

Supplementary Materials

Highly efficient and stable methane dry reforming enabled by confinement-mass transfer balancing of Ni/DFNS catalysts

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Table S1. Summary of the peak position of Ni⁰ and Ni²⁺.

| Catalysts | Ni2p _{3/2} Binding Energy | | The ratio of Ni ⁰ /Ni ²⁺ |
|--------------|------------------------------------|----------------------|--|
| | Ni ²⁺ (eV) | Ni ⁰ (eV) | |
| Ni/DFNS-2-EG | 855.6 | 852.6 | 30.1% |
| Ni/DFNS-4-EG | 855.8 | 852.5 | 44.8% |
| Ni/DFNS-6-EG | 856.1 | 852.9 | 50.1% |
| Ni/DFNS-8-EG | 855.7 | 853.0 | 46.7% |
| Ni/DFNS-6-WI | 856.0 | 852.6 | 24.1% |

Table S2. Summary of the peak position of O 1s

| Catalysts | O1s Binding Energy | | | The ratio of O _{surf} / (O _{latt} +O _{surf} +O _{ads}) |
|--------------|------------------------|------------------------|-----------------------|--|
| | O _{latt} (eV) | O _{surf} (eV) | O _{ads} (eV) | |
| | Ni/DFNS-2-EG | 531.8 | 532.8 | 534.0 |
| Ni/DFNS-4-EG | 531.7 | 532.9 | 533.9 | 81.7% |
| Ni/DFNS-6-EG | 531.8 | 533.1 | 534.1 | 83.1% |
| Ni/DFNS-8-EG | 531.7 | 532.9 | 533.9 | 70.2% |
| Ni/DFNS-6-WI | 531.6 | 533.0 | 534.0 | 68.3% |

Table S3. The CH₄ conversion rates at different GHSV and temperature conditions

| Catalysts | CH ₄ conversion (%) | | | | | Temperature (°C) |
|-----------|--|--------------|-------|------|------|------------------|
| | GHSV (mL • g ⁻¹ • h ⁻¹) | 450 | 470 | 490 | 510 | |
| | | Ni/DFNS-6-EG | 18000 | 7.35 | 9.70 | 13.13 |
| | 72000 | 2.45 | 3.27 | 4.56 | 6.42 | 8.50 |
| | 90000 | 1.98 | 2.79 | 3.63 | 4.67 | 6.06 |

Table S4. Catalytic reaction rate for CH₄ at different GHSV and temperature

| conditions | | | | | | |
|--------------|---|------------------|-------|-------|-------|-------|
| Catalysts | Rate*10 ⁴ (mol · g ⁻¹ · s) | Temperature (°C) | | | | |
| | GHSV (mL · g ⁻¹ · h ⁻¹) | 450 | 470 | 490 | 510 | 530 |
| Ni/DFNS-6-EG | 18000 | 1.642 | 2.165 | 2.930 | 3.840 | 4.902 |
| | 72000 | 2.183 | 2.917 | 4.069 | 5.730 | 7.589 |
| | 90000 | 2.207 | 3.018 | 4.048 | 5.506 | 6.963 |

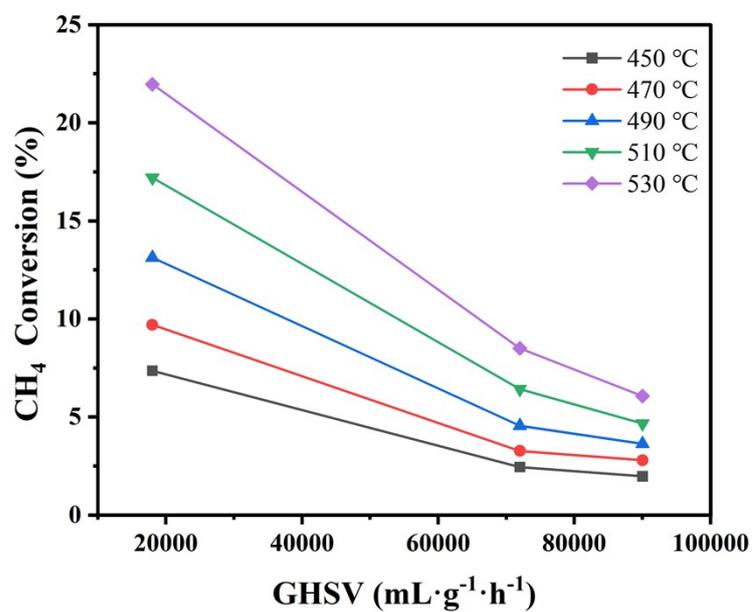


Fig. S1. Effect of external diffusions on the Ni/DFNS-6-EG catalysts.

Computational approach employed in the kinetic analysis:

The reaction rates for CH₄ were determined by employing the formula below:

$$r_i = \frac{X_i * F_{i,in}}{V_m * g_{cat} * wt_{(metal)} \%} \quad (i = \text{CH}_4)$$

Where r_i was the reaction rates for CH₄ (mol_i·g_{cat}⁻¹·s⁻¹), X_i was the conversion for CH₄ (%), $F_{i, in}$ show the inlet flow rate of each component at standard temperature and pressure (mol_i·s⁻¹), g_{cat} was the mass of the catalyst used to test the rate value, V_m represents the standard molar volume, $wt_{(metal)}\%$ represents the actual metal content of the catalyst [1].

The Arrhenius equation was stated as follows:

$$\ln r_i = \ln A - \frac{E_a}{R} \left(\frac{1}{T}\right) \quad (i = \text{CH}_4)$$

Where A was the preexponential factor, E_a was the activation energy (kJ·mol⁻¹), R was the gas constant (8.314 J·mol⁻¹·K⁻¹), and T was the thermodynamic temperature of reaction (K).

According to the Arrhenius equation $\ln(\text{rate}) = -E_a/RT + \ln A$. The logarithm of the reaction rate of the reacting gas, $\ln(\text{rate})_{\text{CH}_4}$, was used as the Y-axis, and the reciprocal of the temperature (1/T) was used as the X-axis. The slope of the resulting graph was calculated and found to be E_a/R .

Experiments were carried out to ensure the negligible effects of external diffusion limitation on the recorded kinetic data. The effects of external limitation were ruled out by varying the GHSV [2, 3]. In Table S3 and Fig. S1, the CH₄ conversion rate of Ni/DFNS-6-EG significantly decreased at a GHSV of 72,000 mL·g⁻¹·h⁻¹, while it further declined and stabilized at 90,000 mL·g⁻¹·h⁻¹. Moreover, in Table S4, the CH₄ reaction rate at GHSV values of 72,000 mL·g⁻¹·h⁻¹ and 90,000 mL·g⁻¹·h⁻¹ exhibited nearly identical values at the same temperature and maintained a stable trend. This indicated that external diffusion limitation was largely eliminated when GHSV exceeded 72000 mL·g⁻¹·h⁻¹. To obtain more accurate data and minimize the effect of external diffusion limitation, we conducted kinetic tests at high space velocity (90,000 mL·g⁻¹·h⁻¹). Meanwhile, the effect of catalyst particle size on internal diffusion

limitation was negligible owing to its uniform and fine particle size^[3, 4]. The DRM reaction was in the kinetic region under the aforementioned reaction conditions and the apparent activation energies approached the intrinsic values.

Supplementary references

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