

Supporting Information

Separation of Taurine and Na₂SO₄ Using in Situ Formation of Deep Eutectic Solvents: Experiments and Computation Simulation

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The identification of present mixture as DES

Based on DSC results, the melting points of Tau/MEA (1:5) DES was 270 K. And the value was expressed in the solid-liquid equilibrium (SLE) diagram as Figure S1. The red lines was obtained by the melting points and $\Delta_{fus}H$ (the enthalpy of fusion) of two pure compounds [1,2]. It can be seen that the melting point of the prepared mixture was lower than the ideal eutectic point represented as $T_{E, \text{ideal}}$. Therefore, the present mixture can be named as DES according to the broad definition.

The melting point of ideal binary mixture was calculated as following,

$$\frac{1}{T_m} = \frac{1}{T_{m,A}} + \frac{R}{H_{fus,A}} \ln \frac{1}{x_A} \quad (\text{S1})$$

Where $T_{m,A}$ is the melting point of pure substance A, $H_{fus,A}$ is the fusion enthalpy of A, x_A is the molar fraction of A, and R is ideal gas constant.

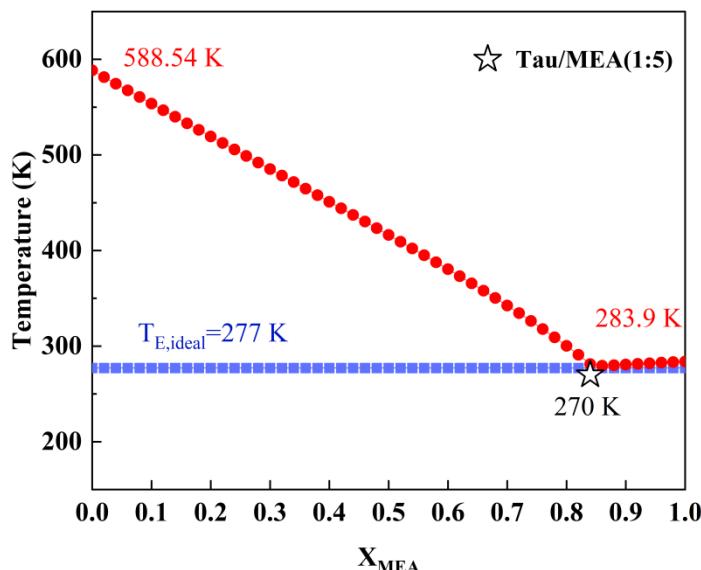


Figure. S1. Melting point and ideal binary solution phase diagram for Tau/MEA (1:5) DES.

[1] X.-W. Han, C.-R. Zhou, X.-H. Shi, Determination of specific heat capacity and standard molar combustion enthalpy of taurine by DSC. *J Therm Anal Calorim* 2012;109:441-6. <https://10.1007/s10973-011-1670-y>.

[2] A. Penttilä, P. Uusi-Kyyny, A. Salminen, J. Seppälä, V. Alopaeus, A comprehensive thermodynamic study of heat stable acetic acid salt of monoethanolamine. *International Journal of Greenhouse Gas Control* 2014;22:313-24. <https://doi.org/10.1016/j.ijggc.2013.12.001>.

The selectivity parameter between taurine and Na₂SO₄

The selectivity parameter between taurine and Na₂SO₄ was calculated to further demonstrate the effectiveness of the separation strategy, which are defined as follows:

$$S = \frac{m_T}{m_S} \quad (\text{S2})$$

where m_T and m_S are the solubility of Tau and Na₂SO₄ in the DES, respectively.

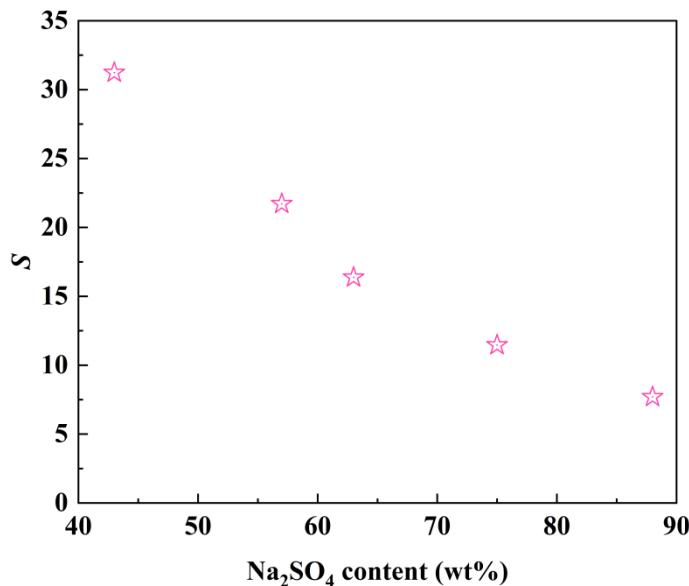


Figure. S2. The selectivity parameter between taurine and Na₂SO₄.

The raw data of Tau yield affected by molar ratio under the condition of Tau:Na₂SO₄ (3:4, mass ratio)

Experiment-1

| Molar ratio (Tau:MEA) | Original Tau/g | Recycled Tau/g | Yield% |
|--------------------------|----------------|----------------|--------|
| 1:5 | 3.7459 | 3.6528 | 97.51 |
| 1:6 | 3.6720 | 3.1593 | 86.04 |
| 1:7 | 3.8438 | 3.1375 | 81.62 |
| 1:8 | 4.3676 | 3.6169 | 82.81 |
| 1:9 | 3.8245 | 3.8171 | 99.08 |

Experiment-2

| Molar ratio (Tau:MEA) | Original Tau/g | Recycled Tau/g | Yield% |
|--------------------------|----------------|----------------|--------|
| 1:5 | 12.3321 | 12.256 | 99.38 |
| 1:6 | 3.9715 | 3.3288 | 83.82 |
| 1:7 | 3.9171 | 3.1375 | 80.10 |
| 1:8 | 3.7206 | 3.2122 | 86.33 |
| 1:9 | 3.4922 | 3.2720 | 93.69 |

Experiment-3

| Molar ratio (Tau:MEA) | Original Tau/g | Recycled Tau/g | Yield% |
|--------------------------|----------------|----------------|--------|
| 1:5 | 3.7525 | 3.6479 | 97.21 |
| 1:6 | 3.7407 | 3.2073 | 85.74 |
| 1:7 | 4.1681 | 3.3919 | 81.38 |
| 1:8 | 3.8427 | 3.2221 | 83.85 |
| 1:9 | 3.5032 | 3.3690 | 96.17 |

Raw data of the experiment affected by Na₂SO₄ content.**Experiment-1**

| Na ₂ SO ₄ content/wt% | Original Tau/g | Recycled Tau/g | Original Na ₂ SO ₄ /g | Removal Na ₂ SO ₄ /g |
|--|----------------|-------------------|--|---|
| 43 | 3.9132 | 3.8349 | 2.9349 | 2.8121 |
| 57 | 3.5955 | 3.5329 | 4.794 | 4.6340 |
| 63 | 3.3728 | 2.9046 | 5.6213 | 5.4439 |
| 75 | 2.0382 | 1.3792 | 6.1146 | 5.9942 |
| 88 | 1.0767 | 0.5706 | 7.5369 | 7.4627 |

Experiment-2

| Na ₂ SO ₄ content/wt% | Original Tau/g | Recycled Tau/g | Original Na ₂ SO ₄ /g | Removal Na ₂ SO ₄ /g |
|--|----------------|-------------------|--|---|
| 43 | 3.6651 | 3.5918 | 2.7488 | 2.6338 |
| 57 | 3.4876 | 3.4269 | 4.6501 | 4.4950 |
| 63 | 3.0383 | 2.6166 | 5.0638 | 4.9040 |
| 75 | 2.4522 | 1.6594 | 7.3566 | 7.2118 |
| 88 | 1.1696 | 0.6199 | 8.1872 | 8.1067 |

Experiment-3

| Na ₂ SO ₄ content/wt% | Original Tau/g | Recycled Tau/g | Original Na ₂ SO ₄ /g | Removal Na ₂ SO ₄ /g |
|--|----------------|-------------------|--|---|
| 43 | 4.0435 | 3.9626 | 3.0326 | 2.9058 |
| 57 | 3.3369 | 3.2788 | 4.4492 | 4.3008 |
| 63 | 2.8642 | 2.4666 | 4.7737 | 4.6230 |
| 75 | 2.2532 | 1.5247 | 6.7596 | 6.6266 |
| 88 | 1.1729 | 0.6216 | 8.2103 | 8.1295 |