### Supplementary Materials for:

## Unveiling microbial single-cell growth dynamics under rapid periodic oxygen oscillations

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Supplementary Materials and Methods



**Figure S1.**  $O_2$  concentration in the fluid channel of the microfluidic chip determined by RTDP lifetime measurement with FLIM under oscillating  $O_2$  environments at various oscillation half-periods (*T*').



**Figure S2.** Single-cell area ( $A_{singlecell}$ ) plotted over time under oscillating O<sub>2</sub> environments at various oscillation half-periods (T').



Figure S3. Geometry of the PDMS chip generated for gas diffusion simulation.

# **Supplementary Materials and Methods**

#### Simulation setup

Fluid and gas flow through the respective channels were computed by solving the time-dependent Navier-Stokes equations for laminar, incompressible flow, as follows.

$$\frac{\delta\rho}{\delta t} + \nabla \cdot (\rho \ u) = 0$$
  
$$\rho \frac{\delta u}{\delta t} + \rho (u \cdot \nabla) u = \nabla \cdot [-pI + K]$$
  
$$K = \mu (\nabla u + (\nabla u)^T)$$

Here,  $\rho$  represents density (kg/m<sup>3</sup>), *u* is velocity vector (m/s), *p* denotes pressure (Pa), *I* is identity matrix, and  $\mu$  is dynamic viscosity (Pa · s). Boundary conditions at the PDMS block and the glass plane are defined as follows.

$$u = 0$$
 (wall)

$$u = -nU_0$$
 (inlet)

$$[-pI+K]n = -p_0n \qquad (outlet)$$

n is the boundary normal vector, pointing outward from the domain, and  $U_0$  is the normal inflow speed.

With *u* defined by the Navier Stokes equations,  $O_2$  transport via convection and diffusion was simulated using the diluted species transport module in COMSOL, incorporating specific boundary conditions as detailed below. The  $O_2$  concentration in the surrounding air is assumed to remain constant at 21%.

$$abla \cdot J_i + u \cdot 
abla c_i = R_i$$
 $J_i = -D_i 
abla c_i$ 

*i* is the index for different domains (water, air, PDMS), and  $D_i$  represents the diffusion coefficient for each domain *i*. The velocity *u* within the PDMS domain is set to 0.  $c_i$  denotes the O<sub>2</sub> concentration (mol/m<sup>3</sup>)

Table S1.	Parameters	used in	simulation	(1	atm, 310.15 k	C)
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	water	PDMS	air (21% O <sub>2</sub> )	air (100% O <sub>2</sub> )
$S (mol/m^3)$	0.218 [1]	1.25 <sup>[1]</sup>	8.1375	-
<i>D</i> (m <sup>2</sup> /s)	$2.7  imes 10^{-9}$ [1]	$7 imes 10^{-9}$ [1]	$2.3  imes 10^{-5}$	-
ho (kg/m <sup>3</sup> )	993.31	-	1.1383	1.24
$\mu$ (Pa · s)	0.00101	-	$1.814\times10^{-5}$	-

in each domain *i*, and *R* describes sources or sinks. Boundary conditions between different domains are defined as follows.

(between PDMS and gas / water channel)	$\frac{c_i}{S_i} = \frac{c_j}{S_j}$
(between PDMS and surrounding air)	$c_{\rm PDMS-air} = S_{\rm PDMS} = 1.25 \text{ mol/m}^3$
(at the glass plate)	$-n \cdot J_i = 0$
(between water and air)	$c_{\text{water-air}} = S_{\text{water}} = 0.218 \text{ mol/m}^3$

 $S_i$  represents the solubility of O<sub>2</sub> (mol/m<sup>3</sup>) in each domain *i* at 1 atm and 310.15 K. The initial solubility in air,  $S_{air}$ , was calculated to be 8.134 mol/m<sup>3</sup>. The parameters used in the simulation were summarized in Table S1.

The mesh for the given geometry was generated using a semi-automated approach. First, a hexahedral mesh was created for the fluid channel. The boundaries adjacent to surrounding parts were then converted to a triangular mesh. Finally, the remaining domains were meshed by a tetrahedral mesh with an "extra-fine" resolution.

## References

1. M.-C. Kim, R. H. W. Lam, T. Thorsen and H. H. Asada, Microfluid. naonfluid., 2013, 15, 285-296.