

## Supplementary Information

### **Synergy of Wettability and Acidity in Carbon-Based Acid Catalysts for Efficient Conversion of Glucose to 5-Hydroxymethylfurfural**

Han Xu<sup>a</sup>, Xinyu Cui<sup>a</sup>, Zhihao Bi<sup>a</sup>, Yang Guo<sup>a\*</sup>, Donghai Xu<sup>a</sup>, Lingzhao Kong<sup>b,c</sup>,  
Pengjie Miao<sup>b,\*</sup>

<sup>a</sup> Key Laboratory of Thermo-Fluid Science and Engineering, Ministry of Education, School of Energy and Power Engineering, Xi'an Jiaotong University, Xi'an, Shaanxi, PR China 710049

<sup>b</sup> Xinjiang Key Laboratory of New Energy and Energy Storage Technology Xinjiang Institute of Technology, Aksu 843100, PR China

<sup>c</sup> School of Environmental Science and Technology Suzhou University of Science and Technology Suzhou, Jiangsu, PR China 215009

Corresponding author: Y. Guo

E-mail: [guoyang@xjtu.edu.cn](mailto:guoyang@xjtu.edu.cn) ORCID ID: 0000-0001-9830-5942

## Supplementary data

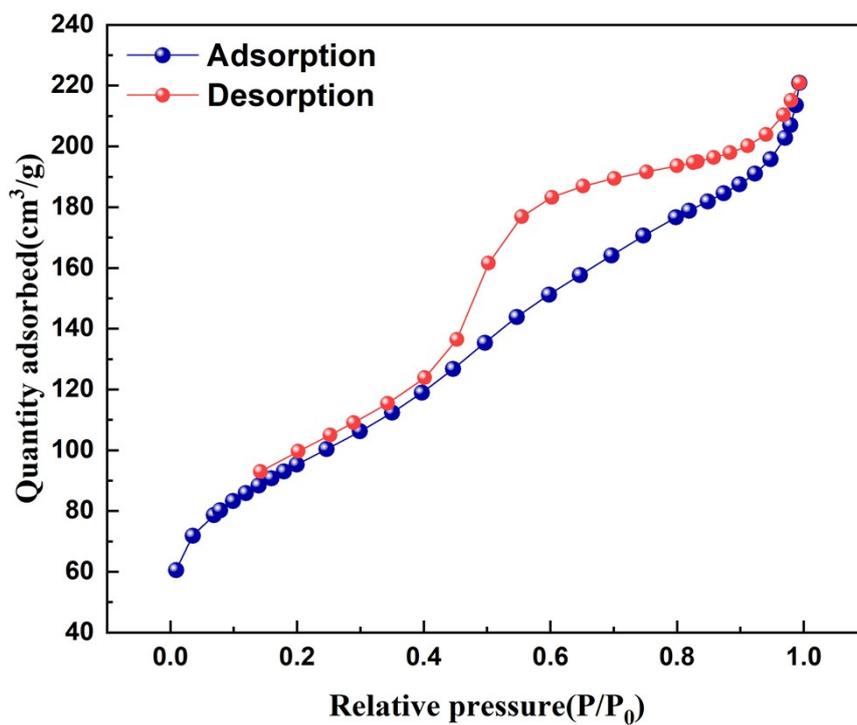
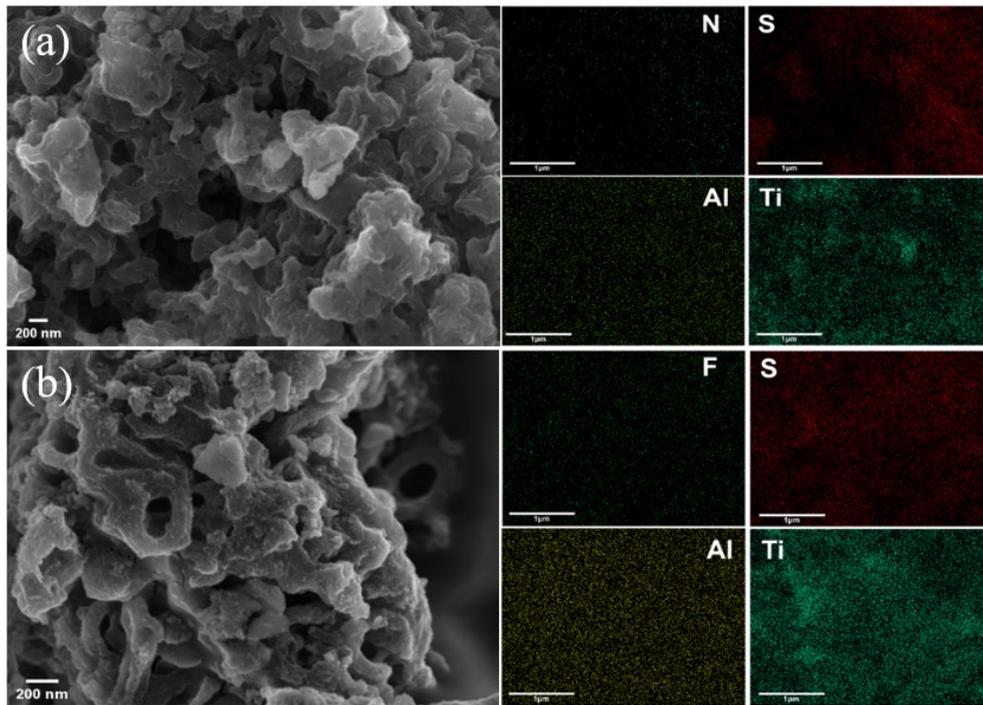


Fig. S1. Nitrogen adsorption and desorption curve of BTPC.



**Fig. S2.** (a)SEM and EDS images of Al-Ti/SBTPC-N; (b) SEM and EDS images of Al-Ti/SBTPC-F

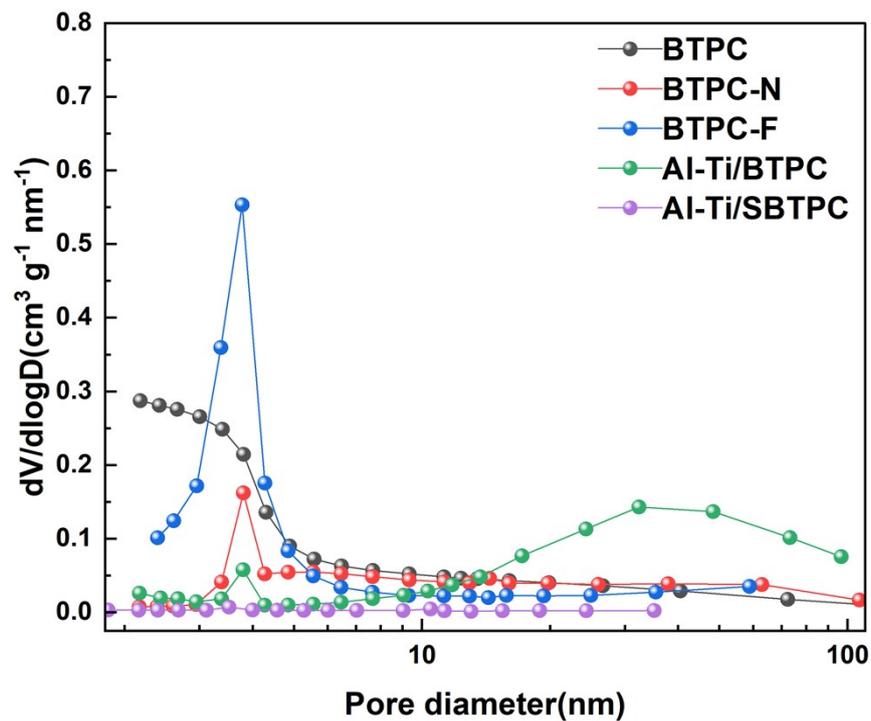


Fig. S3. Pore size distribution of BTPC, BTPC-N, BTPC-F, Al-Ti/BTPC, Al-Ti/SBTPC.

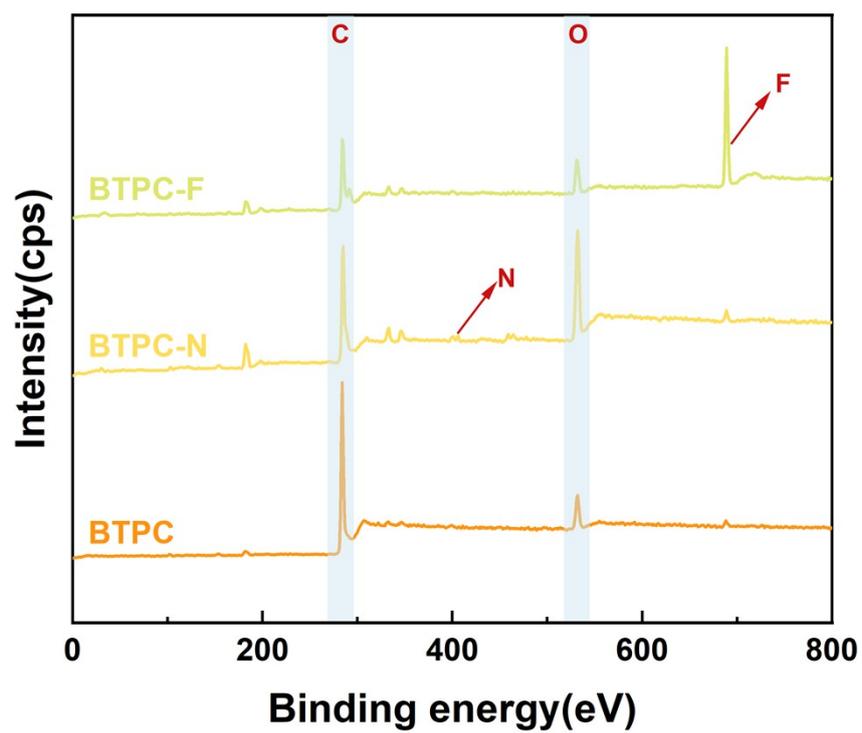
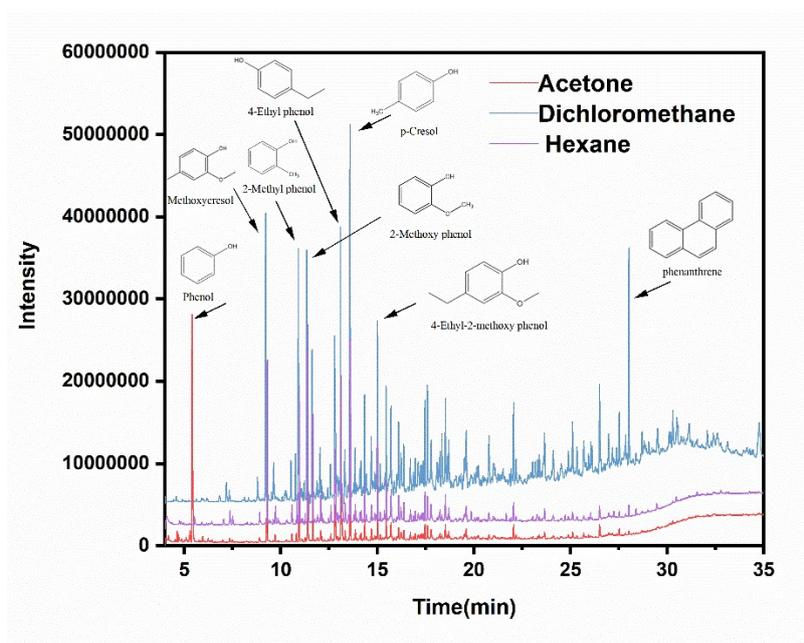


Fig. S4. XPS diagram of BTPC, BTPC-N, BTPC-F.



**Fig. S5** Composition analysis of biomass tars. Reaction conditions. GC-FID test conditions: Nitrogen, hydrogen and air were used as carrier gases. The chromatographic column was initially heated to 80°C and ramped up to 300°C at 20°C/min and dwelled for 25min.

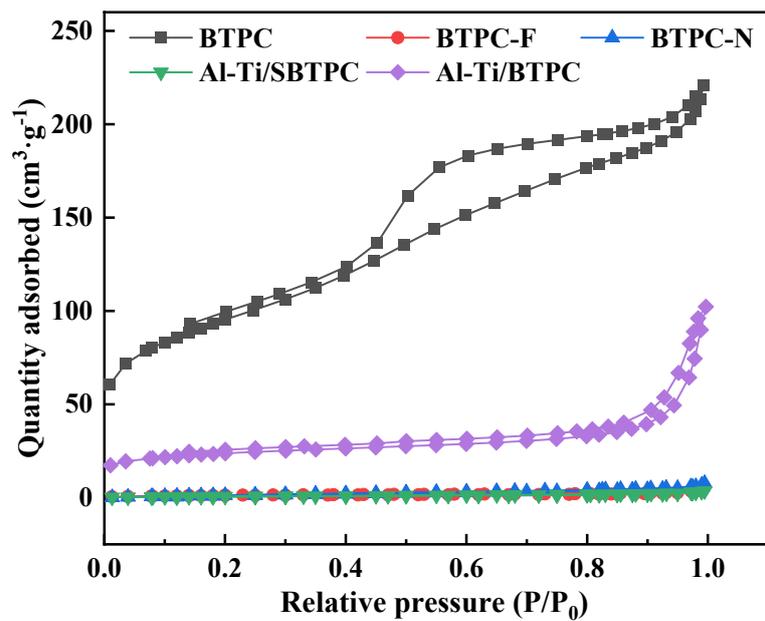


Fig. S6 Typical N<sub>2</sub> adsorption-desorption isotherms.

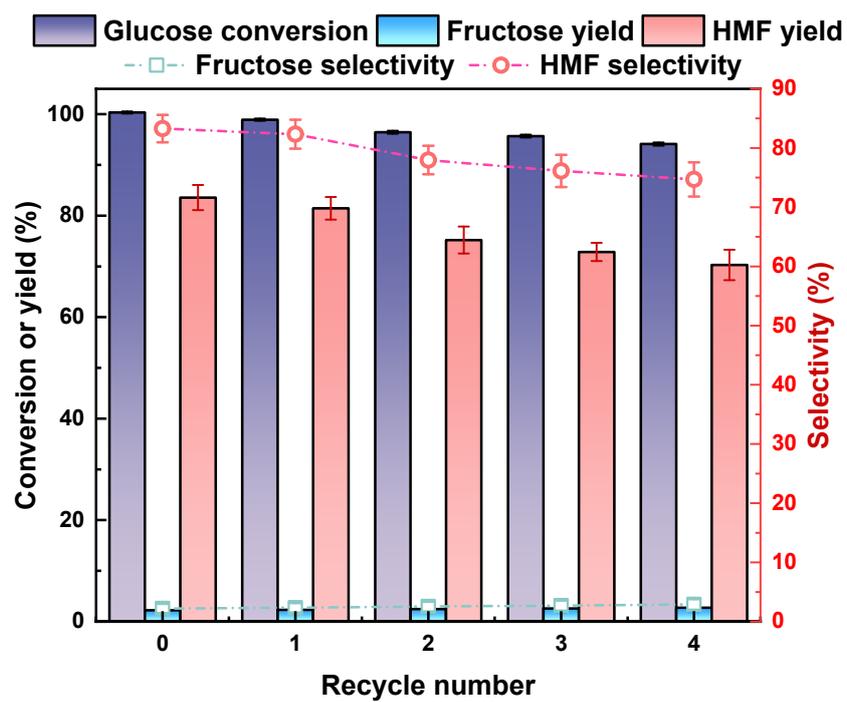


Fig. S7 Stability experiments. Reaction conditions: reaction temperature 140 C, residence time 4h.

Table S1. Specific surface area and average pore size of samples

<b>Catalyst</b>	<b>BTPC</b>	<b>BTPC-N</b>	<b>BTPC-F</b>	<b>Al-Ti/BTPC</b>	<b>Al-Ti/SBTPC</b>
<b>BET(m<sup>2</sup>/g)</b>	340.1	6.9	4.43	84.2	2.9
<b>Average pore size(nm)</b>	4.44	5.18	6.38	17.5	5.57

Table S2 HMF production from glucose using various carbon-based solid acids.

Entry	Substrate	Catalyst	Tem. (°C)	Time (h)	Solvent	HMF yield (%)	Reference
1	Glucose	Al-Ti/SBTPC	140	4	20wt%NaCl-H <sub>2</sub> O/DMSO	83.6	This work
2	Glucose	$\beta$ -cyclodextrin-SO <sub>3</sub> H	180	5	DMSO	47	[1]
3	Glucose	pTsa-Ca/AC	180	24	H <sub>2</sub> O/MIBK	57	[2]
4	Glucose	PAS-CNT	160	4	H <sub>2</sub> O/EA	42.4	[3]
5	Glucose	PCP(Cr)-SO <sub>3</sub> H-Cr (III)	180	4	NaCl-H <sub>2</sub> O/THF	80.4	[4]
6	Glucose	niobia/carbon	170	8	NaCl-H <sub>2</sub> O/THF	53.3	[5]
7	Glucose	SNC	120	8	DMSO	61.3	[6]
8	Glucose	S-TsC	180	0.5	H <sub>2</sub> O/GVL	43.8	[7]

## Reference

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