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# Supporting Information: Acceleration of Butane Vapor Nucleation by Carbon Dioxide Gas

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### S1 Water unary and water-CO<sub>2</sub> binary vapor nucleation

Figure S1 shows the data for the unary nucleation of water (panel A) and for binary nucleation of the water-CO<sub>2</sub> mixture (panel B) as published in Ref.<sup>1</sup>. Here we have re-analyzed the data with the inclusion of  $\xi$  in Eqs. 6 and 9. It should be noted that the rate constants  $k_{1,1}$  for unary water nucleation and  $\beta$  for water-CO<sub>2</sub> binary nucleation increased by a factor of two compared to that reported in Ref.<sup>1</sup>, owing to the inclusion of  $\xi$  in the present model.

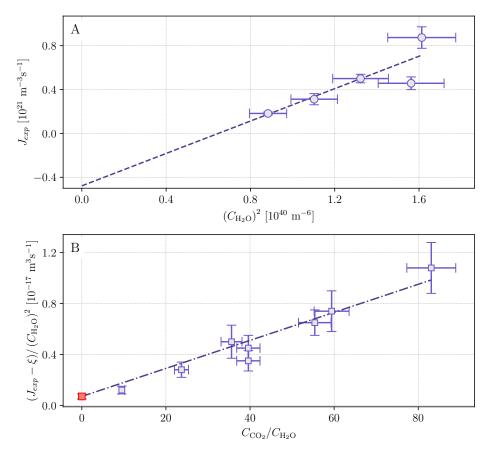


Figure S1: (A) Unary water nucleation. Circles: Experimental data points  $J_{exp}$  as a function of  $(C_{H_2O})^2$ . Dashed line: Linear fit using Eq. 6 and  $J_{exp} = J_{un}$ . (B) Water-CO<sub>2</sub> binary nucleation. The red marker denotes  $k_{1,1}$ . The dashed-dotted line denotes the linear fit according to Equation 10 and  $J_{exp} = J_{bi}$ . The  $\beta$  value obtained in the fit is given in Table 1.

#### S2 Simulated behavior of J

We simulated the behavior of J assuming different experimental artifacts, such as cluster loss during ionization and limitations due to detection. To begin, Eq. 6 was used to generate  $J_{model}$  with  $k_{1,1}$  ( $\xi = 0$ ) for different values of  $C_{\text{Bu}}$ , shown as the solid black lines in Fig. S2. From these values, the total number concentration was obtained by integrating  $J_{model}$  over time,

$$C_{tot}(t_i) = \int_{t_0}^{t_i} J_{model} dt \quad (i = 1, 2, 3, ...).$$
 (S1)

A cluster mass distribution was then generated that resembled the experimental data, ensuring that the total cluster concentration matched  $C_{tot}(t_i)$ .

This simulated distribution was subsequently screened according to the relevant conditions, such as cluster loss or being below the detection limit. The resulting concentrations yielded the simulated nucleation rates,  $J_{sim}$ , which are shown as open circles in Fig. S2. Linear fits through the  $J_{sim}$  values, indicated by the dashed-dotted lines, demonstrate that in both cases the fits pass through the origin.

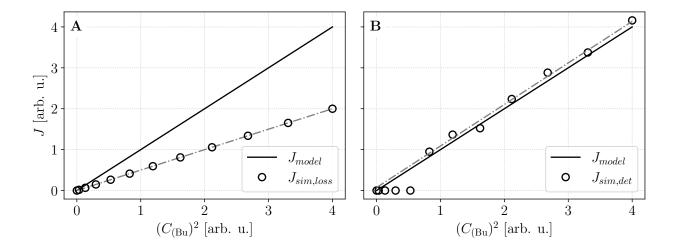


Figure S2: Simulated behavior of unary nucleation rates with monomer number concentration squared for (A) loss of cluster during ionization and (B) due to detection limit of the instrument. Black solid lines: Generated  $J_{model}$  values according to Eq. 6 with  $\xi = 0$ . Black circles: Simulated  $J_{sim}$  data points. Gray dashed-dotted lines: linear fit through the simulated data points using Eq. 6.

### S3 Baseline rise due to mixed clusters

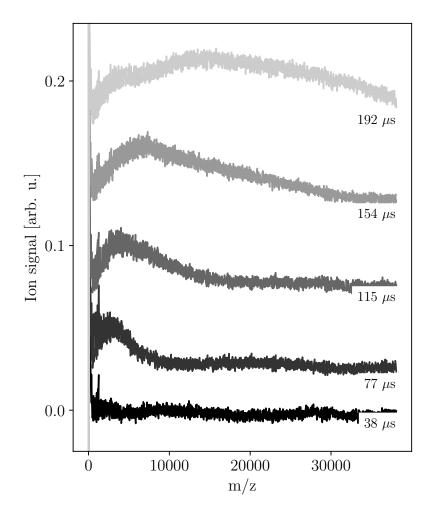


Figure S3: Mass spectra for a mixture of 0.21% Bu  $(1.2 \times 10^{20} \text{ m}^{-3})$  and 12.7% CO2  $(7 \times 10^{21} \text{ m}^{-3})$ , same conditions as Fig. 6 (middle row), without baseline correction. The baseline drifts/rises at larger cluster sizes (masses) are an indication for the formation of mixed clusters. For shorter times, the abundance of mixed clusters with lower masses (Fig. 6) is very low and often below the detection limit. At longer times, the mixed clusters of higher masses are visible in the spectra as baseline drifts/rises ("unresolved bums") as the individual mass peaks can no longer be resolved in the spectra. At shorter nucleation times (black curve) this bump is still small, but the center of this bump moves towards higher masses and becomes broader at longer nucleation times (gray scale).

## $_{30}$ S4 Summary of butane unary and butane CO $_2$ binary results

Table S1: Overview table for unary butane nucleation measurements. The columns contain: The butane concentration, the nitrogen concentration, the argon concentration, the experimental nucleation rate, the error of the experimental nucleation rate, the temperature of the expansion, the pressure in the expansion as well as the supersaturation of the monomer.

$C_{Bu}$	$C_{N_2}$	$C_{Ar}$	$J_{exp} [10^{22}]$	Error [10 <sup>22</sup>	Temp.	Pressure	Sup. sat.
$[10^{20} \text{ m}^{-3}]$	$[10^{21} \text{ m}^{-3}]$	$[10^{22} \text{ m}^{-3}]$	$m^{-3}s^{-1}$	$m^{-3}s^{-1}$	[K]	[Pa]	$[\ln(S)]$
1.08	7.16	4.95	0.45	0.04	50.8	40	45
1.08	7.13	4.94	0.21	0.03	51	40	44
1.1	7.27	5.03	0.08	0.02	50	40	46
1.19	7.12	4.94	0.31	0.05	51	40	44
1.26	7.16	4.97	0.41	0.03	50.7	40	45
1.27	7.22	5.01	0.54	0.06	50.2	40	46
1.32	7.16	4.97	0.81	0.08	50.6	40	45
1.37	7.11	4.94	0.95	0.12	50.9	40	45
1.43	7.15	4.97	1.1	0.16	50.6	40	45
1.73	7.17	5.01	2.87	0.26	50.3	40	46
2.02	7.16	5.02	5.23	0.36	50.1	40	46
2.3	7.09	4.99	6.14	0.57	50.4	40	46

Table S2: Overview table for binary Butane-CO<sub>2</sub> nucleation measurements. The columns contain the butane concentration, the CO<sub>2</sub> concentration, the ratio of CO<sub>2</sub> to butane, the nitrogen concentration, the argon concentration, the experimental nucleation rate, the error of the experimental nucleation rate, the experimental nucleation rate normalized according to equation 10, error of this normalization, flow temperature, pressure in the flow and monomer super saturation. The super saturation was calculated using the Wagner Equation and coefficients from Ref<sup>2</sup> for the equilibrium vapor pressure.

$\sqsubseteq$	$C_{CO_2}/C_{Bu}$ $C_{N_2}$	$C_{N_2}$	$C_{Ar}$	$J_{exp} [10^{21}]$	Error $[10^{21}]$	$(J_{exp} - \xi)/(C_{Bu})^2$	Error	Temp.	Press.	Sup. sat.
$[10^{21} \text{ m}^{-3}]$	$[10^{21}]$	m <sup>-3</sup> ]	$[10^{22} \text{ m}^{-3}]$	$m^{-3}s^{-1}$ ]	$[{\rm m}^{-3}{\rm s}^{-1}]$	$[10^{-18} \text{ m}^3 \text{s}^{-1}]$	$[10^{-18} \text{ m}^3 \text{s}^{-1}]$	[ <u>K</u> ]	[Pa]	$[\ln(S)]$
5 6.61	6.61		4.95	3.99	0.26	1.97	0.33	50.9	40	44
10 6.16	6.16		5.02	2.69	0.52	1.81	0.31	50.1	40	46
10 6.12	6.12		4.99	2.3	0.26	1.8	0.31	50.4	40	45
13.2 5.8	5.8		5.01	5.39	0.95	2.04	0.33	50.2	40	45
20.1 4.99	4.99		4.96	3.53	1.1	1.93	0.33	50.8	40	45
25.1 4.47	4.47		4.98	3.2	0.25	1.88	0.32	50.6	40	45
25.1 4.44	4.44		4.95	4.42	1.53	2.01	0.35	50.9	40	44
30 3.95	3.95		4.99	5.33	1.2	2.05	0.34	50.4	40	45
35 3.4	3.4		4.99	10.49	1.25	2.49	0.37	50.4	40	45
35 3.37	3.37		4.94	4.38	1.26	2.01	0.34	50.9	40	44
40.1	2.83		4.97	7.3	1.55	2.23	0.36	50.6	40	45
45 2.28	2.28		4.92	8.93	1.03	2.42	0.37	51.1	40	44
50.2   1.73	1.73		4.91	6.65	0.64	2.23	0.35	51.2	40	44

Table S3: Mixed clusters and their corresponding masses [amu] observed in Figure 6 D.

	$(Bu)_1$	$(Bu)_2$	$(Bu)_3$	$(Bu)_4$	$(Bu)_5$	(Bu) <sub>6</sub>	(Bu) <sub>7</sub>	(Bu) <sub>8</sub>	(Bu) <sub>9</sub>
$(CO_2)_1$	-	160.25	218.37	276.49	-	392.73	450.85	508.97	567.09
$(CO_2)_2$	146.14	-	262.38	320.5	378.62	436.74	494.86	-	611.1
$(CO_2)_3$	-	-	306.39	364.51	422.63	480.75	538.87	-	655.11
$(CO_2)_4$	234.16	-	350.4	408.52	466.64	524.76	582.88	-	-
$(CO_2)_5$	_	-	394.41	452.53	510.65	568.77	626.89	685.01	-
$(CO_2)_6$	_	-	438.42	496.54	554.66	612.78	670.9	-	-
$(CO_2)_7$	_	-	482.43	540.55	-	656.79	-	-	-
$(CO_2)_8$	-	-	526.44	-	-	-	-	-	-
$(CO_2)_9$	_	-	-	-	-	-	-	-	-
$(CO_2)_{10}$	-	-	614.46	-	-	-	-	-	-

### References

- [1] Stefan Feusi, Felix Graber, Jai Khatri, Chenxi Li, and Ruth Signorell. How  $CO_2$  gas accelerates water nucleation at low temperature. *Journal of Chemical Physics*, 161(18):184304, nov 2024.
- [2] Peter Stephan, Stephan Kabelac, Matthias Kind, Dieter Mewes, Karlheinz Schaber, and Thomas Wetzel, editors. VDI-Wärmeatlas: Fachlicher Träger VDI-Gesellschaft Verfahrenstechnik und Chemieingenieurwesen. Springer Reference Technik. Springer Vieweg, Berlin, Heidelberg, 12 edition, 2019.