

## Coal-derived two-dimensional $\text{MNb}_2\text{O}_6$ (M=Mn, Fe, Co)/C hybrids with superior lithium storage performance

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## Materials

Coal was produced in Kuche, relative analysis on the coal has been reported in previous literature [1]. Niobium(V) oxide ( $\text{Nb}_2\text{O}_5$ , 99%) was purchased from the Aladdin Reagent Company. Manganese (II) chloride, ferric nitrate, and cobaltous nitrate (AR grade) were purchased from Tianjin Zhiyuan Chemical Reagent Co., Ltd. Sulfuric acid ( $\text{H}_2\text{SO}_4$ , 98%), nitric acid ( $\text{HNO}_3$ , 63%), and ( $\text{HCl}$ , 37%) were purchased from Chengdu Cologne Chemicals Co., Ltd. Absolute ethanol (AR grade) was purchased from Tianjin Kemeng Chemical Industry and Trade Co., Ltd. All these reagents were used without purification.

## Characterization

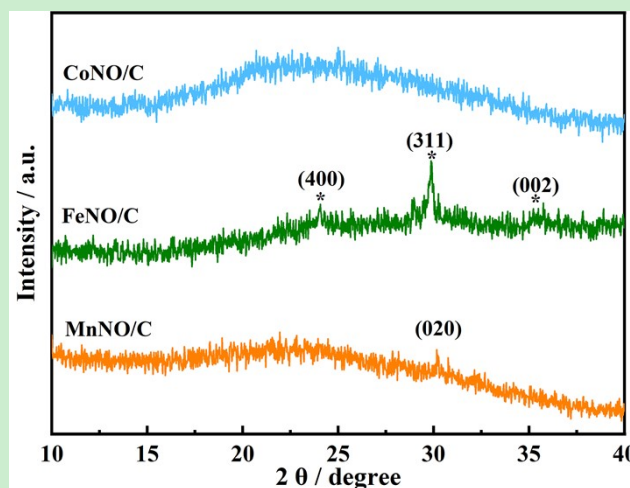
Material composition was characterized by X-ray diffraction (XRD; Bruker D8/Cu  $K\alpha$  radiation). Morphology analysis was tested by employing Hitachi's field-emission scanning electron microscopy (SEM, S-4800) and transmission electron microscopy (TEM) and high-resolution transmission electron microscope (HRTEM, JEOL JEM-2100F). Thermogravimetric analysis (TGA) was carried out by using Netzsch STA 449C in air atmosphere from room temperature to 800 °C with a heating rate of 10 °C min<sup>-1</sup>. Brunauer-Emmett-Teller (BET) specific surface area and pore structure analysis (DFT method) of the samples were measured by nitrogen adsorption/desorption with an Autosorb-iQ Pressure Sorption Analyzer (Quantachrome Instruments USA) at 77 K.

## Electrochemical Characterization

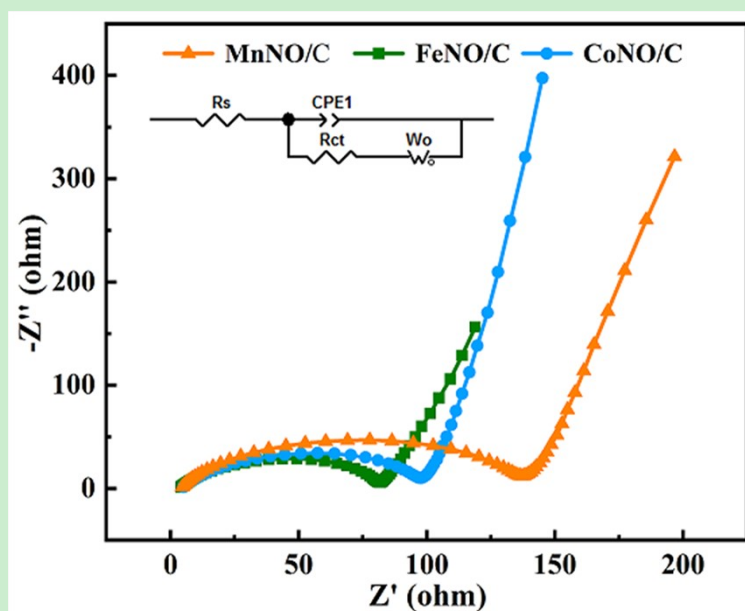
The working electrodes (half-cells) were obtained through the following procedures: mixing the active materials (80 wt%), acetylene black (10 wt%), and polyvinylidene fluoride binder (10 wt%), followed by dropwise addition of N-methyl-2-pyrrolidone (NMP) to form a homogeneous slurry, which was uniformly spread onto a copper foil, then the coated copper foil was dried overnight under vacuum at 110 °C. The assembly of cells was operated in an argon-filled glovebox with suitable water/oxygen concentrations, using lithium metal as the counter electrode, Celgard 2400 membrane as the separator, and LiPF<sub>6</sub> (1 M) in mixed solvents of ethyl carbonate/diethyl carbonate (1:1, v/v) as the electrolyte. Cyclic voltammetry curves were obtained on a CHI-760C workstation with a sweep rate of 0.1 mV s<sup>-1</sup>. Galvanostatic charge and discharge (GCD) measurements were conducted on a Land (CT2001A China) at 0.01-3.00 V (versus Li<sup>+</sup>/Li). Electrochemical impedance spectra (EIS) behaviors were gained within the frequency scope of 100 kHz to 10 mHz. All tests were conducted at room temperature, and the mass loading of the actively materials was about 0.8 mg cm<sup>-2</sup>.

For the preparation of full cell battery, FeNO/C was used as anode, commercial LiFePO<sub>4</sub> was employed as cathode, and the electrolyte was commercially purchased (Guangzhou Tianci Advanced Materials Co., Ltd.). Specifically, LiFePO<sub>4</sub>, N-carbon black, and polyvinylidene fluoride were evenly mixed in a mass ratio of 80:10:10, adding NMP to obtain a homogeneous slurry. Then the slurry was uniformly coated on the Al foil and dried overnight in a vacuum oven, the loading mass of LiFePO<sub>4</sub> is about four times of FeNO/C. Before the assembly of full battery, the half-battery was pre-lithiated at 0.1 A g<sup>-1</sup> for three cycles, and disassembled in the Ar glovebox. The anode electrode was rinsed with commercial electrolyte, and then reassembled with the pre-prepared cathode in the Ar glovebox. The obtained full batteries were operated in the

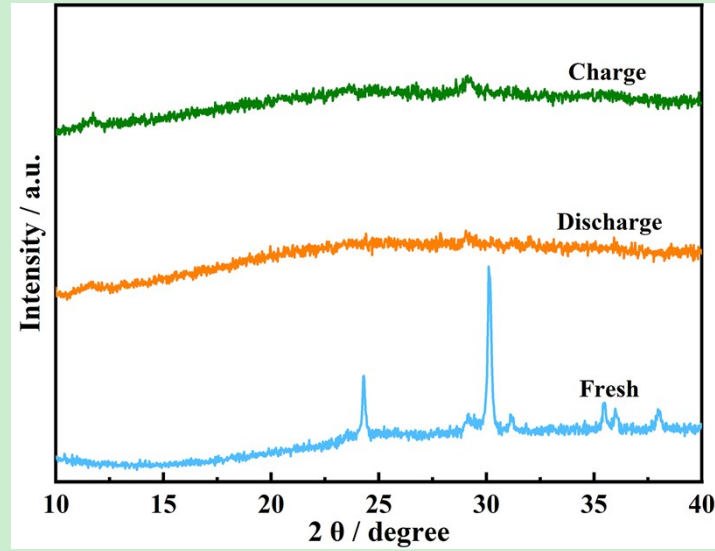
potential range of 1.0-4.5 V, and the specific capacity was calculated based on the cathode material.



**Fig. S1.** XRD patterns of MnNO/C, FeNO/C, and CoNO/C electrodes after 600 cycles.



**Fig. S2.** Electrochemical impedance spectra (EIS) of MnNO/C, FeNO/C, and CoNO/C.

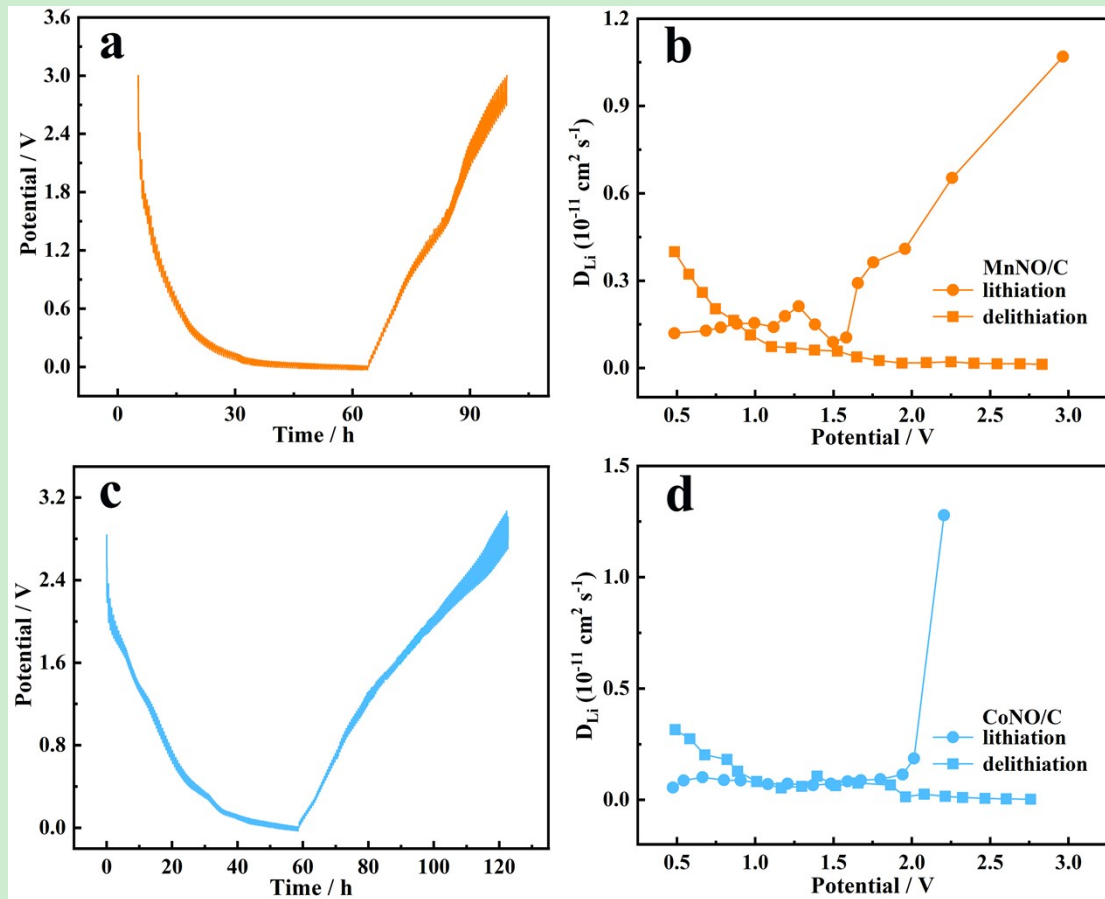


**Fig. S3.** *Ex situ* XRD patterns of CoNO/C after three cycles.

Table S1. Comparison on the  $\text{Li}^+$  diffusion coefficient of M-Nb-O-based anode materials in the reported [literature](#).

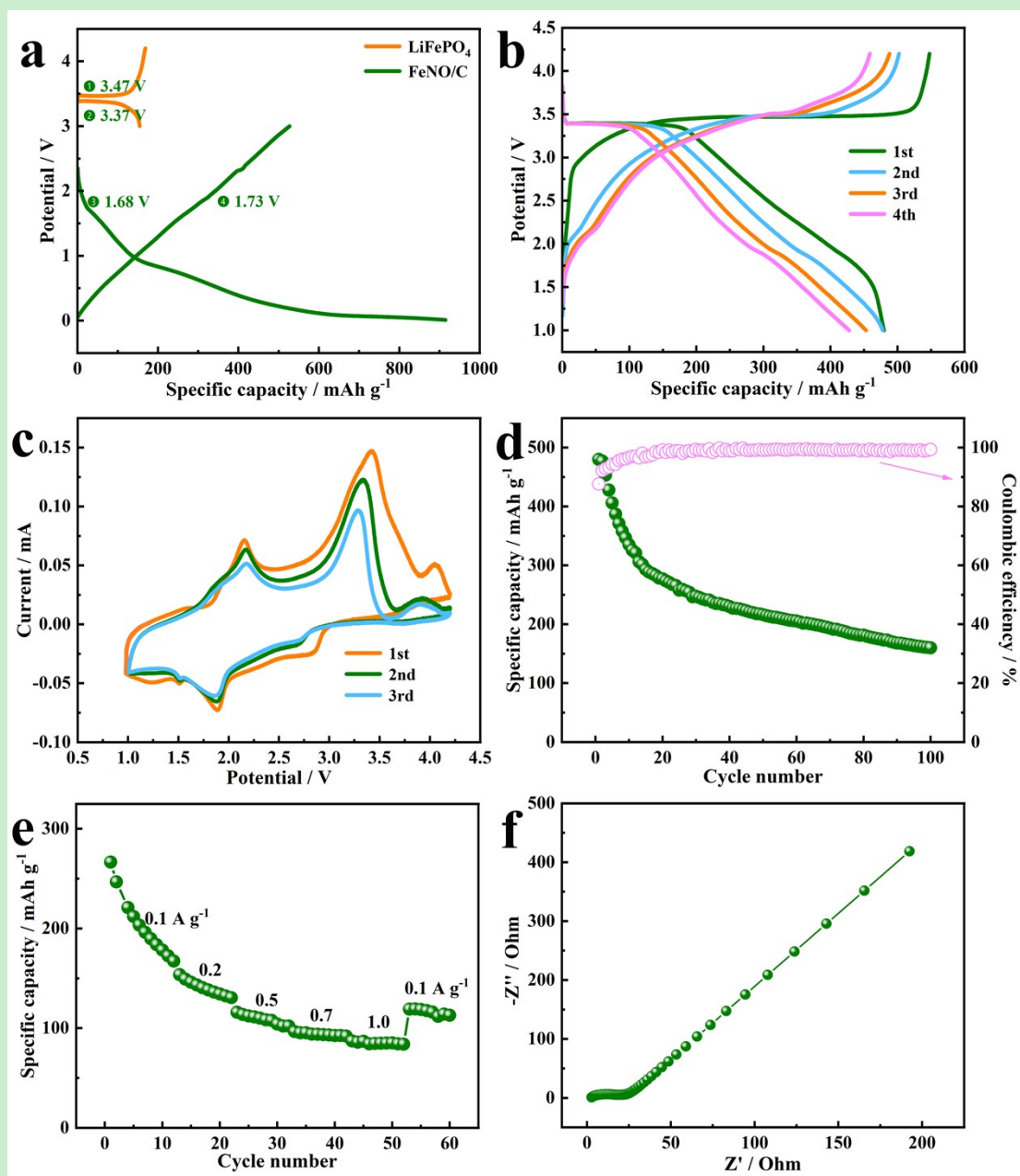
Materials	$D_{\text{Li}^+}(\text{cm}^2/\text{s}, \text{lithiation})$	$D_{\text{Li}^+}(\text{cm}^2/\text{s}, \text{delithiation})$	Test method	Ref
CrNb <sub>11</sub> O <sub>29</sub> nanorods	$1.51 \times 10^{-13}$	$3.57 \times 10^{-13}$	CV	[2]
TNO@C	$2.39 \times 10^{-12}$	$2.13 \times 10^{-12}$	CV	[3]
TiNb <sub>6</sub> O <sub>17</sub>	$1.33 \times 10^{-12}$	$1.59 \times 10^{-12}$	CV	[4]
N-doped TiNb <sub>24</sub> O <sub>62</sub> /C nanowires	$4.11 \times 10^{-12}$	$3.89 \times 10^{-12}$	CV	[5]
GaNb <sub>11</sub> O <sub>29</sub> @C	$4.30 \times 10^{-13}$	$3.67 \times 10^{-13}$	CV	[6]
BaNb <sub>3.6</sub> O <sub>10</sub> nanowires	$2.36 \times 10^{-12}$	$2.79 \times 10^{-12}$	CV	[7]
Mg <sub>2</sub> Nb <sub>34</sub> O <sub>87</sub>	$3.23 \times 10^{-13}$	$6.36 \times 10^{-13}$	CV	[8]
AlNb <sub>11</sub> O <sub>29</sub>	$1.12 \times 10^{-13}$	$2.39 \times 10^{-13}$	CV	[9]
Zn <sub>2</sub> Nb <sub>34</sub> O <sub>87</sub>				
AgNb <sub>13</sub> O <sub>33</sub>	$4.03 \times 10^{-12}$		CV	[10]
ZrNb <sub>14</sub> O <sub>37</sub> nanowire	$4.63 \times 10^{-14}$		CV	[11]
porous ZrNb <sub>24</sub> O <sub>62</sub> nanowires	$2.47 \times 10^{-13}$		EIS	[12]
CrNb <sub>49</sub> O <sub>124</sub> nanotube	$5.29 \times 10^{-13}$		EIS	[13]

N-doped TiNb <sub>2</sub> O <sub>7</sub> @C		$8.81 \times 10^{-18}$	EIS	[14]
TiNb <sub>2</sub> O <sub>7</sub> /C		$4.11 \times 10^{-12}$	EIS	[15]
Popcorn like Nb <sub>2</sub> O <sub>5</sub>		$1.68 \times 10^{-20}$	EIS	[16]
FeNb <sub>11</sub> O <sub>29</sub> nanotubes		$2.51 \times 10^{-12}$	EIS	[17]
Fe <sub>0.5</sub> Nb <sub>24.5</sub> O <sub>62-x</sub> @C nanowires		$4.03 \times 10^{-13}$	EIS	[18]
TiNb <sub>2</sub> O <sub>7</sub> @N–C		$6.07 \times 10^{-11}$	EIS	[19]
Cu <sub>2</sub> Nb <sub>34</sub> O <sub>87</sub>	$3.1 \times 10^{-13}$	$3.9 \times 10^{-13}$	GITT	[20]
Zn <sub>2</sub> Nb <sub>34</sub> O <sub>87</sub> nanofibers	$6.6 \times 10^{-12}$	$6.1 \times 10^{-12}$	GITT	[21]
V <sub>3</sub> Nb <sub>17</sub> O <sub>50</sub> submicron-sized rods	$2.75 \times 10^{-12}$	$2.63 \times 10^{-12}$	GITT	[22]
V <sup>5+</sup> -doped TiNb <sub>2</sub> O <sub>7</sub> microspheres	$\sim 4.1 \times 10^{-13}$	$\sim 5.5 \times 10^{-13}$	GITT	[23]
Microsized MoNb <sub>12</sub> O <sub>33</sub> particles	$2.9 \times 10^{-14}$	$4.8 \times 10^{-14}$	GITT	[24]
partially reduced TiNb <sub>24</sub> O <sub>62</sub>		$7.4 \times 10^{-12}$ (average)	GITT	[25]
BaNb <sub>3.6</sub> O <sub>10</sub>	$1.5 \times 10^{-12}$	$1.8 \times 10^{-12}$	GITT	[26]
Mg <sub>2</sub> Nb <sub>34</sub> O <sub>87</sub>		$5.0 \times 10^{-13}$ (average)	GITT	[27]
AlNb <sub>11</sub> O <sub>29</sub>		$1.22 \times 10^{-13}$ (average)	GITT	[28]
TiNb <sub>2</sub> O <sub>7</sub> /C	$1.41 \times 10^{-13}$	$1.52 \times 10^{-13}$	GITT	[29]
<b>FeNb<sub>2</sub>O<sub>6</sub>/C</b>	<b><math>1.4 \times 10^{-10}</math></b>	<b><math>6.3 \times 10^{-11}</math></b>	<b>GITT</b>	<b>This work</b>



**Fig. S4.** GITT curves (a, c) and varied  $D_{Li^+}$  (b, d) of MnNO/C and CoNO/C.

Similar to FeNO/C, the  $Li^+$  diffusion coefficient ( $D_{Li^+}$ ) of MnNO/C and CoNO/C was also calculated using a GITT test, and the equation for the diffusion coefficients have been described in the main text. As shown in Fig. S4, during the lithiation process, the  $D_{Li^+}$  value of MnNO/C, and CoNO/C ranged from  $1.1 \times 10^{-11}$  to  $1.2 \times 10^{-12}$  and  $1.3 \times 10^{-11}$  to  $5.5 \times 10^{-13} \text{ cm}^2 \text{ s}^{-1}$ , with an average  $D_{Li^+}$  of  $2.7 \times 10^{-12}$  and  $1.7 \times 10^{-12} \text{ cm}^2 \text{ s}^{-1}$ , respectively. And the value during the delithiation process varied in the ranges of  $4.0 \times 10^{-12}$  to  $1.3 \times 10^{-13}$  and  $3.2 \times 10^{-12}$  to  $4.2 \times 10^{-14} \text{ cm}^2 \text{ s}^{-1}$ , with an average  $D_{Li^+}$  of  $1.0 \times 10^{-12}$  and  $8.9 \times 10^{-13} \text{ cm}^2 \text{ s}^{-1}$ , respectively.

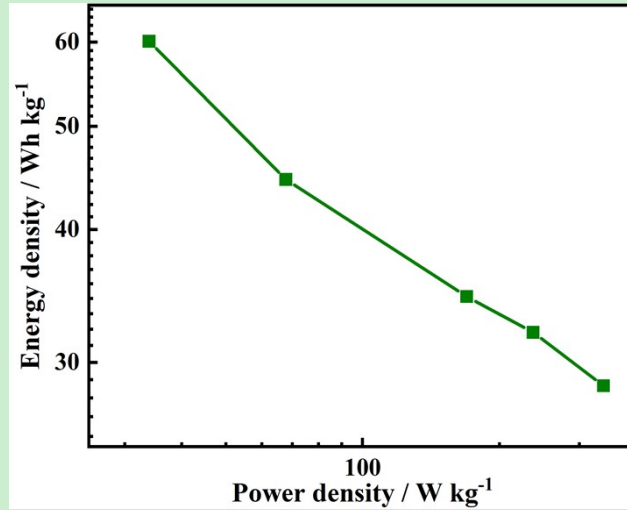


**Fig. S5.** Electrochemical properties of  $\text{LiFePO}_4\|\text{FeNO/C}$  full battery: initial GCD curves of  $\text{FeNO/C}\|\text{Li}$  and  $\text{LiFePO}_4\|\text{Li}$  half batteries at  $0.1 \text{ A g}^{-1}$  (a), GCD curves of the full battery at  $0.1 \text{ A g}^{-1}$  (b), CV curves (c), cyclic performance (d), rate performance (e), and EIS (f).

The excellent cycling performance, favorable rate performance, and competitive diffusion kinetics of  $\text{FeNO/C}$  hybrid nanosheets have inspired the exploration in the field of full batteries, whose capacity can be calculated on the basis of the mass of the cathode active materials. The assembly of the half and full batteries have been described



in the experimental characterization section. As shown in Fig. S5a, the GCD curves of commercial  $\text{LiFePO}_4$  cathode (orange) shows plateaus at 3.47 and 3.37 V, relate to the redox of  $\text{Fe}^{2+}$  and  $\text{Fe}^{3+}$ , and the plateaus appeared at 1.68 and 1.73 V for  $\text{FeNO/C}$  anode (green) can be ascribed to the valence change of  $\text{Nb}^{5+}/\text{Nb}^{4+}$  pair. Correspondingly, the specific capacity of  $\text{LiFePO}_4$  cathode is  $154.6 \text{ mAh g}^{-1}$  at  $0.1 \text{ A g}^{-1}$  for the initial cycle, while  $\text{FeNO/C}$  reaches  $914.5 \text{ mAh g}^{-1}$ . Fig. S5b shows the GCD curves of the full battery for the initial four cycles, which reveals an initial charge/discharge specific capacity of 547.6 and  $479.7 \text{ mAh g}^{-1}$ , respectively, with a coulombic efficiency of 87.6%, and the capacity loss can be attributed to the formation of SEI film and occurrence of irreversible reactions. During the following three cycles, the battery illustrates a charge/discharge capacity of 502.2/477.9, 488/453, and 458.8/ 427.9  $\text{mAh g}^{-1}$ , respectively. In order to further investigate the electrochemical performance of  $\text{LiFePO}_4\|\text{FeNO/C}$  full battery, CV test (Fig. S5c) was conducted at  $0.1 \text{ mV s}^{-1}$ . Similar to the plateaus appeared in the half cells (Fig. S5a), the redox peaks at 3.43 and 2.86 V can be attributed to the (de)intercalation of  $\text{Li}^+$  in  $\text{LiFePO}_4$ , and the peaks around 2.15 and 1.88 V are related to the redox reaction in  $\text{FeNb}_2\text{O}_6$ . Cyclic performance (Fig. S5d) of the full battery shows that the discharge specific capacity presents a gradual decrease trend during cycling, which was caused by the continuous deposition of  $\text{Li}^+$ , leading to a decrease in the lithium metal available for reuse [30], and the discharge specific capacity of the full battery is maintained at  $160 \text{ mAh g}^{-1}$  with an average Coulombic efficiency of 98.4% after 100 cycles. The rate capability (Fig. S5e) shows that the battery displays a specific capacity of 203.3, 146.1, 112.2, 95.3 and  $86.7 \text{ mAh g}^{-1}$  at 0.1, 0.2, 0.5, 0.7 and  $1 \text{ A g}^{-1}$ , respectively, and basically return to the initial level after cycling at  $1 \text{ A g}^{-1}$ , demonstrate its favorable structural stability. EIS analysis (Fig. S5f) reveals a lower charge transfer resistance ( $R_{ct} = 14.1 \Omega$ ), and large slope in the high-frequency region indicate that the battery has a low resistance and fast lithium ion diffusion rate.



**Fig. S6.** Ragone plot of the LiFePO<sub>4</sub>//FeNO/C full battery.

Finally, the relationship between the energy density and power density of the LiFePO<sub>4</sub>//FeNO/C full battery can be calculated from the Rangone curve (Fig. S6), which shows that the energy density of the full battery decreases with the increase of the power density, and the power and energy densities are 33.9 W kg<sup>-1</sup> and 60.1 Wh kg<sup>-1</sup> at 0.1 A g<sup>-1</sup>, respectively.

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