

Supplementary Information

Precise reduction of spent Li-ion battery cathode and new phase transition

mechanism by self-generated H₂ to achieve dual-recycling of resources and energy

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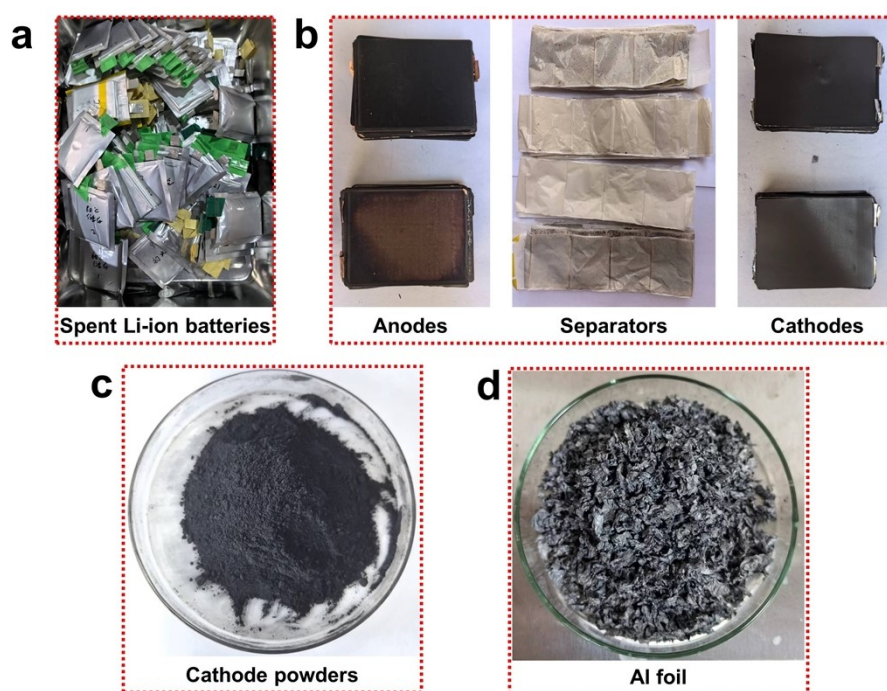


Figure S1. Dismantling process of spent LCO batteries. The digital photos: (a) spent LCO batteries, (b) the main components of spent LCO batteries, (c) cathode powders, (d) Al foil.

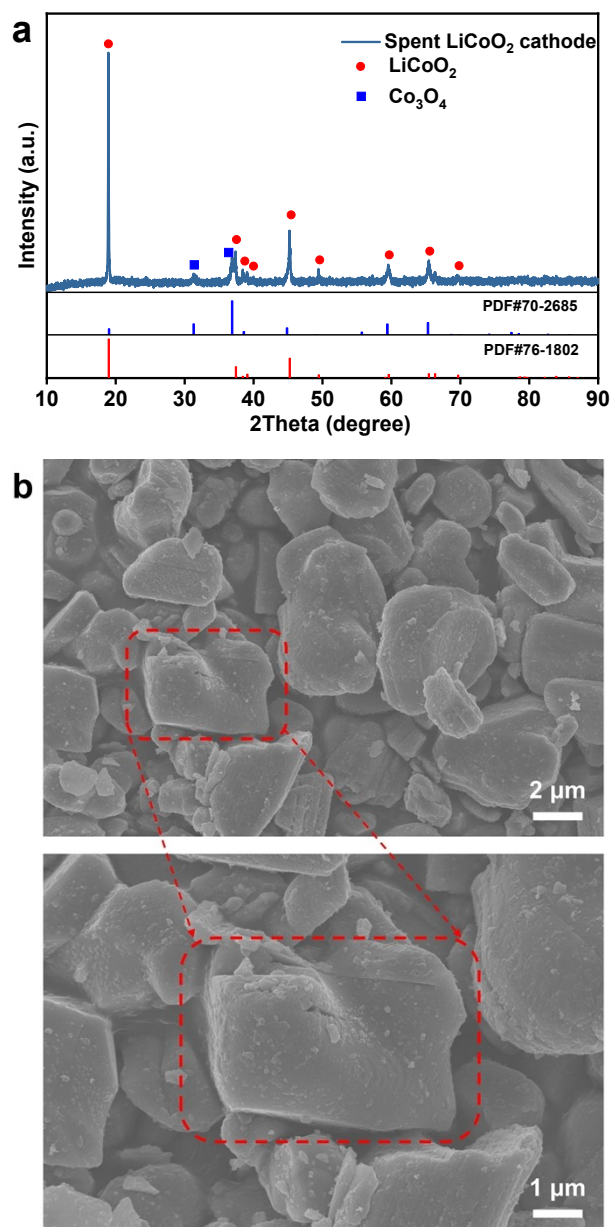


Figure S2. (a) XRD pattern of spent LCO material; (b) SEM images of spent LCO material.

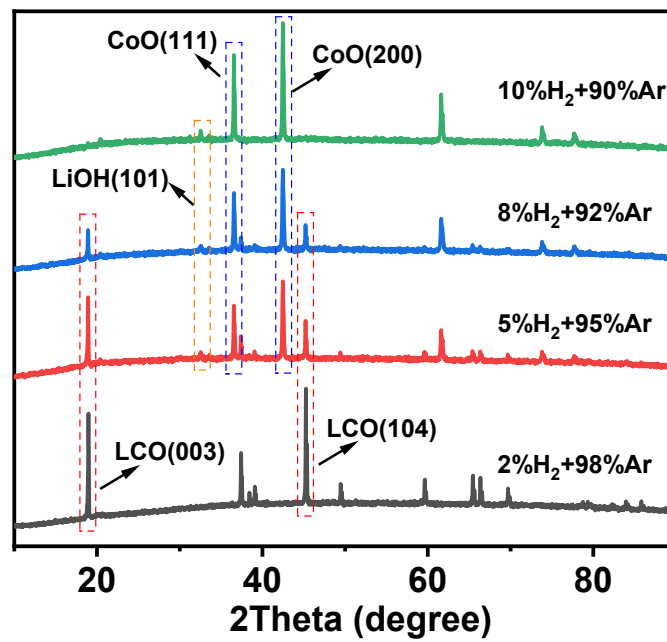


Figure S3. XRD patterns of reduction products at different hydrogen concentrations.

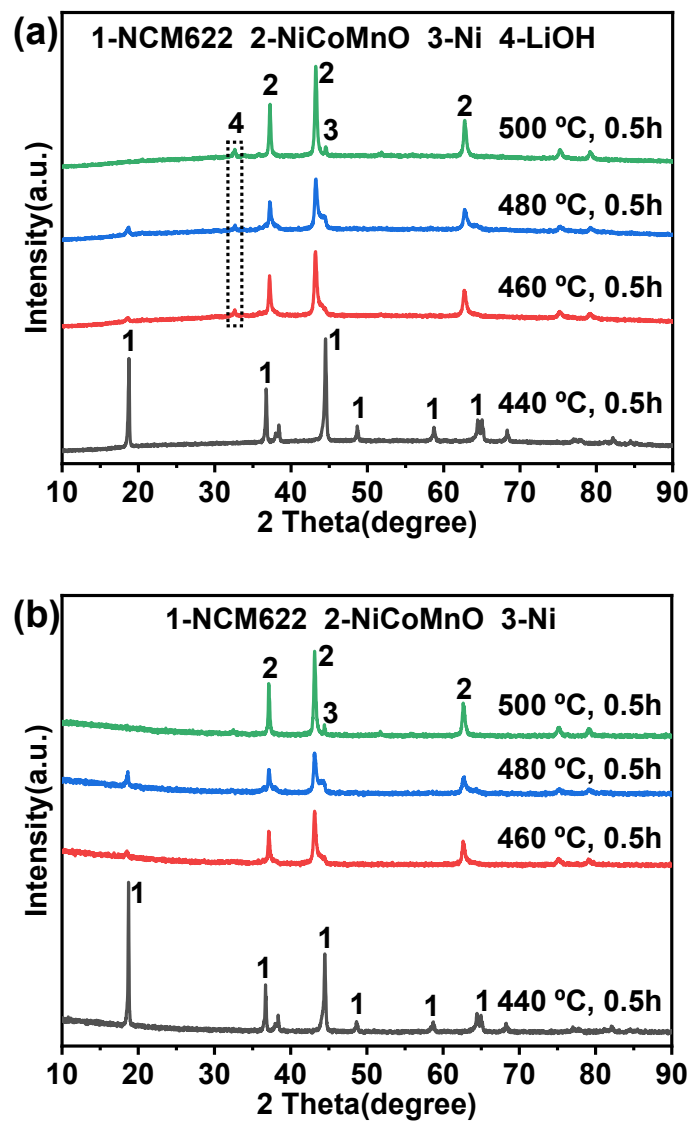


Figure S4. XRD patterns of the H₂ reduction product (a) and the leaching residue (b) of spent LiNi_{0.6}Co_{0.2}Mn_{0.2}O₂ (NCM622).

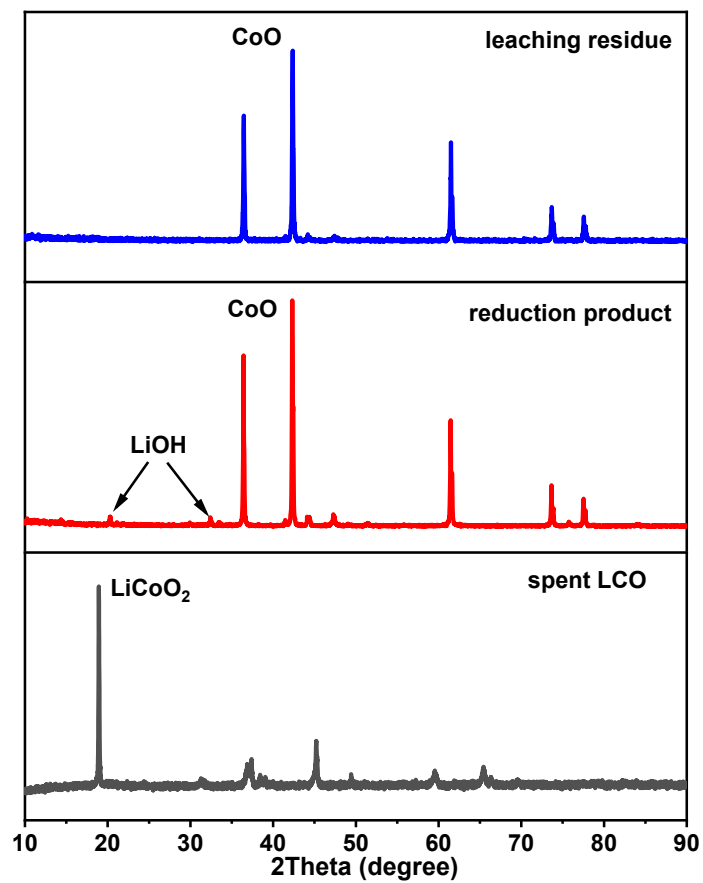


Figure S5. XRD patterns of spent LCO, the reduction product, and the leaching residue.

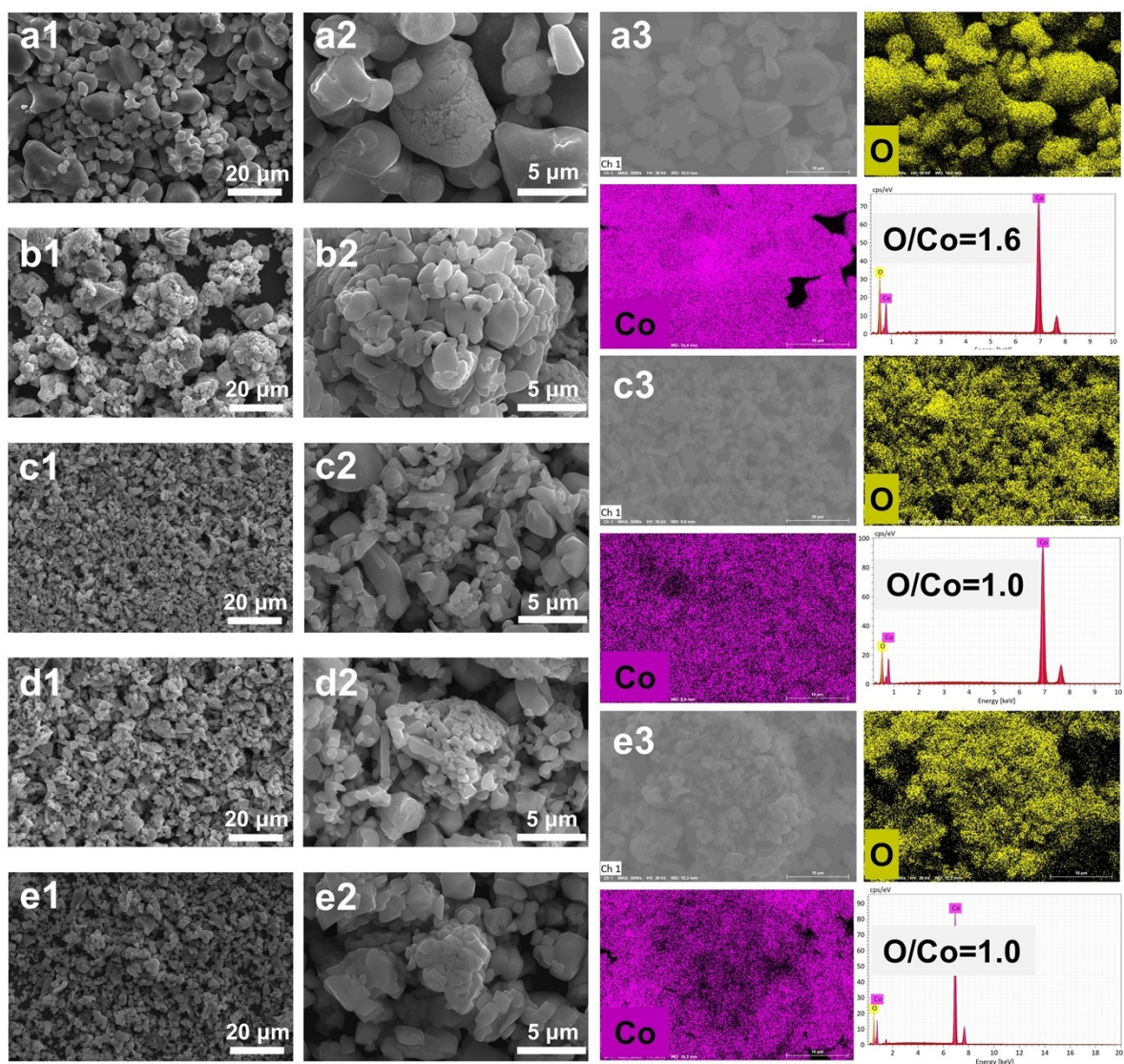


Figure S6. SEM images of leaching residues at different reduction temperatures. (a1, a2) 450 °C, (b1, b2) 470 °C, (c1, c2) 490 °C, (d1, d2) 500 °C, and (e1, e2) 510 °C. EDS-mapping results at (a3) 450 °C, (c3) 490 °C, and (e3) 510 °C.

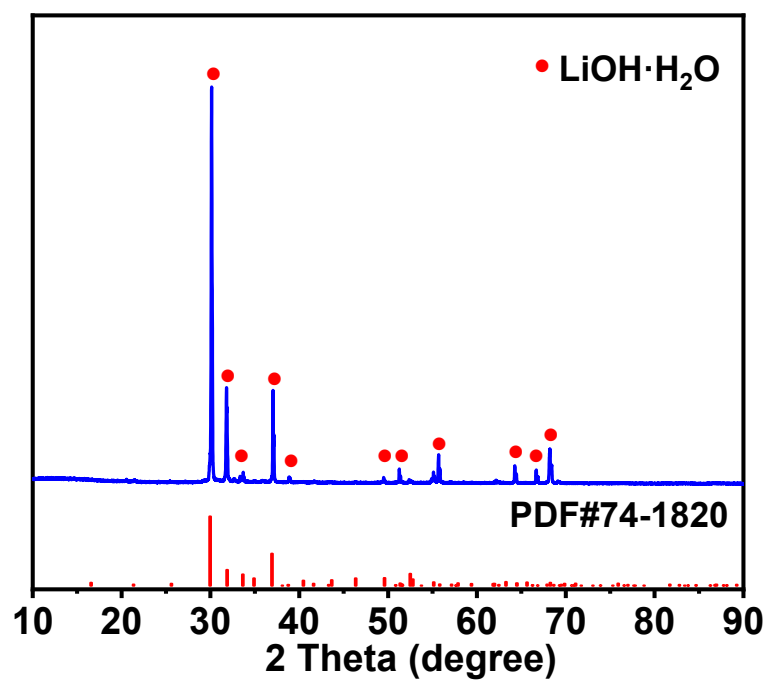


Figure S7. XRD pattern of $\text{LiOH} \cdot \text{H}_2\text{O}$ recovered by evaporation crystallization.

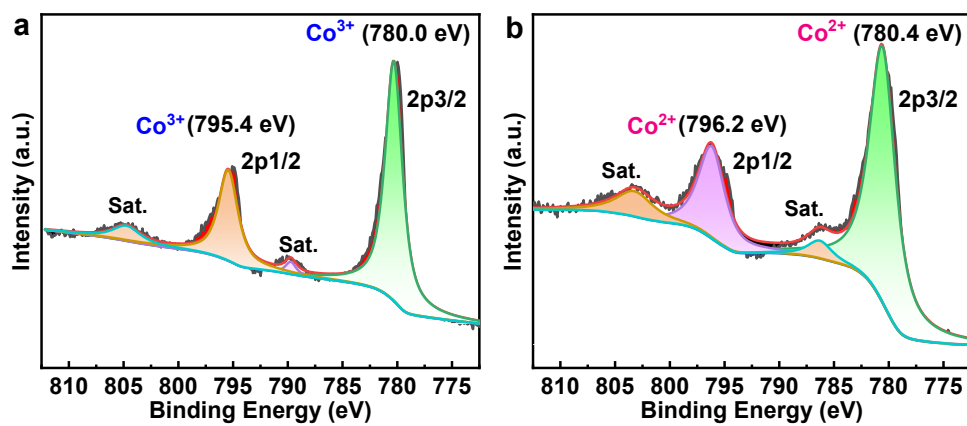


Figure S8. XPS survey spectra of Co₂p of (a) spent LCO and (b) reduction product.

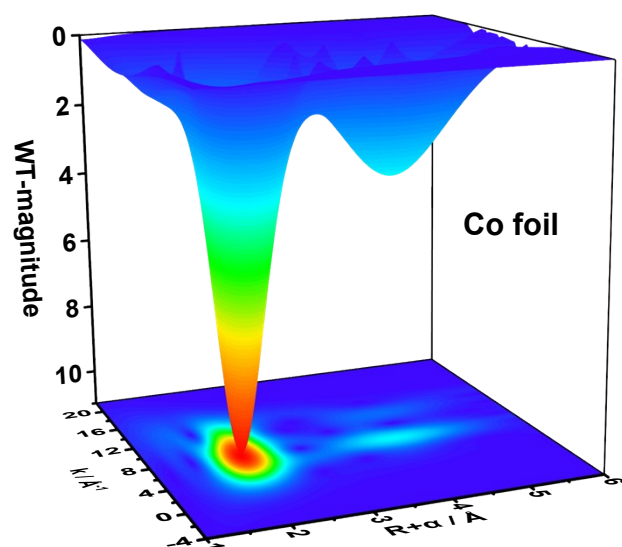


Figure S9. k^3 -weighted Co K_3 -edge WT-EXAFS contour plots of Co-foil.

Table S1. Lattice parameters (a, c) and lattice volume (V) of LCO and LCO (at 500 °C in Ar) powders given with reliability factors of weighed (R_{wp}) profiles and goodness of fit (χ^2) values.

	LCO	LCO at 500 °C in Ar
a (Å)	2.813848	2.866973
c/a	4.992	4.954
V (Å ³)	96.325	101.098
Li at Co site	1.884%	7.872%
$I_{(003)}/I_{(104)}$	1.745	1.094
$(I_{(006)}+I_{(012)})/I_{(101)}$	0.417	0.477
R_p (%)	5.3%	4.9%
R_{wp} (%)	6.8%	6.3%
Gof (χ^2)	1.27	1.53

Table S2. Possible chemical reactions during H₂ reduction process.

	Reactions	ΔH (kJ/mol)	ΔG (kJ/mol)
(1)	$2\text{LiCoO}_2 + \text{H}_2 (\text{g}) = \text{Li}_2\text{O} + 2\text{CoO} + \text{H}_2\text{O} (\text{g})$	40.81	11.78
(2)	$\text{Li}_2\text{O} + \text{H}_2\text{O} (\text{g}) = 2\text{LiOH}$	-130.09	-88.11
(3)	$2\text{LiCoO}_2 + \text{H}_2 (\text{g}) = 2\text{LiOH} + 2\text{CoO}$	-89.28	-76.33
(4)	$\text{CoO} + \text{H}_2 (\text{g}) = \text{Co} + \text{H}_2\text{O} (\text{g})$	-3.88	-14.38
(5)	$2\text{LiCoO}_2 + 3\text{H}_2 = \text{Li}_2\text{O} + 2\text{Co} + 3\text{H}_2\text{O} (\text{g})$	33.04	-16.99

Table S3. Main materials used in different recycling processes*.

Materials	Price (\$/t)	Usage for Pyro-(t)	Usage for Hydro-(t)	Usage for This work (t)
Recycled LCO battery powder (Co=27.5%, Li $\geq$ 3.5%)	5000	1	1	1
HCl	11.6	1.255	/	/
H ₂ O ₂	118.7	/	0.159	/
H ₂ SO ₄	56.3	/	0.705	/
NaOH	343.4	0.353	0.353	/
Na ₂ CO ₃	242.3	0.267	0.267	/
H ₂ O	0.373	29.85	29.85	7.06

*The prices of other metallic compounds are referenced from China Metals Network (www.cbcie.com) and <https://www.100ppi.com>; The prices of recycled LCO black powder are referenced from Mysteel Network (www.mysteel.com).

Table S4. Main products of different recycling processes*.

Materials	Price (\$/t)	Yield for Pyro-(t)	Yield for Hydro-(t)	Yield for This work (t)
Cu	6600	0.205	0.205	0.205
Al	1300	0.103	0.103	0.103
Spent graphite	197	/	0.236	0.236
CoOH ₂	11050	0.410	0.410	/
Li ₂ CO ₃	10552	0.186	0.186	/
LiOH	12960	/	/	0.121
CoO	17610	/	/	0.35

*The price of Li₂CO₃, CoCO₃, LiOH, and CoO are referenced from Shanghai Nonferrous Metals Network (<https://hq.smm.cn/>).

Table S5. Energy consumption of different recycling methods.

Methods	Energy consumption (MJ/t)
Pyrometallurgy	5312
Hydrometallurgy	396
This work	2656

The energy consumption of pyrometallurgical and hydrometallurgical recycling was primarily derived from the EverBatt 2020 database. The dominant pyrometallurgical method usually requires a temperature of over 1000 °C, while this work requires a temperature of 500 °C and a shorter heating time, so we estimate that the energy consumption of this work is only 50% of the pyrometallurgical method.

Table S6. Calculation of total cost and possible profit of different recycling methods (1t LCO).

Methods	Materials cost (\$)	Process cost (\$)		Income (\$)	Profit (\$)
		Chemical cost (\$)	Energy cost (\$)		
Pyrometallurgy	5000	211.68	132.8	7980.07	2635.59
Hydrometallurgy	5000	255.68	9.9	8026.56	2760.98
This work	5000	2.63	66.4	9265.05	4196.02

- [1] B. Ravel, M. Newville, *J. Synchrotron Radiat.* **2005**, *12*, 537-541.
- [2] S. I. Zabinsky, J. J. Rehr, A. Ankudinov, R. C. Albers, M. J. Eller, *Phys. Rev. B* **1995**, *52*, 2995-3009.
- [3] Z. Xia, H. Zhang, K. Shen, Y. Qu, Z. Jiang, *Phys. Rev. B Condens. Matter* **2018**, *542*, 12-19.