## **Supplemental Materials**

Supplemental Materials Caption:

 Table S1 Sorption kinetics and sorption thermodynamics models used in this study.

 Table S2 S1

Table S2 Characteristic values of competitive sorption kinetics model for ENR and TYL on loess

## Table S1

Sorption kinetics and sorption thermodynamics models used in this study.

1	1 2	5			
	Names	Expression equations		Reference	
Sorption kinetics models	Pseudo-first-order	$\frac{1}{q_{t}} = \frac{1}{q_{1}} + \frac{k_{1}}{q_{1}t}$	Eq(1)	Ho and McKay, 1998a, b	
	Pseudo-second-order	$\frac{t}{q_{t}} = \frac{1}{k_2 q_2^2} + \frac{t}{q_2}$	Eq(2)	Ho and McKay, 1998c	
	Intra-particle diffusion	$q_{\rm t} = k_{\rm p} \cdot t^{1/2} + C$	Eq(3)	Weber and Morriss, 1963	
Sorption thermodynamics models	Langmuir	$\frac{1}{C_s} = \frac{1}{K_L \times Q_m \times C_e} + \frac{1}{Q_m}$	Eq(4)	Langmuir, 1918	
	Freundlich	$\lg C_s = \lg K_F + \frac{1}{n} \lg C_s$	Eq(5)	Freundlich, 1906	
	Linear	$C_s = K_d \times C_e$	Eq(6)		

Among these Eq(1)-Eq(9),  $q_1$  and  $q_2$  are the equilibrium sorption capacity (mg/g);  $q_t$  is the sorption capacity (mg/g) with the variable t;  $k_1$  and  $k_2$  are respectively the first order sorption kinetic rate constant (min<sup>-1</sup>) and the quasi-secondary sorption kinetic rate constant[g/ (mg·min)];  $K_p$  is the particle internal diffusion rate constant[mg/ (g·min<sup>1/2</sup>)]. The intercept of the equation yields  $q_1, k_2, k_1$ , and C, with the slope of which is  $q_2, k_p$ .  $q_s$  is the sorption capacity of target pollutants(mg/g);  $C_e$  is the mass concentration of target pollutants in liquid phase (mg/L);  $Q_m$  is the saturated sorption capacity of target pollutants (mg/g);  $K_L$  is the characteristic constant of Langmuir adsorption (L/g);  $K_F$  and n is the characteristic constant of Freundlich model.  $Q_m, K_F$  can be obtained from the intercept of equation.

Table S2 Characteristic values of competitive sorption kinetics model for ENR and TYL on loess

pollutants		Companyation		Pseudo-first-model		Pseudo-second-model					
Main solute	Co-solute	mg/L	q <sub>max,exp</sub>	$\mathbf{k}_1$	q <sub>1</sub> , model	R <sup>2</sup>	$\mathbf{k}_2$	q <sub>2,model</sub>	R <sup>2</sup>	Кр	R2
		0	414	0.720	417	0.903	1099	421	0.999	0.0010	0.482
ENR	TYL	4	494	0.045	497	0.437	274	496	0.999	0.0004	0.224
(10 mg/L)		16	469	0.077	840	0.445	57.3	469	0.998	0.0008	0.304
		24	449	0.479	1080	0.249	4.55	450	0.999	0.0030	0.792
TYL ENR (16 mg/L)		0	389	3.062	416	0.900	2.099	394	0.999	0.0060	0.233
	2	790	0.036	365	0.780	10.9	789	0.999	0.0060	0.485	
	ENR	10	701	0.486	697	0.598	1.81	707	1.000	0.0036	0.792
		18	611	0.239	805	0.865	0.977	613	0.999	0.0060	0.756

Cited references

- Freundlich, H., 1906. Uber die adsorption in losungen (Adsorption in solution). *Physical Chemistry Periodical*, 57: 384–470.
- Ho, Y. S., McKay, G., 1998a. Sorption of dye from aqueous solution by peat. *Chemical Engineering Journal*, 70: 115–124.
- Ho, Y. S., McKay, G., 1998b. The kinetics of sorption of basic dyes from aqueous solution by sphagnum moss peat. *Canadian Journal of Chemical Engineering*, 76: 822–827.
- Ho, Y.S., McKay, G., 1998c. Kinetic models for the sorption of dye from aqueous solution by wood. *Journal of Environmental Science and Health Part B: Process Safety and Environmental Protection*, 76(B2): 183–191.
- Langmuir, I., 1918. The adsorption of gases on plane surfaces of glass, mica and platinum. *Journal of American Chemical Society*, 40: 1361–1403.
- Weber, W.J., Morriss, J.C., 1963. Kinetics of adsorption on carbon from solution. *Journal of Sanitary Engineering Division: American Society of Civil Engineering*, 89: 31–60.