

**The following supplements is included as supporting materials for this paper:**

**Table S1** EIS parameters for bare NF, Co<sub>3</sub>O<sub>4</sub>/NF and Cu-Co<sub>3</sub>O<sub>4</sub>/NF

cathode	R <sub>s</sub> ( $\Omega$ cm <sup>2</sup> )	R <sub>ct</sub> ( $\Omega$ cm <sup>2</sup> )
NF	4.143	24.69
Co <sub>3</sub> O <sub>4</sub> /NF	4.579	7.562
Cu-Co <sub>3</sub> O <sub>4</sub> /NF	4.093	6.059

**Table S2** Energy consumption of different cathodes

Cathode	Applied current (A)	Voltage (V)	Energy consumption (K Wh/g NO <sub>3</sub> <sup>-</sup> -N)
NF	0.2	6.83	5.4099
Co <sub>3</sub> O <sub>4</sub> /NF	0.2	5.82	0.2836
Cu-Co <sub>3</sub> O <sub>4</sub> /NF	0.2	3.52	0.1164

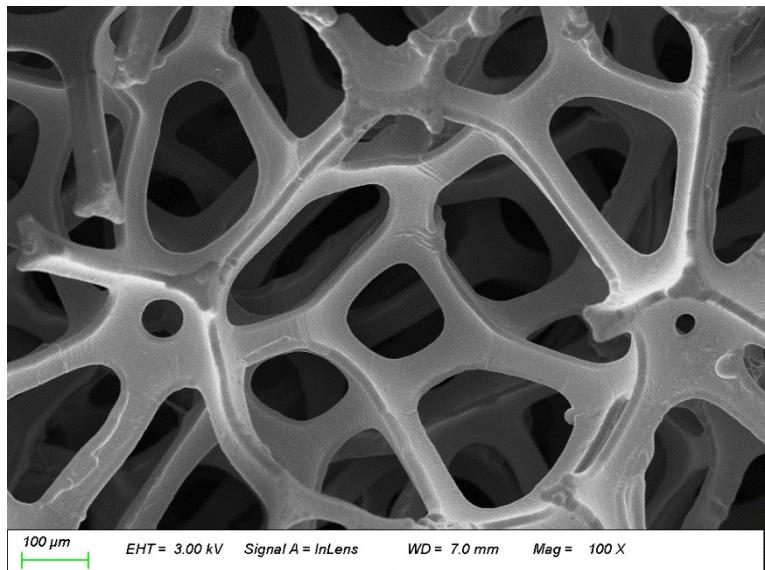
**Table S3** Comparison of eNO<sub>3</sub>RR with other cathodes

Electro-catalysts	Preparation method	Electrolyte	Reaction time	NO <sub>3</sub> <sup>-</sup> -N conversion	NH <sub>4</sub> <sup>+</sup> -N selectivity	Ref.
Cu(I/II)@NF	hydrothermal	50 mg L <sup>-1</sup> NO <sub>3</sub> <sup>-</sup> + 0.05 M Na <sub>2</sub> SO <sub>4</sub>	24 h	95.4%	/	<sup>1</sup>
Porous Cu	coprecipitation + calcination	0.01 M NO <sub>3</sub> <sup>-</sup> + 0.1 M HClO <sub>4</sub>	8 h	98%	94%	<sup>2</sup>
Cu <sub>2</sub> O/CuO/CF	solvent oxidation + electrocatalytic reduction	5 mM NO <sub>3</sub> <sup>-</sup> + 0.1 M KOH	60 h	100%	99.35%	<sup>3</sup>
Co <sub>3</sub> O <sub>4</sub> /NF	hydrothermal + calcination	0.1 M NO <sub>3</sub> <sup>-</sup> + 1.0 M NaOH	2 h	95%	85.36%	<sup>4</sup>
Fe-CoO/CuO@CF	hydrothermal + calcination	0.1 M NO <sub>3</sub> <sup>-</sup> + 3.5 M KCl	2 h	93.8%	/	<sup>5</sup>
Cu <sub>2</sub> O-Cu@Ti	electrodeposition	0.01 M NO <sub>3</sub> <sup>-</sup> + 1 M KOH 30 mg L <sup>-1</sup> NO <sub>3</sub> <sup>-</sup> -N	1.5 h	90%	79%	<sup>6</sup>
Cu-Pt	electrodeposition	+ 12.5 mM Na <sub>2</sub> SO <sub>4</sub>	2 h	94%	84%	<sup>7</sup>
Co-P/TP	electrodeposition	200 mg L <sup>-1</sup> NO <sub>3</sub> <sup>-</sup> + 0.2 M Na <sub>2</sub> SO <sub>4</sub> +	10 h	86.9%	/	<sup>8</sup>
NiCoP/NF	electrodeposition	50 mg L <sup>-1</sup> NO <sub>3</sub> <sup>-</sup> + 0.05 M Na <sub>2</sub> SO <sub>4</sub>	5 h	97.68%	95.44%	<sup>9</sup>
CoO/Cu	electrodeposition + calcination	0.04 M NO <sub>3</sub> <sup>-</sup> + 0.4 M Na <sub>2</sub> SO <sub>4</sub>	0.5 h	87.6%	97.3%	<sup>10</sup>
Cu-Co <sub>3</sub> O <sub>4</sub>	electrodeposition + calcination	50 mg L <sup>-1</sup> NO <sub>3</sub> <sup>-</sup> + 0.01 M Na <sub>2</sub> SO <sub>4</sub>	2 h	96.78%	97.58%	This work

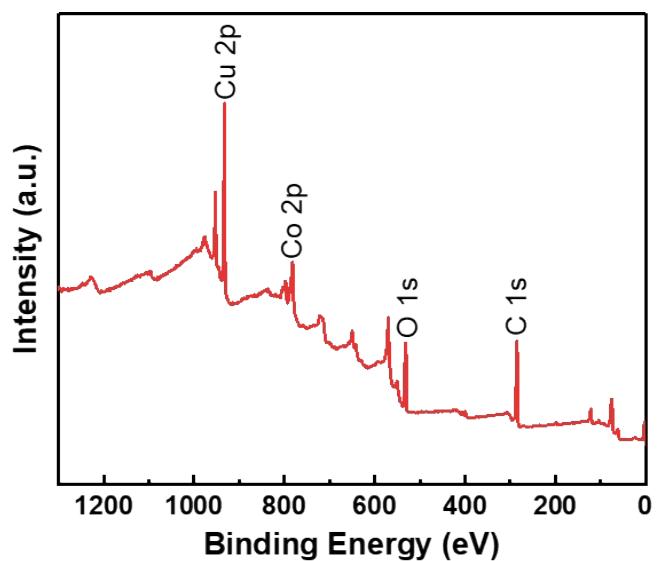
**Table S4** Reaction energy consumption at different electrolyte concentrations\*

Electrolyte concentration (M)	Solution conductivity (μS/cm)	Reaction voltage (V)	NO <sub>3</sub> <sup>-</sup> -N removal rate (%)	Energy consumption (kWh/g NO <sub>3</sub> <sup>-</sup> -N)
0.01	2720	3.52	97.77	0.1164
0.05	8940	2.21	97.58	0.0724
0.1	15530	2.03	96.75	0.0671
0.2	25800	1.87	95.91	0.0624

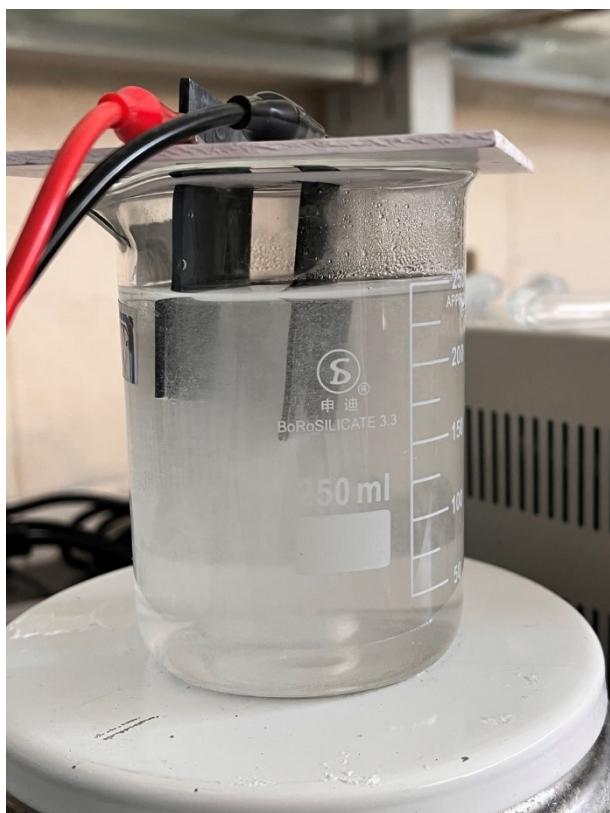
\* data were obtained as the average value of three independent experiments.



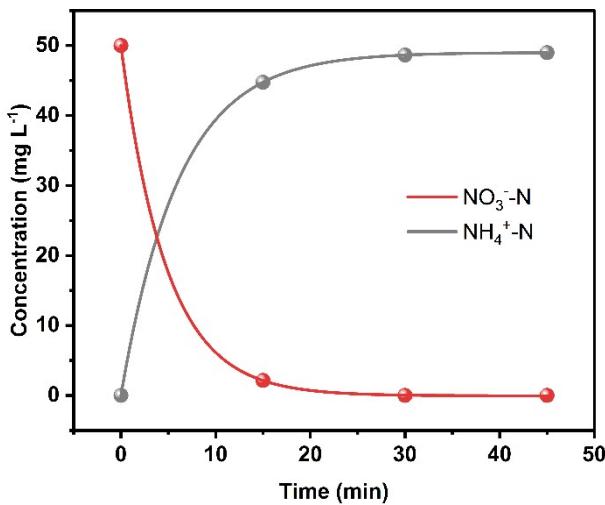
**Fig. S1** SEM image of bare NF



**Fig. S2** XPS survey spectrum for Cu-Co<sub>3</sub>O<sub>4</sub>/NF



**Fig. S3** Hydrogen evolution in high current reaction



**Fig. S4** Time-dependent  $\text{NO}_3^-$ -N and  $\text{NH}_4^+$ -N concentrations in dual-chamber reactor (experimental conditions:  $50 \text{ mg L}^{-1}$   $\text{NO}_3^-$ -N,  $0.2 \text{ M Na}_2\text{SO}_4$ )

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