

Supporting Information

Organo-Interhalogen Chemistry Enables High-Voltage Bromine Redox for Stable Zinc Batteries

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Experimental section

Preparation of aqueous electrolytes: 2 M (mol L⁻¹) ZnSO₄ solution (ZS) was prepared by adding 0.323 g ZnSO₄ to 1 mL of deionized water and stirring for 1 h at room temperature. Then, 0.2 M ZnCl₂ and 0.4 M CA were added to the as-prepared ZS solutions, respectively, and stirred for 2~4 h at room temperature to obtain ZC electrolytes and CA electrolytes. Similarly, other additives (e.g., CP, CIACE, MCA, and CAN) were also introduced into electrolytes at 0.4 M concentration for comparative investigations.

Fabrication of TBABr₃ electrode: TBABr₃, KB, and polyvinylidene fluoride (PVDF) with a ratio of 6:3:1 in methyl-2-pyrrolidinone (NMP) solvent were mixed to form a homogeneous slurry. Subsequently, this slurry was evenly coated onto carbon fiber cloth (CFC), then drying at 45 °C for 12 h. The effective mass loading of active bromine is controlled around 1.0-2.0 mg cm⁻².

Preparation of Br₃⁻ and Br⁺: Br₃⁻ solution was prepared by the reaction between NaBrO₃ and HBr¹: $\text{NaBrO}_3 + 8\text{Br}^- + 6\text{H}^+ \rightarrow 3\text{Br}_3^- + 3\text{H}_2\text{O}$. BrCl₂⁻ solution was prepared through a method reported as follows²: $\text{Cl}_2 + \text{Br}^- \rightarrow \text{BrCl}_2^-$.

Electrochemical measurements: Electrochemical tests were conducted using CR2032 coin cells assembled in ambient environment with a cut-off voltage of 0.5-2.15 V. For the coin cell assembly, 120 μL ZS with different additives were used as the electrolytes, Zn foil with 0.1 mm thickness was used as the anode, TBABr₃ electrode was used as the cathodes, and glass fiber membrane (Whatman) was used as the separators. The mass loading of cathode active material is controlled to *ca.* 2 mg cm⁻². The galvanostatic charge-discharge were performed on the Neware electrochemical test system (CT-4008-10V 50mA-164, Shenzhen, China). The CV, LSV curves, and EIS plots were tested on a Gamry electrochemical workstation, and the frequency of EIS ranged from 100 kHz to 0.1 Hz.

Characterization methods: UV-vis spectra were collected using a Shimadzu UV-visible near-infrared spectrophotometer. Infrared spectra were recorded on an FT-IR spectrometer (Nicolet iS50R, Thermo Scientific). Raman spectra (HORIBA, LabRAM HR800) of the samples were measured at room temperature with laser excitation at 532 nm. Sample morphology was observed using a scanning electron microscope (SEM, Hitachi S-3400 N). Surface roughness of the resultant samples was characterized using laser scanning confocal microscopy (LSCM). The ^1H and ^{13}C NMR spectra were recorded by a Bruker AVANCE III 500 MHz Superconducting Fourier using CDCl_3 as the solvent and trimethylsilane (TMS) as the standard internal substance. For ex-situ ^1H and ^{13}C NMR spectra tests, the cathodes with different states of charge (SOC) were soaked in 0.6 mL CDCl_3 for 30 min filtered to obtain a clear solution, and then transferred to the NMR tube for analysis. XRD analysis was used to determine the phase structures of the anode samples using a Rigaku instrument ($\text{Cu K}\alpha$, $\lambda = 1.5418 \text{ \AA}$). The chemical states of the electrodes after tests were determined by XPS (Thermo Fisher-Escalab 250Xi), and binding energies were calibrated using carbon (284.8 eV for C 1s). The mass spectrum was conducted on Thermo Fisher Scientific LTQ-Orbitrap XL by electrospray ionization to qualitatively determine the charging product of interhalogen. The in-situ hydrogen fluxes are detected by the airtight battery system equipped with gas chromatography-mass spectrometry. In the battery-gas chromatography quantitative analysis measurement, the airtight battery system is connected to gas chromatography (Agilent GC-2014).

Calculation of the activation energy: The activation energy can be calculated by the Arrhenius equation:

$$\frac{1}{R_{ct}} = A \exp\left(-\frac{E_a}{RT}\right)$$

where R_{ct} is the interfacial resistance, A is the frequency factor, R is the gas constant, and T is the absolute temperature.

Theoretical computations: All the DFT calculations were carried out in the DMol³ package of Materials Studio. The exchange-correlation energy was computed using generalized gradient approximation (GGA) with the Perdew-Burke-Ernzerhof (PBE).³ Grimme's DFT-D2 model was also used to take into account Van der Waals interactions.⁴ The core electrons were treated with DFT semi-core pseudopotentials. The simulation was conducted with a global orbital cutoff of 5.0 Å and a Fermi smearing of 0.005 Ha (1 Ha= 27.211 eV). The criteria for convergence in geometric optimization and energy calculation were defined with an energy tolerance of 1.0×10⁻⁵ Ha/atom, a self-consistent field tolerance of 1.0×10⁻⁶ Ha/atom, a maximum force tolerance of 0.002 Ha/Å, and a maximum displacement tolerance of 0.005 Å. The Gibbs free energy of reaction ($\Delta G_{\text{reaction}}$) is typically calculated by determining the free energy of the reactants and products. The formula for the reaction free energy is:

$$\Delta G_{\text{reaction}} = \sum G_{\text{products}} - \sum G_{\text{reactants}}$$

Where $\sum G_{\text{products}}$ stands for the free energy of the products and $\sum G_{\text{reactants}}$ stands for the free energy of the reactants.

Calculation of energy density and power density: The energy density (E) delivered by the battery can be calculated by integrating the voltage (V) over the specific capacity (Q):

$$\text{Energy density } (E) = \frac{\int_{\text{initial}}^{\text{final}} V(Q) dQ}{m}$$

where, $V(Q)$ is the voltage as a function of capacity; Q_{initial} and Q_{final} are the start and end points of the discharge curve; m is the mass of the bromine active material.

The power density (P) delivered by the battery can be calculated using the energy density (E) and discharge time (t):

$$\text{Power density } (P) = \frac{E}{t}$$

where, E is the energy density and t is the discharge time.

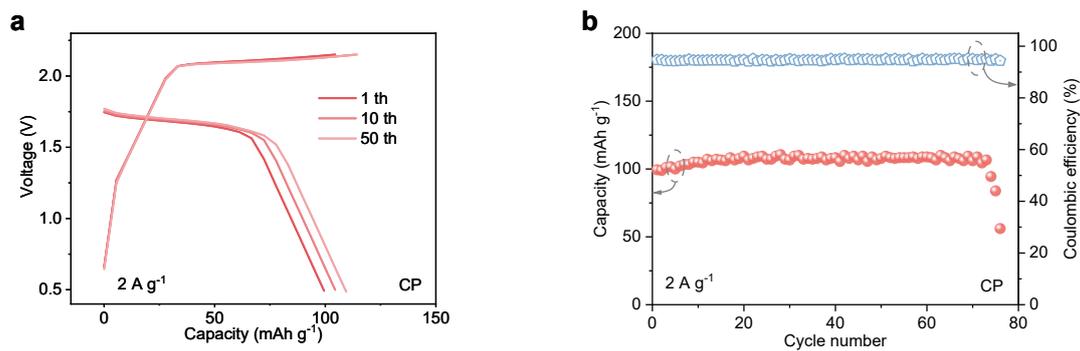


Fig. S1. (a) GCD curves and (b) long-term cycling performance of Zn||TBABr₃ batteries with CP electrolyte at 2 A g⁻¹.

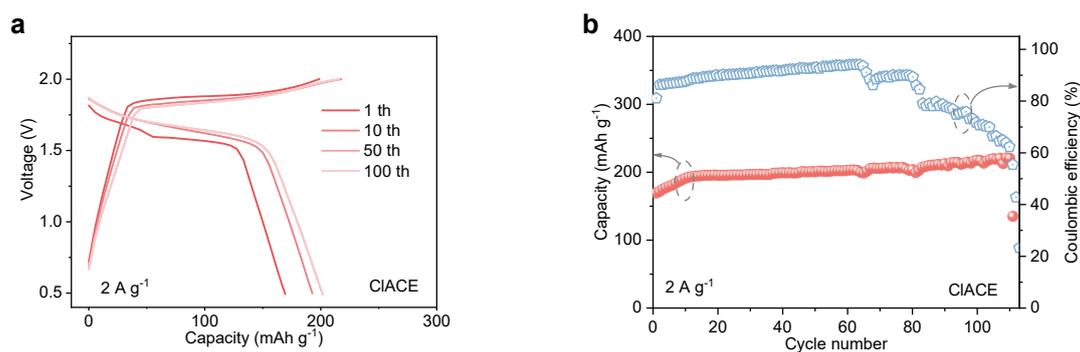


Fig. S2. (a) GCD curves and (b) long-term cycling performance of Zn||TBABr₃ batteries with CIACE electrolyte at 2 A g⁻¹.

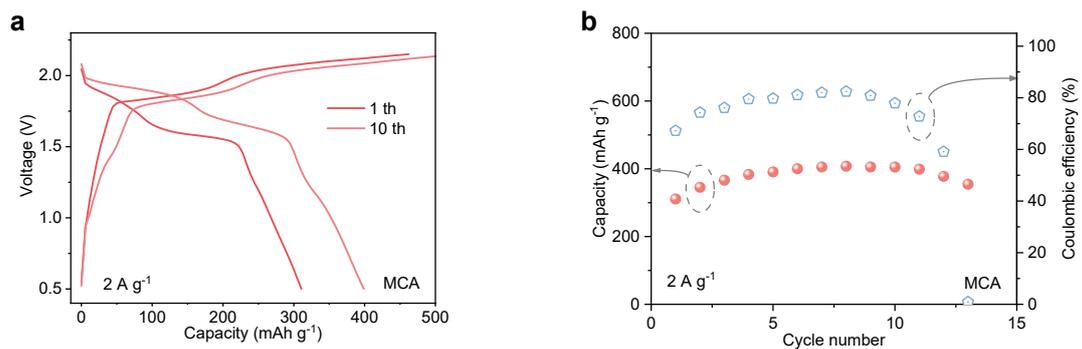


Fig. S3. (a) GCD curves and (b) long-term cycling performance of Zn||TBABr₃ batteries with MCA electrolyte at 2 A g⁻¹.

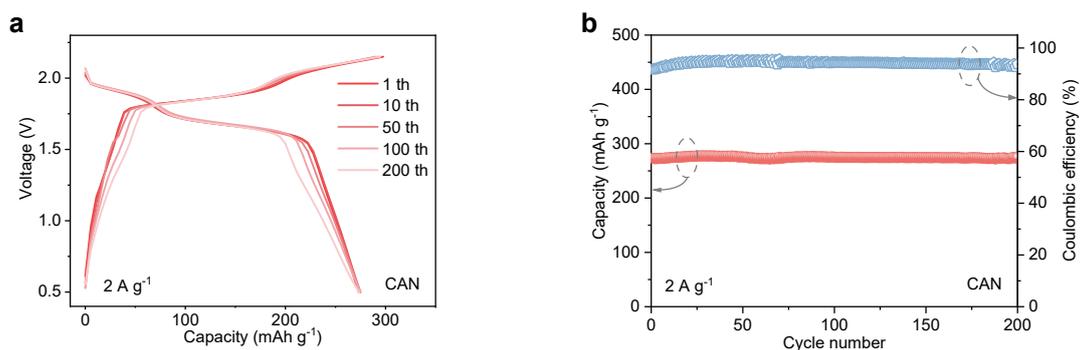


Fig. S4. (a) GCD curves and (b) long-term cycling performance of Zn||TBABr₃ batteries with CAN electrolyte at 2 A g⁻¹.

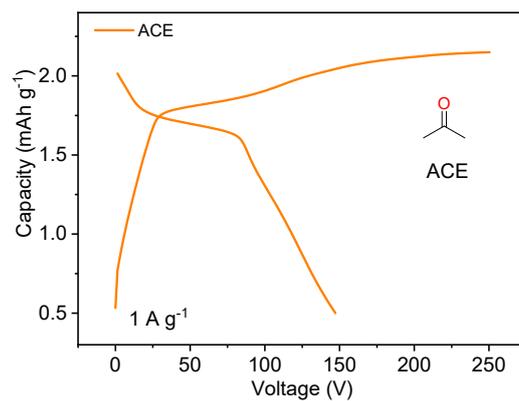


Fig. S5. GCD curves of Zn || TBABr₃ batteries with ACE electrolyte at 1 A g⁻¹.

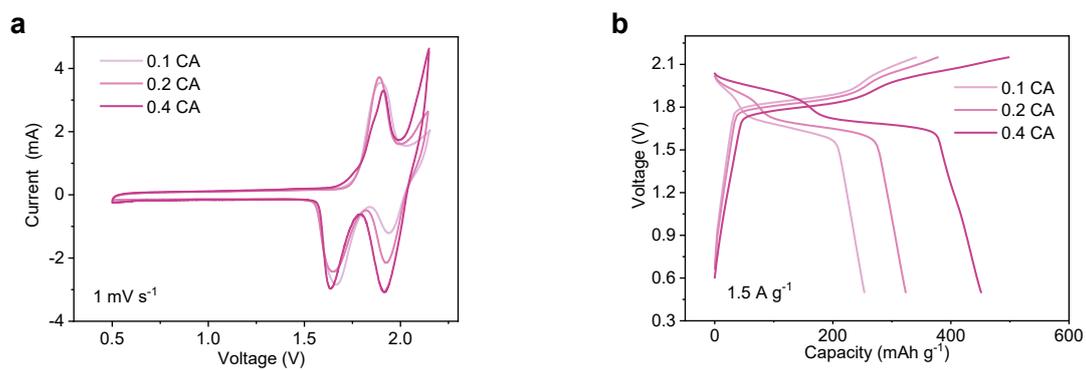


Fig. S6. (a) CV of Zn || TBABr₃ batteries in electrolytes with different CA concentrations at 1 mV s⁻¹ and (b) GCD curves at 1.5 A g⁻¹.

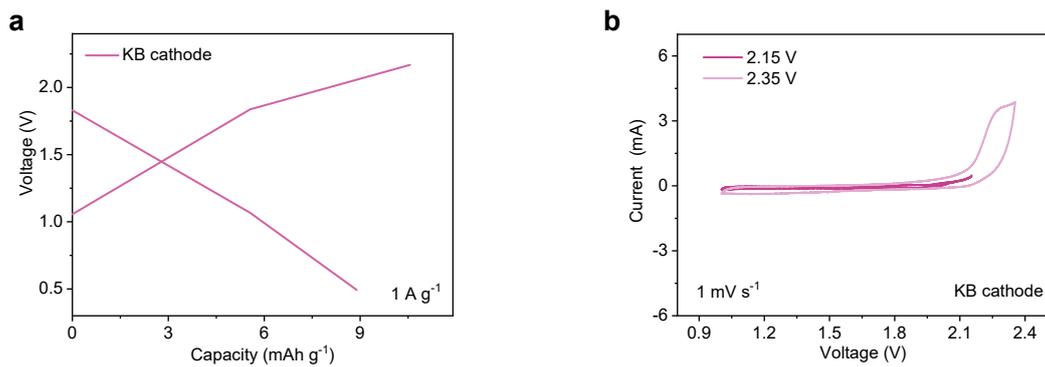


Fig. S7. (a) GCD curves of the Zn||KB battery in CA electrolyte. (b) CV curves of the Zn||KB battery in CA electrolyte at the upper voltage limits of 2.15 V and 2.35 V.

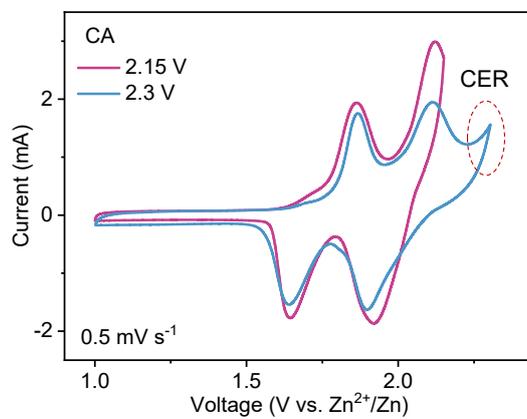


Fig. S8. CV of Zn||TBABr₃ batteries with CA electrolyte with different voltage ranges.

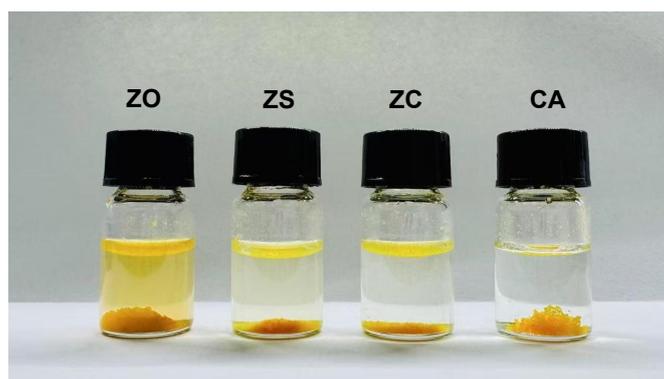


Fig. S9. Photographs of TBABr_3 in four electrolytes: ZO, ZS, ZC, and CA electrolytes; 2 M $\text{Zn}(\text{OTf})_2$ was denoted as ZO.

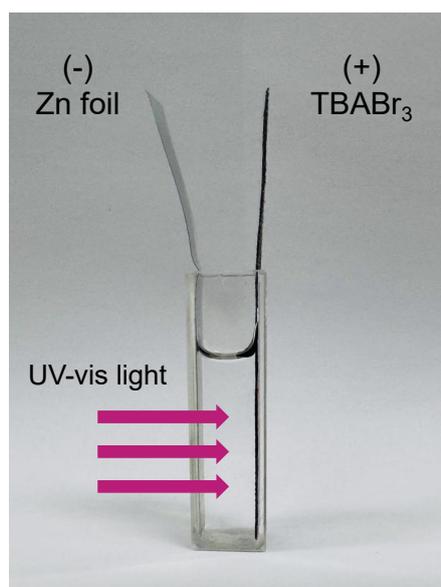


Fig. S10. The cuvette cell for in situ UV-Vis spectral characterization.

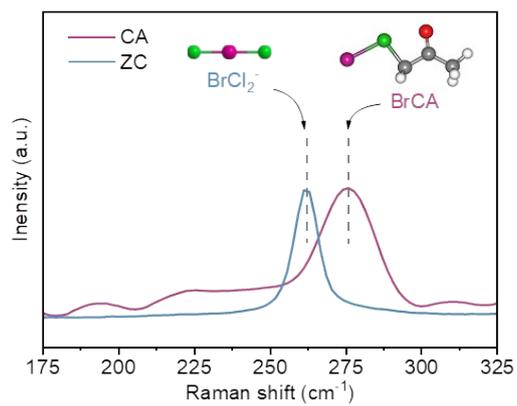


Fig. S11. Raman spectra of the battery cathodes charged to 2.15 V using CA and ZC electrolytes.

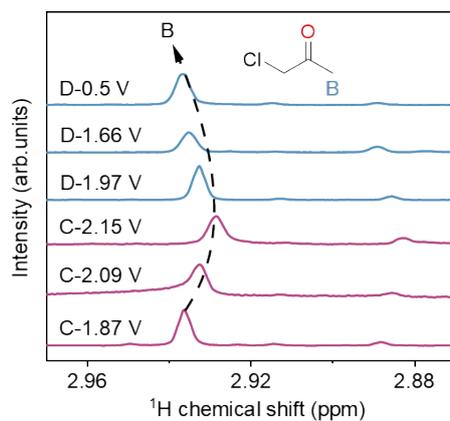


Fig. S12. *Ex-situ* ^1H NMR spectra of cathode during GCD with CA.

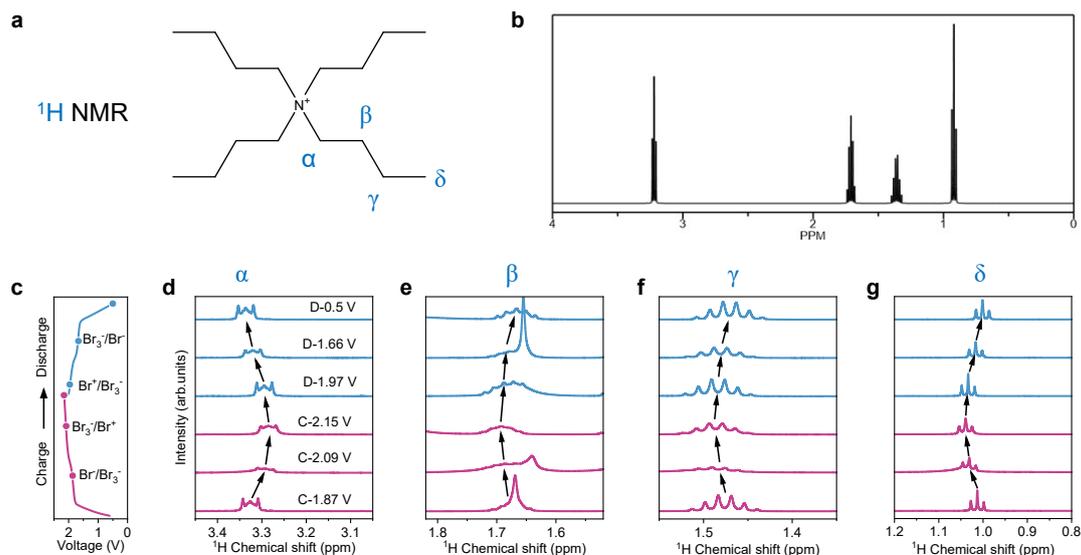


Fig. S13. (a) Molecular structures and (b) ^1H NMR spectrum of TBA^+ . (c) GCD curves of $\text{Zn}||\text{TBABr}_3$ battery with CA electrolyte. (d-g) ^1H NMR spectra of TBA^+ at different states of charge: (d) peak α , (e) peak β , (f) peak γ , (g) peak δ .

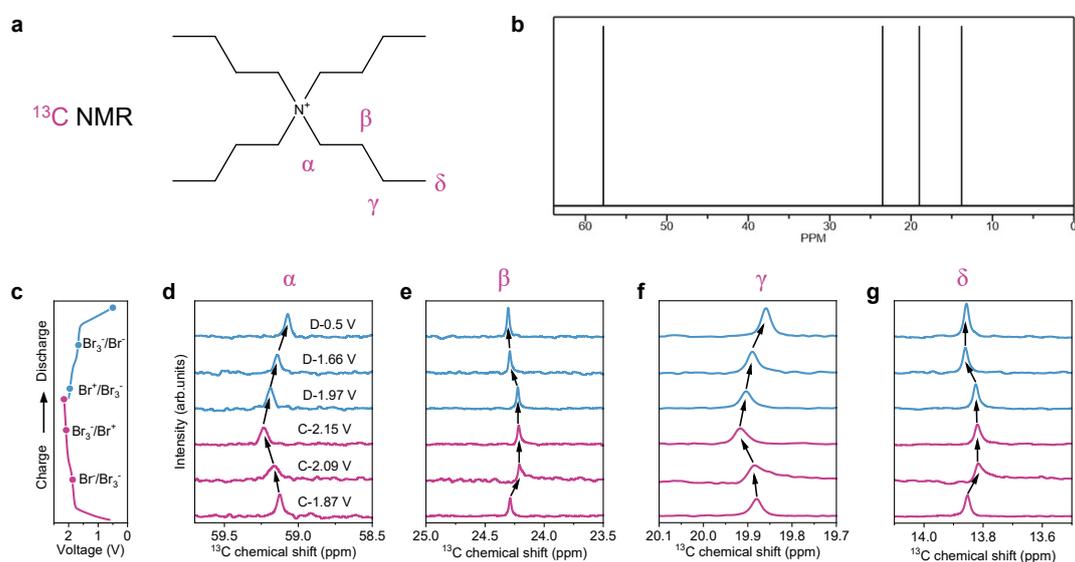


Fig. S14. (a) Molecular structures and (b) ^{13}C NMR spectrum of TBA^+ . (c) GCD curves of $\text{Zn}||\text{TBABr}_3$ battery with CA electrolyte. (d-g) ^{13}C NMR spectra of TBA^+ at different states of charge: (d) peak α , (e) peak β , (f) peak γ , (g) peak δ .

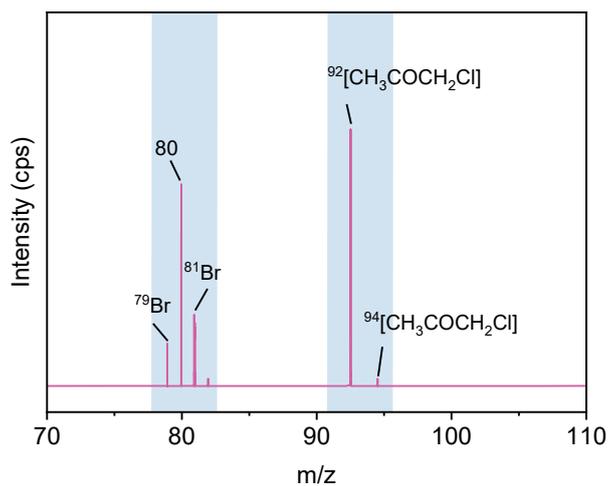


Fig. S15. Mass spectrum of cathodes at of charge to 2.15 V in CA electrolyte.

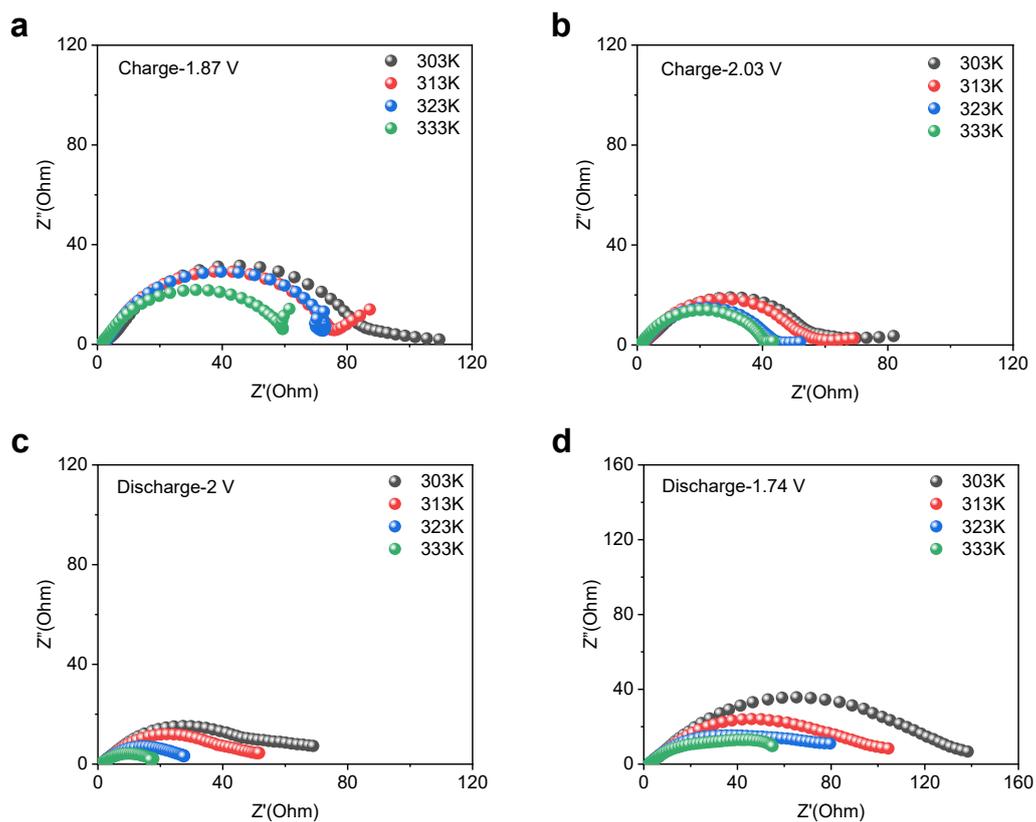


Fig. S16. EIS spectra of Zn||TBABr₃ batteries with ZC electrolytes at different temperatures and charged/discharged states.

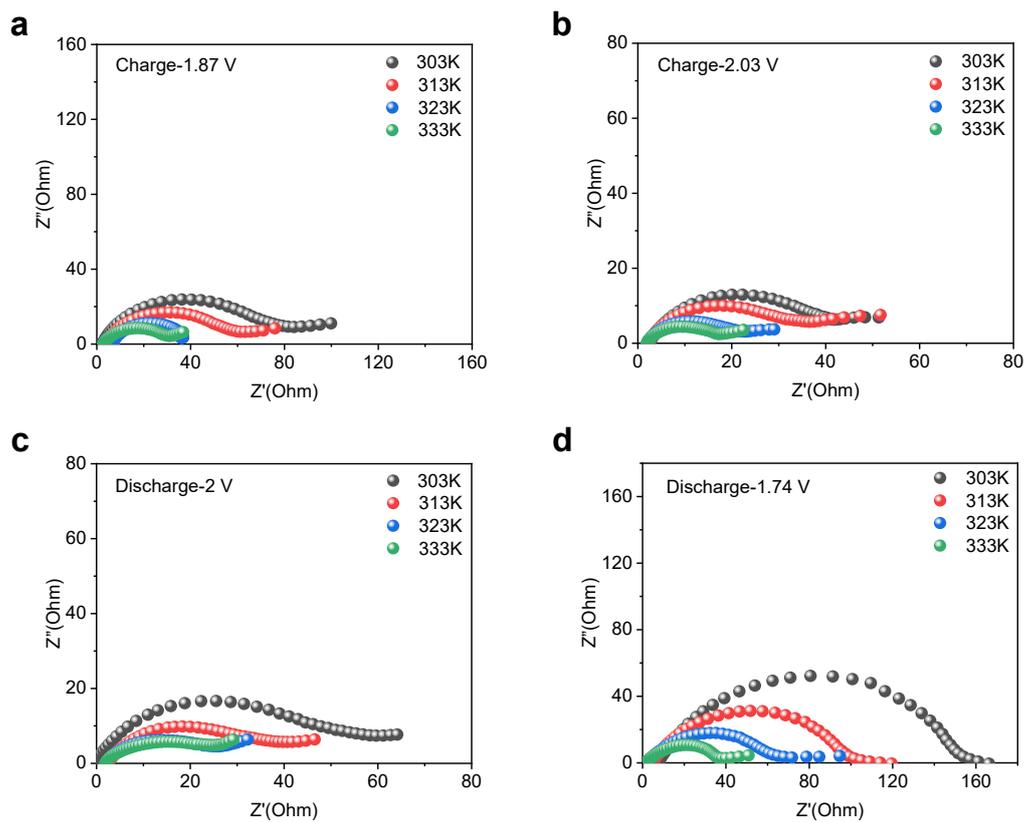


Fig. S17. EIS spectra of Zn||TBABr₃ batteries with CA electrolytes at different temperatures and charged/discharged states.

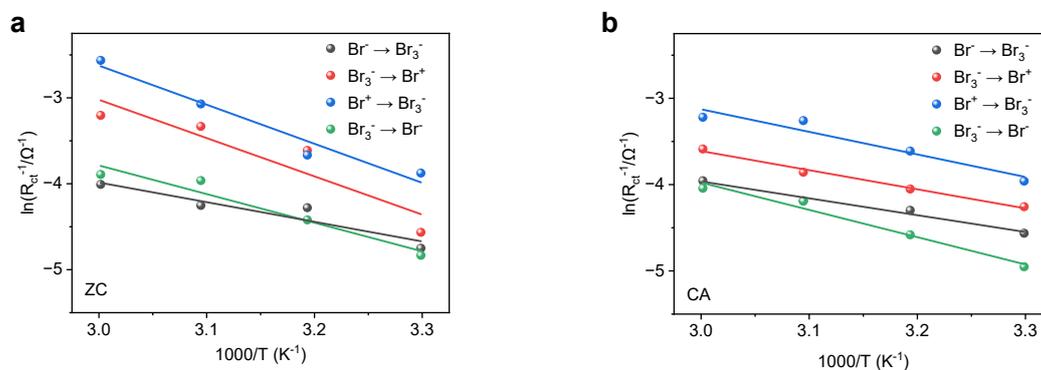


Fig. S18. Arrhenius plots of Zn||TBABr₃ batteries with (a) ZC and (b) CA electrolytes at different temperatures and charged/discharged states.

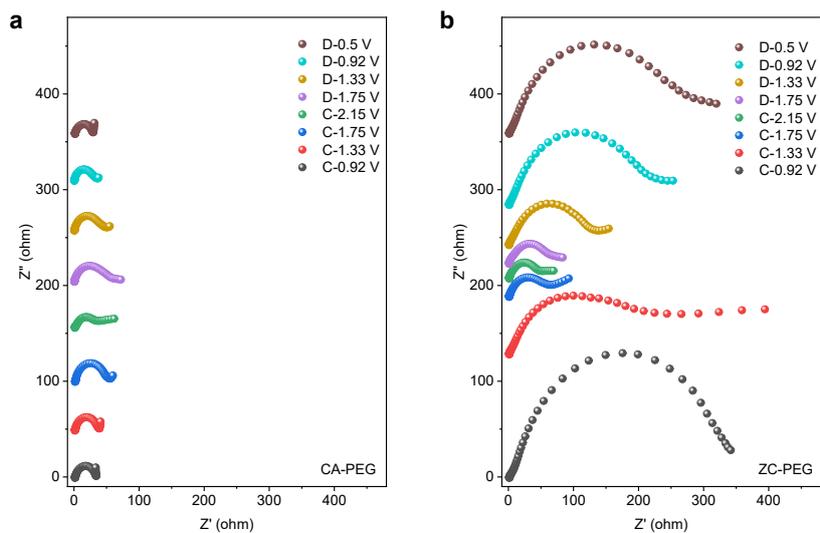


Fig. S19. Nyquist plots for Zn||TBABr₃ batteries using (a) CA-PEG and (b) ZC-PEG electrolytes obtained by in-situ EIS tests.

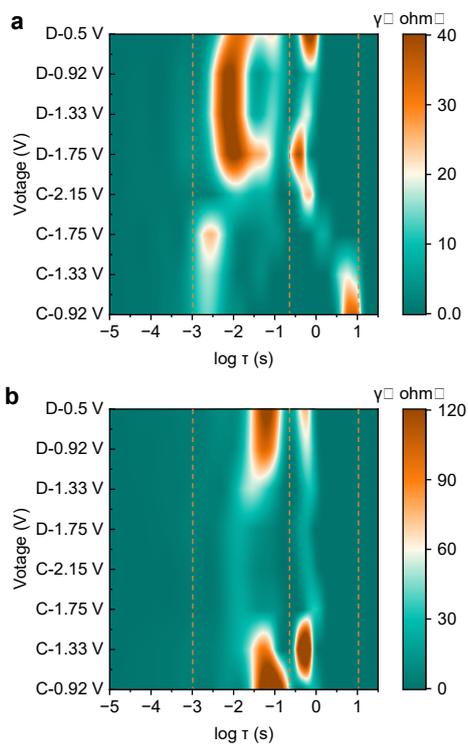


Fig. S20. DRT plots for Zn||TBABr₃ batteries with (a) CA-PEG and (b) ZC-PEG electrolytes at different potentials.

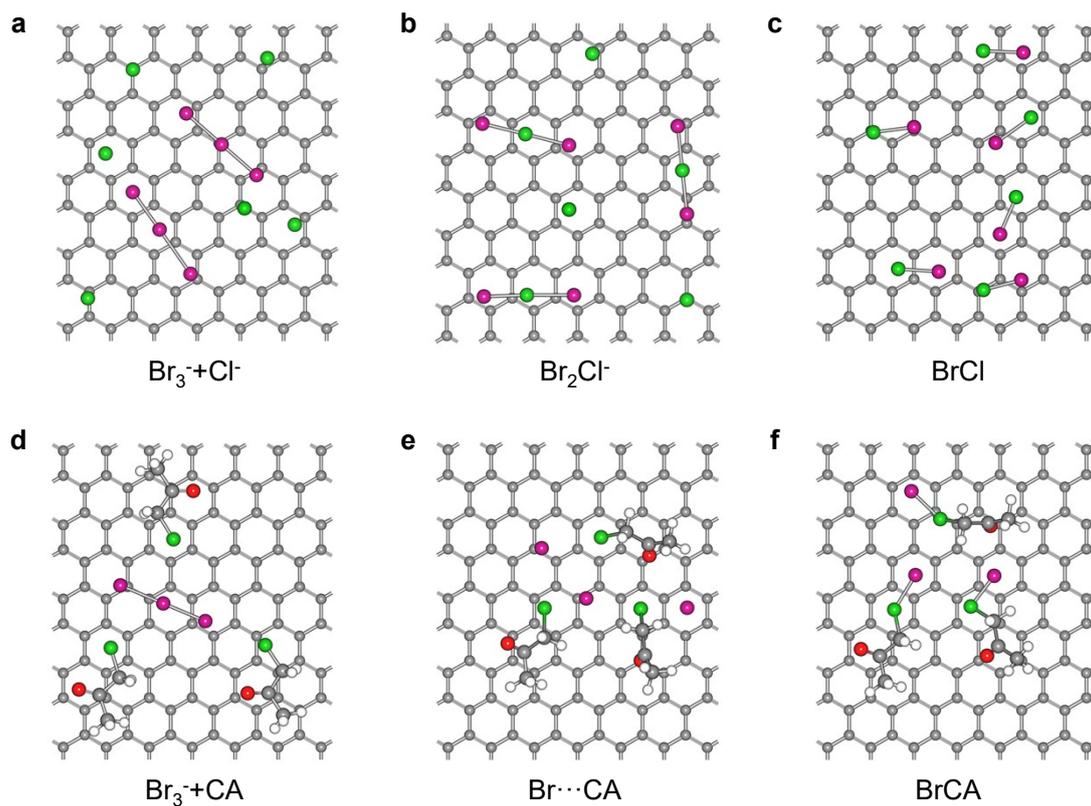


Fig. S21. The Gibbs free energy model for the structures of key species involved in CA- and ZnCl_2 -mediated $\text{Br}_3^-/\text{Br}^+$ redox.

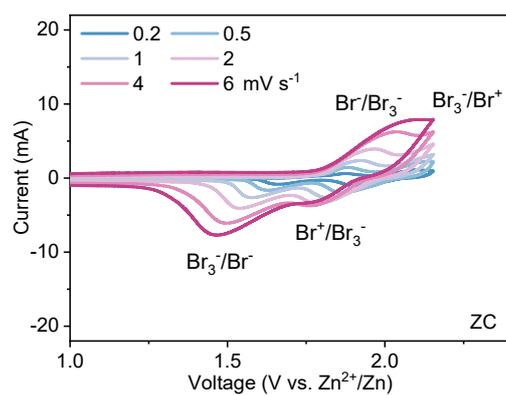


Fig. S22. CV curves of $\text{Zn} | \text{TBABr}_3$ batteries with ZC electrolytes at scan rates of 0.2-6 mV s^{-1} .

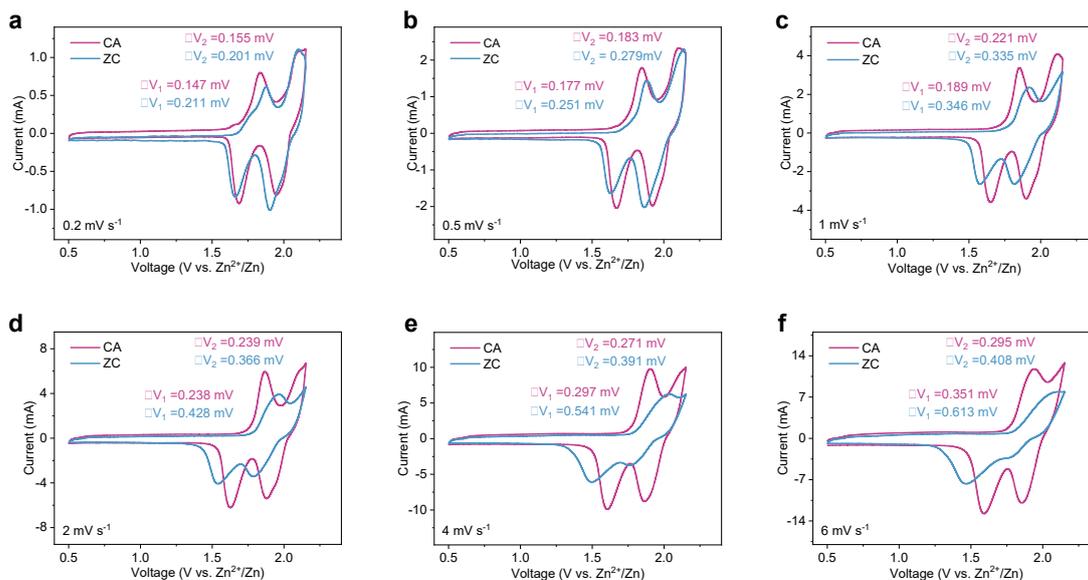


Fig. S23. (a-f) Comparison of CV curves of Zn||TBABr₃ batteries with ZC and CA electrolytes at different scan rates; ΔV_1 and ΔV_2 respectively represent the voltage difference between the oxidation peak and the reduction peak of Br⁻/Br₃⁻ and Br₃⁻/Br⁺.

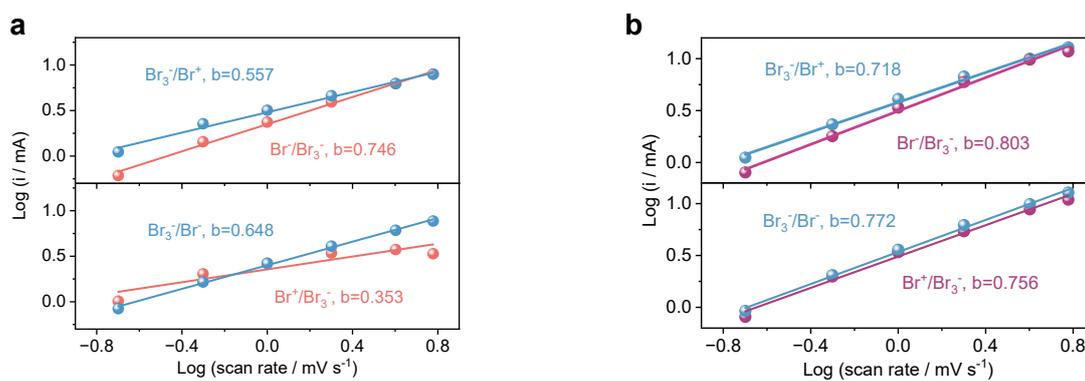


Fig. S24. Logi versus logv plots of the current response with ZC and CA electrolytes.

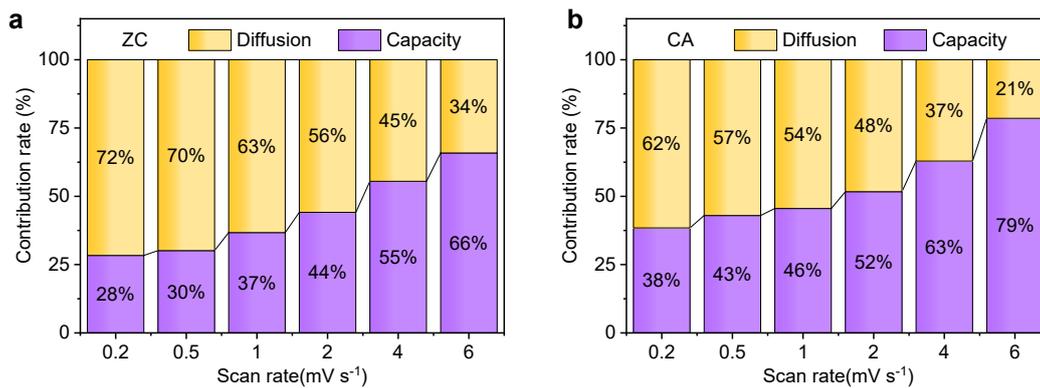


Fig. S25. Diffusion-controlled and capacitive contributions of Zn || TBABr₃ batteries at different scan rates: (a) with ZC electrolyte; (b) with CA electrolyte.

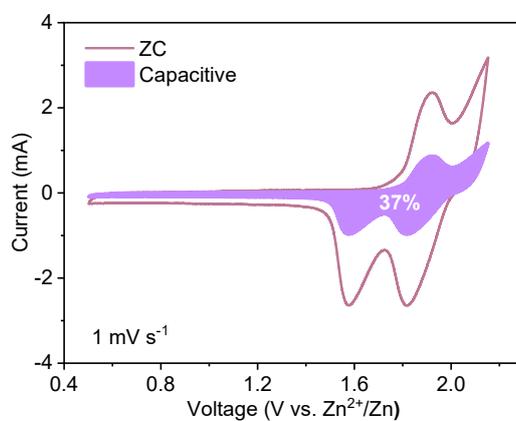


Fig. S26. CV curves and corresponding capacitive contribution (37%, shaded part) of Zn || TBABr₃ batteries with ZC electrolyte at 1 mV s⁻¹.

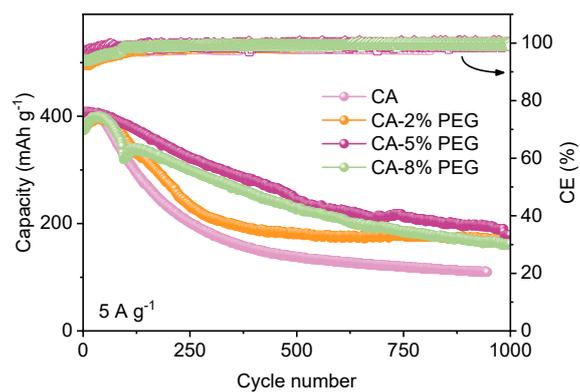


Fig. S27. Cycling stability of Zn|TBABr₃ batteries in CA electrolyte with different PEG 200 concentrations at current densities of 5 A g⁻¹.

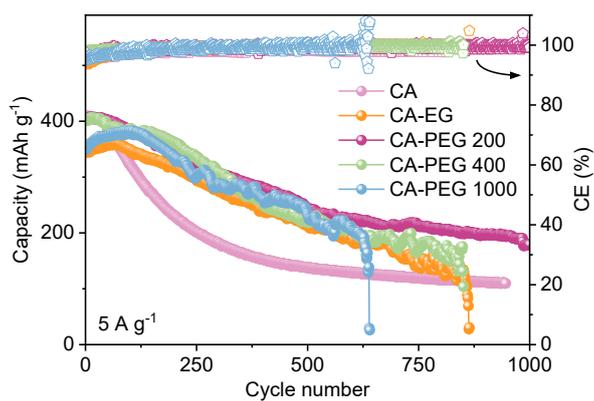


Fig. S28. Cycling stability of Zn|TBABr₃ batteries in CA electrolytes with 5 wt% EG and PEG with different molecular weights (200, 400, and 1000 g mol⁻¹) at current densities of 5 A g⁻¹.

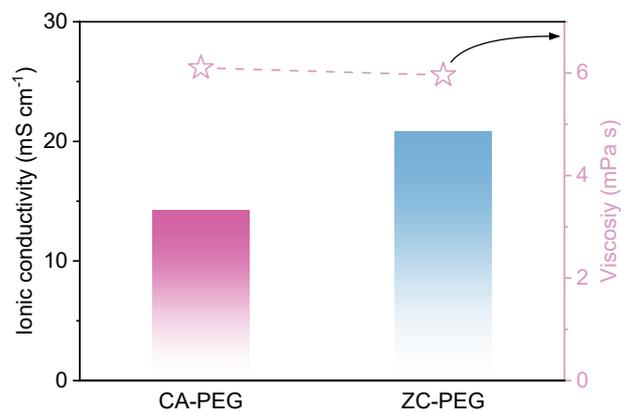


Fig. S29. The ionic conductivity and viscosity of the CA-PEG and ZC-PEG electrolytes.

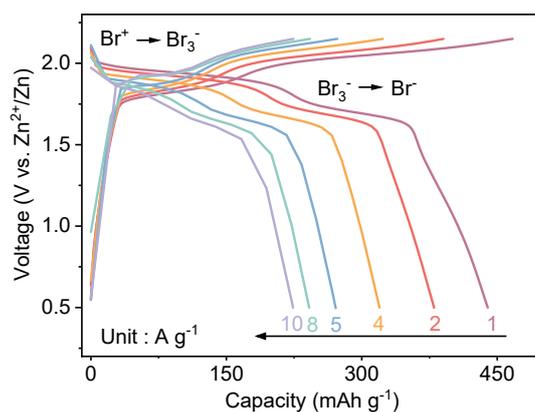


Fig. S30. GCD curves in ZC-PEG electrolytes at current densities of 1, 2, 4, 5, 8, and 10 A g⁻¹.

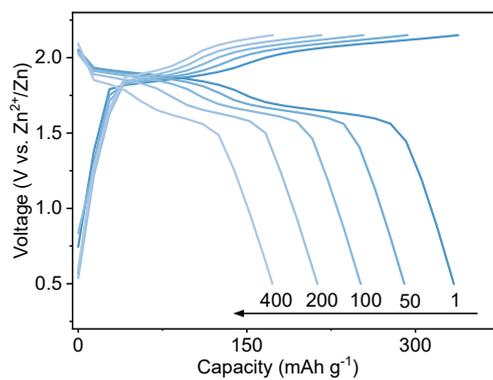


Fig. S31. The GCD curves in ZC-PEG electrolytes at 5 A g⁻¹.

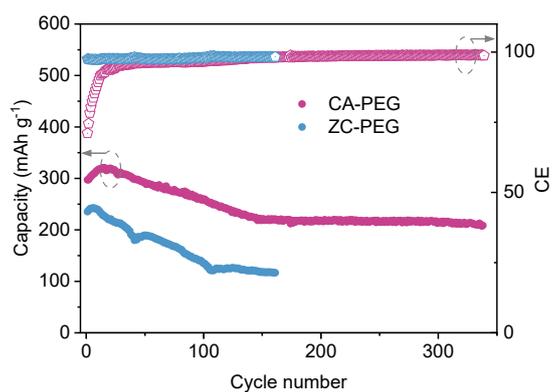


Fig. S32 Cycling performance of full batteries at current densities of 10 A g⁻¹ in CA-PEG and ZC-PEG electrolytes.

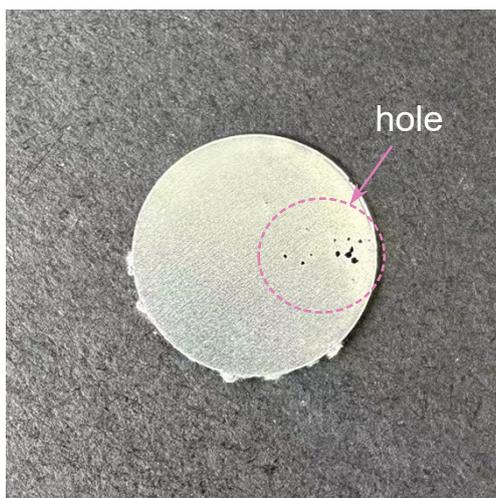


Fig. S33. Photographs of the perforation on the reverse side of the Zn anode after cycling of the Zn || TBABr₃ battery using ZC-PEG electrolyte.

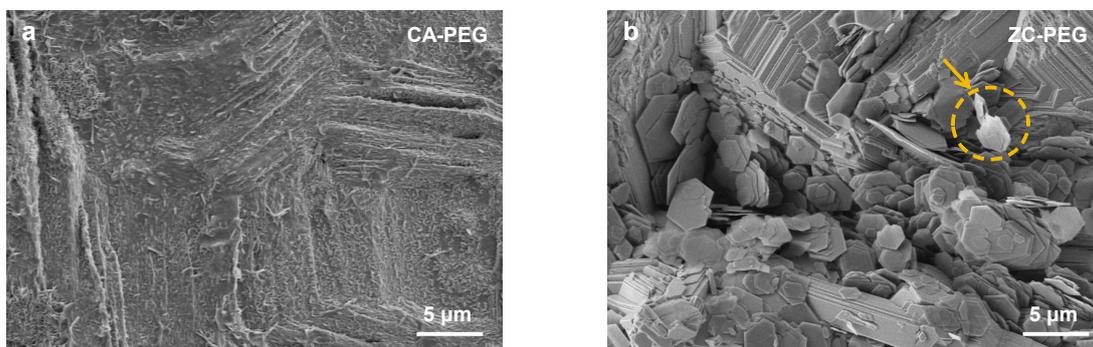


Fig. S34. SEM images of Zn anodes cycled in Zn || Zn symmetric cells at 5 mA h cm⁻², 1 mA cm⁻² after 250 cycles with different electrolytes: (a) ZC-PEG and (b) CA-PEG.

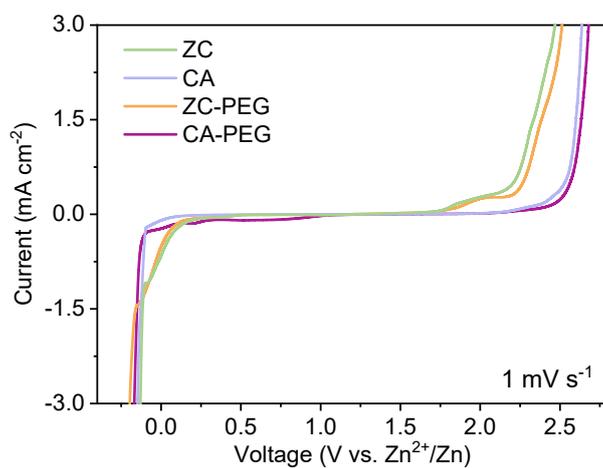


Fig. S35. LSV profiles in ZC-PEG and CA-PEG electrolytes at 1 mV s^{-1} .

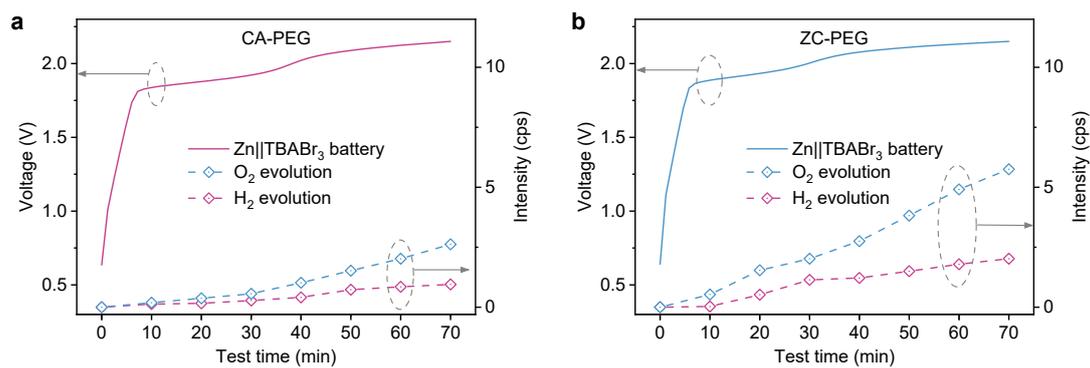


Fig. S36. O_2 and H_2 evolution during the cycling process of $\text{Zn}||\text{TBABr}_3$ batteries using a) CA-PEG and b) ZC-PEG electrolytes was investigated by GC-MS.

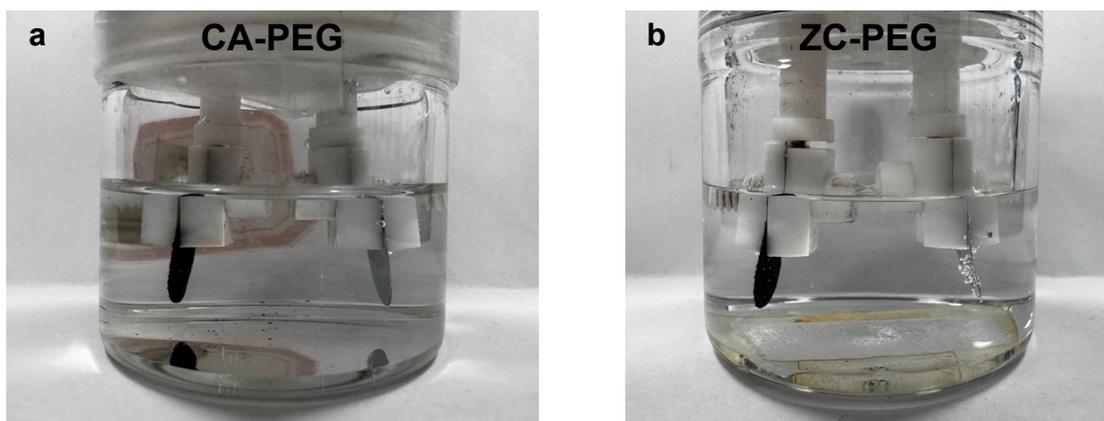


Fig. S37. Optical photos of the beaker batteries used for GC-MS tests after cyclic testing in a) CA-PEG and b) ZC-PEG.

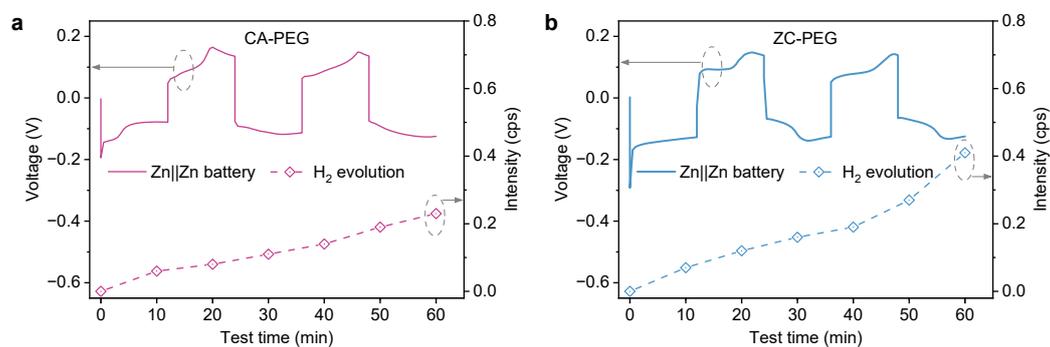


Fig. S38. H₂ evolution during the cycling process of Zn||Zn batteries using a) CA-PEG and b) ZC-PEG electrolytes was investigated by GC-MS.

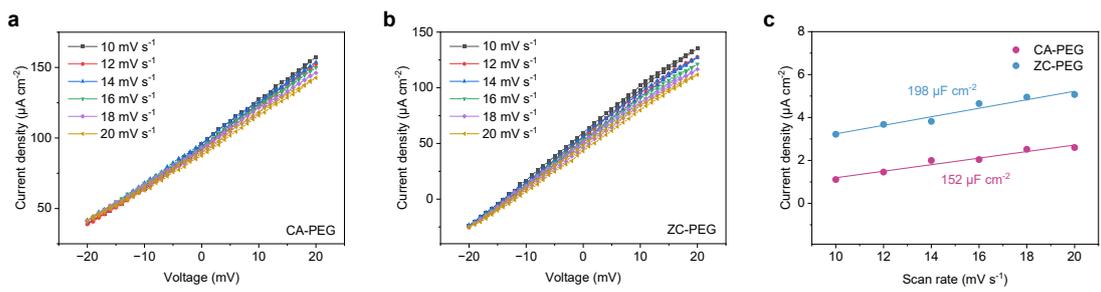


Fig. S39 CV curve of the Zn||Zn symmetric batteries at 10-20 mV s⁻¹ with (a) CA-PEG and (b) ZC-PEG. (c) The electric double layer capacitance with different electrolytes.

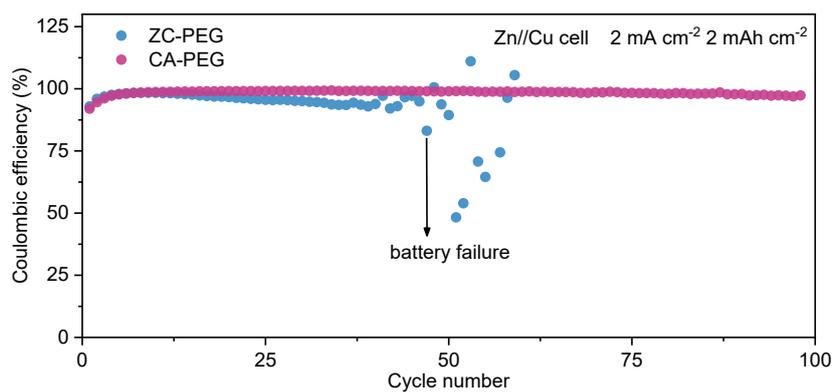


Fig. 40. Cycling performance of Zn||Cu asymmetric cells at 2 mA cm⁻² with 2 mA h cm⁻² in ZC-PEG and CA-PEG electrolytes.

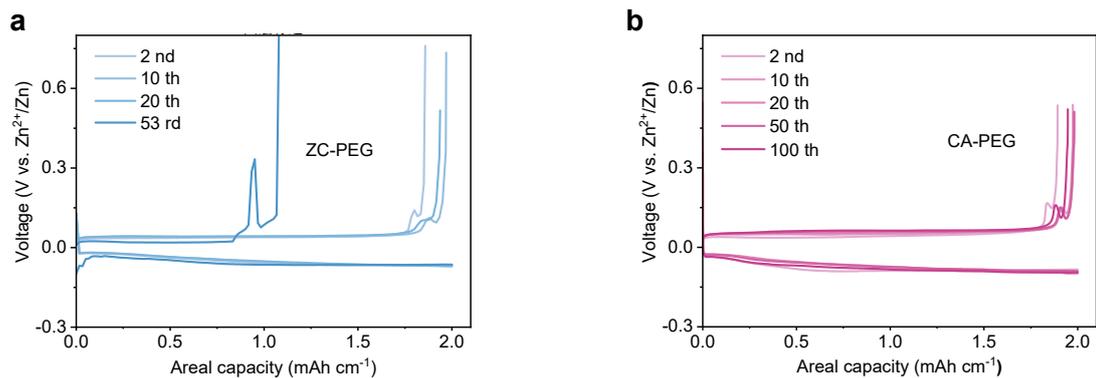


Fig. S41. Charge/discharge profiles corresponding to Zn||Cu asymmetric cells in (a) ZC-PEG and (b) CA-PEG electrolytes.

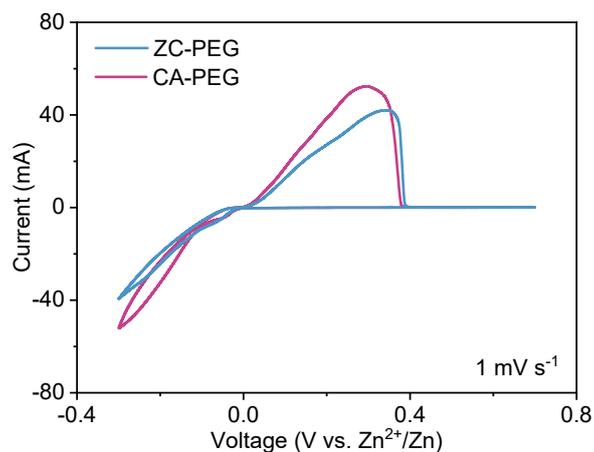


Fig. S42. CV curves of Zn||Cu asymmetric cells at a scan rate of 1 mV s^{-1} in ZC-PEG and CA-PEG electrolytes.

Table S1. Discharge voltage and specific capacity comparison of this work with other cathodes reported previously.

Cathode	Current density (A g ⁻¹)	Specific Capacity (mAh g ⁻¹)	Discharge voltage (V)	Ref.
I ⁻ /I ⁰	0.2	210	1.28	5
	8	89	1.20	
I ⁻ /I ⁰ /I ⁺	1	446	1.65	6
	10	314	1.56	
Br ⁻ /Br ₃ ⁻	0.2	334	1.67	7
	15	187	1.60	
Mn-based	0.2	318	1.41	8
	2.5	173	1.36	
V-based	0.1	388	0.96	9
	5	173	0.91	
PBA-based	0.1	101	1.71	10
	2	52	1.67	
Br ⁻ /Br ₃ ⁻ /BrCl ₂ ⁻	1	439	1.94	Comparison sample
	10	224	1.83	
Br ⁻ / Br ₃ ⁻ /BrCA	1	508	1.95	This work
	10	331	1.87	

Table S2. Energy densities and power densities comparison of this work with other conversion-type cathodes.

Cathode	Power density (W kg ⁻¹)	Energy density (Wh kg ⁻¹)	mass loading (mg cm ⁻²)	Ref.
I ⁻ /I ⁰	662	208	0.8-1.0	11
	16994	148		
I ⁻ /I ⁰ /I ⁺	252	463	4	12
	3729	217		
Br ⁻ /Br ⁰	296	404	1.6	7
	2102	112		
S ⁰ /S ⁴⁺	130	404	2	13
	6657	193		
S ²⁻ /S ⁰	181	444	2	
	789	78		
Se ²⁻ /Se ⁰ /Se ⁴⁺	123	403	3.2	14
	1448	113		
Br ⁻ /Br ₃ ⁻ /BrCl ₂ ⁻	1963	747	2	Control system
	18605	355		
Br ⁻ /Br ₃ ⁻ /BrCA	2095	848	2	This work
	19747	529		

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