

Supporting Information

Pt Single Atoms Anchored on CoO_x Nanoislands for Efficient Biomass-Derived 5-Methylfurfural Production

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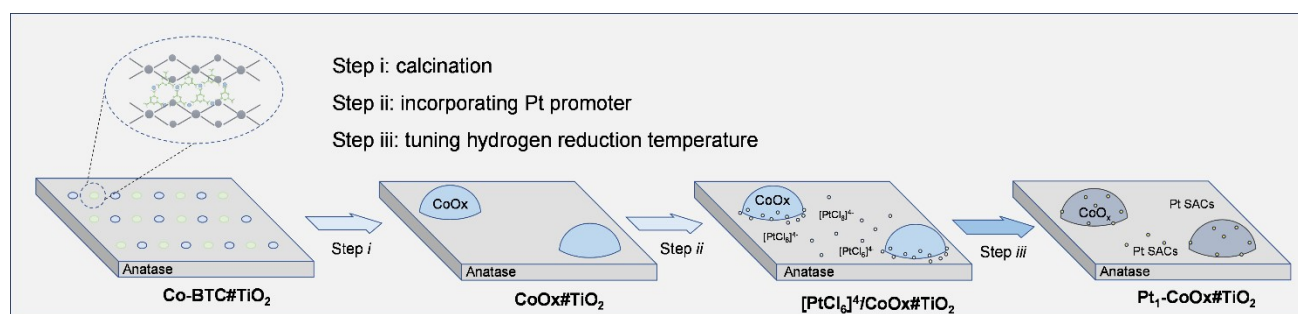
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Figures and Tables



Scheme S1 Schematic illustration of the synthesis process.

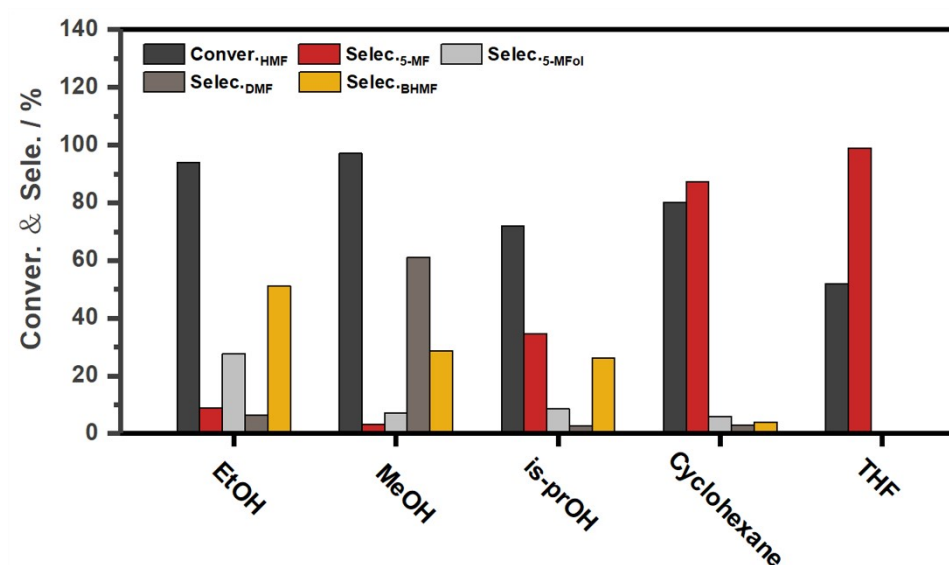


Fig. S1 Solvent screening for hydrolysis of HMF over the $\text{Pt}_1\text{-CoO}_x/\text{TiO}_2$. Reaction, 30 mg catalyst, 0.2 g HMF, 10 mL solvent, reacted at 200 °C for 3 h.

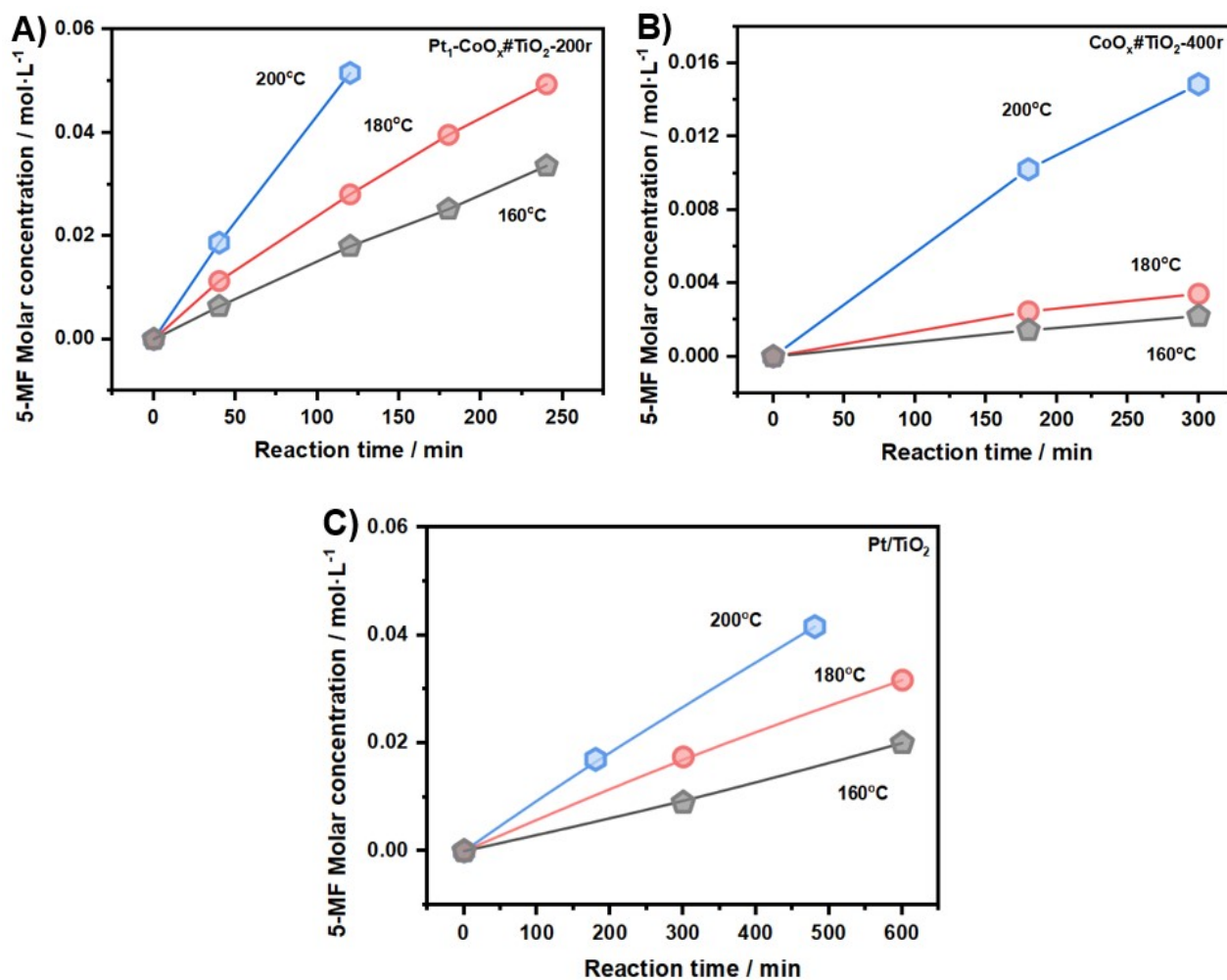


Fig. S2 Hydrogenolysis of HMF as a function of reaction time over different catalyst: (A) $\text{Pt}_1\text{-CoO}_x\#\text{TiO}_2$, (B) $\text{CoO}_x\#\text{TiO}_2$, (C) Pt/TiO_2 .

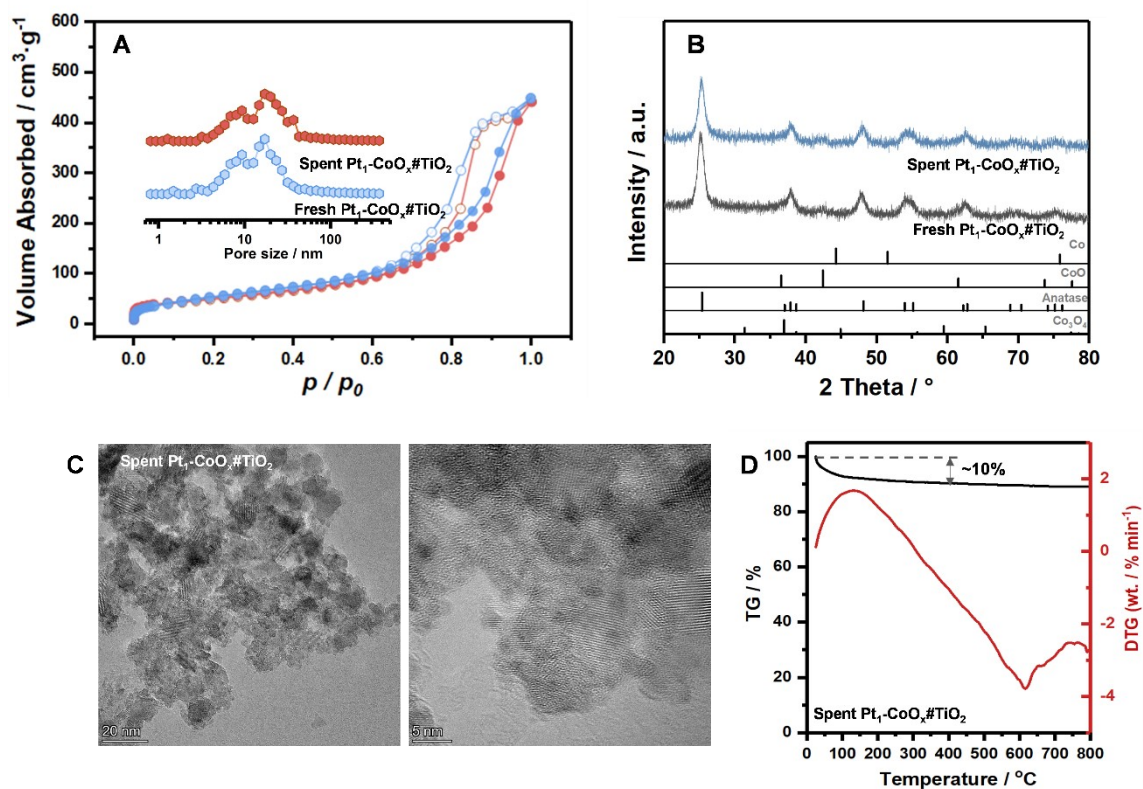


Fig. S3 Structure characterizations of spent $\text{Pt}_1\text{-CoO}_x\#\text{TiO}_2$: (A) Nitrogen sorption, (B) XRD pattern, (C) HRTEM images and (D) TG-DTG plot.

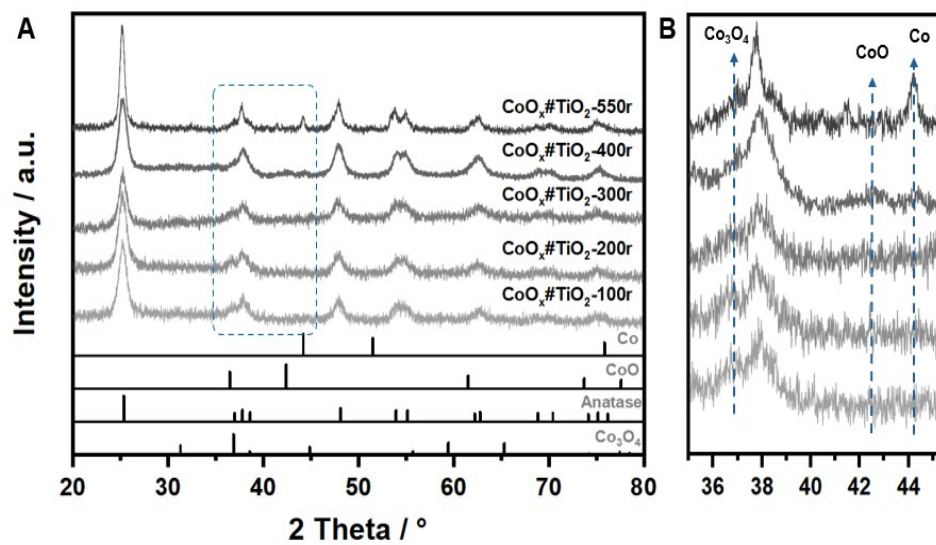


Fig. S4 XRD patterns of a) $\text{CoO}_x\#\text{TiO}_2$ reduced at various temperatures.

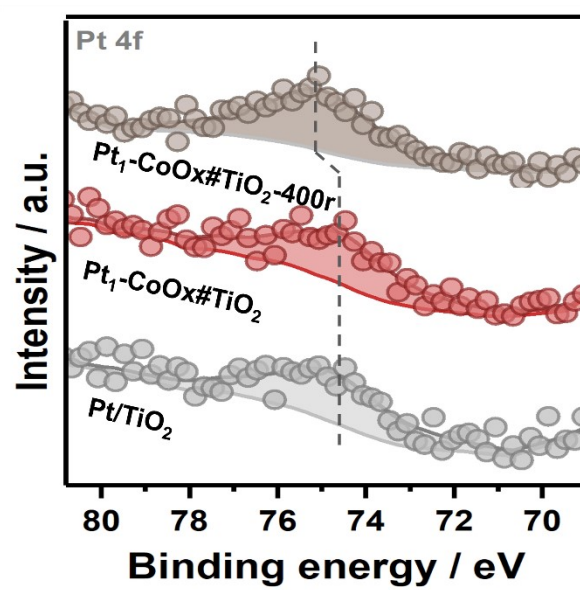


Fig. S5 XPS spectra of Pt 4f for various catalysts

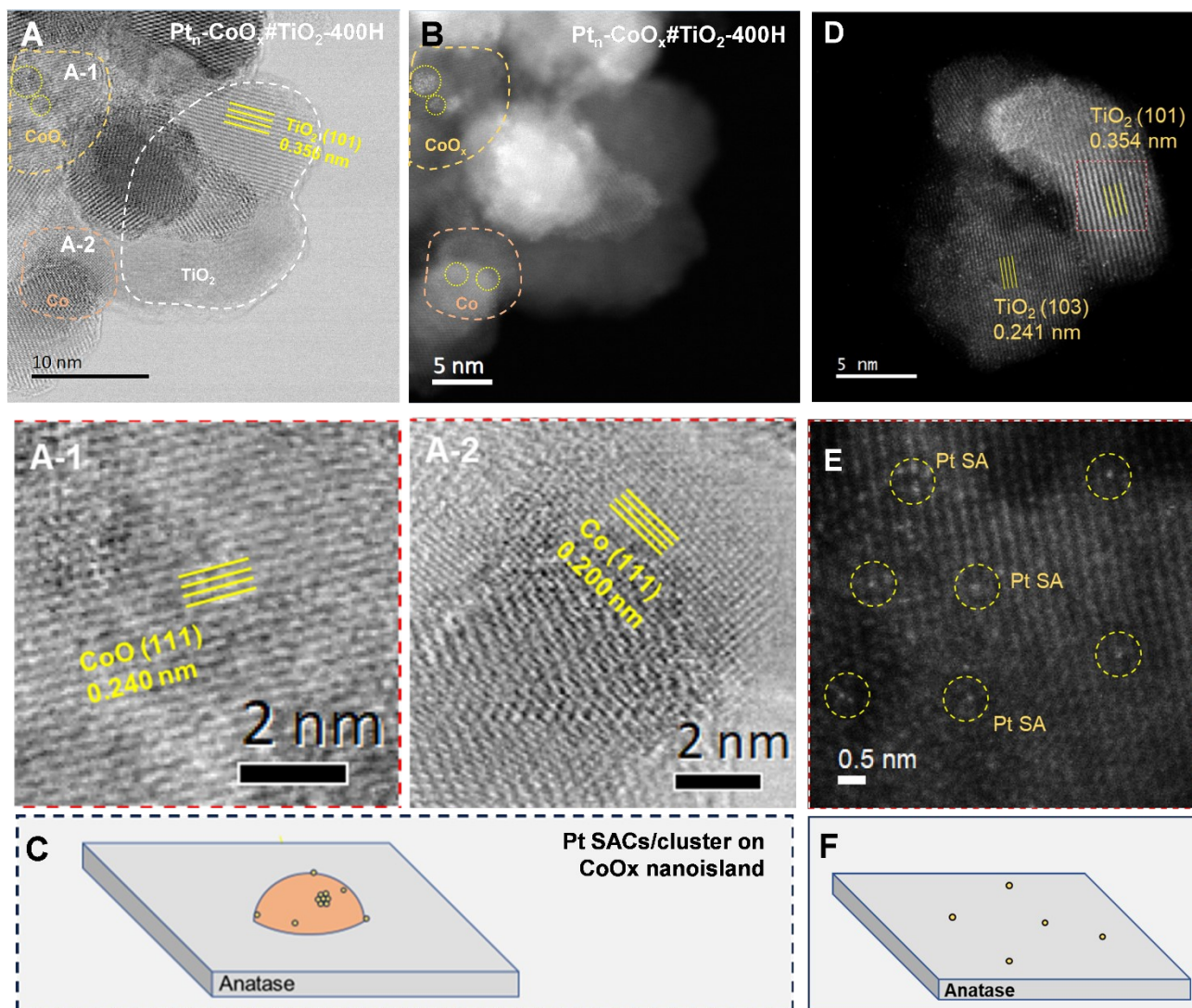


Fig. S6 Aberration corrected HAADF-STEM images showing atomic-scale features of (A-C) $\text{Pt}_n\text{-CoO}_x/\text{TiO}_2\text{-400r}$ and (D-F) Pt/TiO_2 .

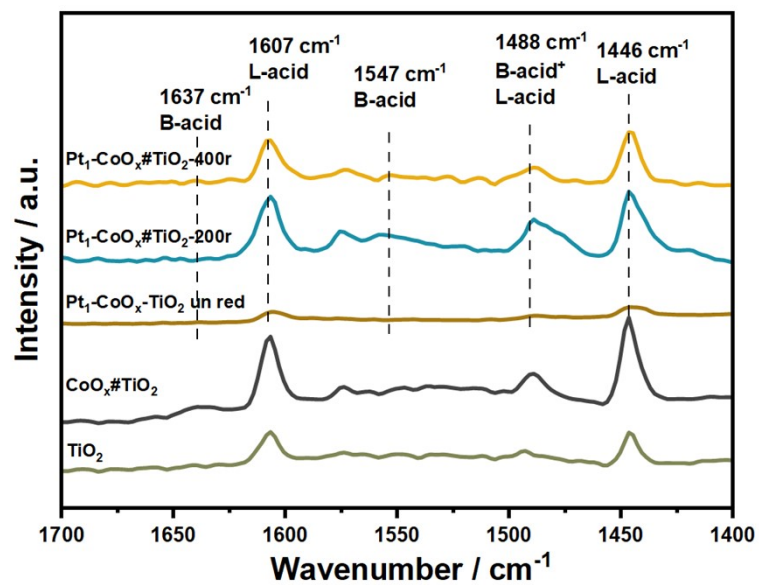


Fig. S7 Pyridine-IR spectrum of various catalysts.

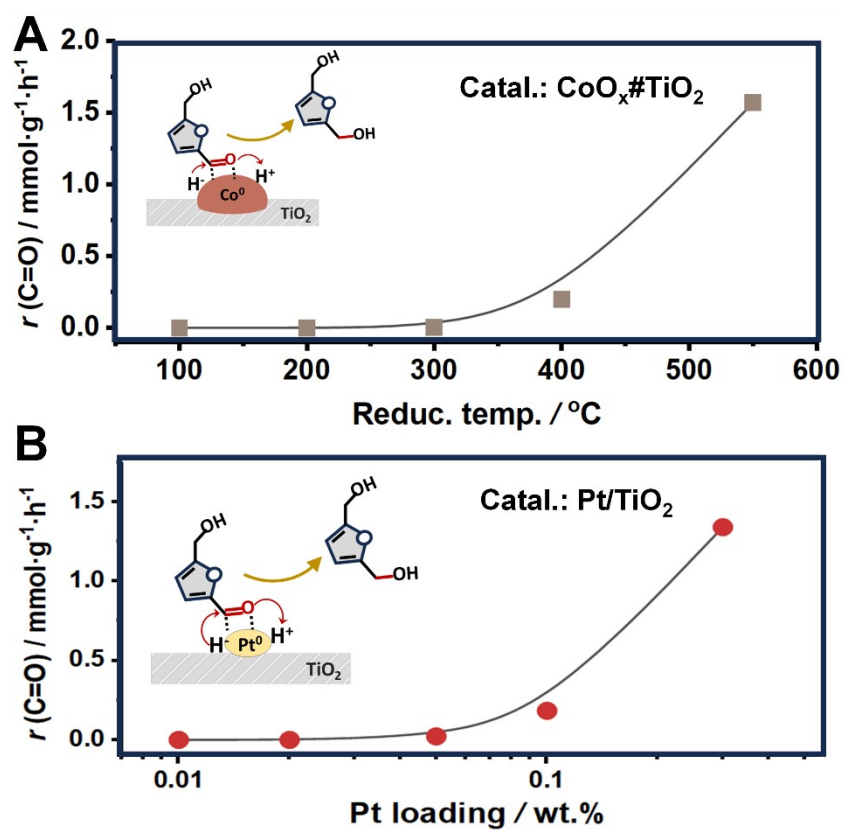


Fig. S8 Aldehyde hydrogenation over $\text{CoO}_x/\text{TiO}_2$ (A) and Pt/TiO_2 (B).

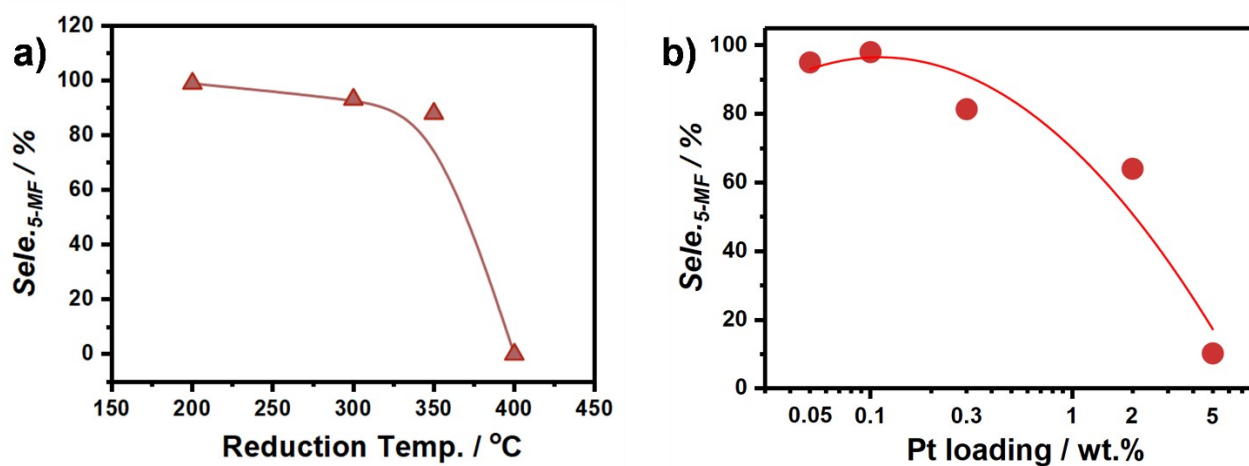


Fig. S9 Hydrodeoxygenation of HMF over the $\text{Pt}_1\text{-CoO}_x/\text{TiO}_2$ catalyst with various reduction temperatures (a) and Pt loadings (b). The 5-MF selectivity remains above 90% when the reduction temperature is 300 °C but begins to decline upon further increasing the temperature. Similarly, when the Pt loading reaches 0.2 wt.% under a reduction temperature of 200 °C, the selectivity drops below 90%. We attribute this critical threshold to the temperature-dependent formation of metallic cobalt species and Pt nanoparticle size evolution under different metal loadings.

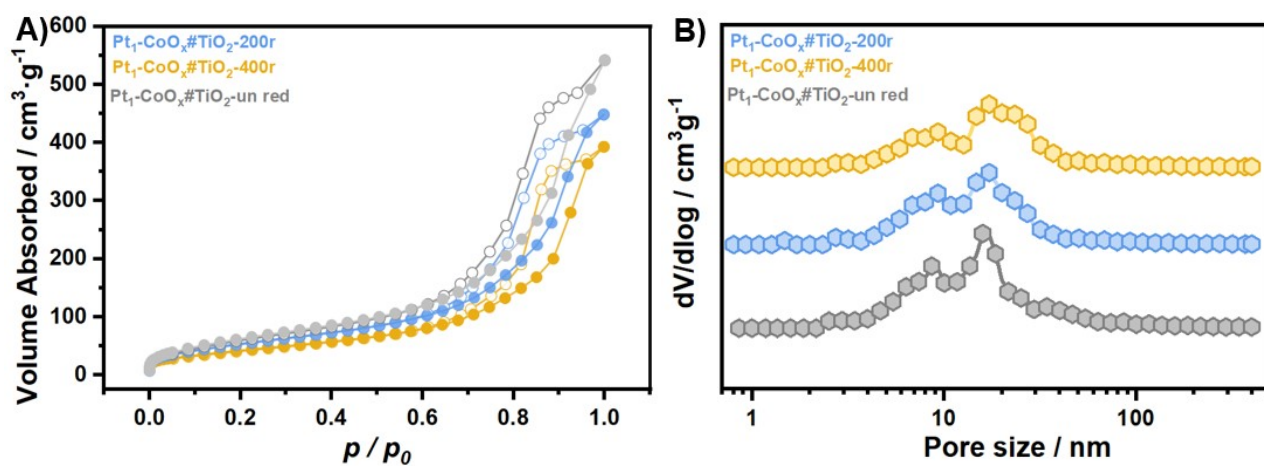


Fig. S10 (A) nitrogen isothermal ads-desorption curves and (B) corresponding pore size distribution plots of Pt₁-CoO_x#TiO₂ reduced with various temperatures.

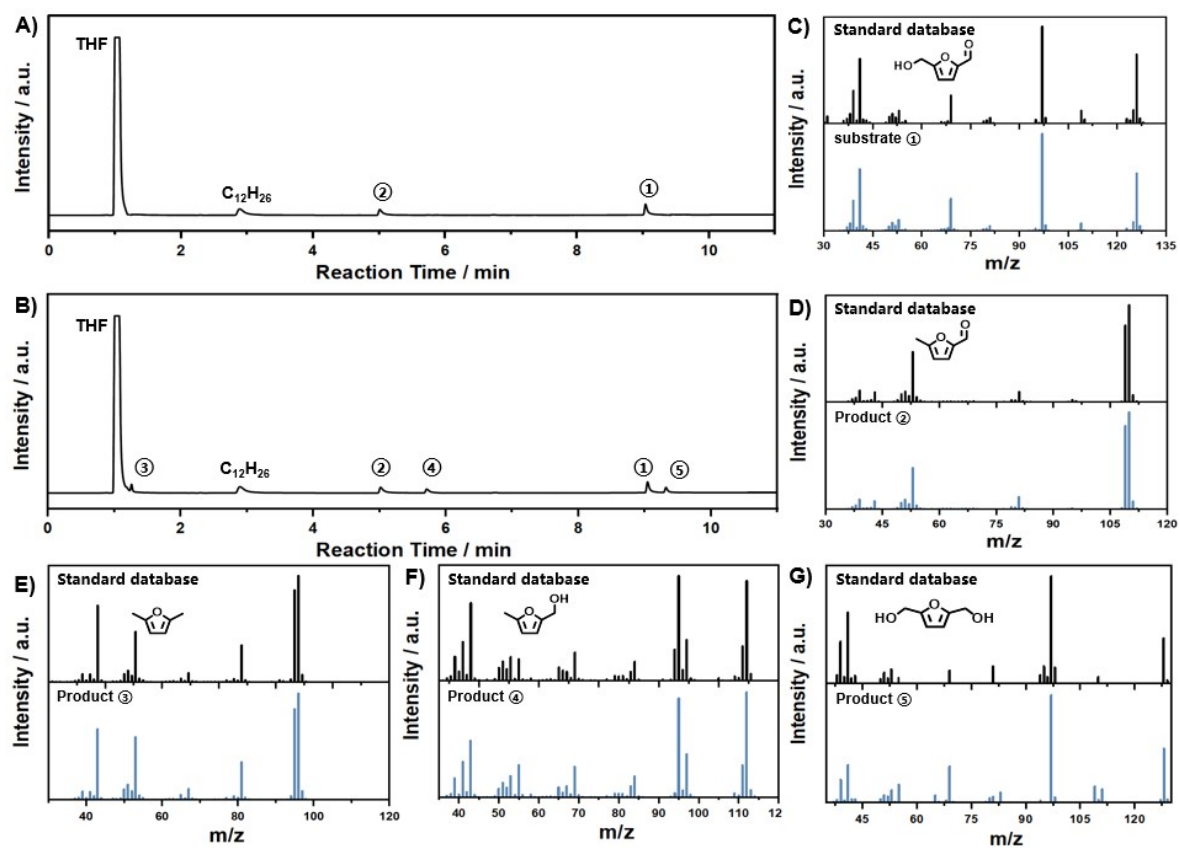


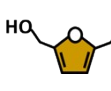
Fig. S11 Representative GC-MASS patterns for HDO of HMF over the different catalysts.

Table S1 Catalyst screening for HDO of HMF into 5-Hydroxymethylfurfural in recent literatures.

Catalyst	P_{H_2}	T/°C	t/h	Con. /%	Sele. ^{5-MF} /%	Productivity / mmol _{5-MF} g _{Catal.} ⁻¹ h ⁻¹	Ref
Pt ₁ -CoO _x #TiO ₂	1.0	160	3	33	100	4.40	This work
Pt ₁ -CoO _x #TiO ₂	1.0	180	3	37	100	4.93	
Pt ₁ -CoO _x #TiO ₂	1.0	200	3	56.4	98	7.37	
Au/a-TiO ₂	5	230	8	99.9	83.0	1.64	1
Au/Nb ₂ O ₅	5	230	8	99.9	61.2	1.21	1
Au/Al ₂ O ₃	5	230	8	81.3	45.6	0.904	1
Au/SiO ₂	5	230	8	99.9	25.6	0.507	1
Pt ₁ /Nb ₂ O ₅ -Ov	4	160	4	99.9	99.9	3.74	2
Pt@PVP/Nb ₂ O ₅	3	140	24	99.9	92	0.287	3
Pd-PVP/C (1:2) ^a	0.5	200	7.5	87	90	4.14	4
FPHS-Pd/C	4	100	12	100	90.1	1.77	5
Mn_N_Graphene	1	160	12	99.9	92	2.30	6
Au-4/TiO ₂ @NPC	-	180	1.5	100	95	1.97	7
Ni@NbO _x	4	160	4	94.3	91.8	2.16	8
Pd/Nb ₂ O ₅	4	160	4	92.9	71	1.65	9

^a The atmosphere is N₂.

Table S2 Hydrogenolysis of 5-Hydroxymethylfurfural over various selected catalysts. Reaction, 30 mg catalyst, 10 ml tetrahydrofuran(solvent), 0.2 g HMF, reacted at 200 °C and 1 MPa for 3 h.

Entry no.	Catalyst	Conver. / %	Selec. / %				
			5-MF	DMF	5-MFOL	BHMF	Others ^d
		HMF 					
1	no catalyst	<1	—	—	—	—	—
2	Pristing TiO ₂	<1	—	—	—	—	—
3	CoO _x #TiO ₂	15	56.8	—	—	—	43.2
4 ^a	CoO _x #TiO ₂	26	64.7	1.4	2.6	4.2	27.1
5	Pt/TiO ₂	18.4	94.1	2.40	3.54	—	—
6 ^b	CoO NPs	99	53	6.4	7.2	5.1	28.3
7	Pt ₁ -CoO _x #TiO ₂	42	69	6.0	9.05	15.6	0.35
8 ^c	Pt ₁ -CoO _x #TiO ₂	44	92	—	—	—	—

^a CoO_x#TiO₂-400r was reduced by hydrogen at 400 °C; ^b CoO nanoparticles (NPs) were purchased from Macklin Agent Cop.; ^c the 6th recycle run after regeneration; ^d others mainly refer to side products derived from aldol condensations, such as 4-(2-furyl)-3-buten-2-one, 1,4-pentadien-3-one, 1,5-di-2-furanyl, etc¹⁰.

Table S3 Sample specifications for various catalysts.

Catalyst	$S_{\text{BET}} / \text{m}^2\text{g}^{-1}$	<i>Pt loading wt.%</i>	<i>Co loading wt.%</i>	$D_{\text{pore}} / \text{nm}$
Pt ₁ -CoO _x #TiO ₂ -un red	241	0.1	11	9.58
Pt ₁ -CoO _x #TiO ₂ -200r	207	0.1	11	9.73
Pt ₁ -CoO _x #TiO ₂ -400r	160	0.1	11	10.7

The mass percentages of Pt and Co were determined by ICP analysis.

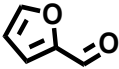
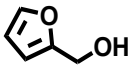
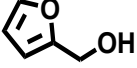
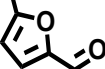
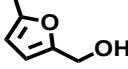
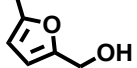
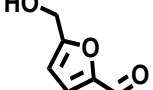
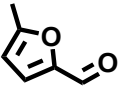
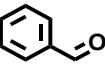
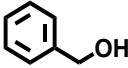
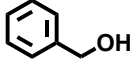
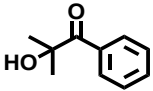
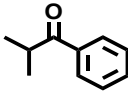
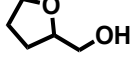
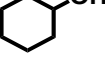
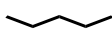
Table S4 Sample specifications over different catalyst.

Sample	H ₂ ads. / mmol g ⁻¹ ^a	Acidity /mmol g ⁻¹ ^b
Pt/TiO ₂	0.31	1.28
CoO _x #TiO ₂	0.21	2.27
Pt ₁ -CoO _x #TiO ₂	1.13	4.33
Pt ₁ -CoO _x #TiO ₂ -400r	2.6	4.54

^a Hydrogen adsorption amount was calculated by data derived from H₂-TPD test;

^b Acidity was calculated by data derived from NH₃-TPD test;

Table S5 Substrate scope over the Pt₁-CoO_x#TiO₂. Reaction, 0.1 g substrate, 30 mg catalyst, 200 °C, 2 MPa, reacted for 3h. For furan compounds (e.g., furfural, 2-methyl furfural, and their corresponding alcohols), the catalyst demonstrated high dehydroxylation activity and low aldehyde hydrogenation activity; yet, this distinct activation behavior toward aldehydes versus alcohols was far less pronounced in benzene-derived aromatic substrates.

Entry No.	Substrate	Conver. (%)	Product	Selec. (%)
1		2		-
2		67		>99
3		<1		-
4		59		59
5		53		98
6a		41		76
7a		28		>99
8		>99		38
9		<1		-
10b		3		>99
11c		10		>99
12		<1		-

^a reaction at 150 °C; ^b reaction at 3.8 MPa H₂; ^b reaction for 5 h.

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