

Supplementary Information

Hydrophobic modification of hydroxyl-rich metallic Sn catalysts for acidic CO₂ electroreduction at high current densities

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23 Characterizations

24 The morphologies of as-prepared catalysts were conducted by transmission electron
25 microscope (TEM, JEOL JEM-F200) and scanning electron microscope (SEM,
26 ZEISS/Sigma 560). The high-resolution TEM (HRTEM) images and energy-dispersive
27 X-ray spectroscopy (EDS) were also taken by JEOL JEM-F200. The crystal structures
28 of the catalysts were studied by powder X-ray diffraction (XRD) using a Panalytical
29 Empyrean diffractometer with Cu-K α radiation. The contact angle (CA)
30 characterization of the samples was tested on POWEREACH (IC200D1). The XPS
31 analyses were carried out with a Thermo SCIENTIFIC Nexsa spectrometer using a
32 monochromatic Al K α source (6 mA, 12 kV). Spectra were calibrated by carbon 1 s
33 spectroscopy with the main line set at 284.8 eV, and then the valence states of the
34 catalysts were analyzed using the Casa XPS software. The detection of hydrogen and
35 carbon monoxide was conducted by gas chromatography (GC 7890). Raman
36 spectroscopy and *in-situ* Raman spectra (LabRAM HR Evolution, France) were
37 collected with a 532 nm laser source. ^1H nuclear magnetic resonance (^1H NMR) spectra
38 were recorded using an AVANCE 400-MHz NMR instrument.

39 Preparation of working electrodes

40 The catalytic activity of CO₂RR in different samples was studied by using a three-
41 electrode flow cell. To prepare the working electrode, the 4 mg catalyst was dispersed
42 in 400 μL ethanol and 40 μL 5% Nafion. The homogeneous catalyst ink with a
43 concentration of 10 mg mL⁻¹ was obtained by 1h ultrasound. After 1h ultrasound, the
44 ink was sprayed on a square (1 \times 1 cm²) hydrophobic treated carbon paper (load: 1 mg
45 cm⁻²) as a cathode electrode for further electrochemical testing. Ag/AgCl electrodes
46 (stored in saturated KCl) and commercial IrTa alloy electrodes were used as reference
47 and counter electrodes, respectively. Nafion 117 was used as the proton exchange
48 membrane to separate the working electrode and the reverse electrode.

49 Catalysts such as Sn-OH@CMK, Sn-OH@CMK-P, Sn@CMK and SnO₂@CMK
50 can be used directly for electrode preparation after preparation. The concentrations of

PTFE solution required for the samples with optimized PTFE content during the preparation process were 0.025wt%, 0.05wt% and 0.1wt% respectively. The amounts of $\text{SnCl}_4 \cdot 5\text{H}_2\text{O}$ required for the samples with optimized $\text{Sn}(\text{OH})_4$ content during the preparation process were 0.1g, 0.2g, 0.4g and 0.8g respectively.

Electrochemical measurements

All electrochemical tests were performed on the CHI660E electrochemical workstation. The catalyst was sprayed on the carbon paper (22BB Gas diffusion layer). The performance of CO_2 reduction was measured by applying different current densities using the time potentiometric method. 0.5 M K_2SO_4 was used as the acid electrolyte (pH = 3). The pH value of the electrolyte was determined by a pH meter. The anode and cathode chambers were both 30 mL, the CO_2 flow rate was 20 sccm, and the electrolyte flow rate was stabilized at 10 mL min^{-1} by the mass flow controller. The duration of each time potentiometric test was 1500 s. Before the test, each catalyst underwent a pre-reduction process at -0.1 A cm^{-2} for 900 s. Before electrolysis, CO_2 gas with a purity of 99.99% was immersed in the electrolyte for 30 min, and the working electrode potential was converted to the RHE reference scale, the formula was as follows:

$$E_{\text{RHE}} = E_{\text{Ag/AgCl}} + 0.0591 \times \text{pH} + 0.197(\text{V})$$

For electrochemical impedance spectroscopy (EIS) measurements, the frequency range was set from 100 000 to 0.1 Hz with an amplitude of 10 mV. The electrochemical double layer capacitance (C_{dl}) of the different samples was determined by the CV method and the electrochemical surface area (ECSA) was then calculated. The linear sweep voltammetry (LSV) plots were measured at a scan rate of 10 mV s^{-1} for the anodic and cathodic reactions. All electrochemical data were not iR-compensation corrected in this work.

In each time potentiometric test, the gas products collected at 1500s are analyzed using gas chromatography (GC, Agilent 7890 gas chromatography system) equipped with a thermal conductivity detector (TCD) and a flame ionization detector (FID).

Argon (99.999%) was used as carrier gas. H₂ was detected by TCD and CO by FID. The liquid products were detected by proton nuclear magnetic resonance (¹H NMR, Bruker 400 M) with dimethyl sulfoxide (DMSO) as the internal standard. The Faraday efficiency of H₂, CO, and HCOOH was calculated as follows:

$$FE = e F \times n / Q = e F \times n / (I \times t) \times 100\%$$

Where e is the number of electrons transferred (for H₂, CO and HCOOH determined as 2), F is the Faraday constant, Q is the charge, I is current, t is the running time and n is the amount of product (in moles) determined by GC or ¹H NMR. SPCE for HCOOH was calculated at 25 °C, 1 atm according to the following equation:

$$SPCE_{HCOOH} = (60s \times n) / [\text{flow rate (sccm)} \times t(s) \times 24.05(l/mol)]$$

Where n is the amount of HCOOH (in moles) determined from ¹H NMR, and the running time (t) is 1000 s for each flow rate.

Computational details

All the geometries were optimized with Vienna Ab initio Simulation Package (VASP) ¹, using the Perdew-Burke-Ernzerhof (PBE) functional² and the projector augmented wave (PAW) method³ to account for core-valence interactions. The kinetic energy cutoff for the plane wave basis set was set to 450 eV. Van der Waals interaction was considered using DFT-D3BJ correction^{4,5}. All surface slabs were modeled with a vacuum layer of 15 Å. The convergence threshold was set to 10⁻⁵ eV energy differences for the electronic SCF step and the convergence threshold for geometry optimization was set to 0.05 eV Å⁻¹ for the maximal force. The Gibbs free energy during reactions was defined as follows:

$$\Delta G = E_{ads} - E_{sur} + \Delta H_{corr} - T\Delta S$$

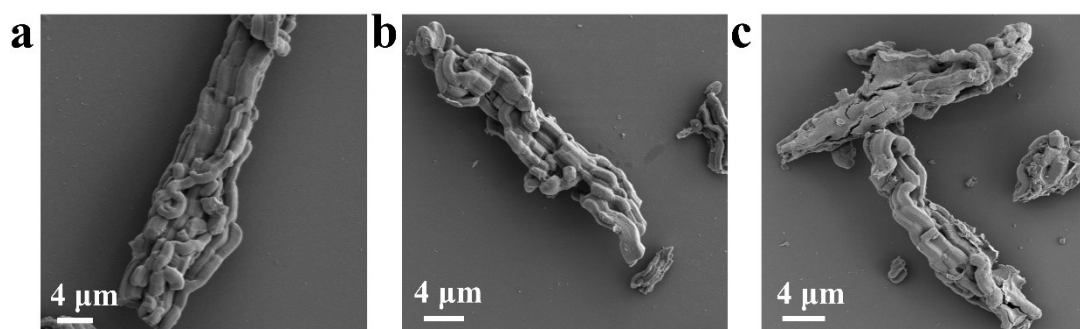
Here, E_{ads} is the electronic energy for the adsorption state; E_{sur} is the electronic energy of the unadsorbed surface; while ΔH_{corr} and ΔS are thermal correction to enthalpy change and entropy change, which were obtained through the aid of VASPKIT, version 1.2.5⁶. the visualization of periodic structures and the analysis of electron density difference are performed by VESTA, Version 3.5.5⁷.

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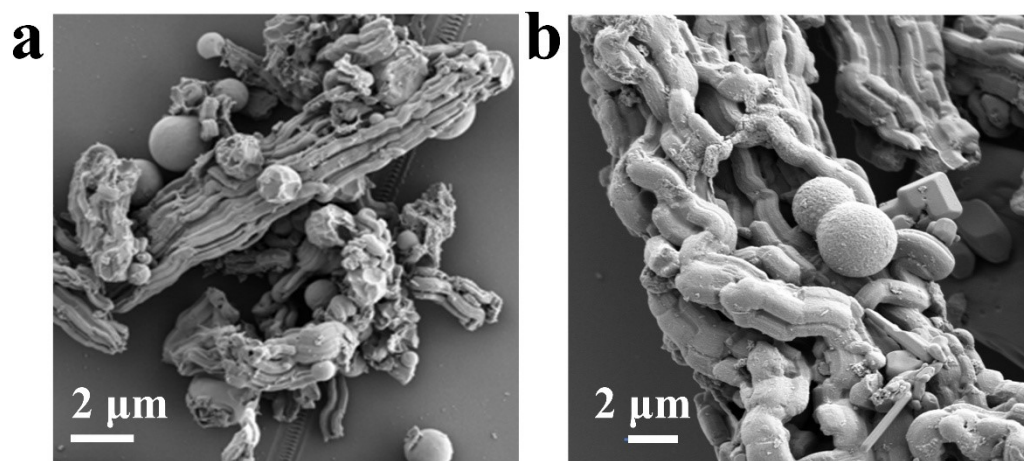
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110 **Figures**



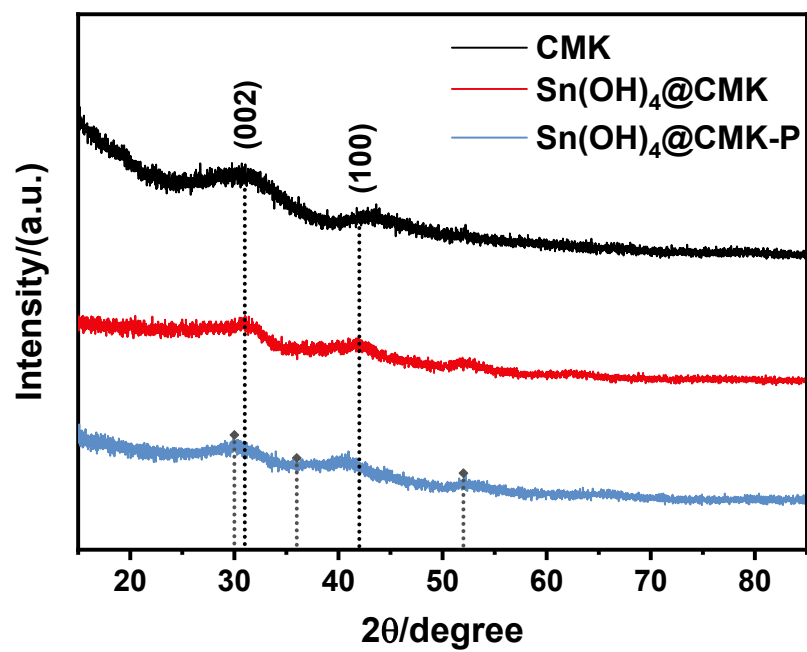
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112 Fig. S1 SEM image of (a) CMK-3, (b) $\text{Sn(OH)}_4\text{@CMK}$, (c) $\text{Sn(OH)}_4\text{@CMK-P}$.



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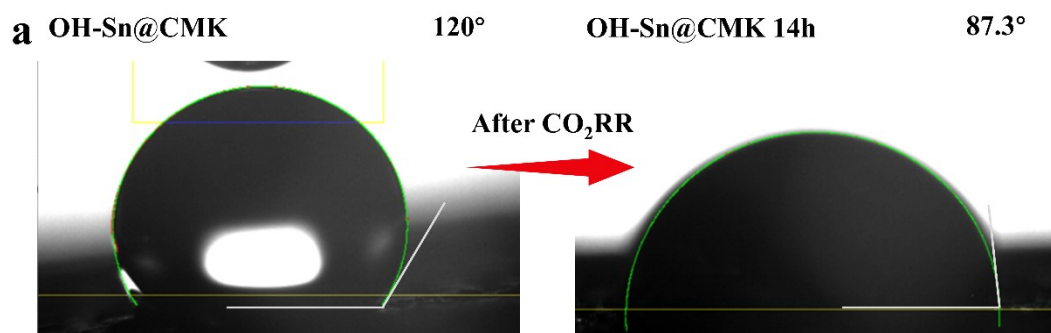
114 Fig. S2 SEM image of (a) Sn@CMK , (b) $\text{SnO}_2\text{@CMK}$.



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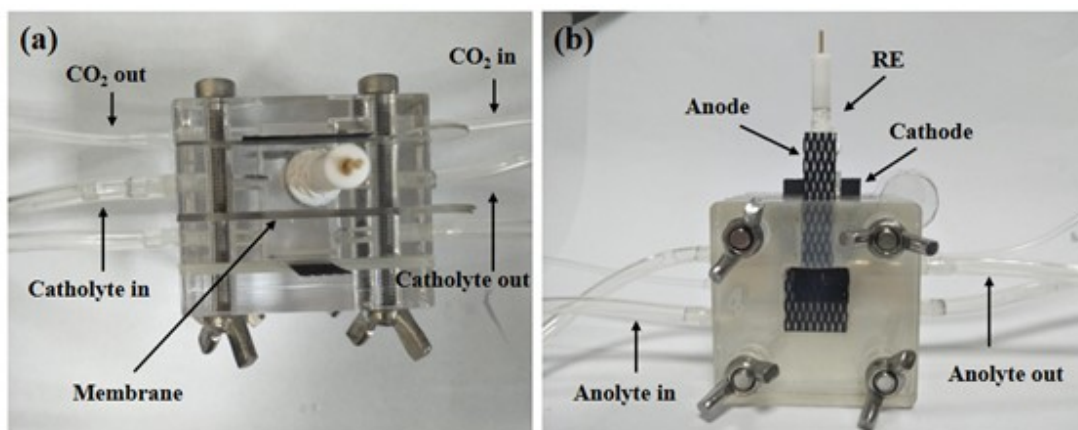
116 Fig. S3 XRD patterns of CMK, Sn(OH)₄@CMK and Sn(OH)₄@CMK-P.

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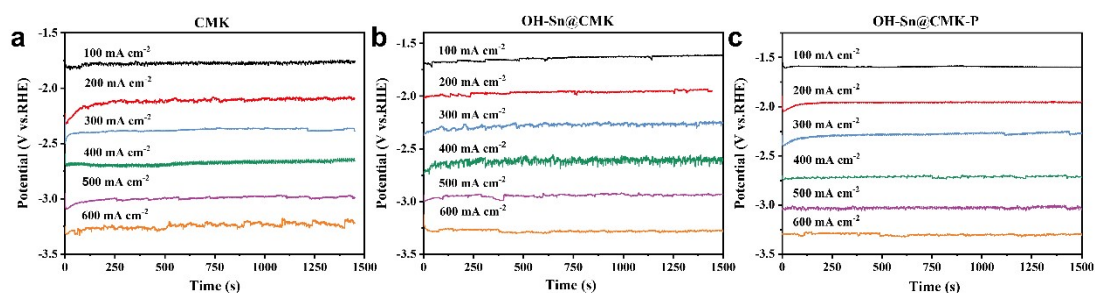
119 Fig. S4 Contact angle measured for OH-Sn@CMK.



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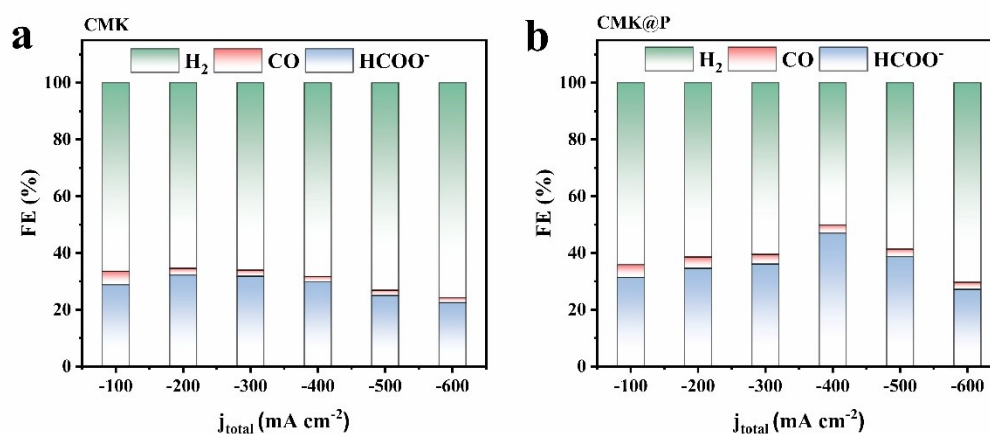
121 Fig. S5 Setup image of the used electrochemical flow cell.

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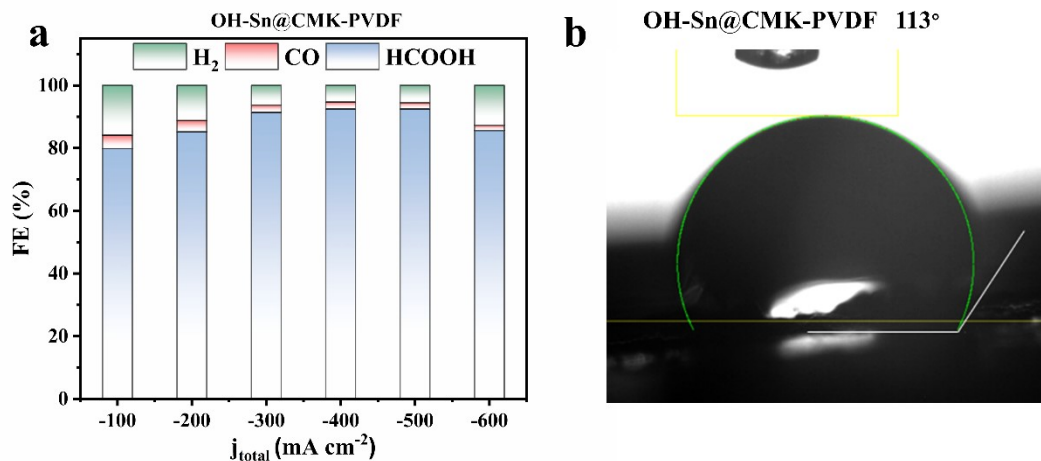
124 Fig. S6 Chronopotentiometry (v-t) curves of (a) CMK, (b) OH-Sn@CMK and (c) OH-
125 Sn@CMK-P catalysts.



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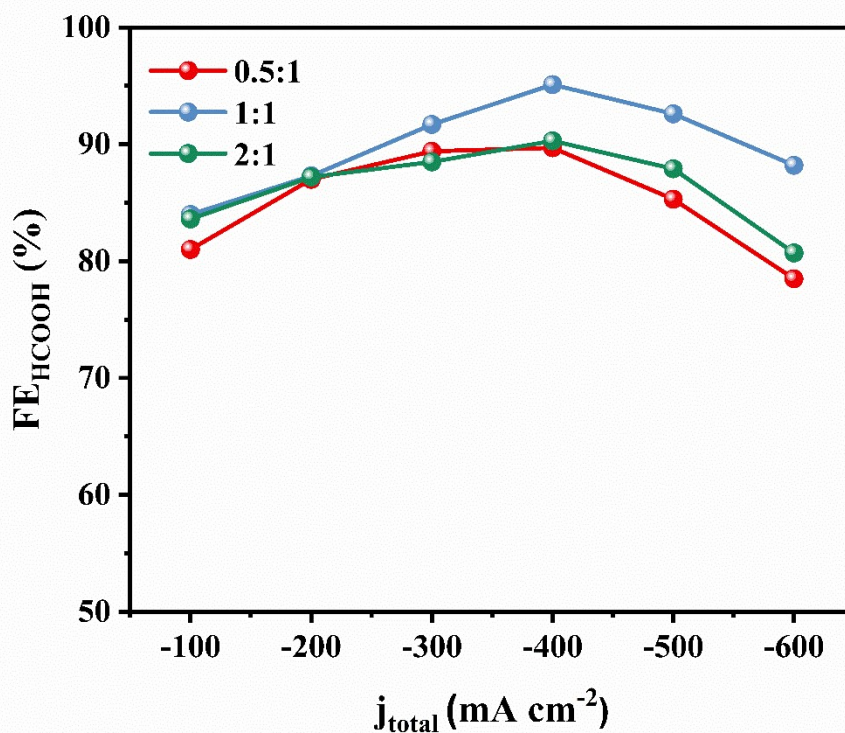
127 Fig. S7 The FEs of HCOO^- , H_2 and CO for (a) CMK and (b) CMK@P in acidic CO_2RR
128 at $\text{pH}=3$.

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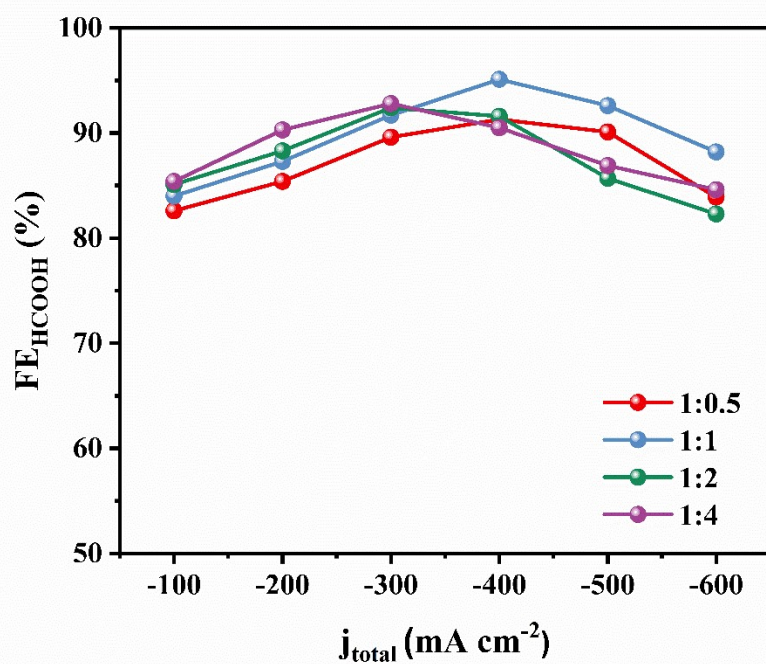
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131 Fig. S8 (a) The FEs of HCOOH (or HCOO⁻), H₂, and CO for OH-Sn@CMK-PVDF in
132 acidic CO₂RR. (b) Contact angle measured for OH-Sn@CMK-PVDF after CO₂RR.



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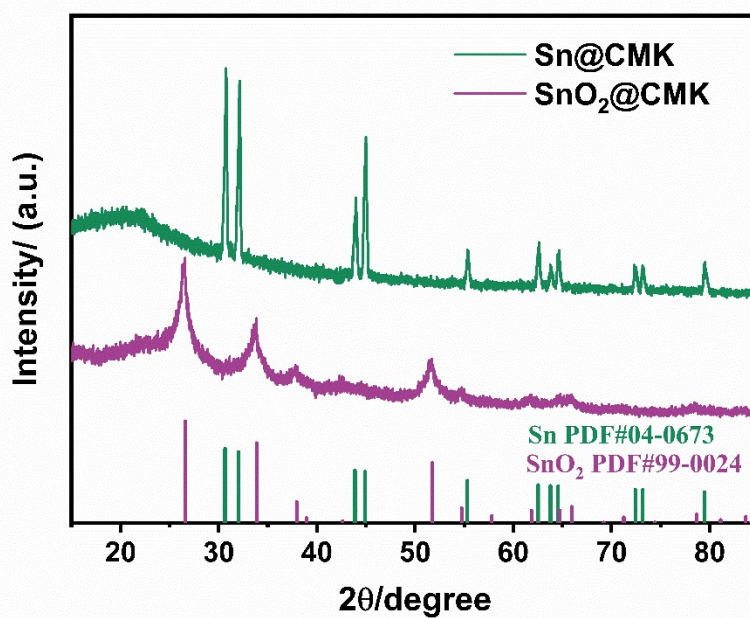
134 Fig. S9 The FEs of HCOOH for OH-Sn@CMK-P in acidic CO₂RR at different scale
135 (0.5:1, 1:1, 2:1).



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137 Fig. S10 FE_{HCOOH} with different $\text{Sn}(\text{OH})_4$ content OH-Sn@CMK-P in acidic CO_2RR

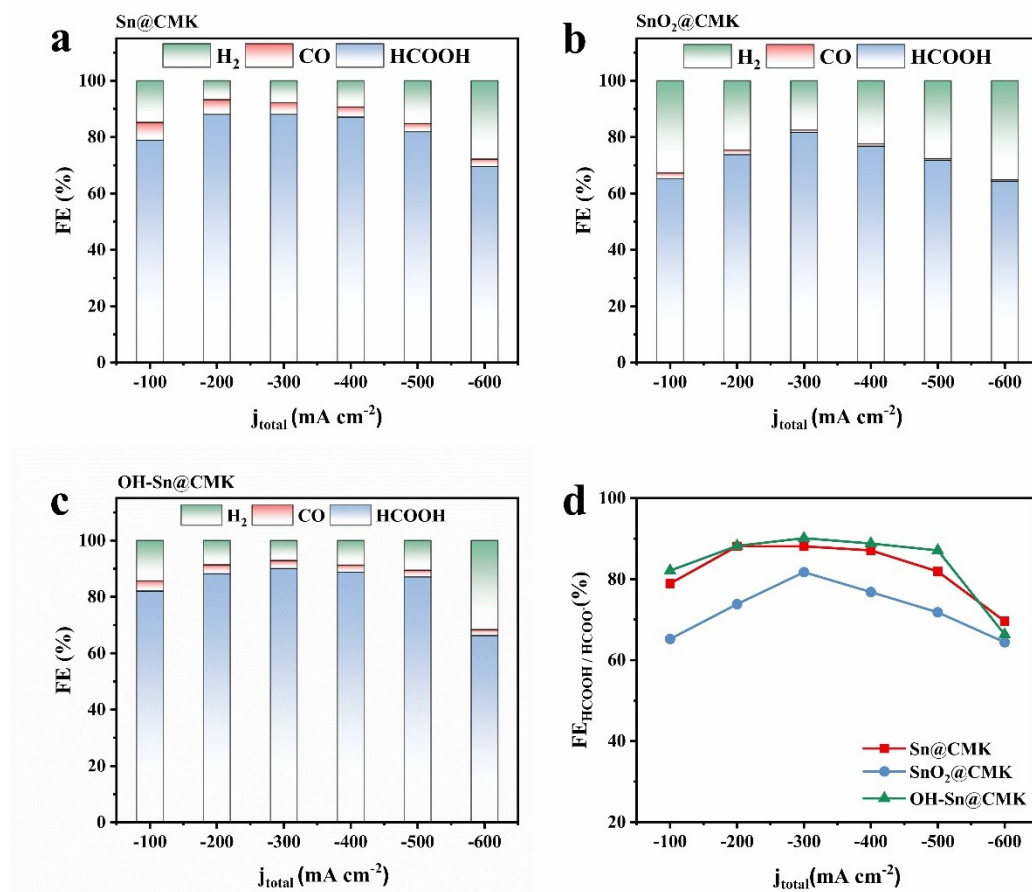
138 (CMK: $\text{Sn}(\text{OH})_4$ = 1:0.5, 1:1, 1:2, 1:4).



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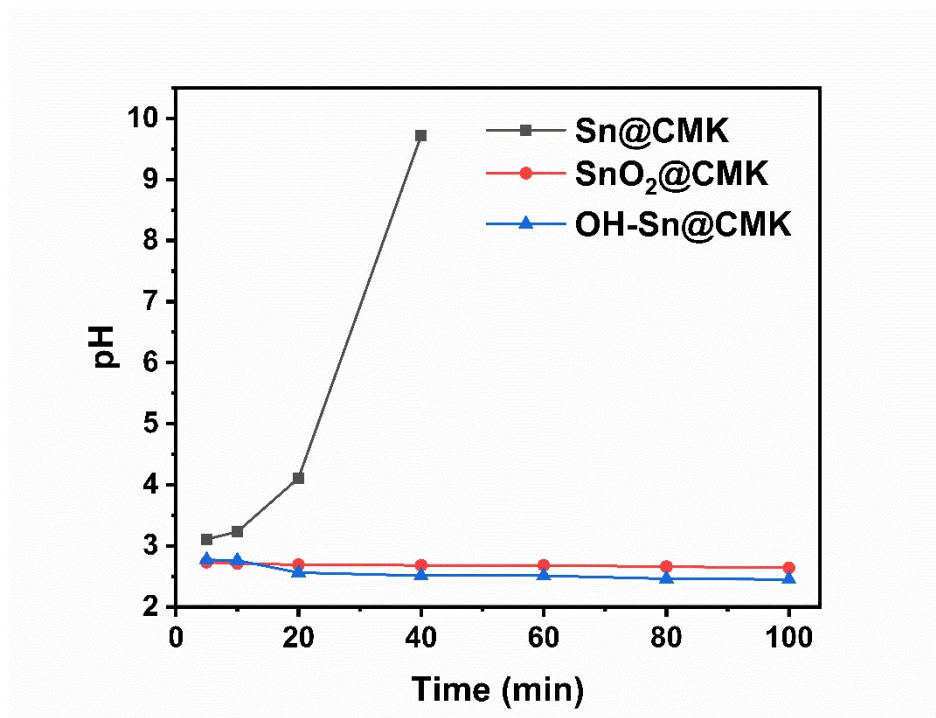
140 Fig. S11 XRD patterns of Sn@CMK and SnO_2 @CMK.

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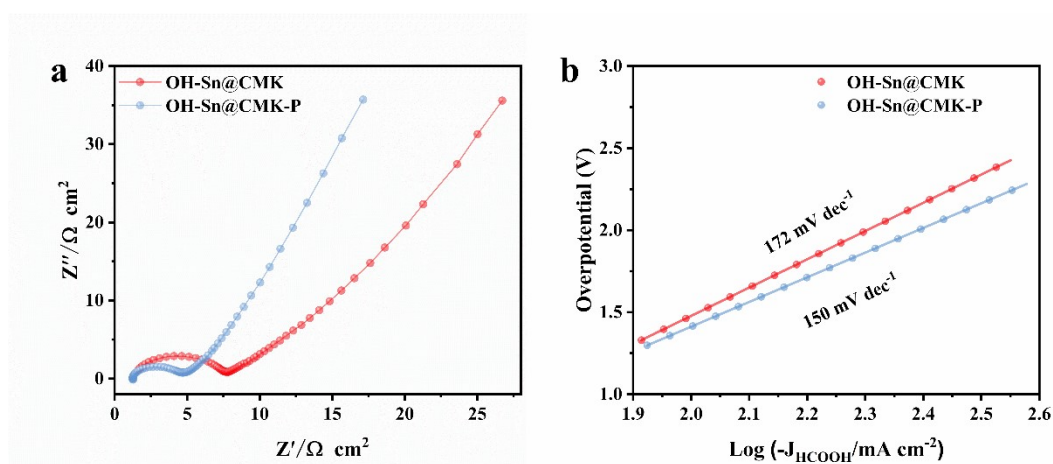
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143 Fig. S12 The FEs of HCOOH (or HCOO⁻), H₂, and CO for (a) Sn@CMK, (b)
144 SnO₂@CMK and (c) OH-Sn@CMK in acidic CO₂RR. (d) Comparison of
145 FE_{HCOOH/HCOO⁻} at Sn@CMK, SnO₂@CMK, and OH-Sn@CMK under different
146 currents.



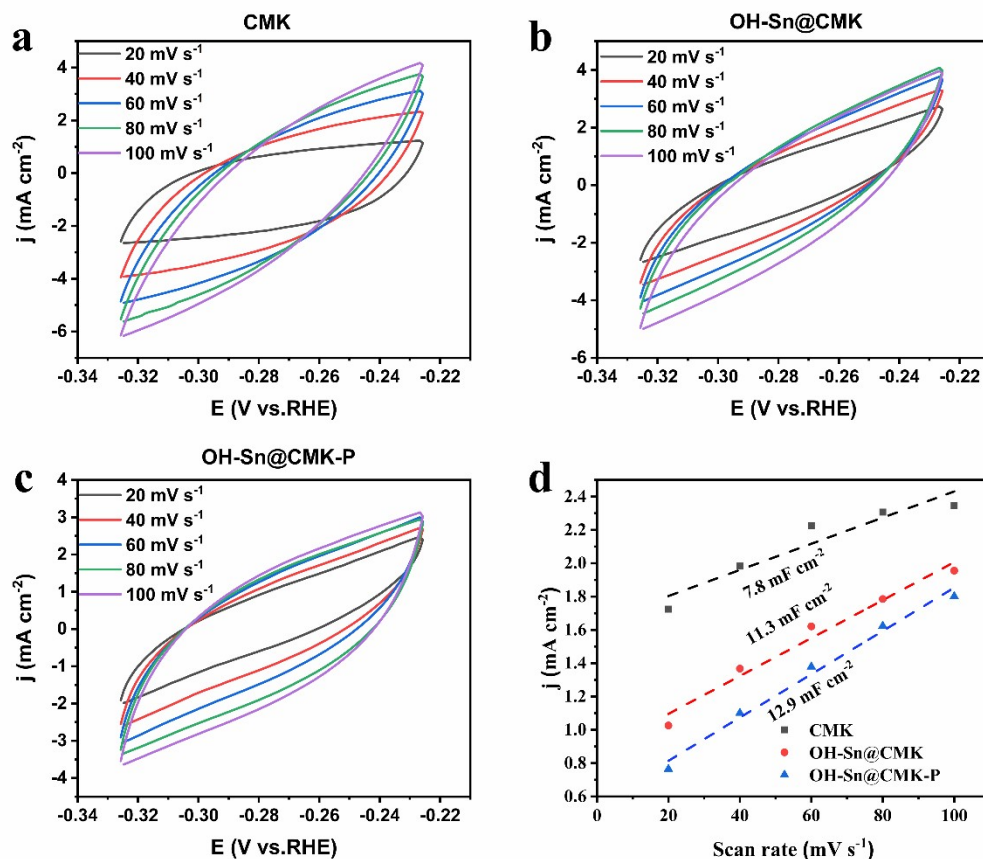
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148 Fig. S13 Sn@CMK, SnO₂@CMK, and OH-Sn@CMK pH test of electrolytes in
149 electroreduction processes.



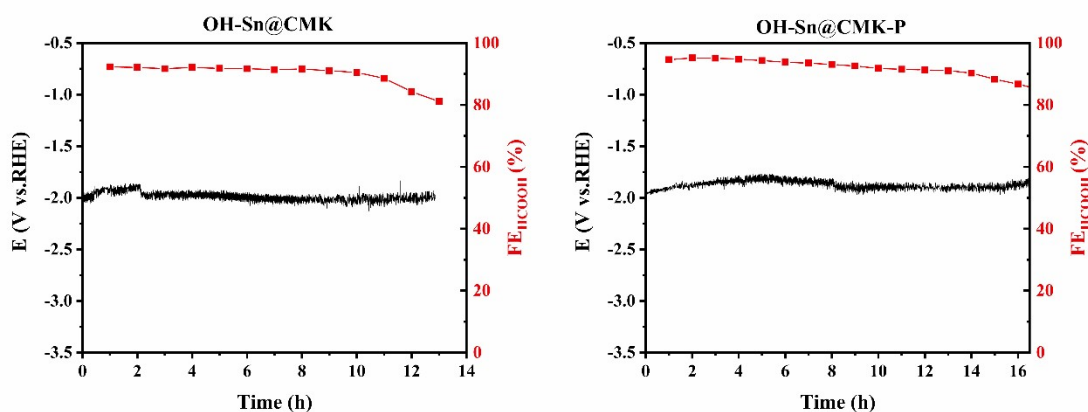
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151 Fig.S14 (a) EIS and (b) Tafel tests for OH-Sn@CMK and OH-Sn@CMK-P.



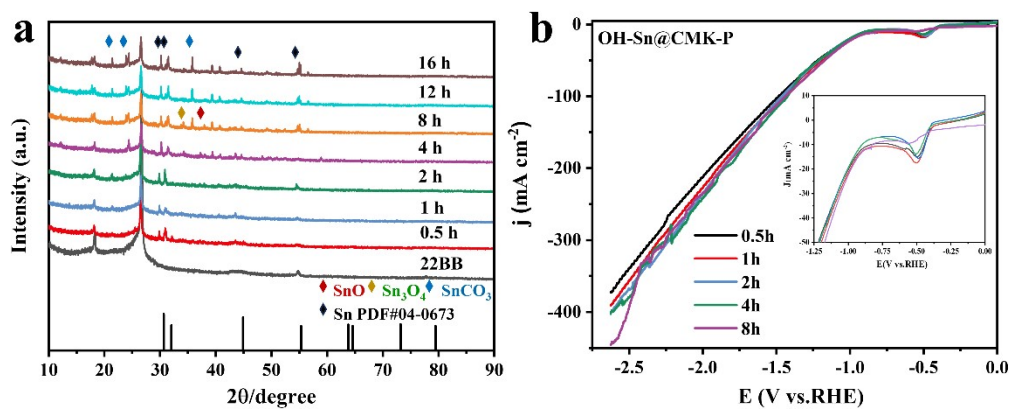
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153 Fig. S15 Cyclic voltammetry taken over a range of scan rates for (a) CMK, (b) OH-
 154 Sn@CMK, and (c) OH-Sn@CMK-P. (d) Current due to double-layer charging plotted
 155 against cyclic voltammetry scan rate for CMK, OH-Sn@CMK, and OH-Sn@CMK-P.



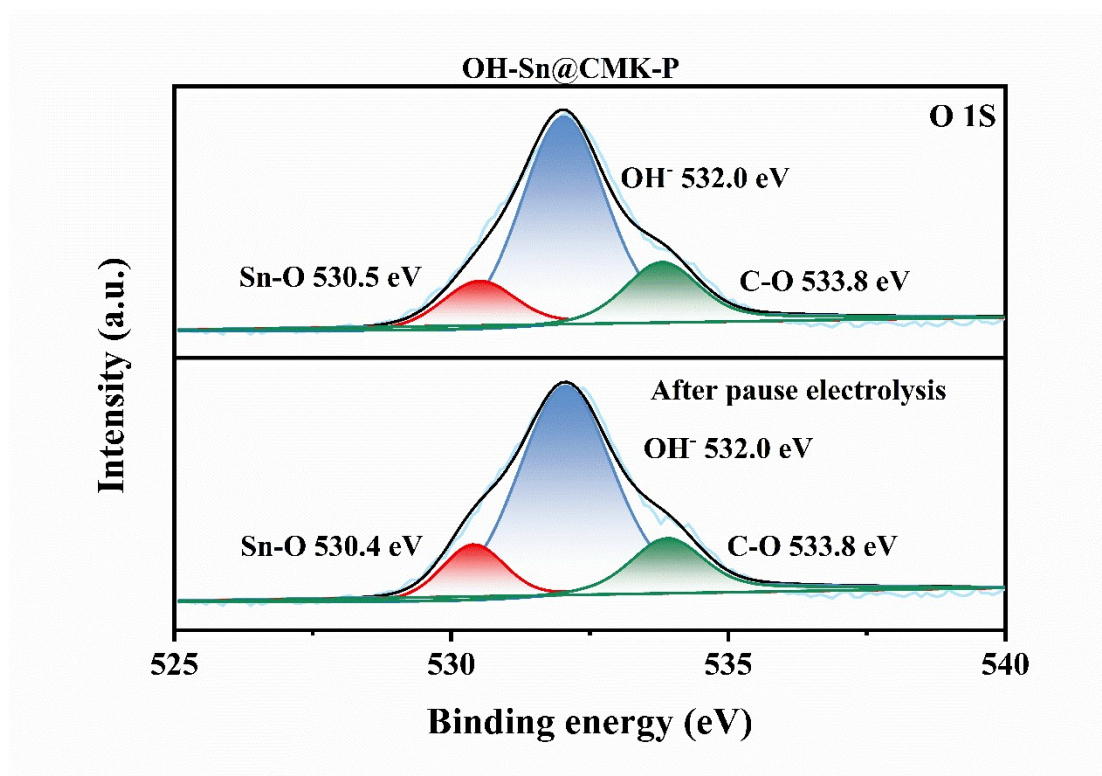
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157 Fig. S16 The stability of (a) OH-Sn@CMK and (b) OH-Sn@CMK-P at -200 mA cm^{-2}
 158 under the $\text{pH}=3$ electrochemical environment in CO_2 RR.



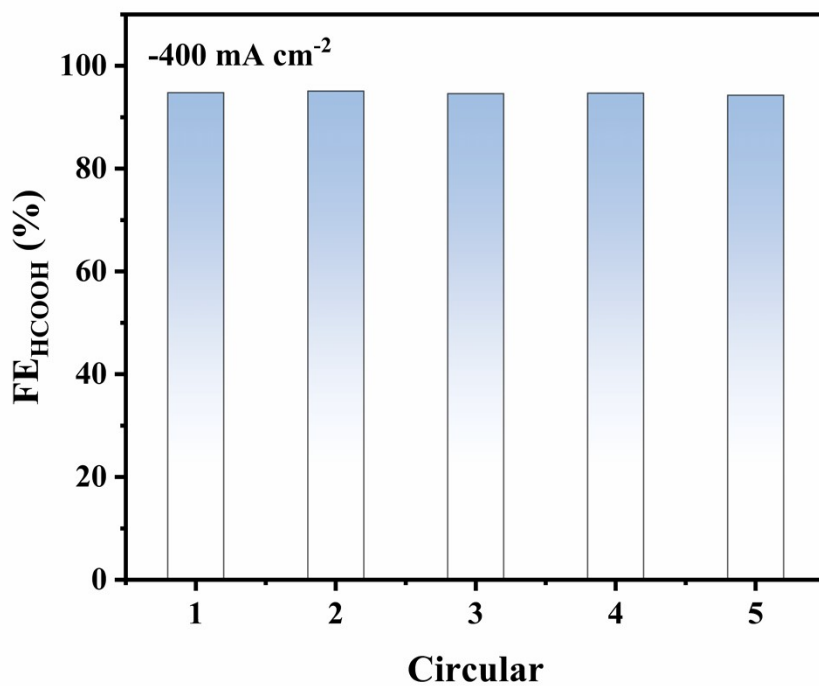
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160 Fig. S17 (a) XRD and (b) LSV images of OH-Sn@CMK-P catalyst in CO₂RR process.



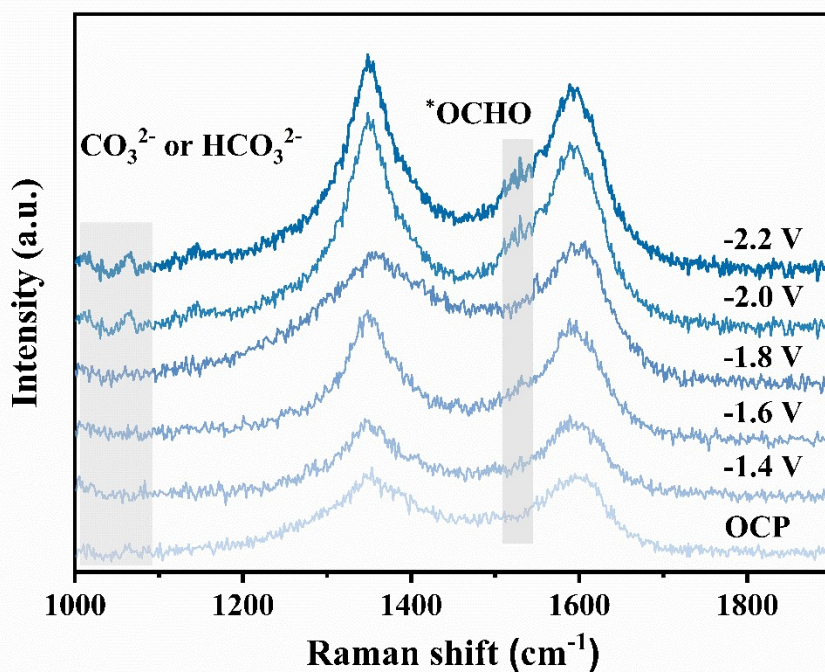
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162 Fig. S18 The XPS spectrum of the electrode surface of OH-Sn@CMK-P before and
163 after suspension at -200 mA cm⁻² for 30 min



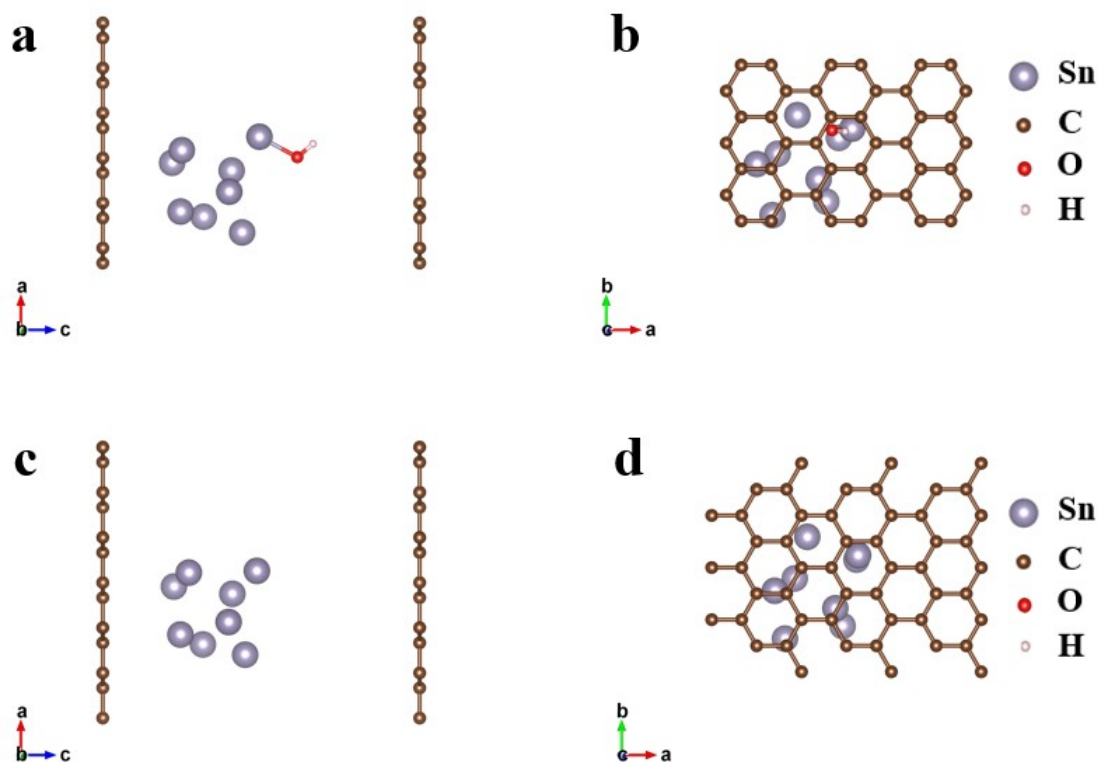
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165 Fig. S19 The cycle test diagram of OH-Sn@CMK-P.



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167 Fig. S20 In situ Raman spectra recorded at different cathodic potentials over Sn@CMK.

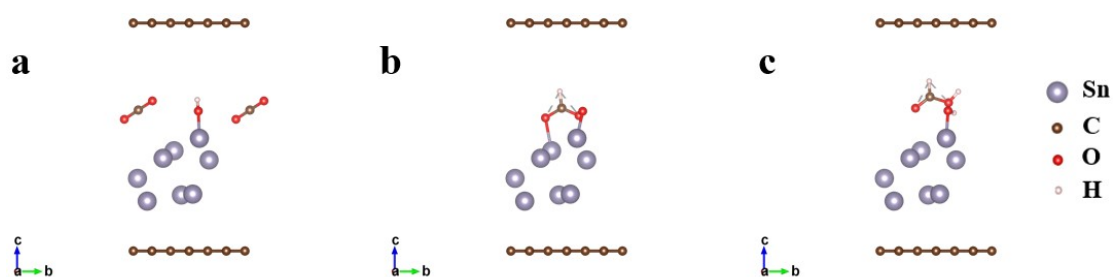


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169 Fig. S21 Schematic catalyst structures: (a) side and (b) top views of OH-Sn@CMK.

170 Schematic catalyst structures: (c) side and (d) top views of Sn@CMK.

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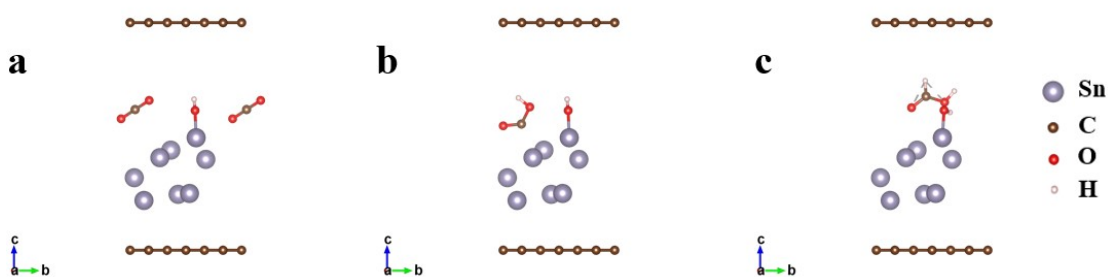


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173 Fig. S22 Intermediate state of HCOOH pathway during CO₂RR over OH-Sn@CMK:

174 (a-c) CO₂*, *OCHO, *HCOOH.

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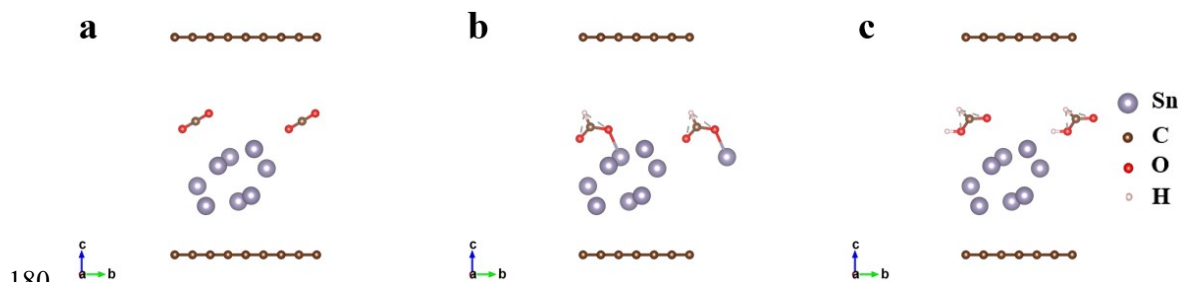


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177 Fig. S23 Intermediate state of HCOOH pathway during CO₂RR over OH-Sn@CMK:

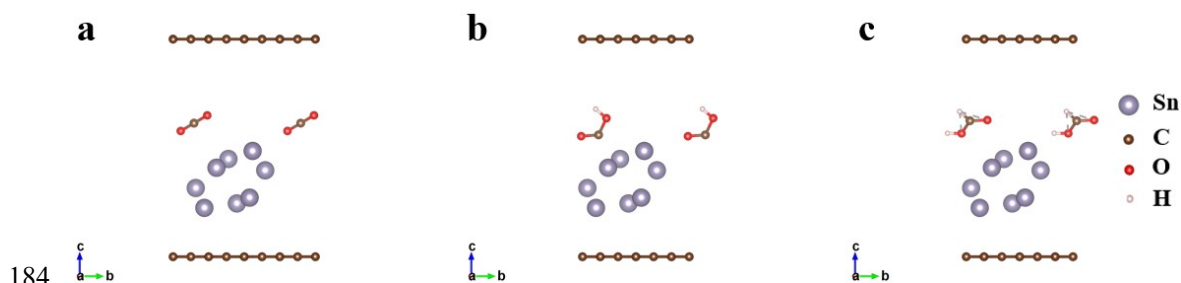
178 (a-c) CO_2^* , $^*\text{COOH}$, $^*\text{HCOOH}$.

179



181 Fig. S24 Intermediate state of HCOOH pathway during CO_2RR over Sn@CMK : (a-c)
182 CO_2^* , $^*\text{OCHO}$, $^*\text{HCOOH}$.

183



185 Fig. S25 Intermediate state of HCOOH pathway during CO_2RR over Sn@CMK : (a-c)
186 CO_2^* , $^*\text{COOH}$, $^*\text{HCOOH}$.

187 REFERENCES

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