

## Supplementary Information

### **Functionalized Mg/Fe layered double hydroxides for high adsorption capacity of rare earth from waste water**

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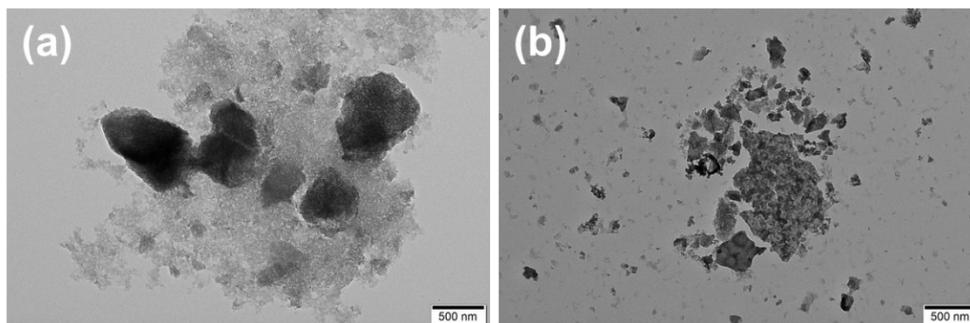
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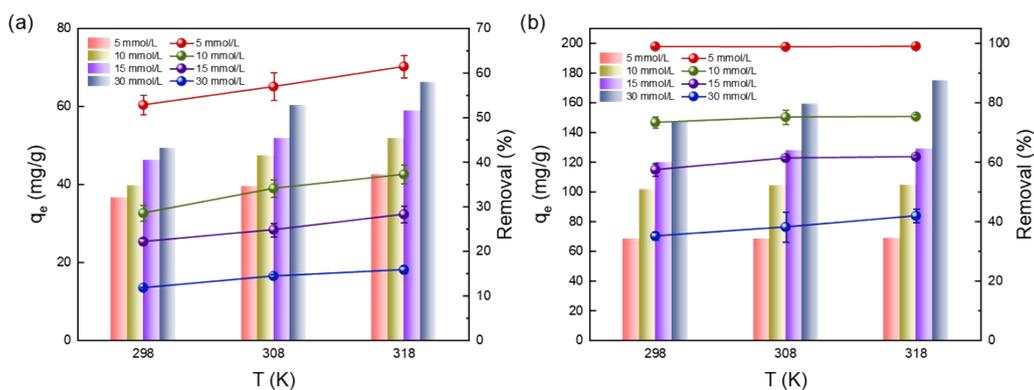
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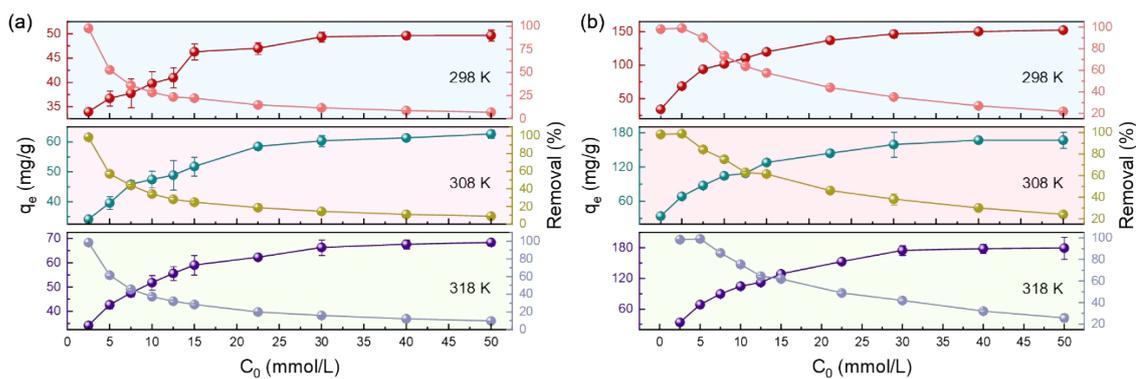
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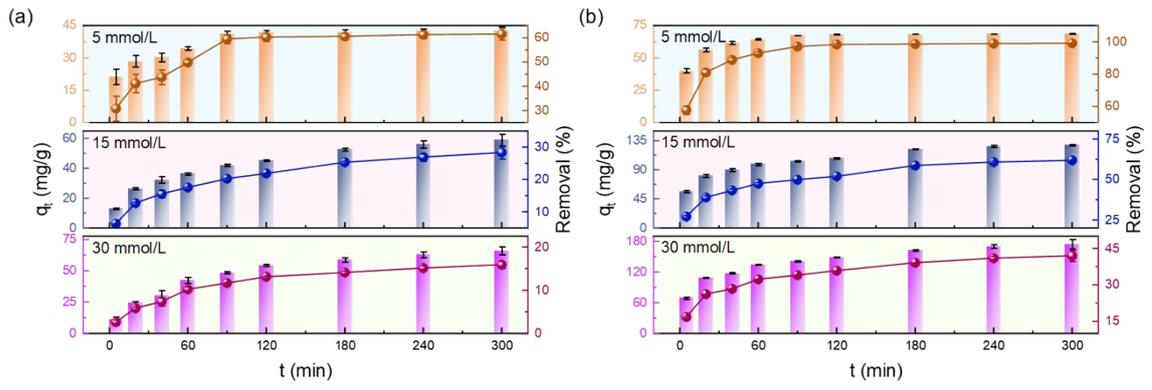
**Figure S.1** (a) TEM images of TC-MgFe LDH; (b) TEM images of TC-MgFe LDH@La<sup>3+</sup>.



**Figure S.2** Effect of different temperatures on the adsorption of La<sup>3+</sup> by (a) MgFe LDH and (b) TC-MgFe LDH.



**Figure S.3** Effect of initial concentration on the adsorption of La<sup>3+</sup> by (a) MgFe LDH and (b) TC-MgFe LDH at different temperatures.



**Figure S.4** Effect of contact time on the adsorption of La<sup>3+</sup> by **(a)** MgFe LDH and **(b)** TC-MgFe LDH at different initial concentrations.

## Adsorption isotherm Equations:

The Langmuir adsorption isotherm model is expressed by formula (S.1):

$$q_e = \frac{q_m K_L C_e}{1 + K_L C_e} \quad (\text{S.1})$$

$C_e$  (mg/L) and  $q_e$  (mg/g) are the equilibrium concentration in the liquid phase and the equilibrium adsorption capacity during the adsorption process, respectively.  $q_m$  (mg/g) represents the maximum adsorption capacity, and the adsorption rate constant  $K_L$  (L/mg) characterizes the affinity between LDH and  $\text{La}^{3+}$ .

The Freundlich adsorption isotherm model is expressed by formula (S.2):

$$q_e = K_F C_e^{1/n} \quad (\text{S.2})$$

$K_F$  is the Freundlich constant related to adsorption capacity and represents a measure of the surface area of the adsorbent. The heterogeneity of the LDH surface and the degree of adsorption can be quantified by the size of  $1/n$ . The  $1/n$  value for favorable adsorption ranges from 0-1, with larger values indicating greater attraction between LDH and  $\text{La}^{3+}$  and a more uneven distribution of the adsorbent.

The Temkin adsorption isotherm model is expressed by formula (S.3):

$$q_e = A_T + B_T \ln C_e \quad (\text{S.3})$$

The D-R adsorption isotherm model is expressed by formula (S.4):

$$q_e = q_m \exp(-k_D \varepsilon^2) \quad (\text{S.4})$$

$$\varepsilon = RT \ln\left(1 + \frac{1}{C_e}\right) \quad (\text{S.5})$$

$$E = (2 \times k_D)^{-\frac{1}{2}} \quad (\text{S.6})$$

In the above formula,  $k_D$  is a parameter related to the adsorption free energy  $E$ , and the symbol  $\varepsilon$  is the Polanyi potential, and its correlation can be expressed by formula (S.5). When the adsorbent is transferred from the solution to the solid surface, the

average E of each adsorbent molecule can be evaluated by the D-R parameter  $k_D$ , which can be calculated using formula (S.6).

### **Adsorption kinetic Equations:**

The two kinetic models can be expressed by formulas (S.7) and (S.8) respectively.

$$q_t = q_e(1 - e^{-k_1 t}) \quad (\text{S.7})$$

$$q_t = \frac{k_2 q_e^2 t}{1 + k_2 q_e t} \quad (\text{S.8})$$

In the above formula,  $q_e$  (mg/g) is the equilibrium adsorption capacity, and  $q_t$  (mg/g) is the adsorption capacity at time t. The constants  $k_1$  ( $\text{min}^{-1}$ ) and  $k_2$  (g/mg·min) are the rate constants of the PFO and PSO kinetic models, respectively.

**Table S.1** The maximum adsorption amount of  $\text{La}^{3+}$  on MgFe LDH and TC-MgFe LDH at different temperatures.

Adsorbent	Temperature (K)	$q_m$ (mg/g)
MgFe LDH	298	49.65
	308	62.68
	318	68.38
TC-MgFe LDH	298	152.32
	308	166.97
	318	179.38