

Supporting information

The selective oxidation of methanol to formaldehyde using novel iron molybdate catalysts prepared by supercritical antisolvent precipitation

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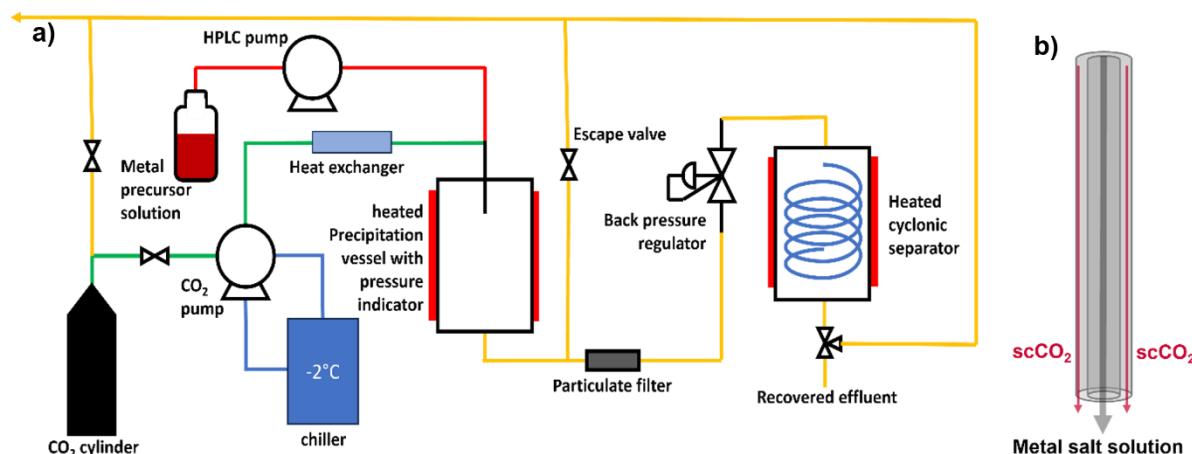


Fig S1. a) Schematic of Sci-Med custom apparatus for supercritical antisolvent precipitation with flow indications for CO₂ (green), coolant (blue), metal precursor solution (red) and ventilation (yellow). b) Coaxial nozzle design, highlighting the feed of CO₂ and metal precursor solution into the precipitation vessel.

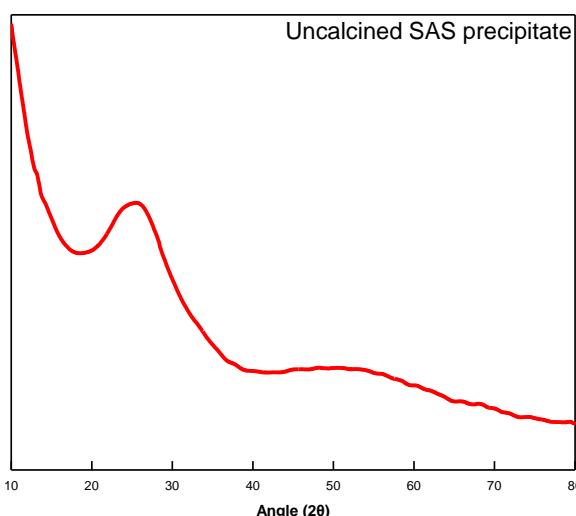


Fig S2. XRD diffractogram of a FeMo SAS precipitate, showing no well-defined crystalline structure.

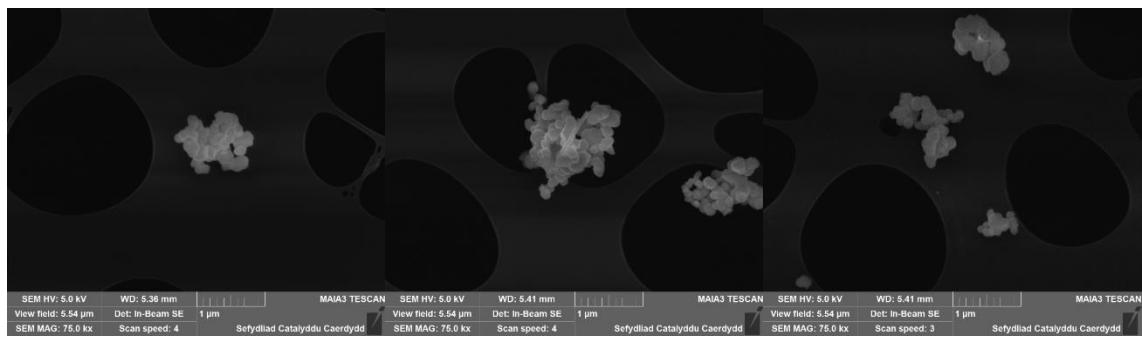


Fig S3. SEM images of FeMo₁₄₀P-10C-20W-7.5F.

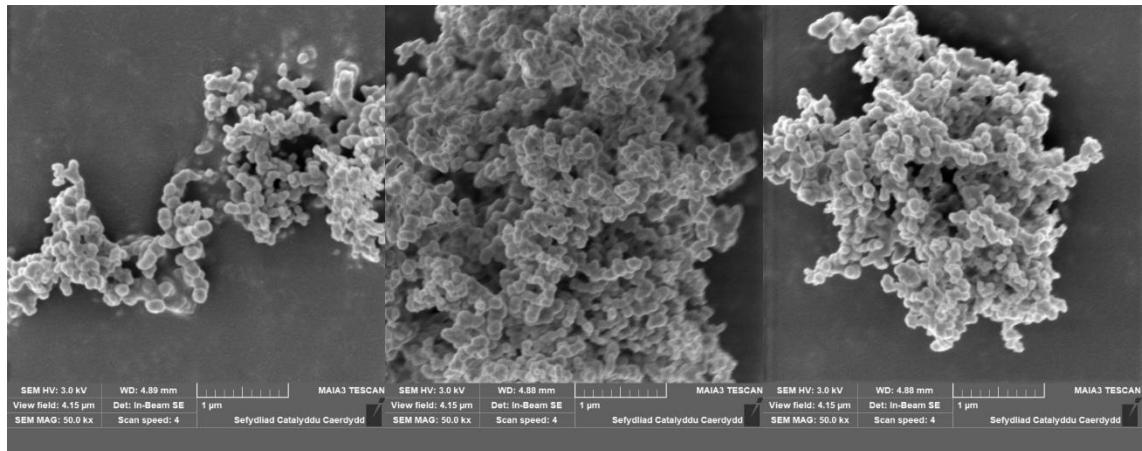


Fig S4. SEM images of FeMo₁₁₀P-5C-20W-5F.

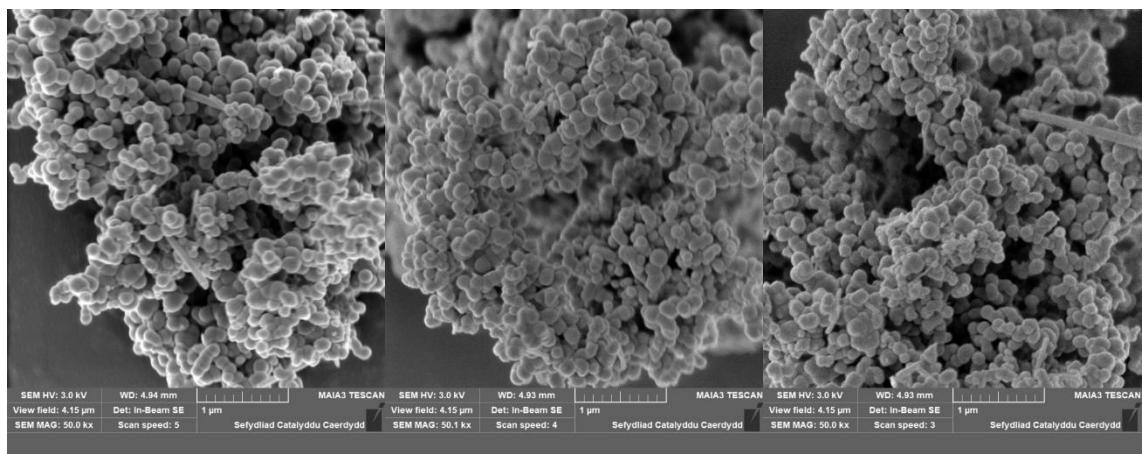


Fig S5. SEM images of FeMo₁₄₀P-10C-10.5W-5F.

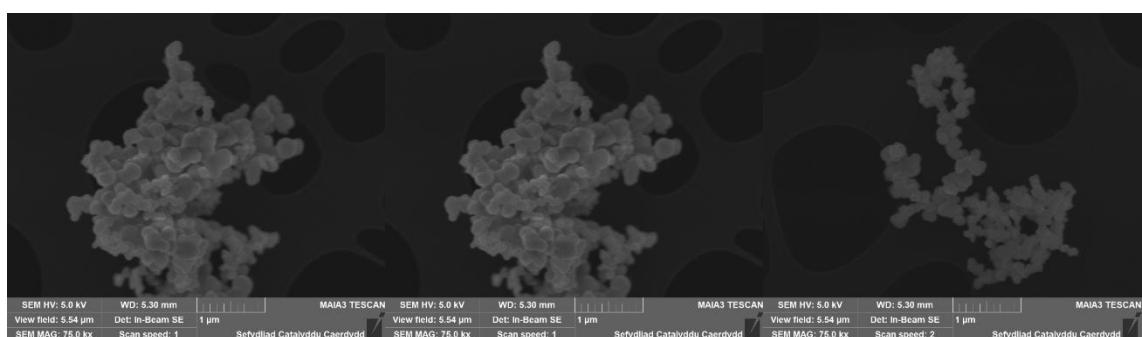


Fig S6. SEM images of FeMo₈₀P-7.5C-20W-5F.

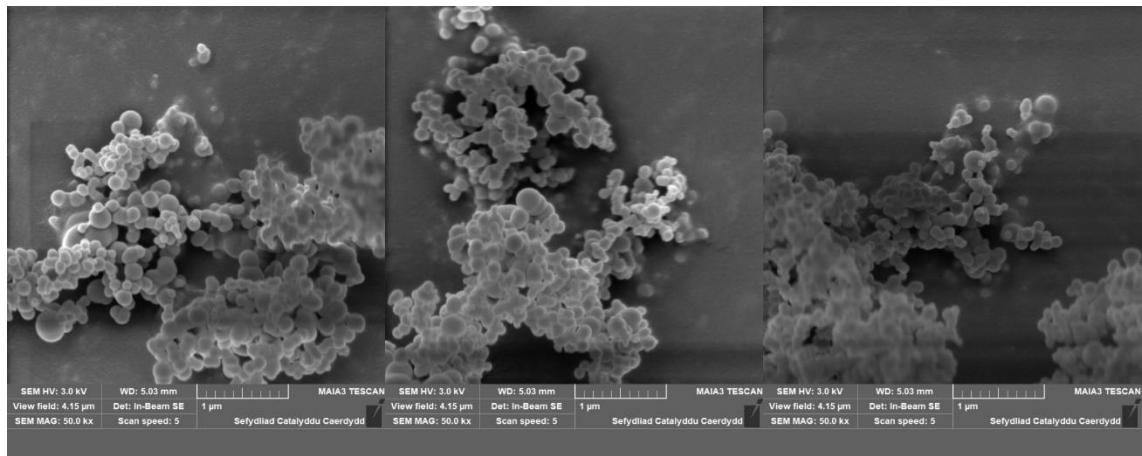


Fig S7. SEM images of FeMo_80P-10C-1W-5F

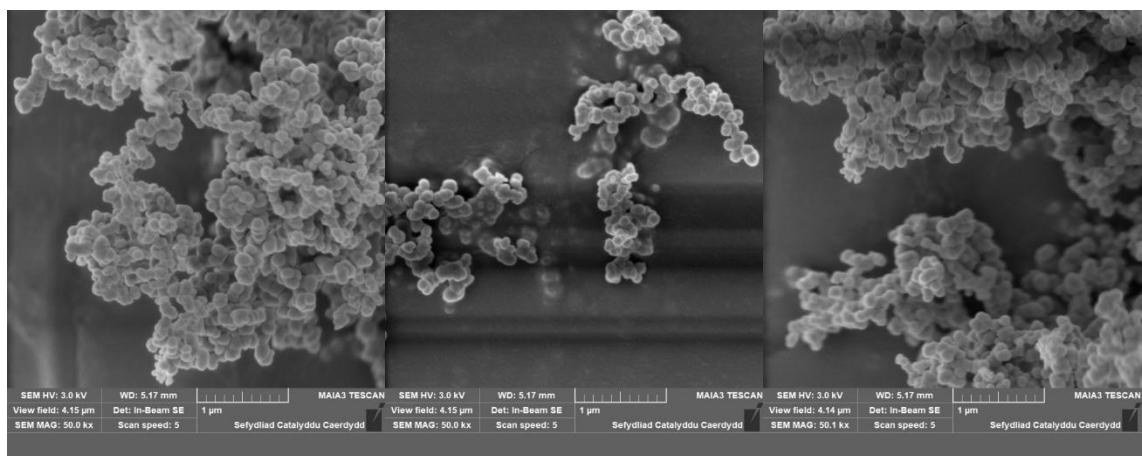


Fig S8. SEM images of FeMo_140P-5C-20W-10F.

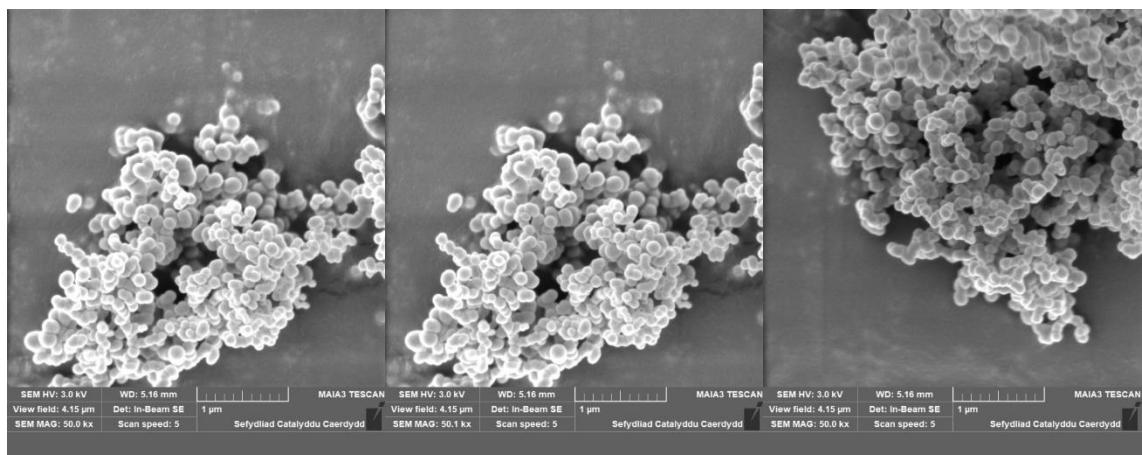
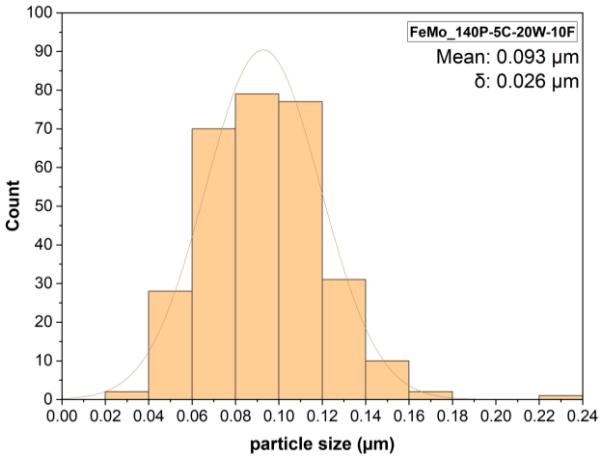
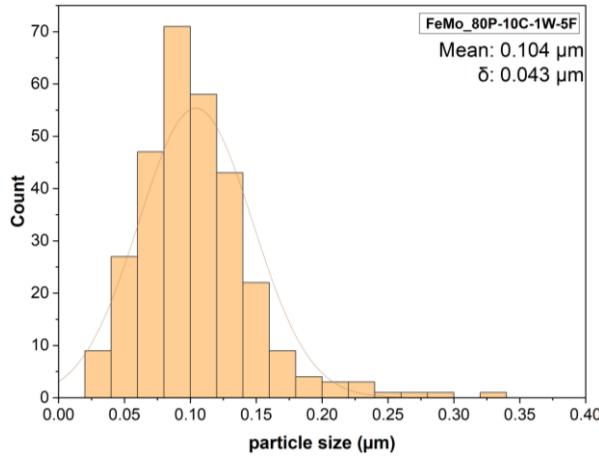
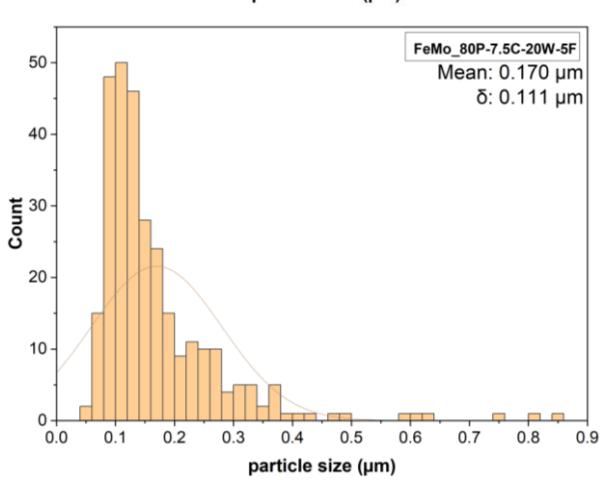
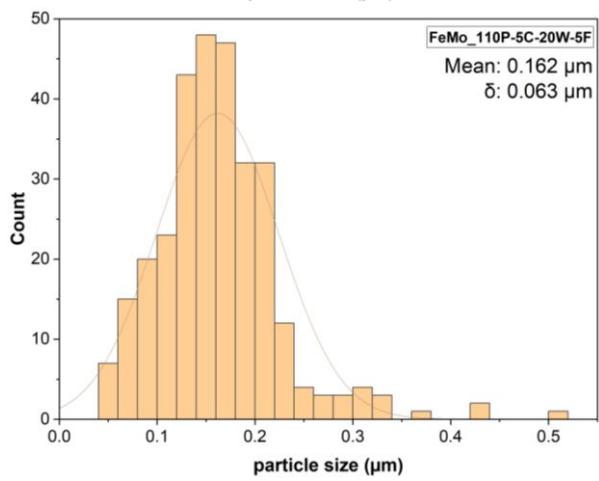
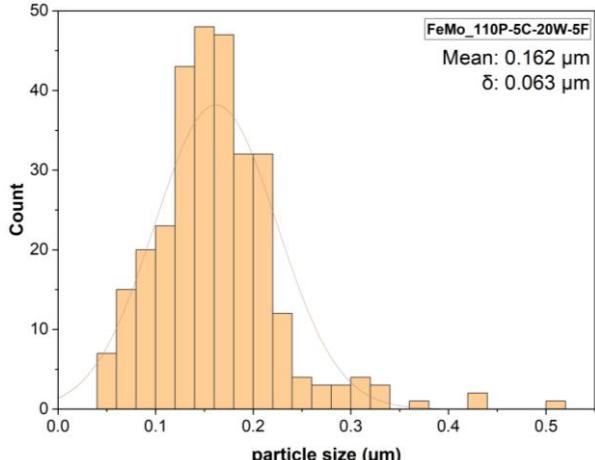
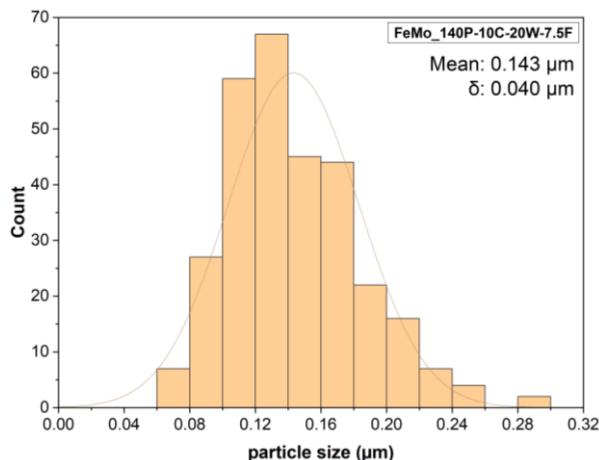


Fig S9. SEM images of FeMo_110P-7.5C-10.5W-7.5F.



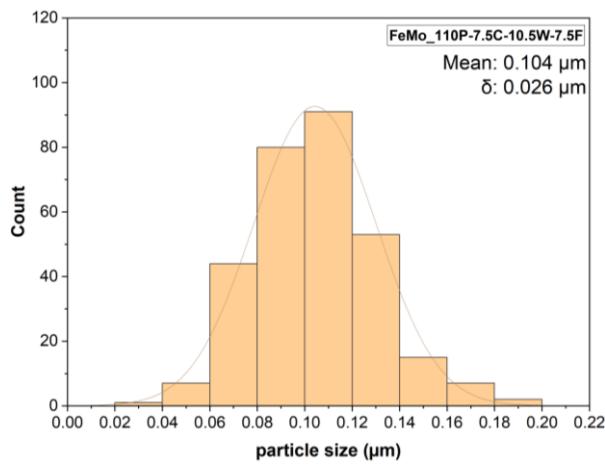
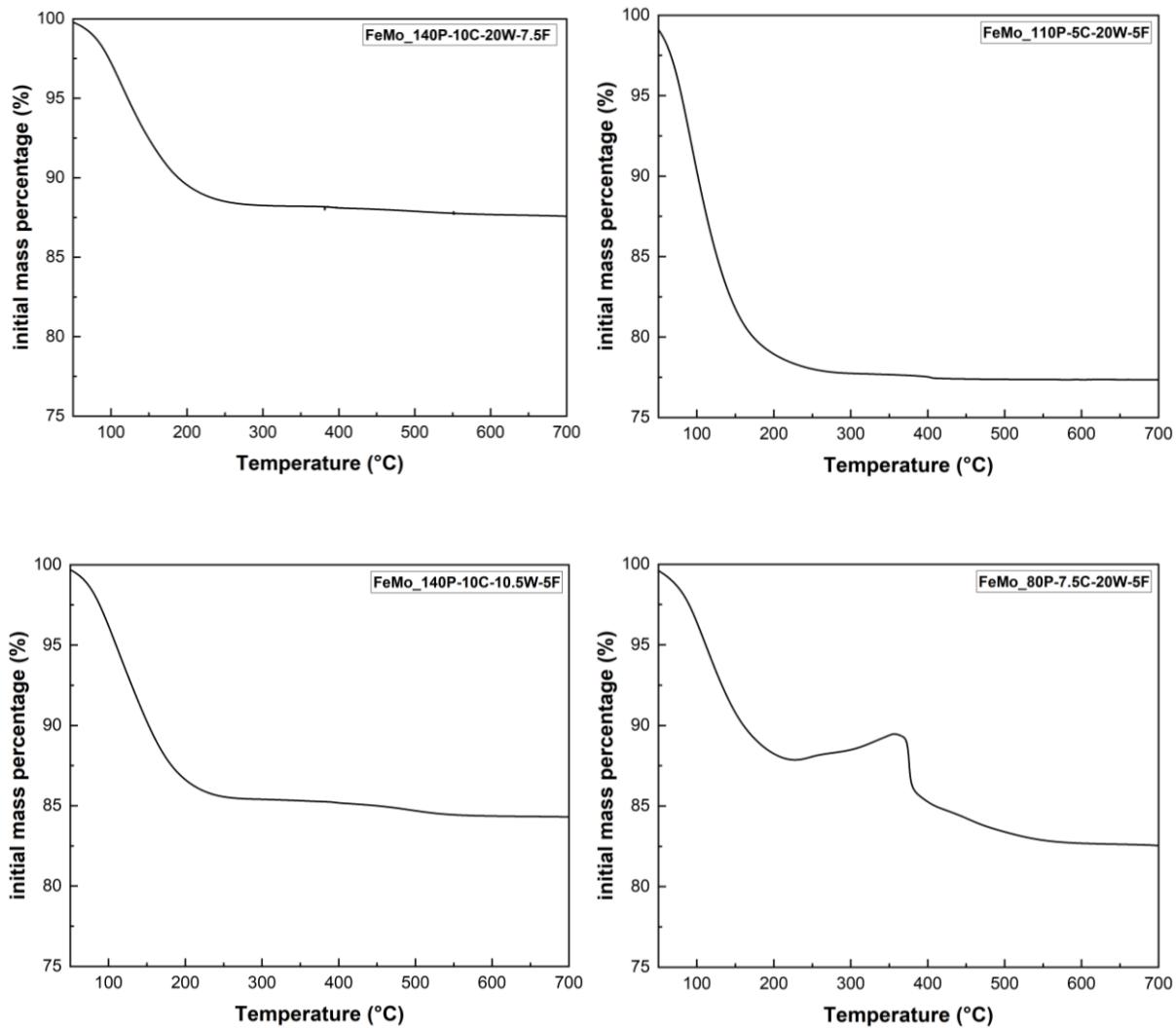


Fig S10. Particle size distribution of catalyst precursors.



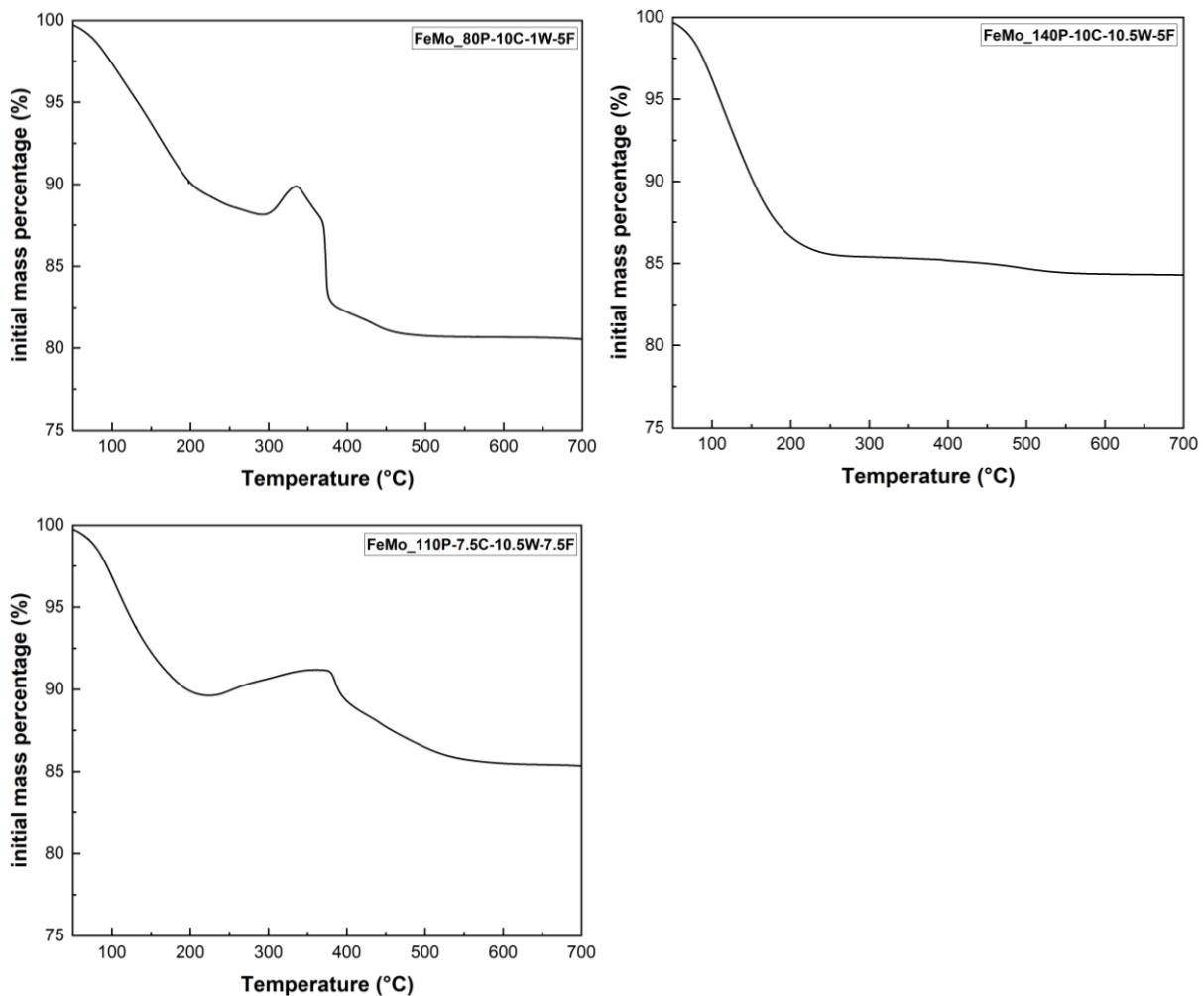


Fig S11. Thermogravimetric analysis of all catalyst samples formed by SAS precipitation.

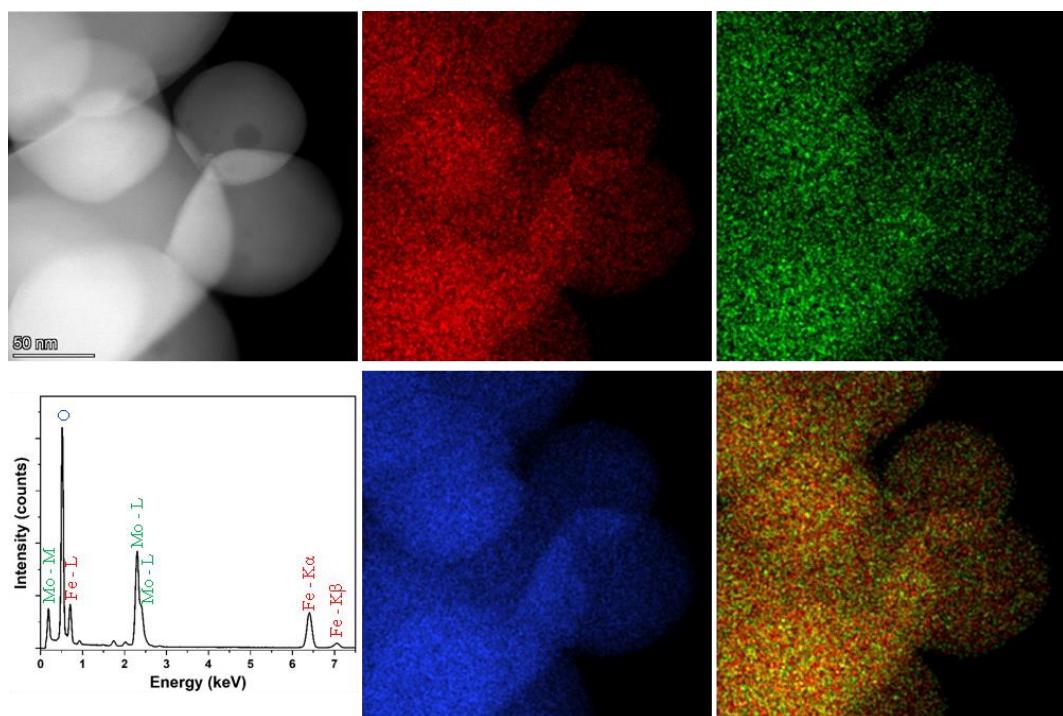


Fig S12. EDX Analysis of HAADF STEM images for FeMo_80P-10C-1W-5F.

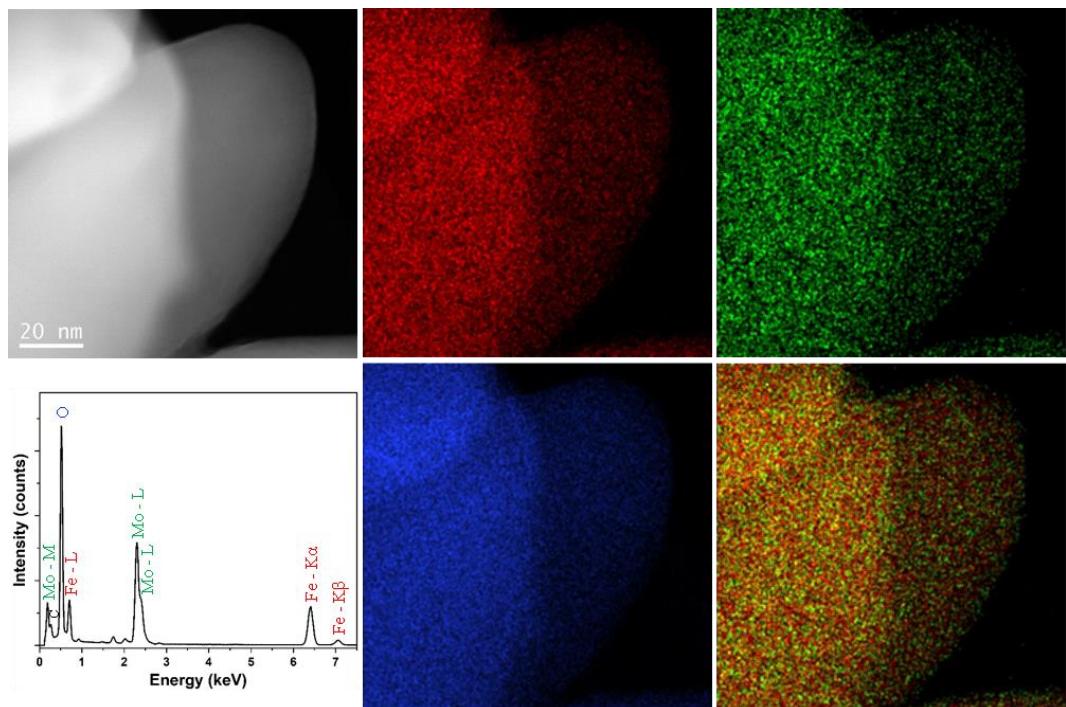


Fig S13. EDX Analysis of HAADF STEM images for FeMo₁₁₀P-5C-20W-7.5F.

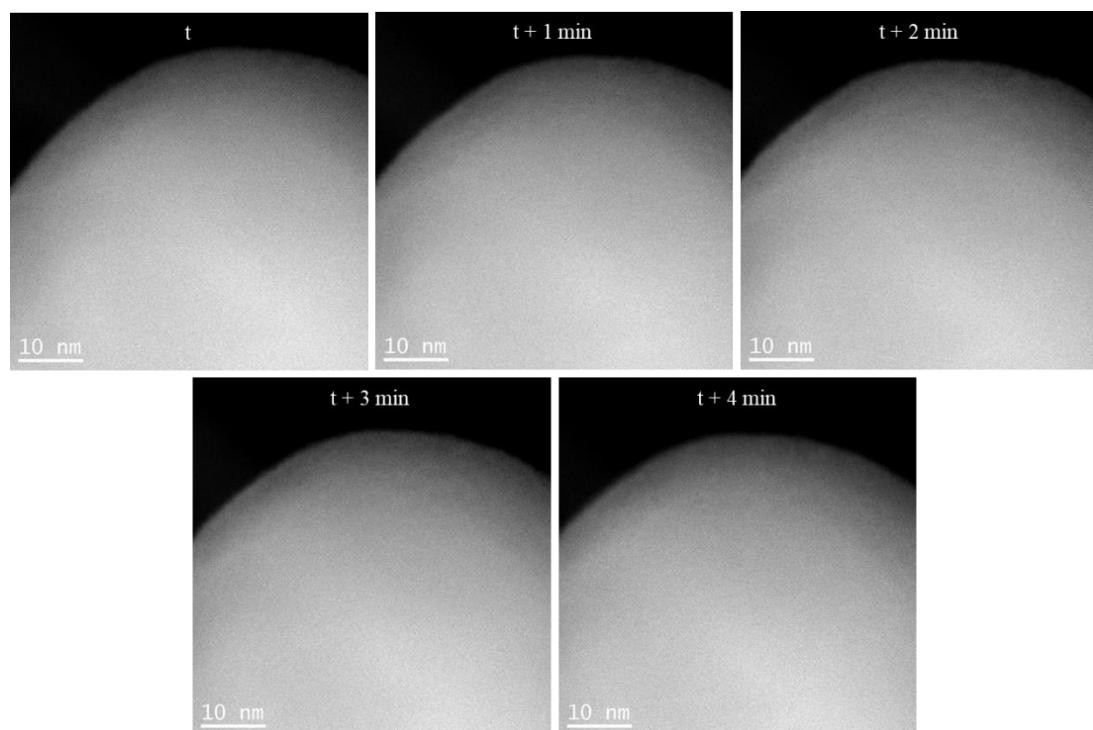


Fig S14. High resolution HAADF-STEM images of FeMo₈₀P-10C-1W-5F showing the effects of the electron beam on the amorphization of the structure. Electron dose is ~6600 e⁻/Å² for each image.

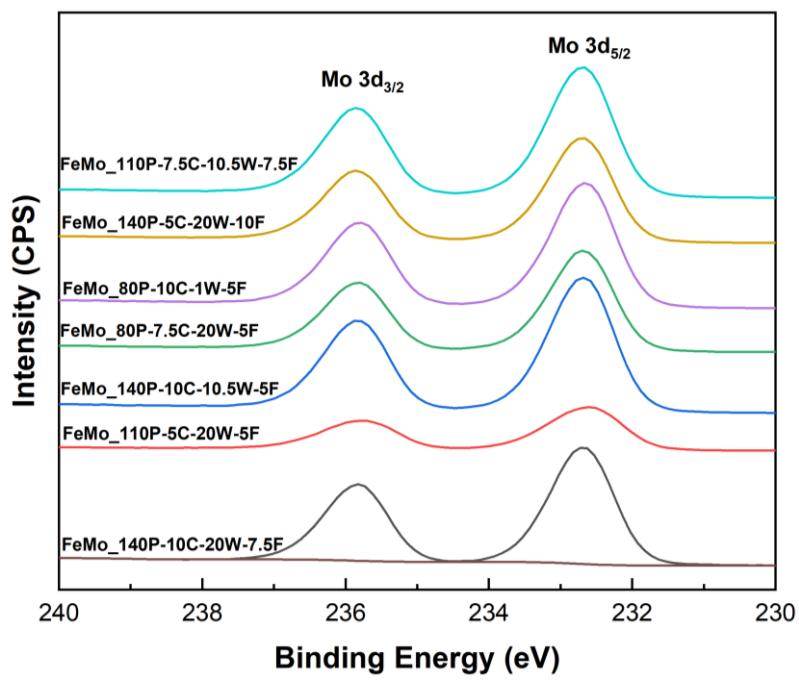


Fig S15. Mo 3d XPS spectra of novel iron molybdate catalysts formed.

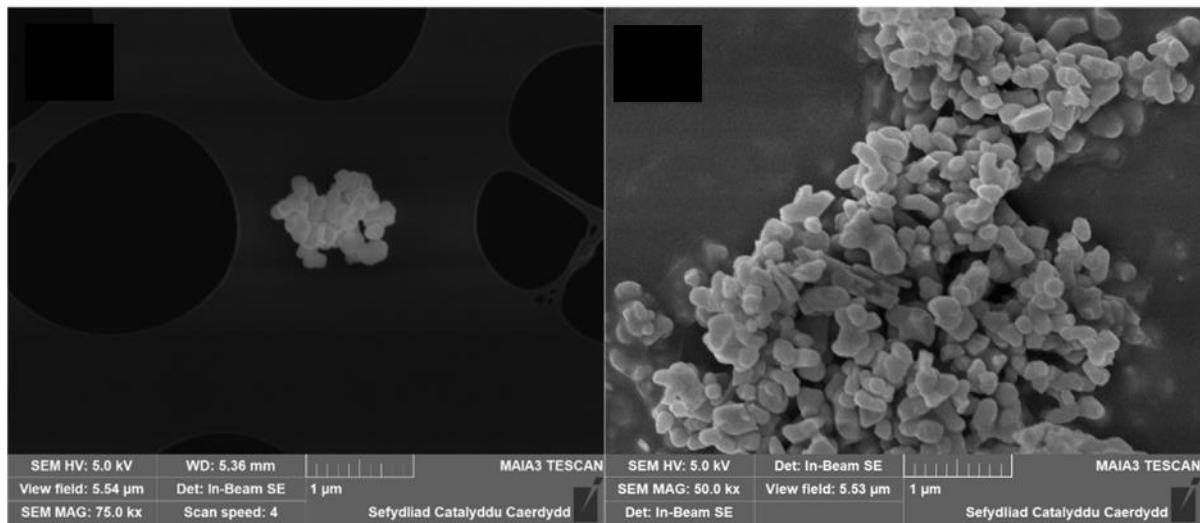


Fig S16. Comparison of precursor (left) and catalyst (right) morphology for FeMo_140P-10C-20W-7.5F.

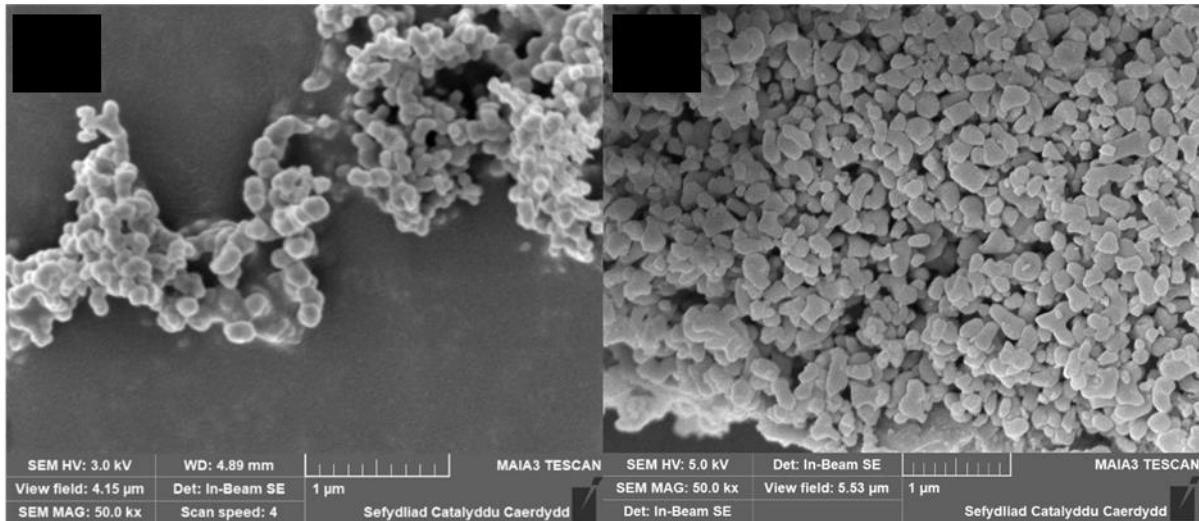


Fig S17. Comparison of precursor (left) and catalyst (right) morphology for FeMo_110P-5C-20W-5F.

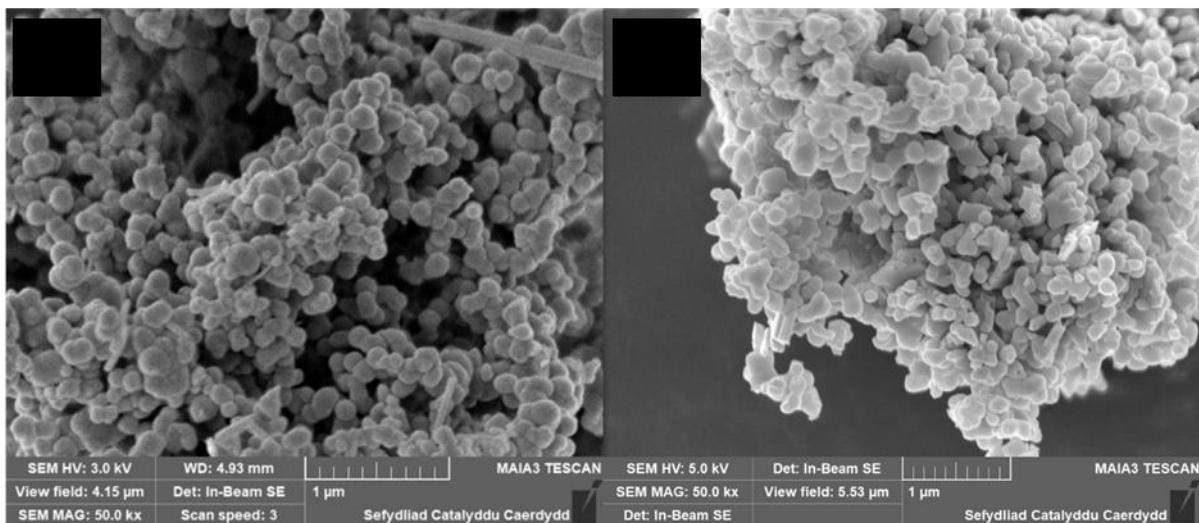


Fig S18. Comparison of precursor (left) and catalyst (right) morphology for FeMo_140P-10C-10.5W-5F.

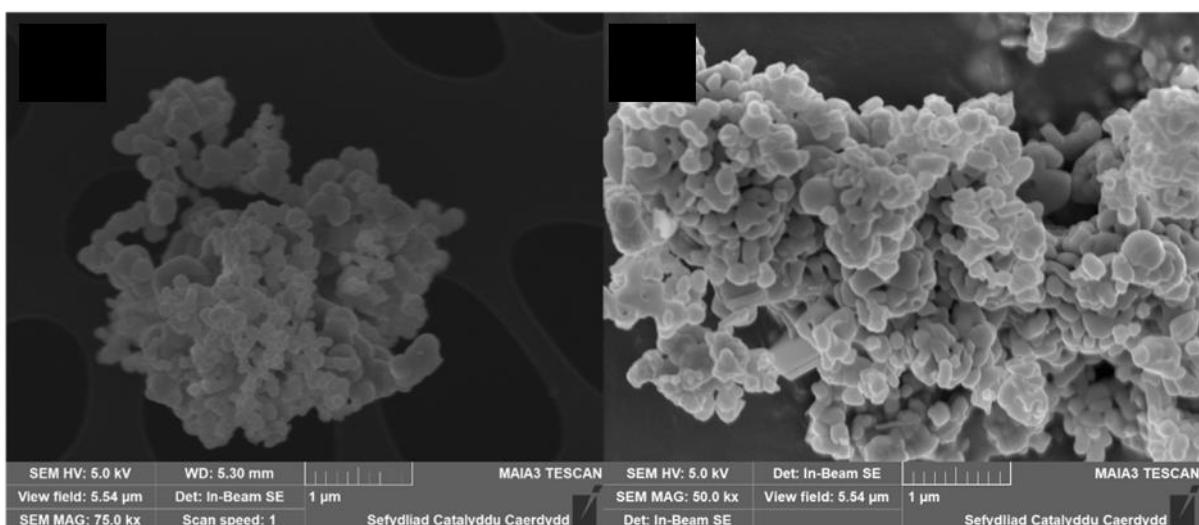


Fig S19. Comparison of precursor (left) and catalyst (right) morphology for FeMo_80P-7.5C-20W-5F.

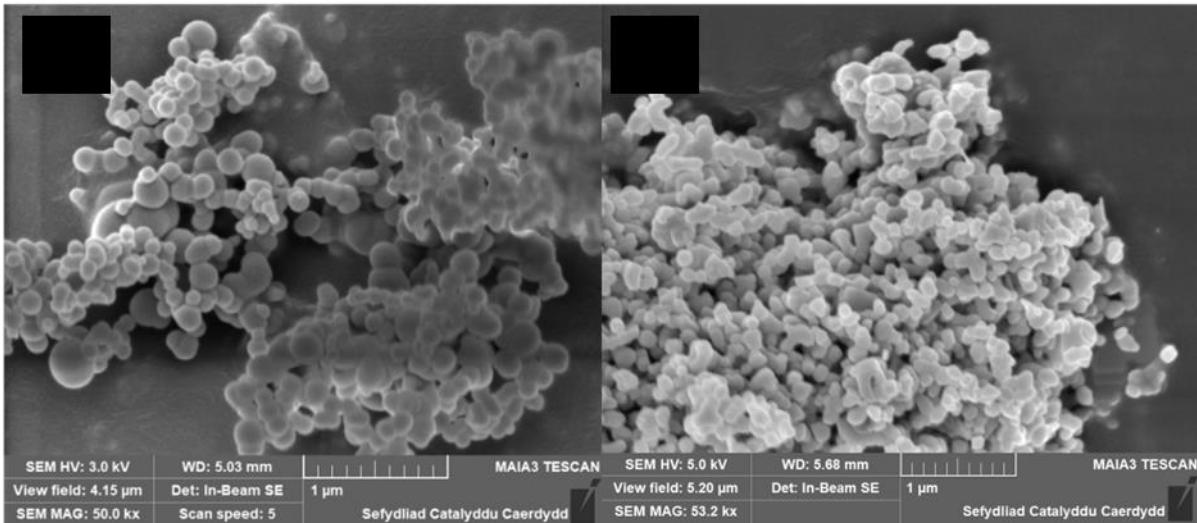


Fig S20. Comparison of precursor (left) and catalyst (right) morphology for FeMo_80P-10C-1W-5F

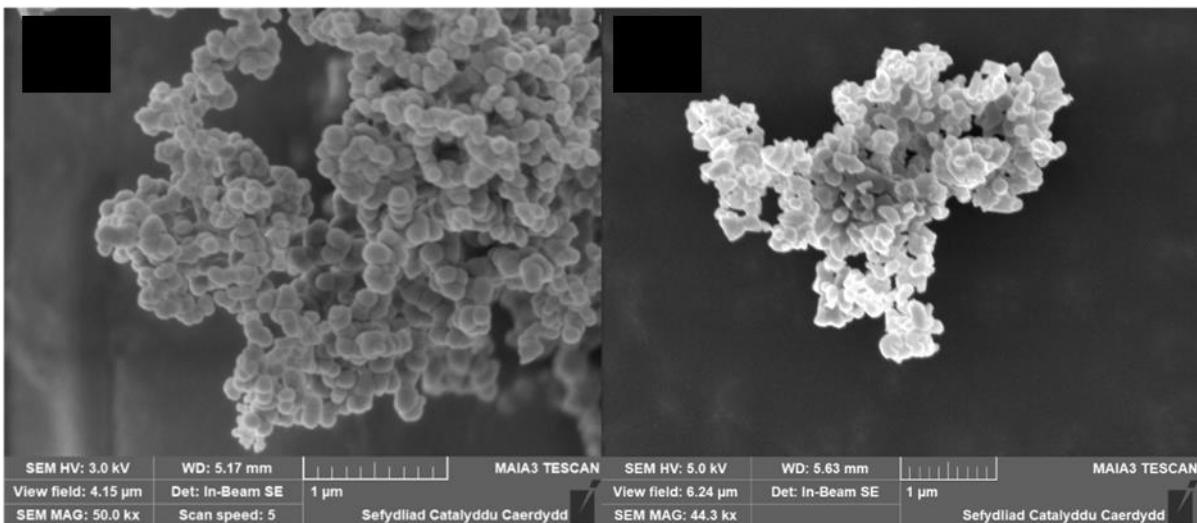


Fig S21. Comparison of precursor (left) and catalyst (right) morphology for FeMo_140P-5C-20W-10F.

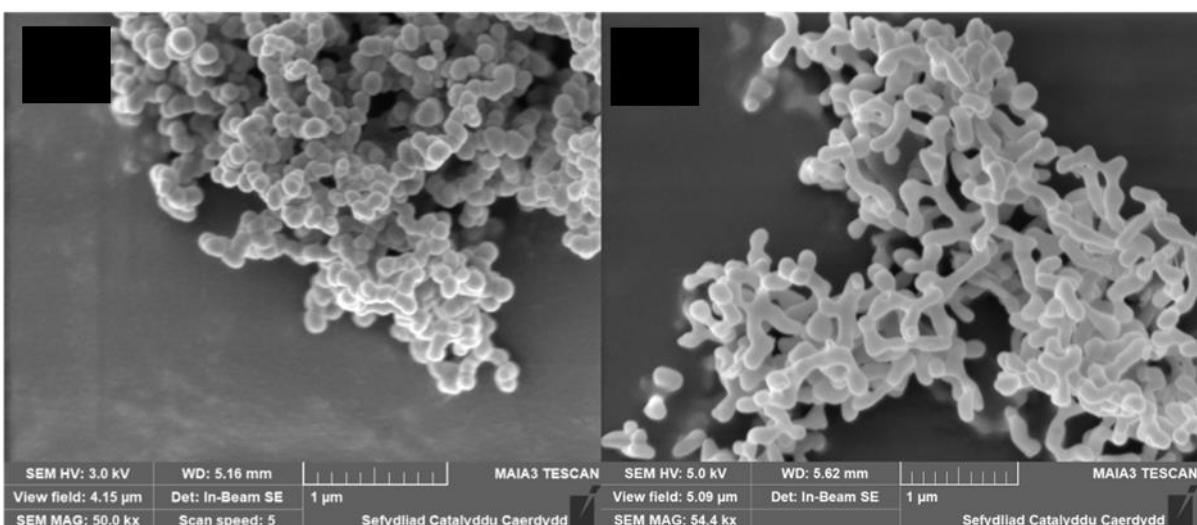


Fig S22. Comparison of precursor (left) and catalyst (right) morphology for FeMo_110P-7.5C-10.5W-7.5F.

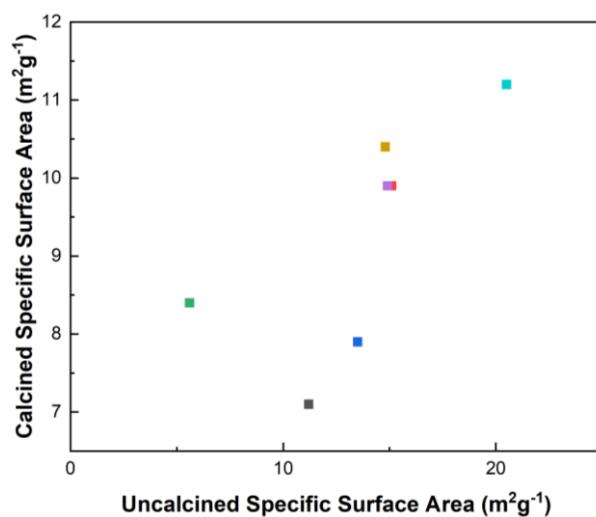


Fig S23. Relationship between uncalcined and calcined specific surface area.

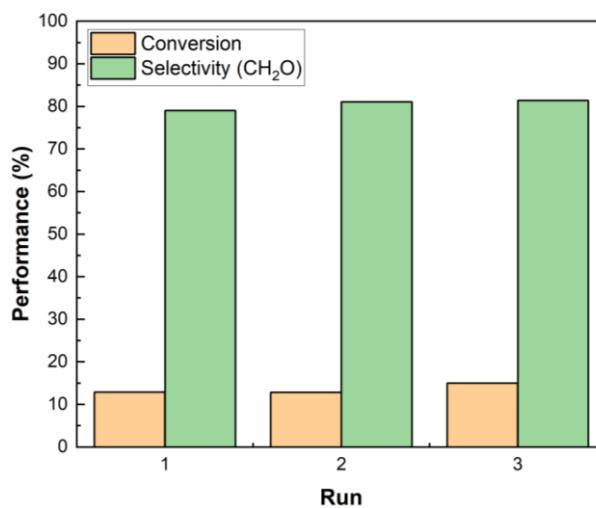


Fig S24. Repeat catalyst testing of FeMo_140P-5C-20W-10F for the selective methanol oxidation to formaldehyde. Isoconversion studies were conducted at 250 °C. The MeOH:O₂:N₂ ratio was 5:10:85 for all testing, with a total flow rate of 30 mL min⁻¹.

<p>Low flow rate, low water content</p>  <p>droplets $t = t_1$ precipitate</p> <p>Larger initial droplets. higher miscibility = limited droplet growth before precipitation = smaller particle size</p>	<p>low flow rate, high water content</p>  <p>droplets $t = t_1$ droplets $t = t_2 > t_1$ precipitate</p> <p>Larger initial droplets lower miscibility = expansion of droplet before precipitation = larger particle size</p>
<p>High flow rate, low water content</p>  <p>droplets $t = t_1$ precipitate</p> <p>Smaller initial droplets. higher miscibility = limited droplet growth before precipitation = smaller particle size</p>	<p>High flow rate, high water content</p>  <p>droplets $t = t_1$ droplets $t = t_2 > t_1$ precipitate</p> <p>Smaller initial droplets lower miscibility = expansion of droplet before precipitation = larger particle size</p>

Fig S25: proposed relationships between particle size, solution flow rate and water content for SAS preparation.

Table S1. Comparison of productivity of catalysts formed in comparison to catalysts in literature.

Catalyst	Fe:Mo (1:x)	Temperature °C	WHSV g _{MeOH} g _{cat} ⁻¹ hr ⁻¹	Productivity mmol _{CH₂O} g _{cat} ⁻¹ hr ⁻¹	Reference
FeMo_140P-10C-20W-7.5F	1.58	250	7.4	25.4	This work
FeMo_110P-5C-20W-5F	1.37	250	10.7	42.5	This work
FeMo_140P-10C-10.5W-5F	1.66	250	7.9	33.7	This work
FeMo_80P-7.5C-20W-5F	1.55	250	8.4	26.6	This work
FeMo_80P-10C-1W-5F	1.61	250	6.7	25.6	This work
FeMo_140P-5C-20W-10F	1.50	250	9.8	33.3	This work
FeMo_110P-7.5C-10.5W-7.5F	1.60	250	9.4	36.6	This work
FeMo _x catalysts formed from metal oxalate precursor	1.5	260	0.785	18.6	¹
Fe ₂ (MoO ₄) ₃ /MoO ₃ nanorods	1.6	260	0.785	12.8	²
FeMo _x catalysts formed from metal malonate precursor	1.5	260	0.785	6.35	³
Co-FeMo _x (Co:Mo = 0.05:1)	2.6	285	0.785	22.9	⁴
5 wt% MoO ₃ -CaHAP – MoO ₃ supported on Ca doped hydroxyapatite		250	23.56	18.4	⁵
10 wt% MoO ₃ -CaHAP – MoO ₃ supported on Ca doped hydroxyapatite		250	23.56	26.0	⁵

References

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