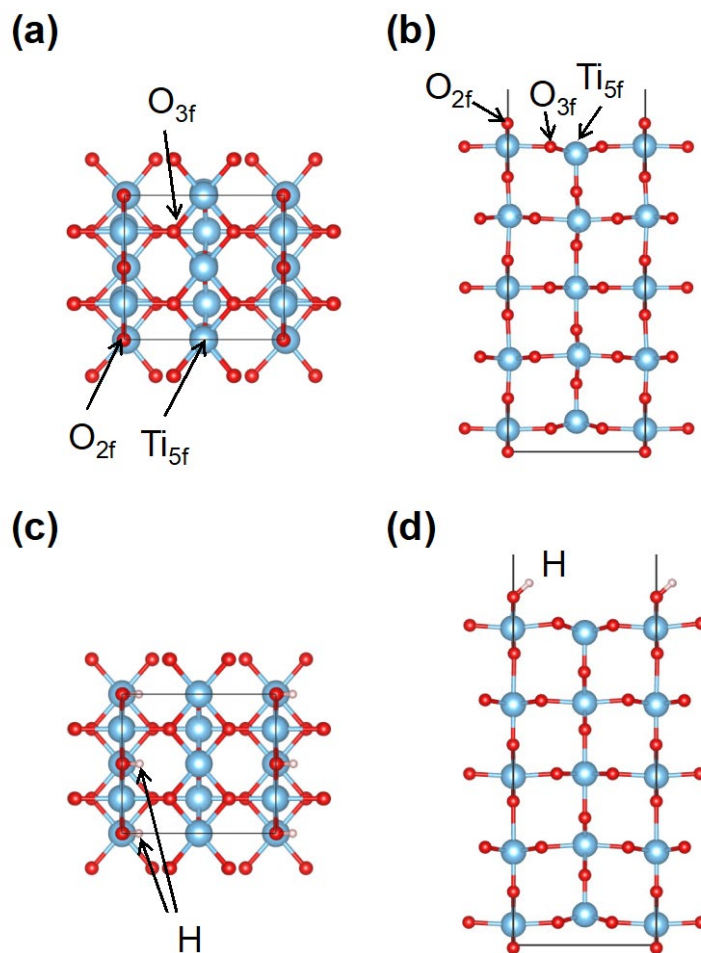


**Figure S3:** Histograms of the five different profile metrics at 70°C with applied bias. Some of the histograms are roughly normal (Gaussian) but others are clearly not. This figure (and S4) employs logarithmic plotting of all metrics because statistical analysis after logarithmic transformation is a well-established method<sup>7,8</sup> for improving the skewness of a data set by attenuating departures from the mean at the upper end of the range and amplifying them at the lower end. Logarithmic transformation is akin to working with solution pH rather than hydronium ion concentration.



**Figure S4:** Histograms of the profile metrics for water without applied bias. Data were originally taken in the range 30-80°C as described previously,<sup>9</sup> and transformed to a single temperature of 70°C according to Arrhenius linear regression as described in Ref. [9]. For water without applied bias, profiles exhibited no counterpart to the  $\lambda_2$  region elicited by applied bias. Some of the histograms are roughly normal (Gaussian), but others are clearly not.

Either with or without applied bias, non-normal distributions arise partly because the assumption of complete independence does not hold for all data. For water without applied bias, Ref. [9] reported that metrics measured at different points on a given specimen clustered together more closely than for different specimens. Similar clustering occurred here with applied bias, with the distributions at 70 °C affected by heavily sampled specimens at +0.2V and  $\pm 0.4$ V. In both cases, the diameter of the region sampled by SIMS was about 1 mm. For  $W$  and  $C_{min}$ , additional systematic bias arises because a few profiles exhibited fractionation that did not reach below natural abundance. These profiles are not included because no fractionation metrics can be determined using the definitions employed here.



**Figure S5.** Atomic geometry of (a,b) pristine TiO<sub>2</sub>(110) terrace and (c,d) adsorbed bridging hydroxyl. (a,c) show top views and (b,d) show side views. Shading colors respectively represent blue for Ti, red for O, and white for H.

**Table S3.** Adsorption energy and Bader charge of adsorbed O on TiO<sub>2</sub>(110): Ti-rich conditions

TiO <sub>2</sub> (110) surface conditions	Adsorption configuration	Adsorption energy (eV)		Bader charge (e <sup>-</sup> )		Charge state
		$E_F=0$ eV	$E_F=3.1$ eV	adsorbed O atom	neighboring O atom	
Pristine	Dumbbell	6.23	6.23	-0.43	-0.69	0
	Split	6.38	0.32	-1.11	-0.94	-2
	On-top	8.06	5.03	-0.61	-1.09	-1
Bridging hydroxylated	Dumbbell	5.91	5.91	-0.54	-0.71	0
	Split	5.13	-0.93	-1.12	-1.03	-2
	On-top	3.22	0.20	-0.87	-1.13	-1

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