Supporting Information

Catalytic Static Mixers Enable the Continuous Hydrogenation of Cannabidiol and Tetrahydrocannabinol

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Table of Contents

| 1. | GENERAL INFORMATION | 4 |
|-------|---|-----|
| 1.1. | CATALYTIC STATIC MIXERS | 4 |
| 1.2. | HIGH FIELD NMR | 4 |
| 1.3. | GC-FID ANALYSIS | 5 |
| 1.4. | GC-MS Analysis | 8 |
| 1.5. | ICP-MS Analysis | 9 |
| 1.6. | SEM AND EDS IMAGES | 9 |
| 1.6.1 | . Pd/alumina | .10 |
| 1.6.2 | P. Pt/alumina | .11 |
| 1.6.3 | Ru/alumina | .12 |
| 1.7. | EXPERIMENTAL SETUP | .12 |
| 1.8. | Batch Synthesis of Δ^8 -THC | .14 |
| 1.9. | Purifications by Biotage Isolera | .15 |
| 2. | CATALYTIC STATIC MIXER RESULTS | .16 |
| 2.1. | Hydrogenation of CBD over Pd-electroplated (PdEP) CSMs | .16 |
| 2.1.1 | Solvent Screening | .16 |
| 2.1.2 | Temperature Screening | .16 |
| 2.1.3 | Residence Time Screening | .16 |
| 2.2. | Hydrogenation of CBD over Pd/allimina CSMs. | .17 |
| 2.2.1 | H/S Ratio Screening | .17 |
| 2.2.2 | . Temperature Screening | .17 |
| 2.2.3 | Long Run with CBD at 160 °C | .17 |
| 2.3. | Hydrogenation of THC over Ru/alumina CSMs | .18 |
| 2.3.1 | . Temperature Screening | .18 |
| 2.3.2 | Catalyst Recoverability by Washing with Acetone | .19 |
| 2.4. | Hydrogenation of CBD over Pt/alumina CSMs | .20 |
| 2.4.1 | Blank Experiment | .20 |
| 2.4.2 | P. H/S Ratio Screening | .21 |
| 2.4.3 | CBD Concentration Screening | .21 |
| 2.4.4 | Design of Experiments (DoE): Influence of Temperature and Pressure | .22 |
| 2.4.5 | Temperature Screening | .23 |
| 2.4.6 | 6. Residence Time Screening | .24 |
| 2.4.7 | Long Run for the Hydrogenation of CBD to H4CBD Based on Unoptimized Conditions | .24 |
| 2.4.8 | Long Run for the Synthesis of H4CBD at Optimized Conditions | .25 |
| 2.4.9 | D. Long Run for the synthesis of H2CBD at Optimized Conditions | .25 |
| 2.5. | Hydrogenation of H2CBD to H4CBD over Pt/alumina CSMs | .26 |
| 2.5.1 | . Temperature Screening | .26 |
| 2.6. | Hydrogenation of THC over Pt/alumina CSMs | .26 |
| 2.6.1 | . Hydrogenation of Δ^9 -THC: Screening of Temperature and Residence Time | .26 |
| 2.6.2 | Long Run for the Synthesis of HHC from Δ^9 -THC at Optimized Conditions | .27 |
| 2.6.3 | Hydrogenation of Δ^8 -THC: screening of Temperature and Residence Time | .27 |
| 2.6.4 | Long Run for the Synthesis of HHC from Δ^8 -THC at Optimized Conditions | .28 |
| 3. | KINETICS INVESTIGATION | .29 |
| 3.1. | Experimental Methods | .29 |
| 3.1.1 | . Preparation of the Stock Solution | .29 |
| 3.1.2 | Deconvolution of GCFID Peaks | .29 |
| 3.2. | KINETICS RESULTS | .30 |
| 3.2.1 | . Matlab Model | .30 |
| 3.2.2 | 2. Dynochem Model | .33 |
| 3.2.3 | Residence time vs. Real Residence Time | .34 |
| 4. | CSMS DEACTIVATION STUDY | .35 |

| 4.1. | Experimental Methods | 35 |
|--------|--|-----|
| 4.1.1. | Reactor Configuration | 35 |
| 4.1.2. | GC-FID Chromatograms | 35 |
| 4.1.3. | GC-FID Calibration for CBD | 36 |
| 4.2. | Results | 37 |
| 4.2.1. | Hydrogenation of Limonene | 37 |
| 4.2.2. | Hydrogenation of Limonene in the Presence of Resorcinol | 38 |
| 5. C | CALCULATIONS | 38 |
| 6. S | SPECTRA | 40 |
| 6.1. | GC-MS Analysis | 41 |
| 6.1.1. | CBD (1) | 41 |
| 6.1.2. | H2CBD (2) | 41 |
| 6.1.3. | CisH4CBD (3) | 42 |
| 6.1.4. | TransH4CBD (4) | 42 |
| 6.1.5. | Δ ⁹ -THC (5) | 43 |
| 6.1.6. | Δ ⁸ -THC (6) | .43 |
| 6.1.7. | R-HHC (7) | .44 |
| 6.1.8. | S-HHC (8) | .44 |
| 6.2. | NMR Spectra | 45 |
| 6.2.1. | Cannabidiol (CBD) | .45 |
| 6.2.2. | Dihydro Cannabidiol (H2CBD) | .45 |
| 6.2.3. | Tetrahydro Cannabidiol (H4CBD) | .46 |
| 6.2.4. | Δ^{g} -Tetrahydro Cannabinol (Δ_{g} -THC) | .46 |
| 6.2.5. | Δ_8 -Tetrahydro Cannabinol (Δ_8 -THC) | .47 |
| 6.2.6. | Hexahydro Cannabinol (HHC) | .47 |
| 7. F | REFERENCES | 60 |

1. General Information

1.1. Catalytic Static Mixers

Catalytic static mixers (Precision Catalysts, 316L12F150-A) with the dimensions 11.8 mm x 150 mm were used in the investigation. The CSMs used for the experimental campaign are reported in Table S 1.

| Table S 1: Catal | vtic static | mixers used | (Note: LF | R – Lona Run). |
|------------------|-------------|-------------|-----------|----------------|
| | , | | 1.10101 | · |

| Entry | CSM | Serial Number | Experimental Note |
|-------|-------------|---------------|----------------------------|
| 1 | Pd-EP | 346001-8-A042 | Screening experiments |
| 2 | Pd-EP | 346001-8-A043 | Screening experiments |
| 3 | Pd/alumina | 346131-8-A007 | Screening experiments |
| 4 | Pd/alumina | 346131-8-A008 | Screening experiments |
| 5 | Ru/alumina | 344131-4-A015 | Screening experiments |
| 6 | Ru/alumina | 344131-4-A017 | Screening experiments |
| 7 | Pt/alumina | 378131-8-A013 | Screening experiments |
| 8 | Pt/alumina | 378131-8-A014 | Long run to prepare H2CBD |
| 9 | Pt/alumina | 378131-8-A015 | Long run to prepare H2CBD |
| 10 | Pt/alumina | 378131-8-A016 | Screening experiments |
| 11 | Pt/alumina | 378131-8-A017 | Kinetics with A020 (CSM A) |
| 12 | Pt/alumina | 378131-8-A018 | Long run to prepare H2CBD |
| 13 | Pt/alumina | 378131-8-A019 | Long run to prepare H2CBD |
| 11 | Dt/alumina | 270121 0 4020 | Hydrogenation of limonene |
| 14 | Pt/alullina | 576151-0-AUZU | Kinetic study (CSM A) |
| 1 5 | Dt/alumina | 246121 9 4226 | Long run to prepare H4CBD |
| 15 | Pt/alumna | 340131-8-AZ30 | Long run to prepare HHC |
| 10 | Dt/alumina | 246121 0 4220 | Long run to prepare H4CBD |
| 10 | Pt/alumna | 340131-8-AZ38 | Long run to prepare HHC |
| | | | Long run to prepare H4CBD |
| 17 | Pt/alumina | 346131-8-A240 | Kinetic study (CSM B) |
| | | | Long run to prepare HHC |
| | | | Long run to prepare H4CBD |
| 18 | Pt/alumina | 346131-8-A241 | Kinetics with A240 (CSM B) |
| | | | Long run to prepare HHC |

1.2. High Field NMR

NMR spectra were obtained by using a Bruker 300 MHz instrument (¹H: 300 MHz, ¹³C: 75 MHz). All the samples were prepared in acetonitrile-d₃. The chemical shifts of ¹H and ¹³C are given in ppm, relative to the peak of the solvent. Coupling constants are given in Hertz (Hz). Multiplicity is indicated with the following abbreviations: s-singlet, d-doublet, t-triplet, q-quartet and m-multiplet. Carbon and hydrogen spectra are reported at the end of this document from Figure S 39 to Figure S 50.

1.3. GC-FID Analysis

GC-FID analysis was performed by using a Shimadzu GC-FID 230 with a flame ionization detector, suing an RTX-5MS column (30 m x 0.25 mm ID x 0.25 μ m) and helium as carrier gas (40 cm/sec linear velocity) and a split ratio of 5. The temperature of the injector was set to 280 °C. After 1 min at 50 °C, the temperature increased by 25 °C/min to 300 °C and kept constant at 300 °C for 4 min. Hydrogen and synthetic air (5.0 quality) were used to ignite the flame of the detector. Examples of chromatograms are provided in Figure S 1 for the processing of CBD and Figure S 2 for the processing of THC.





Figure S 1: Example of GC-FID chromatogram for the hydrogenation of CBD over Pd/alumina CSMs. Retention times: CBD (1) (11.46 min); H2CBD (2) (11.54 min); cis-H4CBD (3) (11.58 min); trans-H4CBD (4) (11.64 min). Top – Zoomed in chromatogram; Bottom – Full chromatogram.



Figure S 2: Example of GC-FID Chromatogram for the hydrogenation of Δ 9-THC (**5**) to HHC over Pt/alumina. Retention times: R¬HHC (**7**) 11.55 min; S-HHC (**8**) 11.62 min; Δ ⁸-THC 11.72 min (**6**); Δ ⁹-THC 11.82 min (**5**). Top – Zoomed in chromatogram; Bottom – Full chromatogram.

The results obtained with the GCFID were validated using ¹H-NMR. The parity plots are

reported in Figure S 3.



Figure S 3: Parity plots for the content of different species, as measured by NMR and GC-FID.

1.4. GC-MS Analysis

GC-MS analysis was performed using a Shimadzu GCMS-QP2010 SE, using an RTX5MS column (30 m x 0.25 mm x 0.25 μ m) and helium as carrier gas with a linear velocity of 40 cm/sec. The injector temperature was set to 280 °C. After 1 min at 50 °C, the oven temperature increased by 25 °C/min to 300 °C and kept for 3 min. The mass detector

was a quadrupole with pre rods and electron impact ionization. The following settings were used in the detector: ion source temperature 200 °C, interface temperature 310 °C, solvent cut time 2.5 min, acquisition mode scan, mass range m/z = 50400. The spectra are reported at the end of this document from Figure S 31 to Figure S 37.

1.5. ICP-MS Analysis

The leaching of platinum was assessed by inductively coupled plasma mass spectrometry (ICPMS) (Agilent 7900). Three liquid samples were submitted, all from the processing of CBD. Before the ICP-MS analysis, the samples were diluted with ultrapure water and $1\%_{v}$ HNO₃ + 0.5%_v HCl. All the samples showed negligible amounts of metal (<1 ppb).

1.6. SEM and EDS Images

Scanning electron microscopy (SEM) images and energy dispersive X-ray spectroscopy (EDS) analysis were performed using a Zeiss Gemini DSM 982 field emission SEM. The EDS-based quantitative elemental analysis and element distribution mapping were performed using an Oxford Instruments Ultim Max 40 silicon drift detector. All imaging and EDS analyses were made with an acceleration voltage of 10 kV and a working distance of 11 mm. For quantification and EDS map generation, we used the software package provided with the Oxford Instruments AZTec (v.6.1), using the available standard EDS quantification library. In the following section we report three SEM imaging with the EDS traces for Pd/alumina (Figure S 4, Table S 2), Pt/alumina (Figure S 5, Table S 3) and Ru/alumina (Figure S 6, Table S 4).

1.6.1. Pd/alumina



Figure S 4: SEM and EDS measurement for palladium on alumina CSM.

Table S 2: Elemental content for the CSM.

| Element | Line | %w | Error %w |
|---------|----------|--------|----------|
| 0 | K series | 42.06 | |
| F | K series | 1.03 | 0.06 |
| Al | K series | 44.39 | 0.16 |
| S | K series | 0.42 | 0.03 |
| Cl | K series | 0.59 | 0.04 |
| Cr | L series | 0.00 | 1.37 |
| Fe | L series | 1.61 | 0.20 |
| Pd | L series | 9.91 | 0.16 |
| Total | | 100.00 | |

1.6.2. Pt/alumina



 Al Kα1
 Pt Mα1

 Image: Prime state stat

Figure S 5: SEM and EDS imaging of two sections of a platinum on alumina CSMs. Table S 3: Elemental content for the CSM.

| Element | Line | %w | Error %w |
|---------|----------|--------|----------|
| 0 | K series | 42.13 | 0.20 |
| F | K series | 0.77 | 0.07 |
| Na | K series | 0.34 | 0.04 |
| Al | K series | 46.87 | 0.21 |
| Si | K series | 3.24 | 0.07 |
| Ni | L series | 1.22 | 0.12 |
| Pd | L series | 0.00 | 0.15 |
| Pt | M series | 5.44 | 0.26 |
| Total | | 100.00 | |

1.6.3. Ru/alumina



Figure S 6: SEM and EDS measurement for ruthenium on alumina CSM. Table S 4: Elemental content for the CSM.

| Element | Line | %w | Error %w | |
|---------|----------|--------|----------|--|
| 0 | K series | 46.49 | 0.17 | |
| Na | K series | 0.33 | 0.04 | |
| Al | K series | 47.48 | 0.17 | |
| Р | K series | 0.00 | 0.04 | |
| S | K series | 0.17 | 0.04 | |
| Cl | K series | 0.50 | 0.07 | |
| Fe | L series | 0.00 | 0.23 | |
| Ru | L series | 5.04 | 0.19 | |
| Total | | 100.00 | | |
| | | | | |

1.7. Experimental Setup

A labeled image of the flow configuration is given in Figure S 7. The liquid feed was delivered by a HPLC pump (Knauer AZURA P 4.1S). Hydrogen was delivered by a H-Genie hydrogen generator (ThalesNano), with an integrated mass flow controller (MFC), operated with HPLC grade water. The HGenie was also fitted with a pressure sensor to monitor the pressure of the whole setup. A sixway valve was used for screening experiments. Either a 4 mL or a 10 mL sample loop was used in the screening experiments. The gas and the liquid streams were combined in a Y-connector made of PEEK, immediately before entering the Ehrfeld Modular MicroReaction System (MMRS) system via a 1/16" input connector, through transparent tubing (PFA, 0.8 mm i.d.). The hydrogenation reactions were performed using an Ehrfeld Miprowa reactor (0224-2-

2004-F, Hastelloy C-276). This reactor comprises 8 channels with a rectangular crosssection (1.5 mm x 12 mm x 300 mm), and an internal volume of each channel, after the insertion of the CSMs, previously estimated by Lebl to be 3.4 mL.¹ Only 4 channels were used during this investigation (i.e. half of the reactor). Each channel can house up to 2 CSMs. During the investigation, either 1 (limonene hydrogenation only), 2 or 4 CSMs were used, and they were housed in the top channels (i.e. 5A, 5B, 8A and 8B, where A and B refer respectively to the right and the lefthand side of the channel). The remaining channels were filled with stainless steel fishbone mixers. The temperature of the reactor was controlled by a Huber CC-304 thermostat and was monitored by an internal thermocouple located in the recirculation loop. After the reactor, the process stream was cooled down in a 1 mL stainless steel coil (0.8 mm i.d.) which was submerged in a water bath at room temperature. The pressure inside the system was then controlled by a back pressure regulator (BPR) (Equilibar HC 276, maximum pressure 34 Bar; max temperature 300 °C). At ambient pressure, the excess hydrogen was separated by a custom-made gas-liquid separator. The liquid stream was then collected into a flask for subsequent offline analysis and processing. A description of the CSMs and a description of the Miprowa reactor can be found in previous works.^{1,2}



Figure S 7: Hydrogenation setup. Items: solvent reservoir (1), HPLC pump (2), six¬way valve (3), sample loop (4), Miprowa reactor (5), cooling coil (6), BPR (7), gas¬liquid separator (8), collection flask (9) and thermostat (10). The H¬Genie is not displayed.

1.8. Batch Synthesis of Δ^8 -THC

Scheme S 1: Reaction for the synthesis of Δ^8 -THC.

A procedure described in literature was used.³ The reaction is presented in Scheme S 1. CBD (3.0 g, 1 eq.) was inserted into a round flask along with a solution of *p*-toluene sulphonic acid (PTSA) (300 mg, 0.1 eq.) in toluene (150 mL) under a nitrogen atmosphere. The solution was refluxed at 110 °C for 2.5 h and then it was diluted with diethyl ether (200 mL) and poured into 100 mL of cold water. The upper layer was recovered, washed first with a saturated solution of NaHCO₃ (100 mL) and then with water (100 mL). The organic layer was then dried over Na₂SO₄ anhydrous, filtrated and

evaporated under vacuum. The recovered red oil was purified with column chromatography (Section 1.9) to obtain Δ^8 -THC (1.93 g, yield 61%, purity 94%). The chromatogram of the compound post purification is represented in Figure S 8.



Figure S 8: GC-FID chromatogram of Δ^8 -THC after purification. Some residual CBD and some Δ^9 -THC can be observed in the smaller plot.

1.9. Purifications by Biotage Isolera

Purification of Δ^8 -THC and H4CBD was performed using a Biotage Isolera 1. Ethyl acetate was used as high polarity solvent (A) and petroleum ether as low polarity solvent (B). Two wavelengths were set on the detector, 254 nm and 280 nm. Silica was used as a solid phase. Biotage DS 25 g columns were used. The gradients used for the purification of Δ^8 THC and H4CBD are reported in Table S 5. Separation of H2CBD from CBD was attempted but proved to be challenging.

Table S 5: Gradients of solvents A used for the purification of Δ^8 -THC and H4CBD.

| Length | Start | End |
|--------|-------|-----|
| [CV] | [% |] |
| 3 | 0 | 0 |
| 10 | 0 | 3 |
| 15 | 3 | 5 |
| 5 | 5 | 10 |
| 10 | 10 | 10 |
| 7 | 10 | 25 |

2. Catalytic Static Mixer Results

2.1. Hydrogenation of CBD over Pd-electroplated (PdEP) CSMs

The results of the screening from the hydrogenation of CBD over Pd-electroplated CSMs are reported in the following sections.

2.1.1. Solvent Screening

The results for the experiments performed with either ethyl acetate or ethanol, at 60 $^\circ\mathrm{C}$

and 100 °C, are reported in Table S 6. For all further experiments reported in the ESI, the

solvent used was ethyl acetate.

Table S 6: Results for the solvent screening in the hydrogenation of CBD over Pd–EP CSMs. Conditions: [0.09 M] CBD, 20 bar; H/S 11.3; 102 s.

| Entry | Solvent | Temperature | Conversion | Selectivity | | | |
|-------|---------|-------------|------------|-------------|---------|---------|------|
| | | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. |
| | | [°C] | | | [%] | | |
| 1 | EtOH | 60 | 14.3 | 81.9 | 0 | 3.1 | 15.0 |
| 2 | EtOH | 100 | 49.3 | 65.8 | 13.7 | 5.4 | 15.1 |
| 3 | EtOAc | 60 | 18.2 | 81.2 | 5.5 | 2.7 | 10.6 |
| 4 | EtOAc | 100 | 51.6 | 70.6 | 12.1 | 4.8 | 12.5 |

2.1.2. Temperature Screening

The results for the impact of temperature on the hydrogenation of CBD are reported in

Table S 7.

Table S 7: Results for the temperature screening in the hydrogenation of CBD over Pd-EP CSMs. Conditions: [0.09 M] CBD, 20 bar; H/S 11.3; 102 s.

| Entry | Temperature | Conversion | Selectivity | | | |
|-------|-------------|------------|-------------|---------|---------|------|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. |
| | [°C] | | | [%] | | |
| 1 | 60 | 18.2 | 81.2 | 5.5 | 2.7 | 10.6 |
| 2 | 100 | 51.6 | 70.6 | 12.1 | 4.8 | 12.5 |
| 3 | 120 | 83.2 | 47.7 | 27.3 | 11.6 | 13.5 |
| 4 | 140 | 89.7 | 36.1 | 35.5 | 15.7 | 12.7 |

2.1.3. Residence Time Screening

The results for the screening of different residence times for the hydrogenation of CBD at 140 °C are reported in Table S 8. There was evidence of deactivation due to the irregularity in the trend with increasing residence time at the same temperature.

| Table S 8: F | Results f | or the | screening | of re | sidence | time I | in the | hydrogenation | of | CBD | over | Pd-EP | CSMs. |
|--------------|-----------|--------|-------------|-------|-----------|--------|--------|---------------|----|-----|------|-------|-------|
| Conditions: | [0.09 M] | CBD, 2 | 20 bar; H/S | 11.3 | ; 140 °C. | | | | | | | | |

| Entry | Residence Time | Conversion | Selectivity | | | |
|-------|-----------------------|------------|-------------|---------|---------|------|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. |
| | [s] | | | [%] | | |
| 1 | 102 | 89.7 | 36.1 | 35.5 | 15.7 | 12.7 |
| 2 | 204 | 89.3 | 42.1 | 30.0 | 15.7 | 12.2 |
| 3 | 408 | 91.6 | 42.5 | 27.4 | 17.2 | 12.8 |

2.2. Hydrogenation of CBD over Pd/alumina CSMs

The results of the screening for the hydrogenation of CBD over Pd/alumina CSMs are reported in the following sections.

2.2.1. H/S Ratio Screening

The hydrogen to substrate ratio (H/S) was screened at 25 mL_n/min and 75 mL_n/min, at

140 °C and at a liquid flow of 2 mL/min. The results are presented in Table S 9.

Table S 9: Results for the H/S ratio screening in the hydrogenation of CBD over Pd/alumina CSMs. Conditions: [0.1 M] CBD, 20 bar, 102 s, 140 °C.

| Entry | H/S Ratio | Conversion | | | | |
|-------|-----------|------------|-------|---------|---------|------|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. |
| | [-] | | | [%] | | |
| 1 | 5.7 | 98.9 | 7.6 | 48.1 | 25.8 | 18.5 |
| 2 | 17.2 | 98.9 | 7.3 | 48.3 | 26.5 | 17.9 |

2.2.2. Temperature Screening

The results for the screening of the hydrogenation of CBD at different temperatures in

the range 60 to 160 °C are reported in Table S 10.

Table S 10: Results for the temperature screening in the hydrogenation of CBD over Pd/alumina CSMs. Conditions: [0.1 M] CBD, 20 bar; H/S 11.3, 102 s.

| Entry | Temperature | Conversion | Selectivity | | | | |
|-------|-------------|------------|-------------|---------|---------|------|--|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. | |
| | [°C] | | | [%] | | | |
| 1 | 60 | 64.5 | 44.3 | 21.8 | 9.8 | 24.1 | |
| 2 | 100 | 95 | 14.9 | 46.9 | 21.6 | 16.6 | |
| 3 | 120 | 98 | 7.5 | 54.4 | 25.2 | 12.9 | |
| 4 | 140 | 99.2 | 4.1 | 58.7 | 27 | 10.2 | |
| 5 | 160 | 99.7 | 3.0 | 58.5 | 28.5 | 10.1 | |

2.2.3. Long Run with CBD at 160 °C

The system was operated for a total of 40 min. During the experiment, 8 fractions were collected and analyzed by GCFID. The results are presented in Table S 11 and Figure S 9.

| Sample | Collection Time | Conversion | | Sele | ectivity | | Cis:Tran s |
|--------|-----------------|------------|-------|---------|----------|------|---------------|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. | |
| | [min] | | | [%] | | | [-] |
| 1 | 5 | 99.6 | 3.6 | 54.9 | 28.6 | 12.9 | 1.92 |
| 2 | 10 | 99.7 | 4.1 | 54.2 | 28.9 | 12.7 | 1.88 |
| 3 | 15 | 99.7 | 4.4 | 53.3 | 28.6 | 13.7 | 1.86 |
| 4 | 20 | 99.6 | 4.9 | 53.2 | 27.8 | 14.0 | 1.91 |
| 5 | 25 | 99.6 | 4.9 | 51.2 | 28.5 | 15.4 | 1.80 |
| 6 | 30 | 99.2 | 5.9 | 50.1 | 26.8 | 17.1 | 1.87 |
| 7 | 35 | 99.4 | 5.7 | 50.0 | 27.0 | 17.2 | 1.86 |
| 8 | 40 | 99.5 | 5.9 | 49.3 | 26.8 | 17.8 | 1.84 |
| Averag | | 99.5 | 4.9 | 52.0 | 27.9 | 15.1 | 1.87 |

Table S 11: Long run with Pd/alumina CSMs. Conditions: [0.1 M] CBD, 160 °C, 20 bar, 102 s, H/S 11.3.



Figure S 9: Long run trend for the reaction of CBD (1) at 160 °C, see Table S11 for the full set of conditions.

2.3. Hydrogenation of THC over Ru/alumina CSMs

2.3.1. Temperature Screening

The results from the screening of temperature for the hydrogenation of Δ^8 -THC over Ru/alumina CSMs are reported in Table S 12 and Figure S 10. No impurities were observed.

Table S 12: Results for the temperature screening in the hydrogenation of Δ^8 -THC over Ru/alumina CSMs. Note: different Conditions: [0.1 M] Δ^8 -THC, 20 Bar, 408 s, H/S 178.

| Entry | Temperature | Conversion | Selectivity | | |
|-------|-------------|--------------------|-------------|------|--|
| | | ∆ ⁸ THC | RHHC | SHHC | |
| | [°C] | | [%] | | |
| 1 | 70 | 74.3 | 54.2 | 45.8 | |



Figure S 10: Results for the temperature screening as area %.

2.3.2. Catalyst Recoverability by Washing with Acetone

The influence of an acetone wash on the recoverability of the catalyst was investigated by testing the hydrogenation of CBD over a previously used Ru/alumina CSM at 60 °C, 102 s and 20 Bar. The catalyst was first washed online with pure ethyl acetate during a long run where the performance was decreasing over time (Figure S 11). After washing, no changes were seen regarding the performance of the catalyst. The catalyst was then tested at 60 °C, taken offline, washed with acetone and re-tested and the results are reported in Figure S 12. A strong recovery in activity was observed as demonstrated with the increase in H4CBD formed.



Figure S 11: Long run for the conversion of CBD over Ru/alumina with a washing step at 45 min.



Figure S 12: Results for the conversion of CBD over Ru/alumina before and after a washing step with acetone. The increase in H4CBD after a wash demonstrated the increase in the catalytic activity.

2.4. Hydrogenation of CBD over Pt/alumina CSMs

The results of the screening for the hydrogenation of CBD, H2CBD and THC over Pt/alumina CSMs are reported in the following sections.

2.4.1. Blank Experiment

The Blank experiments were performed with a 0.1 M solution of CBD at 60 °C and 80 °C, 408 s, 20 bar, over Pt/alumina CSMs, without hydrogen. The GC profiles before and after the run are reported in Figure S 13. No conversion of CBD or formation of impurities were observed.



Figure S 13: GC-FID traces of the blank experiment (CBD peak in the square).

2.4.2. H/S Ratio Screening

The results from the screening of the hydrogen flow rates to avoid mass transfer limitations are reported for two residence times in Table S 13 and in Figure S 14.



Table S 13: Results for the screening of different hydrogen flows at different residence times. Conditions: [0.1 M] CBD, 20 bar, 80 °C.



2.4.3. CBD Concentration Screening

The results for the screening of different concentrations of CBD are reported in Table S 14 and in Figure S 15.

| Entry | Concentration | Residence Time | Conversion | Selectivity | | | |
|-------|---------------|-----------------------|------------|-------------|---------|---------|------|
| | | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. |
| | [M] | [s] | | | [%] | | |
| 1 | 0.1 | 68 | 87.6 | 71.1 | 25.4 | 2.7 | 0.8 |
| 2 | 0.3 | 68 | 85.9 | 73.4 | 23.0 | 2.9 | 0.7 |
| 3 | 0.1 | 136 | 95.7 | 59.1 | 36.1 | 4.2 | 0.6 |
| 4 | 0.3 | 136 | 94.9 | 61.2 | 33.6 | 4.6 | 0.6 |

Table S 14: Results for the screening of concentrations. Conditions: [0.1 M] CBD, 20 bar, 65 °C, H/S 59.5.



Figure S 15: Results for the screening of two different concentrations.

Further screening was performed with a concentration of CBD of up to 0.5 M, with the results shown in Table S 15 and Figure S 16. Some differences can be seen above 0.3 M, where the performance decreases. It is difficult to say if it is due to a change in kinetics or due to a faster rate of deactivation caused by an increase in concentration.



Table S 15: Screening of different concentrations of CBD. Conditions: 60 °C, 11 bar, 215 s, H/S 22.3.

Figure S 16: Screening of different concentrations of CBD.

2.4.4. Design of Experiments (DoE): Influence of Temperature and Pressure

The factors and the levels used in the DoE are reported in Table S 16. The results of the DoE are reported in Table S 17.

Table S 16: Factors and Levels used for the DoE.

| | | -1 | 0 | +1 | |
|-------------|-------|-----|----|-----|--|
| Temperature | [°C] | 60 | 80 | 100 | |
| Pressure | [Bar] | 5.5 | 13 | 21 | |

| Entry | Temperature | Pressure | Conversion | Selectivity | | | |
|-------|-------------|----------|------------|-------------|---------|---------|------|
| | | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. |
| | [°C] | [bar] | | | [%] | | |
| 1 | 100 | 21 | >99 | 3.0 | 82.5 | 14.5 | 0 |
| 2 | 100 | 5.5 | >99 | 1.2 | 81.6 | 17.2 | 0.1 |
| 3 | 80 | 13 | >99 | 22.3 | 66.5 | 10.6 | 0.6 |
| 4 | 80 | 13 | >99 | 25.8 | 63.4 | 10.2 | 0.6 |
| 5 | 60 | 21 | 98.2 | 76.6 | 20.8 | 2.2 | 0.4 |
| 6 | 60 | 5.5 | 99.1 | 67.4 | 27.7 | 3.8 | 1.1 |

Table S 17: Results of DoE. Conditions: [0.1 M] CBD, 204 s; H/S 22.3.

The parity plots and the summary of fit obtained with Modde v.13 are reported in Figure S 17.



Figure S 17: Results from the analysis of the data in Modde.

2.4.5. Temperature Screening

The results for the screening in the range 60 to 100 °C are reported in Table S 18.

Table S 18: Results for the temperature screening over Pt/alumina. Conditions: [0.1 M], 20 bar, 102 s, H/S 11.2.

| Entry | Temperature | Conversion | | | | |
|-------|-------------|------------|-------|---------|---------|------|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. |
| | [°C] | | | [%] | | |
| 1 | 60 | 87.8 | 13.1 | 74.8 | 9.7 | 2.4 |
| 2 | 80 | 94.8 | 9.6 | 78.4 | 10.6 | 1.4 |
| 3 | 100 | 98.1 | 5.1 | 82.9 | 10.8 | 1.2 |

2.4.6. Residence Time Screening

The results for the screening in the range 204 to 544 s, at 80 °C are reported in Table S 19.

Table S 19: Results of the residence time screening over Pt/alumina CSMs. Conditions: [0.1 M] CBD, 80 °C, 20 bar. The H/S ratio varied based on the liquid flow rate at a fixed gas flow of 200 mL_n/min.

| Entry | Residence Time | Conversion | Selectivity | | | |
|-------|----------------|------------|-------------|---------|---------|------|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. |
| | [s] | | | [%] | | |
| 1 | 544 | >99 | 1.0 | 80.0 | 18.5 | 0.5 |
| 2 | 408 | >99 | 2.1 | 74.8 | 22.6 | 0.5 |
| 3 | 272 | 99.3 | 6.0 | 73.5 | 19.5 | 1.0 |
| 4 | 204 | 98.9 | 11.9 | 69.9 | 16.5 | 1.7 |

2.4.7. Long Run for the Hydrogenation of CBD to H4CBD Based on Unoptimized Conditions

The system was operated for 90 min with a 0.1 M feed solution of CBD. The solution was pumped at a flow rate of 1.50 mL/min, giving a residence time of 272 s. The reaction temperature was 80 °C. During the experiment 6 fractions were collected and analyzed on the GC-FID (Table S 20 and Figure S 18). The solvent was removed under vacuum to obtain 5.03 g of crude product mixture.

| Entry | Collection Time | Conversion | | Select | ivity | | Cis:Trans |
|---------|------------------------|------------|-------|---------|---------|------|-----------|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. | |
| | [min] | | | [%] | | | [-] |
| 1 | 15 | 99.4 | 12.0 | 70.2 | 16.0 | 1.8 | 4.4 |
| 2 | 30 | 99.3 | 13.3 | 69.6 | 15.2 | 1.9 | 4.6 |
| 3 | 45 | 99.3 | 12.5 | 70.2 | 15.5 | 1.8 | 4.5 |
| 4 | 60 | 99.4 | 12.1 | 71.4 | 14.7 | 1.9 | 4.9 |
| 5 | 75 | 99.4 | 12.2 | 71.6 | 14.3 | 1.9 | 5.0 |
| 6 | 90 | 99.4 | 13.6 | 69.4 | 15.0 | 2.0 | 4.6 |
| Average | | 99.4 | 12.6 | 70.4 | 15.1 | 1.9 | 4.7 |

Table S 20: Measured conversion and selectivity during the long run for the preparation of H4CBD.



Figure S 18: Results in area % over time in the long run for the preparation of H4CBD

2.4.8. Long Run for the Synthesis of H4CBD at Optimized Conditions

The system was operated for 180 min with a 0.1 M solution of CBD at 80 °C. The solution was pumped at a flow rate of 0.75 mL/min, giving a residence time of 544 s. The H/S ratio was equal to 119. During the experiment, 6 fractions were collected and analyzed on the GC-FID (Table S 21). The solvent was removed under vacuum to afford H4CBD (3.69 g, 86% yield, 92.3% purity, cis:trans ratio 5.5) as a transparent oil. The productivity was about 1.23 g/h.

| Sample | Collection Time | Conversion | | Select | ivity | | Cis:Trans |
|---------|------------------------|------------|-------|---------|---------|------|-----------|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. | |
| | [min] | | | [%] | | | [-] |
| 1 | 30 | 99.8 | 4.2 | 77.6 | 16.3 | 1.0 | 4.8 |
| 2 | 60 | 99.8 | 3.6 | 78.3 | 16.3 | 0.9 | 4.8 |
| 3 | 90 | 99.8 | 4.2 | 77.8 | 16.1 | 1.0 | 4.8 |
| 4 | 120 | 99.8 | 3.6 | 78.1 | 16.4 | 1.0 | 4.8 |
| 5 | 150 | 99.8 | 3.5 | 78.0 | 16.5 | 1.0 | 4.7 |
| 6 | 180 | 99.8 | 3.2 | 78.7 | 16.4 | 0.9 | 4.8 |
| Average | | 99.8 | 3.7 | 78.1 | 16.3 | 1.0 | 4.8 |

Table S 21: Results for the long run for the preparation of H4CBD

2.4.9. Long Run for the synthesis of H2CBD at Optimized Conditions

The system was operated for 55 min with a 0.1 M feed solution of CBD. The solution was pumped at a flow rate of 2.0 mL/min, giving a residence time of 204 s. A H/S ratio of 11.7, a pressure of 11.2 bar and a temperature of 60 °C were used. During the experiment 4 fractions were collected and analyzed on the GC-FID (Table S 22). The solvent was removed under vacuum to give H2CBD (2.80 g, 89% purity) as a transparent

oil. Further purification of the product with column chromatography proved difficult due to the similarity of the compounds present in the mixture (CBD and H4CBD).

| Entry | Collection Time | Conversion | Selectivity | | | |
|---------|-----------------|------------|-------------|---------|---------|------|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. |
| | [min] | | | [%] | | |
| 1 | 15 | 97.2 | 91.6 | 7.4 | 0.7 | 0.3 |
| 2 | 30 | 96.7 | 91.9 | 6.9 | 0.8 | 0.3 |
| 3 | 45 | 96.1 | 93.0 | 6.4 | 0.4 | 0.2 |
| 4 | 55 | 95.8 | 94.1 | 4.9 | 0.8 | 0.2 |
| Average | | 96.5 | 92.7 | 6.4 | 0.7 | 0.3 |

Table S 22: Conversion and selectivity in the long run for the hydrogenation of CBD to H2CBD

2.5. Hydrogenation of H2CBD to H4CBD over Pt/alumina CSMs

2.5.1. Temperature Screening

The results for the screening of the hydrogenation of H2CBD at different temperatures are reported in Table S 23.

Table S 23: Results for the temperature screening for the synthesis of H4CBD from H2CBD. Conditions: 102 s; H/S 11.2, 20 bar.

| Entry | Temperature | Conversion | | Select | ivity | |
|-------|-------------|------------|-------|---------|---------|------|
| | | CBD | H2CBD | c-H4CBD | t-H4CBD | Imp. |
| | [°C] | | | [%] | | |
| 1 | 60 | 99.7 | 20.4 | 70.5 | 8.2 | 0.9 |
| 2 | 80 | 99.8 | 12.2 | 77.3 | 9.8 | 0.7 |
| 3 | 100 | >99 | 7.2 | 81.5 | 10.7 | 0.6 |

2.6. Hydrogenation of THC over Pt/alumina CSMs

2.6.1. Hydrogenation of Δ^9 -THC: Screening of Temperature and Residence Time

The results for the screening of temperatures and residence time for the hydrogenation of Δ^9 -THC are reported in Table S 24.

Entry Temperature **Residence Time** Conversion Selectivity ∆⁹THC RHHC SHHC ∆⁸THC Imp. [°C] [s] [%] 0.5 1 60 408 92.3 51.3 39.0 9.2 2 70 408 98.4 60.6 34.0 4.9 0.5 3 204 35.3 7.7 0.4 80 95.0 56.6 4 408 99.5 67.0 30.9 1.7 1.1 80 5 80 544 99.7 67.7 30.5 1.3 1.1 6 90 408 >99 61.2 36.9 1.4 0.5

Table S 24: Results for the screening of temperature and residence time in the hydrogenation of Δ^9 -THC. Conditions: [0.1 M], 20 bar. Note: a constant flow of 200 mL_n/min of H₂ was used.

2.6.2. Long Run for the Synthesis of HHC from Δ^9 -THC at Optimized Conditions

The system was operated for 25 min with a 0.1 M solution of Δ^9 THC. The solution was pumped over 4 CSMs at a flow rate of 1.0 mL/min, giving a residence time of 408 s. A H/S ratio of 118, 20 bar and 80 °C were used. During the experiment 5 fractions were collected and analyzed on the GC-FID (Table S 25 and Figure S 19). The solvent was removed under vacuum to afford HHC (0.69 g, 87% yield, 97.7% purity, R:S ratio 2.4) as a transparent oil. The productivity of the process was equal to 1.62 g/h.

| Entry | Entry Collection Time Conversion Selectivity | | | R:S | | |
|---|--|---------------------|--------------|-------|------|-----|
| | | Δ ⁹ -THC | RHHC | SHHC | Imp. | |
| | [min] | | [%] | | | [-] |
| 1 | 5 | >99 | 69.4 | 30.6 | - | 2.3 |
| 2 | 10 | >99 | 70.7 | 29.3 | - | 2.4 |
| 3 | 15 | >99 | 71.3 | 28.7 | - | 2.5 |
| 4 | 20 | >99 | 70.9 | 29.1 | - | 2.4 |
| 5 | 25 | >99 | 71.0 | 29.0 | - | 2.4 |
| Average | | >99 | 70.7 | 29.3 | - | 2.4 |
| NMR Average | | >99 | 65.7 | 27 | 2.3 | 2.4 |
| 100 % 75 EV 4 50 25 0 | • | | • | | | |
| | 0 5 | 10 15 Time [min] | 20 | 25 | 30 | |
| | ···• cis-HHC | trans-HHC | ···· ①···· Δ | 9-THC | | |

Table S 25: Conversion and selectivity in the long run for the hydrogenation of Δ^9 -THC.

Figure S 19: Results in the long run for the hydrogenation of Δ^9 -THC.

2.6.3. Hydrogenation of Δ^8 -THC: screening of Temperature and Residence Time

The results for the screening of temperatures and residence time for the hydrogenation of Δ^{8} -THC are reported in Table S 26. No impurities were observed.

Table S 26: Results for the screening of temperature in the hydrogenation of Δ^8 -THC. Conditions: [0.1 M], 408 s, 20 bar, H/S 89.

| Entry | Temperature | Conversion Selectivi | | tivity |
|-------|-------------|----------------------|------|--------|
| | | Δ ⁸ -THC | RHHC | SHHC |
| | [°C] | | [%] | |
| 1 | 60 | 90.7 | 56.7 | 43.3 |
| 2 | 70 | 95.1 | 64.0 | 36.0 |
| 3 | 80 | 98.3 | 68.4 | 31.6 |

2.6.4. Long Run for the Synthesis of HHC from Δ^8 -THC at Optimized Conditions

The system was operated for 55 min with a 0.1 M solution of Δ^{8} -THC (94% purity of starting material). The solution was pumped at a flow rate of 1.0 mL/min, giving a residence time of 408 s. A H/S ratio of 118, 20 Bar and 80 °C were used. During the experiment 6 fractions were collected and analyzed on the GC-FID (Table S 27 and Figure S 20). The solvent was removed under vacuum to afford HHC (1.8 g, 97% yield, 94% purity) as a light brown oil. The throughput was equal to 1.8 g/h. The number of impurities remained constant at the same value as the starting solution. For this reason, the impurities are omitted in the table.



Table S 27: Conversion and selectivity in the long run for the hydrogenation of Δ^{8} -THC.

Figure S 20: Results for the long run for the hydrogenation of Δ^{8} -THC.

3. Kinetics Investigation

3.1. Experimental Methods

3.1.1. Preparation of the Stock Solution

1 L of a [0.1 M] internal standard solution of hexadecane (22.645 g, 0.1 mol) was used to prepare a 1 L of a [0.1 M] solution of CBD (31.5 g, 0.1 mol).

3.1.2. Deconvolution of GCFID Peaks

Peak deconvolution was performed with hplcpy, a Python package developed by Chure and Cremer.⁴ An example of a deconvoluted spectrum is reported in Figure S 21. The results obtained from the deconvolution of different mixtures were compared against those derived from a simple peak integration assuming peak splitting. The parity plot for this comparison is presented in Figure S 22. Overall, we observed that fitting the whole spectra did not yield good results as the size of the peaks of ISTD and compounds were quite dissimilar. We therefore decided to fit the two regions (ISTD and reaction peaks) separately. Moreover, the recognition of the small peaks was not always feasible (Figure S 21, left) and it was possible only for some of the spectra after changing of the input parameters. We therefore decided to use the simpler peak integration for kinetic analysis.



Figure S 21: Example of peak deconvolution. Left: small peak not detected. Right: Complete detection.



Figure S 22: Parity plot between the concentration measured by peak integration and that measured by peak deconvolution.

3.2. Kinetics Results

3.2.1. Matlab Model

Table S 28 reports the different sum of squares error (SSE) for the different scenarios considered in the kinetic fitting of the data measured at 60 °C.

Table S 28: Sum of square errors for different deactivation models, kd = rate constant for deactivation

| | SSE |
|------------------|-------|
| One kd for all | 0.376 |
| kd for H4CBD | 0.417 |
| kd for H2CBD | 0.498 |
| kd for cis-H4CBD | 0.466 |
| no kd | 0.562 |

The fitted kinetic trends for Pt/alumina CSM (A) are reported in Figure S 23. The Arrhenius plot is presented in Figure S 24. The values of the kinetic constants are reported in Table S 29.



Figure S 23: Kinetic fittings at different temperature for CSMs A.



Figure S 24: Arrhenius plot for CSMs A.

Table S 29: Fitted kinetic constants for CSMs A at different temperatures.

| Temperature | k1 | k2 | k3 | kd |
|-------------|-------|-------|---------|--------|
| [°C] | | l | [1/s] | |
| 50.5 | 0.026 | 0.004 | 0.0003 | 0.0048 |
| 60.5 | 0.024 | 0.005 | 0.0006 | 0.0045 |
| 80.3 | 0.049 | 0.013 | 0.0019 | 0.0078 |
| 70.4 | 0.024 | 0.006 | 0.00072 | 0.0049 |

The errors of the Arrehenius parameters are reported in Table S 30.

| | k 1 | L | k2 | 2 | ka | 3 | k | d |
|---------------|------------|-------|---------|-------|---------|-------|---------|--------|
| Fitting | -2078.8 | 2.615 | -4581.7 | 8.454 | -6224.8 | 11.18 | -1669.1 | -0.294 |
| SE 95% | 1614.9 | 4.777 | 1316.4 | 3.894 | 1297.5 | 3.838 | 1029.8 | 3.047 |
| R2 | 0.453 | 0.314 | 0.858 | 0.256 | 0.920 | 0.252 | 0.568 | 0.200 |
| F-test | 1.657 | 2 | 12.11 | 2 | 23.02 | 2 | 2.627 | 2 |
| SSreg. SSres. | 0.163 | 0.197 | 0.791 | 0.131 | 1.46 | 0.127 | 0.105 | 0.0800 |

Table S 30: Errors of Arrhenius fittings.

The fitted kinetic trends for Pt/alumina CSM (B) are reported in the manuscript. The Arrhenius plot is reported in Figure S 25.



Figure S 25: Arrhenius plot for CSMs B.

The kinetic constants are in Table S 31.

| Table S 31: Fitted kinetic constants | s for CSMs B | at different | temperatures |
|--------------------------------------|--------------|--------------|--------------|
|--------------------------------------|--------------|--------------|--------------|

| Temperature | k1 | k2 | k3 | deact |
|-------------|-------|--------|---------|---------|
| [°C] | | l | [1/s] | |
| 50.5 | 0.021 | 0.0035 | 0.00034 | 0.00237 |
| 60.1 | 0.025 | 0.0039 | 0.00035 | 0.00408 |
| 80.4 | 0.042 | 0.0102 | 0.00136 | 0.00500 |
| 70 | 0.027 | 0.0049 | 0.00050 | 0.00441 |
| | | | | |

The errors of the Arrehenius parameters are reported in Table S 32.

| | k: | 1 | k2 | 2 | k | 3 | k | ł |
|---------------|---------|--------|---------|-------|---------|--------|---------|--------|
| Fitting | -2569.2 | 4.010 | -3930.3 | 6.348 | -5207.4 | 7.866 | -2666.0 | 2.320 |
| SE 95% | 633.6 | 1.875 | 1195.2 | 3.538 | 1779.8 | 5.268 | 845.5 | 2.503 |
| R2 | 0.892 | 0.123 | 0.844 | 0.233 | 0.811 | 0.346 | 0.833 | 0.165 |
| F-test | 16.44 | 2 | 10.81 | 2 | 8.560 | 2 | 9.942 | 2 |
| SSreg. SSres. | 0.250 | 0.0304 | 0.585 | 0.108 | 1.027 | 0.2400 | 0.269 | 0.0542 |

Table S 32: Errors of Arrhenius fittings.

3.2.2. Dynochem Model

The model structure fitted using the Dynochem software is reported at the top of Figure S 26. *Rxn4* is the deactivation of platinum. The middle section shows the general process scheme applied to the modeling and the bottom part the experimental scenarios that were fitted.



| Sce | enarios | | | | | | | | | |
|-----|---------|-------------------------|--------------------------------------|--|-----------------|--------------------------------------|---|--------------------------------------|--------------------------|----------------------|
| M | Nodel | Mass Mole Concentration | n Equiva | alents | | | | | | |
| Ш | ld | Scenario | Solution Volume L v | Solution Temperatur C v | re CBD mol/L | Solution Pt mol/L * | Headspace Pressure bar • | Headspace H2 mmol • | Headspace kLac 1/s | GLE H2.Henry - |
| | expt1 | * Base Case 50.5°C | 1 | 50.5 | 0.104176 | 0.0549 | 20 | 1000 | 0.5 | 9.46402 |
| | expt2 | Base Case 80.4°C | 1 | 80.3 | ••• 0.110988 | 0.0549 | 20 | 1000 | 0.5 | 7.45048 |
| | expt3 | Base Case 60.1°C | 1 | 60.5 | 0.11113 | 0.0549 | 20 | 1000 | 0.5 | 8.76411 |
| 4 | expt4 | Base Case 70°C | 1 | 70.4 | 0.108275 | 0.0549 | 20 | 1000 | 0.5 | 8.095 |

Figure S 26: Dynochem model.

3.2.3. Residence time vs. Real Residence Time

As mentioned in the manuscript, along one kinetic profile, the catalyst was operated for a given time which increases with residence time. This is because the points collected at longer residence times were also collected after the catalyst had been subjected to the flow of starting material for a time which equaled the sum of the purging time for all the points located ahead of a given point. This can be seen in Figure S 27. This implies that the rate of deactivation is distributed over a longer time than that assigned to the residence time.



Figure S 27: Residence time vs. real residence time.

4. CSMs Deactivation Study

4.1. Experimental Methods

4.1.1. Reactor Configuration

Scheme S 2 pictures a schematic representation of the setup used in the study of the mechanism of deactivation using the hydrogenation of limonene to p-menthene and p-menthane (cis and trans), at different contents of resorcinol, as surrogate reaction.



Scheme S 2: Experimental setup used for the hydrogenation of limonene.

4.1.2. GC-FID Chromatograms

A chromatogram of the different species forming from the hydrogenation is reported in Figure S 28. The chromatogram for a starting solution containing both limonene and resorcinol is reported in Figure S 29.



Figure S 28: Example of GC-FID chromatogram for the product mixture derived from the hydrogenation of limonene. Retention times: Limonene (**10**) (4.72 min); p-menthene (**11**) (4.67 min); trans-p-menthane (**12**) (4.45 min); cis-p-menthane (**13**) (4.33 min).



Figure S 29: Example of GC-FID chromatogram of a mixture of limonene and resorcinol. Retention times: Limonene (10) (4.72 min); Resorcinol (14) (6.25 min).

4.1.3. GC-FID Calibration for CBD

The calibration of CBD was performed at the concentrations reported in Table S 33, along with the ratios for the application of the internal standard calibration. The calibration plot is reported in Figure S 30.

| Sample | Concentration | | C_{CBD}/C_{ISTD} | Area | | A_{CBD}/A_{ISTD} | |
|------------|---------------|-------|--------------------|--------|-------|--------------------|--|
| | CBD | ISTD | | CBD | ISTD | | |
| | [M |] | [-] | [a.u | u.] | [-] | |
| 0 | 0.297 | 0.099 | 2.985 | 143878 | 40148 | 3.584 | |
| 1 | 0.223 | 0.099 | 2.238 | 98727 | 42658 | 2.314 | |
| 2 | 0.148 | 0.099 | 1.492 | 68783 | 43328 | 1.588 | |
| 3 | 0.074 | 0.099 | 0.746 | 31181 | 44971 | 0.693 | |
| 4 | 0.028 | 0.099 | 0.280 | 12012 | 40148 | 0.299 | |
| 5 | 0.0148 | 0.099 | 0.149 | 4329 | 41323 | 0.105 | |
| 6 | 0.00742 | 0.099 | 0.075 | 2550 | 48253 | 0.053 | |

Table S 33: GC-FID internal standard calibration.



Figure S 30: Calibration curve.

The slope is equal to 1.034 with a 95% standard error of 0.017.

4.2. Results

4.2.1. Hydrogenation of Limonene

A 0.1 M solution of limonene was hydrogenated at two temperatures: 60 °C and 100 °C. The results for hydrogenation at 60 °C are reported in Table S 34. Those for the hydrogenation at 100 °C are reported in Table S 35.

Table S 34: Conversion and selectivity in the hydrogenation of limonene. Conditions: 60 °C, 20 bar, 51 s, H/S 11.2.

| Entr Y | Collection Time | Conversion | | Selectivity | |
|-----------|-----------------|------------|------------|--------------|--------------|
| | | Limonene | p-menthene | t-p-menthane | c-p-menthane |
| | [min] | | | [%] | |
| 1 | 5 | 82.0 | 80.8 | 9.7 | 9.5 |
| 2 | 15 | 81.2 | 80.3 | 10.1 | 9.6 |
| 3 | 25 | 79.3 | 80.7 | 9.6 | 9.7 |
| 4 | 35 | 77.5 | 81.7 | 9.2 | 9.1 |
| 5 | 45 | 77.2 | 81.9 | 9.0 | 9.1 |

Table S 35: Conversion and selectivity in the hydrogenation of limonene. Conditions: 100 °C, 20 bar, 51 s, H/S 11.2.

| Entr y | Collection Time | Conversio n | Selectivity | | |
|-----------|-----------------|----------------|-------------|--------------|--------------|
| | | Limonene | p-menthene | t-p-menthane | c-p-menthane |
| | [min] | | | [%] | |
| 1 | 5 | 94.7 | 39.8 | 29.6 | 30.6 |
| 2 | 15 | 93.1 | 45.0 | 27.1 | 28.0 |
| 3 | 25 | 91.9 | 48.2 | 25.8 | 26.0 |
| 4 | 35 | 91.1 | 51.8 | 23.7 | 24.5 |
| 5 | 45 | 89.9 | 55.6 | 22.0 | 22.4 |

4.2.2. Hydrogenation of Limonene in the Presence of Resorcinol

A 0.1 M solution of limonene containing 0.1 M of resorcinol was hydrogenated at two temperatures: 60 °C and 100 °C. The results for the hydrogenation at 60 °C are reported in Table S 36. Those for the hydrogenation at 100 °C are reported in Table S 37. In both cases the concentration of resorcinol remained constant throughout the investigation.

Table S 36: Conversion and selectivity in the hydrogenation of limonene with resorcinol. Conditions: 60 °C, limonene [0.1 M] + resorcinol [0.1 M], 60 °C, 20 bar, 51 s, H/S 11.2.

| Entr | Collection Time | Conversio | | Selectivity | |
|------|-----------------|-----------|-------------|--------------|--------------|
| У | conection mile | n | Selectivity | | |
| | | Limonene | p-menthene | t-p-menthane | c-p-menthane |
| | [min] | | | [%] | |
| 1 | 5 | 68.8 | 87.2 | 6.5 | 6.2 |
| 2 | 15 | 64.7 | 88.5 | 5.9 | 5.6 |
| 3 | 25 | 60.5 | 89.5 | 5.4 | 5.2 |
| 4 | 35 | 59.7 | 90.1 | 5.0 | 4.9 |
| 5 | 45 | 56.4 | 90.7 | 4.7 | 4.6 |

Table S 37: Conversion and selectivity in the hydrogenation of limonene with resorcinol. Conditions: limonene [0.1 M] + resorcinol [0.1 M], 100 °C, 20 bar, 51 s, H/S 11.2.

| Entr | Collection Time | Conversio | Selectivity | | |
|------|------------------------|-----------|-------------|--------------|--------------|
| У | | n | | | |
| | | Limonene | p-menthene | t-p-menthane | c-p-menthane |
| | [min] | | | [%] | |
| 1 | 5 | 85.9 | 68.8 | 15.6 | 15.5 |
| 2 | 15 | 85.0 | 73.9 | 13.0 | 13.1 |
| 3 | 25 | 83.1 | 76.4 | 11.8 | 11.8 |
| 4 | 35 | 81.6 | 78.7 | 10.7 | 10.6 |
| 5 | 45 | 78.1 | 80.2 | 9.8 | 10.0 |

5. Calculations

An estimation of the impact of the internal mass transfer diffusional limitation can be obtained either with the Weisz-Prater criterium, or by calculating the diffusional Damköhler number (Da_{II}).^{5,6} We opted for this second option, as it is less reliant on physical parameters that can be difficult to estimate or calculate (e.g. bed density) and it would not require the rate of reaction per volume of pellet to be computed. The reactions were considered as pseudo-first order reactions, and the Damköhler number could be computed using the following equation:

$$Da = \frac{k \cdot L^2}{D_{eff}}$$

Where k is the kinetic constant, L is the particle diameter and D_{eff} is the effective diffusion coefficient.

We made the following assumptions:

• For the calculation of the effective diffusion coefficient, we used the equation suggested by Ternan⁷ and Ashraf⁸:

$$D_{eff} = D \cdot \frac{(1-\lambda)^2}{(1+P\cdot\lambda)}$$

With λ is the ratio of the molecule radius and the pore diameter and P is a fitting factor, which Ashraf set to 16.3.

• We assumed that CBD had a similar size for the molecule of CBD to the one used by Ashraf (0.5 nm), and we assumed a pore diameter of 20 nm, according to the manufacturer. This yielded a ratio equal to

$$\frac{D_{eff}}{D} = 0.68$$

- To account for errors in the diameter of the molecule and the pore size (sensitivity analysis), we tested different values of D/D_{eff} in the range of 0.4-0.7.
- The bulk diffusion coefficients of organic molecules in organic solvents were reported by different sources to assume values between 0.5·10⁻⁹ and 1.5·10⁻⁹ m²s⁻¹.^{6,9} An average value of 10⁻⁹ m²s⁻¹ was selected.
- The particle diameter was assumed in the range between 5 to 100 $\mu\text{m}.^{10}$
- The kinetic constants at two temperatures (50 °C and 80 °C) as low and high points in the investigation were considered. Moreover, all three kinetic constants were considered.

The results of the calculations are reported in the table below.

| Exp. | k [s ⁻¹] | L [m] | Diffusion Correction factor | Deff [m² s ⁻¹] | Da |
|-----------------------|----------------------|---------|-----------------------------------|----------------------------|---------|
| k ₁ (50°C) | 0.0210 | 5.0E-06 | 4.0E-01 | 4.0E-10 | 1.3E-03 |
| k ₁ (80°C) | 0.0420 | 5.0E-06 | 4.0E-01 | 1.0E-09 | 1.1E-03 |
| k ₁ (50°C) | 0.0210 | 1.0E-04 | 4.0E-01 | 1.0E-09 | 2.1E-01 |
| k ₁ (80°C) | 0.0420 | 1.0E-04 | 4.0E-01 | 1.0E-09 | 4.2E-01 |
| k ₂ (50°C) | 0.0040 | 5.0E-06 | 4.0E-01 | 1.0E-09 | 1.0E-04 |
| k ₂ (80°C) | 0.0130 | 5.0E-06 | 4.0E-01 | 1.0E-09 | 3.3E-04 |
| k ₂ (50°C) | 0.0040 | 1.0E-04 | 4.0E-01 | 1.0E-09 | 4.0E-02 |
| k ₂ (80°C) | 0.0130 | 1.0E-04 | 4.0E-01 | 1.0E-09 | 1.3E-01 |
| k ₃ (50°C) | 0.0003 | 5.0E-06 | 4.0E-01 | 1.0E-09 | 7.5E-06 |
| k ₃ (80°C) | 0.0019 | 5.0E-06 | 4.0E-01 | 1.0E-09 | 4.8E-05 |
| k ₃ (50°C) | 0.0003 | 1.0E-04 | 4.0E-01 | 1.0E-09 | 3.0E-03 |

| | k ₃ (80°C) | 0.0019 | 1.0E-04 | 4.0E-01 | 1.0E-09 | 1.9E-02 | |
|---|-----------------------|--------|---------|---------|---------|---------|--|
| | k ₁ (50°C) | 0.0210 | 5.0E-06 | 7.0E-01 | 7.0E-10 | 7.5E-04 | |
| | k ₁ (80°C) | 0.0420 | 5.0E-06 | 7.0E-01 | 7.0E-10 | 1.5E-03 | |
| | k ₁ (50°C) | 0.0210 | 1.0E-04 | 7.0E-01 | 7.0E-10 | 3.0E-01 | |
| | k ₁ (80°C) | 0.0420 | 1.0E-04 | 7.0E-01 | 7.0E-10 | 6.0E-01 | |
| | k ₂ (50°C) | 0.0040 | 5.0E-06 | 7.0E-01 | 7.0E-10 | 1.4E-04 | |
| | k ₂ (80°C) | 0.0130 | 5.0E-06 | 7.0E-01 | 7.0E-10 | 4.6E-04 | |
| | k ₂ (50°C) | 0.0040 | 1.0E-04 | 7.0E-01 | 7.0E-10 | 5.7E-02 | |
| | k ₂ (80°C) | 0.0130 | 1.0E-04 | 7.0E-01 | 7.0E-10 | 1.9E-01 | |
| | k ₃ (50°C) | 0.0003 | 5.0E-06 | 7.0E-01 | 7.0E-10 | 1.1E-05 | |
| | k ₃ (80°C) | 0.0019 | 5.0E-06 | 7.0E-01 | 7.0E-10 | 6.8E-05 | |
| | k ₃ (50°C) | 0.0003 | 1.0E-04 | 7.0E-01 | 7.0E-10 | 4.3E-03 | |
| _ | k ₃ (80°C) | 0.0019 | 1.0E-04 | 7.0E-01 | 7.0E-10 | 2.7E-02 | |

As can be seen, Da<<1 for all the scenarios: we can confirm that the reaction is kinetically controlled.

6. Spectra

The results of the spectra were found to be in accordance with literature.^{11,12,13}

6.1. GC-MS Analysis

6.1.1. CBD (1)



Figure S 31: Mass fragmentation of CBD.

6.1.2. H2CBD (2)



Figure S 32: Mass fragmentation of H2CBD.





Figure S 33: Mass fragmentation of cis-H4CBD.

6.1.4. TransH4CBD (4)



Figure S 34: Mass fragmentation of trans-H4CBD.





Figure S 35: Mass fragmentation of Δ^9 -THC.

6.1.6. Δ⁸-THC (6)



Figure S 36: Mass fragmentation of Δ^8 -THC.





Figure S 37: Mass fragmentation of R-HHC.

6.1.8. S-HHC (8)



Figure S 38: Mass fragmentation of S-HHC.

6.2. NMR Spectra

6.2.1. Cannabidiol (CBD)



White Powder

¹H NMR (300 MHz, Acetonitrile-d3) δ 6.13 (s, 1H), 5.28 (tq, J = 2.5, 1.2 Hz, 1H), 4.46 (ddt, J = 3.6, 1.9, 1.1 Hz, 1H), 3.89 (ddp, J = 11.2, 4.7, 2.4 Hz, 1H), 2.79 – 2.65 (m, 1H), 2.39 (t, 1H), 2.29 – 2.13 (m, 1H), 2.05 (q, J = 3.3 Hz, 0H), 1.99 (q, J = 3.3 Hz, 0H), 1.94 (p, J = 2.5 Hz, 0H), 1.79 – 1.71 (m, 1H), 1.70 (dd, J = 2.8, 1.5 Hz, 2H), 1.64 (t, J = 1.1 Hz, 2H), 1.59 – 1.47 (m, 1H), 1.40 – 1.21 (m, 2H), 0.89 (t, J = 6.9 Hz, 2H).

¹³C NMR (75 MHz, CD₃CN) δ 149.1, 142.2, 135.8, 124.9, 114.2, 109.7, 45.4, 35.8, 35.0, 31.3, 30.6, 30.2, 29.1, 22.7, 22.3, 18.4, 13.4, 1.2, 0.9, 0.6, 0.4, 0.1, -0.2, -0.5.

6.2.2. Dihydro Cannabidiol (H2CBD)



 $H_2CBD(2)$

Colorless oil

¹H NMR (300 MHz. Acetonitrile-d3) δ 6.17 (s, 1H), 5.32 (s, 0H), 3.77 (d, J = 14.1 Hz, 0H), 2.48 – 2.34 (m, 1H), 2.17 (s, 1H), 2.15 – 2.00 (m, 1H), 1.71 (s, 2H), 1.61 – 1.42 (m, 2H), 1.40 – 1.25 (m, 3H), 0.89 (t, J = 6.9 Hz, 1H), 0.83 (d, J = 3.1 Hz, 2H), 0.81 (d, J = 2.9 Hz, 1H).

¹³C NMR (75 MHz. CD3CN) δ 181.4, 157.0, 143.4, 138.4, 126.0, 115.2, 43.9, 36.3, 36.0, 32.3, 31.6, 31.3, 28.9, 23.6, 23.2, 23.2, 21.9, 16.6, 14.3.



H₄CBD (3,4)

Yellow Oil

¹H NMR (300 MHz. Acetonitrile-d3) δ 6.54 (s, 1H), 6.48 (s, 1H), 6.15 (d, J = 1.5 Hz, 1H), 6.09 (d, J = 1.4 Hz, 1H), 2.98 (td, J = 11.6, 3.3 Hz, 1H), 2.45 – 2.34 (m, 3H), 2.21 (s, 2H), 2.12 (ddd, J = 11.4, 8.6, 2.9 Hz, 2H), 1.80 – 1.24 (m, 16H), 1.10 – 0.96 (m, 3H), 0.95 – 0.84 (m, 7H), 0.81 (d, J = 7.0 Hz, 3H), 0.67 (s, 2H).

¹³C NMR (75 MHz. CD3CN) δ 157.5, 156.2, 142.4, 116.2, 108.8, 108.1, 45.4, 44.5, 40.7, 38.8, 37.4, 36.4, 35.9, 34.4, 33.0, 32.6, 32.3, 31.6, 29.6, 29.4, 26.0, 23.2, 22.9, 21.9, 21.7, 20.1, 18.4, 16.0, 14.3.

6.2.4. Δ^9 -Tetrahydro Cannabinol (Δ_9 -THC)



⊿⁹-THC (5)

Colorless oil

¹H NMR (300 MHz. Acetonitrile-d3) δ 6.79 (s. 1H). 6.32 (h. J = 1.7 Hz. 1H). 6.17 (d. J = 1.7 Hz. 1H). 6.10 (d. J = 1.7 Hz. 1H). 3.13 (dq. J = 10.5. 2.5 Hz. 1H), 2.46 – 2.36 (m. 2H). 2.18 (s, 1H), 2.16 (s, 0H), 1.91 (dddd, J = 16.1, 5.3, 3.6, 1.6 Hz, 1H), 1.64 (dq, J = 2.3, 1.0 Hz, 3H), 1.61 – 1.48 (m, 3H), 1.35 (s, 4H), 1.34 – 1.24 (m, 2H), 1.20 (t, J = 7.1 Hz, 3H), 1.02 (s, 3H).

¹³C NMR (75 MHz. CD3CN) δ 171.6, 156.5, 155.7, 143.5, 134.2, 125.2, 110.0, 109.9, 108.2, 77.7, 60.9, 46.8, 36.0, 34.5, 32.2, 31.8, 31.6, 27.8, 25.7, 23.5, 23.2, 21.1, 19.5, 14.5, 14.3, 2.1, 1.8, 1.6, 1.3, 1.0, 0.7, 0.5.



Colorless oil

¹H NMR (300 MHz. Acetonitrile-d3) δ 6.17 (d, J = 1.7 Hz, 1H), 6.11 (d, J = 1.7 Hz, 1H), 5.48 – 5.37 (m, 1H), 3.29 – 3.14 (m, 1H), 2.60 (td, J = 11.1, 4.7 Hz, 1H), 2.46 – 2.37 (m, 2H), 2.33 (s, 2H), 2.20 (s, 3H), 1.84 (ddt, J = 14.1, 4.3, 2.1 Hz, 1H), 1.73 – 1.62 (m, J = 3.7 Hz, 4H), 1.54 (dq, J = 9.7, 7.2 Hz, 2H), 1.39 – 1.23 (m, 8H), 1.03 (s, 3H), 0.89 (t, J = 6.9 Hz, 3H), ¹³C NMR (75 MHz. CD3CN) δ 157.0, 155.7, 143.5, 135.3, 120.5, 111.4, 109.9, 108.3, 77.1, 46.0, 36.7, 36.0, 32.5, 32.2, 31.6, 28.5, 27.8, 23.6, 23.2, 18.7, 14.3.

6.2.6. Hexahydro Cannabinol (HHC)





Pale Yellow Oil

¹H NMR (300 MHz. Acetonitrile-d3) δ 6.71 (s, 1H), 6.67 (s, 0H), 6.12 (t, J = 2.2 Hz, 2H), 6.07 (t, J = 1.6 Hz, 2H), 3.12 – 3.00 (m, 1H, R-HHC), 2.99 – 2.89 (m, 1H, S-HHC), 2.62 (td, J = 11.2, 3.0 Hz, 1H), 2.39 (dd, J = 9.2, 6.2 Hz, 4H), 2.16 (s, 2H), 1.83 (dt, J = 11.2, 2.3 Hz, 2H), 1.69 – 1.57 (m, 0H), 1.53 (ddd, J = 7.8, 6.4, 1.5 Hz, 2H), 1.45 – 1.33 (m, 3H), 1.33 – 1.26 (m, 9H), 1.20 (t, J = 7.1 Hz, 1H), 1.10 (d, J = 7.2 Hz, 2H), 1.01 (d, J = 7.3 Hz, 5H), 0.95 – 0.84 (m, 8H).

¹³C NMR (75 MHz. CD3CN) δ 157.0, 156.1, 155.8, 143.3, 118.3, 111.4, 111.2, 109.8, 108.2, 77.4, 77.3, 51.0, 50.1, 39.7, 36.7, 36.3, 35.9, 33.6, 33.0, 32.2, 31.6, 30.2, 28.8, 28.7, 28.0, 27.9, 23.7, 23.2, 22.9, 19.3, 19.2, 19.0, 14.5, 14.3, 2.1, 1.8, 1.6, 1.3, 1.0, 0.7, 0.5.



Figure S 39: ¹H NMR spectrum of CBD (**1**).



Figure S 40: ¹³C NMR spectrum of CBD (1).



Figure S 41: ¹H NMR spectrum of H2CBD (**2**).



Figure S 42: ¹³C NMR spectrum of H2CBD (**2**).



Figure S 43: ¹H NMR spectrum of H4CBD diastereomers mixture (**3**, **4**).



Figure S 44: ¹³C NMR spectrum of H4CBD diastereomers (**3**, **4**).



Figure S 45: ¹H NMR spectrum of Δ^9 -THC (**5**).



Figure S 46: ¹³C NMR spectrum of Δ^9 -THC (**5**).



Figure S 47: ¹H NMR of Δ^8 -THC (**6**).



Figure S 48: ¹³C NMR of Δ^8 -THC (**6**).



Figure S 49: ¹H NMR spectrum of HHC diastereomers (**7**, **8**).



Figure S 50: ¹³C NMR spectrum of HHC diastereomers (**7**, **8**).

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