Supporting information

Breaking the Selectivity-Activity Seesaw in Ethane Oxidative Dehydrogenation via the Synergetic Effects of Doping and Electrochemical Activation

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Experiments

Material synthesis and cell fabrication

Solid-phase reaction method was used to prepare double perovskite $Sr_2Ti_{0.8}CoO_{6-\delta}(STC)$, $Sr_2Ti_{0.8}Co_{0.6}Fe_{0.6}O_{6-\delta}(STCF)$, and $Sr_2Ti_{0.8}FeO_{6-\delta}(STF)$ electrode material powders with different Fe/Co ratios, and the three materials were prepared by basically the same method, only changing $SrCO_3$, TiO_2 , Co_3O_4 and Fe_2O_3 (Macklin, China) stoichiometric ratios, and then mixed with appropriate amount of ethanol and then ball milled for 24 h. The dried mixture was calcined in a muffle furnace for 8 h at 1200 °C.

The La_{0.8}Sr_{0.2}Ga_{0.83}Mg_{0.17}O_{3- δ} (LSGM) electrolyte was synthesized by mixing powders of La₂O₃, MgO, SrCO₃ and Ga₂O₃ with ethanol and being ball-milled for 24 h. The obtained LSGM mixture was pressed into a pellet and pre-sintered at 1250 °C for 10 h. The obtained pellet was ground into powder and were then pressed into pellet again. After further sintering at 1450 °C for 10 h, the LSGM electrolyte support was successfully prepared.

The electrode slurry was prepared by mixing electrode material powders and graphite in a weight ratio of 10:2 with a binder composed of α -terpineol and Polyvinyl Butyral, followed by grounding with mortar for 3 h. The STCF cathodes and anodes (STC, STCF and STF) were fabricated by printing the slurry onto both sides of the LSGM electrolyte support. After sintering at 1150 °C for 3 h, the complete electrolyte-supported single cell was finally achieved, denoted as STCF/LSGM/STC,STCF and STF. The electrode effective area of every cell was 0.5 cm².

Pulsed laser deposition (PLD) was used for preparing the thin film cell in this work. The PLD targets were acquired by pressing the corresponding powders into pellets and then sinter at 1300 °C for 6 h. A thin layer of STC, STCF and STF electrode was deposited on single crystal yttria stabilized zirconia (YSZ) substrate by PLD using a KrF excimer laser with laser energy of 300 mJ and wavelength of 248 nm. The deposition was carried out at 600 °C under the oxygen pressure of about 1 Pa. The distance from PLD targets to substrates was set to be 6 cm. After deposition, thin-film samples were cooled down to room temperature with the rate of 5 °C min⁻¹ under oxygen pressure of 200 Pa. A thin layer of gadolinium-doped cerium oxide (GDC) was deposited between STC, STCF and STF films and YSZ electrolyte as a buffer layer.

Electrochemical measurements and gas product analysis

For the electrochemical measurement, while the cathode electrode side was fed with pure CO_2 with a flow rate of 20 mL min⁻¹, the mixture of C_2H_6/Ar was supplied to the anode side. The flow rate is controlled to be 16 mL min⁻¹ for Ar and 4 mL min⁻¹ for ethane, giving a total flow rate of 20 mL min⁻¹ (20 percent ethane). All gas flows are precisely controlled by mass flow meters (Alicat, USA).

Electrochemical tests were performed on the electrochemical workstation (IM6, Zahner, Germany). The composition of the reaction products was analyzed using gas chromatography (GC9790II, Fuli Instruments). Two different Hydrogen Flame Ionization Detector (FID) detectors in our chromatography system (GC9790II model from Zhejiang Fuli Instruments, China) for detecting CO/CO2 (FID I) and CH4/C2H6/C2H4 (FID2) respectively. A methanator (catalytic conversion module) is incorporated into the FID2 detectors to enable the detection of CO and CO₂. The conversion of ethane (C_{C2H6}) and the selectivity of products (S_i) were calculated following the equations:

$$[C]_{total} = [CH_4] + [CO] + [CO_2] + 2[C_2H_4] + 2[C_2H_6]$$

$$C_{C2H6} = 1 - 2[C_2H_6]/[C]_{total}$$

$$S_{C2H4} = 2[C_2H_4] / ([C]_{total} - 2[C_2H_6])$$

$$S_{CH4} = [CH_4] / ([C]_{total} - 2[C_2H_6])$$

$$S_{CO} = [CO] / ([C]_{total} - 2[C_2H_6])$$

$$S_{CO2} = [CO_2] / ([C]_{total} - 2[C_2H_6])$$
"

where $[C]_{total}$ is the total amount of C in the exit gas. $[CH_4]$, [CO], $[CO_2]$, $[C_2H_4]$, and $[C_2H_6]$ are the amounts of methane, carbon monoxide, carbon dioxide, ethylene, and ethane in the exit gas.

Thermogravimetric test

The samples tested were placed on a test bench and heated up to 900 $^{\circ}$ C at 10 $_{\circ}$ C-min⁻¹ under N₂ atmosphere and the change in weight of the material was recorded.

Programmed warming reduction/desorption test

 O_2 -TPD test: The sample was placed in a test tube and pretreated at 300 °C and He gas. Adsorption was carried out by passing 30% O_2 /He mixture for 1 h at 50 °C, then switched to He gas flow for purging, and after the baseline was stabilized, the temperature was raised to 500 °C, and the stripped gas was detected by TCD.

Material characterizations

The crystal structure of the materials was analyzed by X-ray diffraction (XRD, Bruker D8 Advance, Germany) with Cu-Kα radiation. High resolution X-ray diffraction (HRXRD, Rigaku, Japan) with Cu-Kα radiation was used to characterize the crystal structure and lattice constants of the thin film system. The topography was investigated by scanning electron microscopy (SEM, SU8010, Hitachi, Japan). The microstructure and local composition were probed by transmission electron microscopy (TEM) which was coupled with energy dispersive X-ray spectroscopy (EDS) analysis (JEM 2100F, JEOL, Japan) operating at 200 kV.

Density Functional Theory Calculations

All theoretical studies were performed by spin-polarized density functional theory (DFT) with the Vienna ab Initio Simulation Package (VASP)^{1, 2}. The projected-augmented wave (PAW) pseudopotentials were utilized to address the core electrons, and a plane-wave kinetic energy cutoff was set to 400 eV^{3, 4}. The generalized gradient approximation (GGA) proposed by Perdew, Burke and Ernzerhof (PBE) was used for the exchange-correlation energies⁵.

To reduce the computational time, Sr_2TiCoO_6 , $Sr_2TiCo_{0.5}Fe_{0.5}O_6$, and Sr_2TiFeO_6 models were created for the STC, STCF, and STF chalcogenide calculations. For the

Brillouin zone of the bulk and flat plate models, $6 \times 6 \times 6$ and $3 \times 3 \times 1$ Monkhorst Pack k-points, respectively, were used for sampling. For DOS calculations, $13 \times 13 \times$ 13 Monkhorst Pack k-point sampling was used. Based on our experimental characterization and the model of Ref. The chalcogenide BO₂ capped (001) flat plate structure consists of 8 layers (the bottom 3 layers are fixed) and ~20 Å vacuum spacing in the direction perpendicular to the surface. GGA+U approach was used to correct the significant self-interaction, and Ueff was added to the open-shell d-electrons, 4.4 eV for Ti, 4.0 eV for Fe and 3.4 eV for $Co^{6, 7}$. The converge criterion of the energy was 1 x 10^{-10} ⁵ eV for the self-consistent-field (SCF) iterations. Based on a force-based conjugated gradient algorithm, geometries were relaxed until the forces on each atom were within 0.03 eV/Å. The Janak-Slater (JS) transition state method was used to calculate the core level energy, which considers the half occupancy of the core level when estimating the O 1s binding energies (BEs).^{8,9} The BEs were determined by reference to the vacuum energy level, which was determined by the VASPKIT 426 function as the electrostatic potential energy. The Gibbs free energy was calculated with zero-point energy and entropy as follows:

 $\Delta G = \Delta E + \Delta Z P E - T \Delta S,$

where E is the DFT-calculated energy, ZPE is the zero-point energy, T is the temperature, 1073K and S is the entropy. We assume that the entropy of the adsorbed species is zero. The NIST database was used to obtain the standard entropy of gas molecules¹⁰. For the ZPE correction, we calculated the vibration frequencies by using the density functional perturbation theory.

The p-band center was calculated by

$$\varepsilon_{p} = \frac{\int_{-\infty}^{\infty} E\rho(E)dE}{\int_{-\infty}^{\infty} \rho(E)dE},$$

where E is the energy, E_f is the Fermi-level energy, and ρ is density of state. The adsorption energy of H* ($\Delta E_{ads, H}$) was calculated by

 $\Delta E_{ads, H} = E_{H*} - E_{slab} - 1/2E_{H2}$,

in which E_{H2} , E_{slab} are the energies for gaseous H_2 , pristine slab model and E_{H^*} is the total energy of the slab model when the H^* is adsorbed on the lattice oxygen. The adsorption energy of $C_2H_5^*$ was derived from the following equation:

 $\Delta E_{ads, C2H5} = E_{C2H5*} - E_{slab} - (E_{C2H6} - 1/2E_{H2}),$

where E_{C2H5*} is the total energy of the slab model when the C_2H_5* is adsorbed on the surface, E_{C2H6} is the energies for gaseous C_2H_6 . The oxygen vacancy formation energy (E_{Ov}) was calculated from the total energies of each slab models,

 $E_{Ov} = (E_{Vo} + 1/2E_{O2}) - E_{slab},$

where E_{Ov} is the total energy of the system containing an oxygen vacancy, and E_{O2} is the energies for gaseous O_2 .



Figure S1. (a) XRD patterns and (b) SEM image and EDS spectra of STF, STCF and STC powder.



Figure S2. (a-c) TEM image and EDS spectra of STC, STCF and STF powder.



Figure S3. XPS spectra of Sr 3d (a,b) of STC, STCF and STF.



Figure S4. EPR spectra of STC, STF samples.



Figure S5. Oxygen Defect/Lattice Oxygen for STC and STF



Figure S6. $\mathrm{N_2}\text{-}\mathrm{TG}$ curves for STC, STCF and STF.



Figure S7. Three modeling systems, named STC, STCF, and STF.



Figure S8. Model diagram of oxygen vacancy formation energy for surface (a) and bulk phase (b) in three model systems.



Figure S9. (a) bulk electronic structure of oxygen; (b) Oxygen vacancy formation energy for bulk phase in three model systems (STC, STCF, and STF).



Figure S10. The configuration of reaction intermediate of ethane dehydrogenation pathways on the three systems (STC, STCF and STF).



Figure S11. The configuration of the H₂O formation and desorption pathways on the

three systems.



Figure S12. Schematic and physical photograph of the reactor used for electrochemical testing.



Figure S13. SEM images of anode and electrolyte for three different anode materials (STC, STCF, STF).



Figure S14. Proportion of C_2H_4 (a) and CO_x (b) gas composition; CO_x (c) selectivity in three types of cells anode products with different anode materials (STC, STCF, and STF) with a 20% C_2H_6 /Ar flow rate of 20 mL·min⁻¹.



Figure S15. (a) XRD pattern, (b) Raman spectra (inset shows Raman spectra of graphite), XPS spectra of (c) O 1s and (d) Sr 3d of anode side electrode material (STC, STCF, and STF) after electrolytic testing for 300 min of powder cells at 0.8 V with a 20% C₂H₆/Ar flow rate of 20 mL⋅min⁻¹.

Sample	Lattice	Oww.com	Surface OH- /CO3 ²⁻		Oxygen	
	Lattice	dafaata		Surface H ₂ O	defects/Lattice	
	oxygen defects	defects			oxygen	
STC	11.31	24.75	58.45	5.48	2.18	
STCF	17.04	27.10	51.22	4.62	1.59	
STF	17.50	26.16	50.27	6.06	1.49	

 Table S1. O 1s XPS peak deconvolution results.

No. Reactant	Catalyst	Conversion	Selectivity	Temperature	Yield	Dof	
	Reactant	Catalyst	(%)	(%)	(°C)	(%)	Kti.
1 C ₂ H ₆ +CO ₂		γ-	5.9	90	600	5.3	
		$Al_2O_3/La_{0.6}Sr_{0.4}Co_{0.2}Fe_{0.8}O_{3} \text{-}$					11
	δ (SOEC)						
2	$C_2H_6+CO_2$	Pt, Sn/Mg(Al)O	6.1	98.7	600	6.0	12
3	$C_2H_6+CO_2$	VO _x /Al ₂ O ₃ -ZrO ₂	8.5	82	525	6.9	13
4	$C_2H_6+CO_2$	MoO _x /Al ₂ O ₃	10	85	600	8.5	14
5	$C_2H_6+CO_2$	Fe/NiO-MgO-ZrO ₂	11.9	79	600	9.4	15
6	$C_2H_6+CO_2$	CeO ₂ (SOEC)	10	95	600	9.5	16
7	$C_2H_6+CO_2$	$La_{0.2}Sr_{0.8}TiO_{3\pm d}Cl_{\sigma}~(SOEC)$	14	71.4	600	10.0	17
8	C ₂ H ₆ +CO ₂	Fe/Mo ₂ C	14	80	600	11.2	18
9	C ₂ H ₆ +CO ₂	CrO _x /Al ₂ O ₃	14	90	700	12.6	19
10	C ₂ H ₆ +CO ₂	CeO ₂	14	95	750	13.3	20
11	C ₂ H ₆ +CO ₂	NiAl	26.2	52.5	700	13.7	21
12	C ₂ H ₆ +CO ₂	Ni-Nb-Cr-O	26	65	450	16.9	22
13	C ₂ H ₆ +CO ₂	Ga ₂ O ₃	19.6	95	650	18.6	23
14	C ₂ H ₆ +CO ₂	LSF@10Li2CO3	29	75.5	720	21.9	24
15 C ₂ H ₆ +CO ₂		Cr ₂ O ₃ -ZSM-5 (membrane	43	80	750	34.4	25
		reactor)					25
16	C ₂ H ₆ +CO ₂	Fe ₃ Ni ₁ /CeO ₂	67.3	63.5	800	42.7	26
17	C ₂ H ₆ +CO ₂	Co-BaCO ₃	48	92.2	650	44.2	27
18	C ₂ H ₆ +CO ₂	Ca-ThO ₂	46	97	725	44.6	28
19	C ₂ H ₆ +CO ₂	Cr/TS(30)	52.7	90	650	47.4	29
20	C ₂ H ₆ +CO ₂	Co-Cr ₂ O ₃ /ZrO2	61	80	650	48.8	30
21	C ₂ H ₆ +CO ₂	Cr/H-ZSM-5	70	70	650	49	31
22	C ₂ H ₆ +CO ₂	CoO _x /MgAl ₂ O ₄ -HT	55.2	89.5	650	49.4	32
23	C ₂ H ₆ +CO ₂	Li-promoted La _x Sr _{2-x} FeO _{4-δ}	61	90	700	54.9	33
24	C ₂ H ₆ +CO ₂	Zn _{2.92} /NaS50	70	90	650	63	34
25	C ₂ H ₆ +CO ₂	$Sr_{2}Ti_{0.8}Co_{0.6}Fe_{0.6}O_{6-\delta}$	76.6	86.5	800	66.2	35
26 C ₂ H ₆		STF (SOEC)	83.5	84.5	800	70.6	This
	C ₂ H ₆ +CO ₂						work

Table S2. Comparison of the performance of ethane oxide dehydrogenation using carbon dioxide as an oxidant in this work with other reported results.

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