## Unlocking High Selectivity and Stability of Cobaltbased Catalyst in *n*-Butanol Amination Reaction

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## **Supplementary Tables**

Catalysts	Co content <sup>a</sup> (wt.%)	$S_{BET}^{b}$ $(m^2/g)$	S <sub>ext</sub> (m <sup>2</sup> /g)	V <sub>total</sub> <sup>c</sup> (cm <sup>3</sup> /g)	V <sub>micro</sub> (cm <sup>3</sup> /g)
3Co/SSZ-13	3.2	712	32	0.30	0.26
3Co/USY	3.3	840	127	0.64	0.27
3Co/S1	3.3	432	124	0.30	0.12
$3Co/Al_2O_3$	3.5	204	203	0.53	
3Co/SiO <sub>2</sub>	3.3	294	282	0.91	

Table S1 Textural properties and Co content of cobalt-based catalysts using different supports.

<sup>a</sup> Co content was determined by XRF analysis;

<sup>b</sup> Specific surface area calculated by the BET method;

 $^{\rm c}$  Total pore volume measured at P/P\_0 = 0.99.

Table S2 Calculated proportions of CoO <sub>x</sub> nanoparticles and nanoclusters on nCo/S1	catalysts
based on H <sub>2</sub> -TPR hydrogen consumption.	

Catalysts	Co content <sup>a</sup> (wt.%)	CoO <sub>x</sub> nanoparticles <sup>b</sup> (%)	CoO <sub>x</sub> nanoclusters <sup>b</sup> (%)
5Co/S1	5.4	97	3
1Co/S1	1.1	26	74

<sup>a</sup> Co content was determined by XRF analysis;

 $^{\rm b}$  Relative contents of  ${\rm CoO}_x$  nanoparticles and nanoclusters were estimated by deconvoluting the H\_2-TPR profiles.

Table S3 Quantita	tive XPS analysis of	surface cobalt oxi	dation states in	nCo/S1 catalysts.
	Catalysts	Co <sup>3+</sup> (%)	Co <sup>2+</sup> (%)	
	5Co/S1	49	51	
	1Co/S1	17	83	

Catalysts	${ m S_{BET}}^{ m a}$ $(m^2/g)$	S <sub>ext</sub> (m <sup>2</sup> /g)	V <sub>total</sub> <sup>b</sup> (cm <sup>3</sup> /g)	V <sub>micro</sub> (cm <sup>3</sup> /g)	
3Co/S1	432	124	0.30	0.12	
3Co/S1-250 h	260	58	0.20	0.08	
3Co/S1-250 h-C	413	144	0.27	0.11	

Table S4 Texture properties of 3Co/S1, 3Co/S1-250 h and 3Co/S1-250 h-C.

<sup>a</sup> Specific surface area calculated by the BET method;

<sup>b</sup> Total pore volume measured at  $P/P_0 = 0.99$ .

Catalysts	Co content <sup>a</sup> (wt.%)	$S_{BET}^{b}$ $(m^2/g)$	$S_{ext}$ (m <sup>2</sup> /g)	V <sub>total</sub> <sup>c</sup> (cm <sup>3</sup> /g)	V <sub>micro</sub> (cm <sup>3</sup> /g)
S1		431	128	0.30	0.12
3Co/S1	3.3	432	124	0.30	0.12
3Co/S1-AW-1.7	2.7	373	170	0.27	0.11
3Co/S1-AW-2.5	1.9	354	199	0.29	0.08

 Table S5 Textural properties and Co content of 3Co/S1 catalysts before and after acid treatment.

<sup>a</sup> Co content was determined by XRF analysis;

<sup>b</sup> Specific surface area calculated by the BET method;

 $^{\rm c}$  Total pore volume measured at P/P\_0 = 0.99.

 Table S6 Quantitative XPS analysis of surface cobalt oxidation states in 3Co/S1 catalysts before and after acid treatment.

Catalysts	Co <sup>3+</sup> (%)	Co <sup>2+</sup> (%)			
3Co/S1	43	57			
3Co/S1-AW-1.7	40	60			
3Co/S1-AW-2.5	33	67			

## **Supplementary Figures**



Fig. S1. N<sub>2</sub> adsorption and desorption isotherms of Co-based catalysts with different supports.



Fig. S2. SEM images of (A) 3Co/S1, (B) 3Co/USY, (C) 3Co/SSZ-13, (D) 3Co/SiO<sub>2</sub> and (E) 3Co/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub>.



Fig. S3. FTIR spectra of adsorbed *n*-butanol on 1Co/S1 and 5Co/S1.



**Fig. S4.** *n*-Butanol conversion, product distribution, and *n*-butylamine yield over 3Co/S1 catalyst under varying reaction conditions.

Reaction conditions: (A) T = 200 °C, WHSV = 1 h<sup>-1</sup>, molar ratio H<sub>2</sub>: *n*-butanol = 9; (B) T = 200 °C, molar ratio H<sub>2</sub>: NH<sub>3</sub>: *n*-butanol = 9:8:1; (C) molar ratio H<sub>2</sub>: NH<sub>3</sub>: *n*-butanol = 9:8:1, WHSV = 1.5 h<sup>-1</sup>; (D) T = 180 °C, molar ratio NH<sub>3</sub>: *n*-butanol = 8:1, WHSV = 1.5 h<sup>-1</sup>.



Fig. S5. N<sub>2</sub> adsorption and desorption isotherms of 3Co/S1, 3Co/S1-250 h and 3Co/S1-250 h-C.



Fig. S6. XRD patterns of 3Co/S1, 3Co/S1-250 h and 3Co/S1-250 h-C.



Fig. S7. XRD patterns of 3Co/S1 catalysts before and after acid treatment and support S1.



Fig. S8. N<sub>2</sub> adsorption and desorption isotherms of 3Co/S1 catalysts before and after acid treatment and support S1.



Fig. S9. H<sub>2</sub>-TPR profiles of 3Co/S1 catalysts before and after acid treatment.



**Fig. S10.** H<sub>2</sub>-TPR profiles of 3Co/S1 catalyst before and after reduction. Reduction condition: 500 °C in the fix bed for 2 h with 50 ml/min of H<sub>2</sub>.



Fig. S11. Effect of reduction temperature on *n*-butanol conversion and product distribution over 3Co/S1 catalyst.
Reaction conditions: T reaction = 180 °C; molar ratio H<sub>2</sub>: NH<sub>3</sub>: *n*-butanol = 4:8:1;

WHSV =  $1.5 h^{-1}$ .