Supplementary Information (SI) for Nanoscale. This journal is © The Royal Society of Chemistry 2025

# Supplementary Information (SI<sup>†</sup>)

Breaking scaling relationship limitations in peroxymonosulfate activation through

electronegativity-driven Fe-Mn dual-metal synergy

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mg L<sup>-1</sup>.

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#### 1. Materials

Iron(III) chloride (FeCl<sub>3</sub>, >99%), manganese(II) chloride (MnCl<sub>2</sub>, >99%), formamide solution (FA), dicyandiamide (C<sub>2</sub>H<sub>4</sub>N<sub>4</sub>, 99.0%), zinc chloride (ZnCl<sub>2</sub>, >99%), bisphenol-A (BPA,  $\geq$ 99%), phenol( $\geq$ 99%), 4-chlorophenol (4-CP, >99%), 2,4-dichlorophenol (2,4-DCP, 99%), 2,4,6-trichlorophenol (2,4,6-TCP, 99%), sulfamethazine (SMT, >99%), sulfamethazole (SMT, >99%), ofloxacin (OFX, 99%), p-nitrophenol (4-NP, 99%), acetaminophen (AcP, 99%), 4methoxyphenol (MQ, 99%), 4-bromophenol (BP, 99%), 4-hydroxybenzaldehyde (HBAI, 99%), hydroxybenzoic acid (HBA,99%), o-nitrophenol (2-NP, 99%), ethanol (75%), 2KHSO<sub>5</sub>•KHSO<sub>4</sub>•K<sub>2</sub>SO<sub>4</sub> (PMS, 42%–46%), benzoic acid (BA, 99%), nitrobenzene (NB, 99%), parachlorobenzoic-acid (*p*-CBA, 99%), furfuryl alchohol (FFA,  $\geq$ 99.5%), sodium thiocyanate (NaSCN, 99%), methanol (MeOH,  $\geq$ 99%), tert-butanol (TBA,  $\geq$ 99.5%), chloroform (CF,  $\geq$ 99.5%), potassium iodide (KI,  $\geq$ 99%), methyl phenyl sulfoxide (PMSO, 98%), humic acid (HA, >99%), 2,2-azino-bis (3-ethylbenzothiazoline-6-sulfonate) (ABTS, >99%), and boric acid buffer were acquired from Macklin and Aladdin Biochemical Technology Co. Ltd. without further purification.

#### 2. Preparation of Catalysts

NC preparation. ZnCl<sub>2</sub> (2.59 g) was dissolved in formamide solution (200 mL) under strong stirring at 30 °C for 1 h to form a homogeneous solution. The resulting solution was then transferred to a Teflon-lined steel autoclave and heated at 180 °C for 12 h, followed by cooling overnight. The resulting precipitate was filtered and washed several times with ethanol and deionized water and dried at 60 °C for 24 h. Subsequently, the precursor was calcined at 900 °C for 2 h under N<sub>2</sub> atmosphere at a heating rate of 5 °C min<sup>-1</sup> to obtain NC.

Fe-SAC preparation. In the synthesis of Fe-N<sub>4</sub> SAC, FeCl<sub>3</sub>· $6H_2O$  (81.1 mg) and ZnCl<sub>2</sub> (2.59 g) were dissolved in formamide solution (200 mL), and the mixture was stirred continuously for 1 h to ensure homogeneity. This homogeneous solution was heated at 180 °C for 12 h in a

Teflon-lined autoclave. After cooling to room temperature, the resulting precipitate was washed with ethanol and DI water and then dried in an oven at 60 °C for 24 h. The dried powder was subsequently calcined at 900 °C at a heating rate of 5 °C min<sup>-1</sup> for 1 h under N<sub>2</sub> atmosphere to obtain Fe-N<sub>4</sub> SAC.<sup>1</sup>

Mn-SAC preparation. In the synthesis of Mn-N<sub>4</sub> SAC, dicyandiamide (5.0 g) was heated to 550 °C at a rate of 2.5 °C min<sup>-1</sup> and maintained at this temperature for 4 h in a muffle furnace. After cooling to room temperature, the yellow residue was grinded to obtain  $C_3N_4$ . Subsequently,  $C_3N_4$  (0.5 g) and MnCl<sub>3</sub> (40.32 mg) were thoroughly grinded in a mortar. The resulting mixture was then calcinated at 550 °C, at a rate of 2.5 °C min<sup>-1</sup> under N<sub>2</sub> atmosphere for 4 h. Finally, the product was washed with DI water, dried at 60 °C for 12 h, and collected after grinding to obtain Mn-N<sub>4</sub> Mn-SAC.<sup>2</sup>

#### 3. Electrochemical Measurements

An electrochemical workstation (CHI 760E, Chenhua Instrument Co., China) utilizing a threeelectrode configuration was used to assess electrochemical impedance spectroscopy (EIS), linear sweep voltammetry (LSV), and current-time (i-t) measurements. The catalysts were coated on a glassy carbon electrode (GCE), serving as the working electrode, while platinum (Pt) and silver/silver chloride (Ag/AgCl) electrodes acted as the counter and reference electrodes, respectively. To prepare the catalyst-modified GCE, 10 mg of the catalyst was dispersed into a mixture of 0.2 mL of 5% Nafion solution, 0.1 mL of isopropanol, and 2.7 mL of DI water. This mixture was then subjected to ultrasonic treatment for 30 min to form a homogeneous catalyst ink. Subsequently, 5  $\mu$ L of this ink was deposited onto the GCE surface. Before each test, the GCE was polished with alumina slurries on a felt pad, rinsed with DI water, and coated with the catalyst ink. EIS measurements were conducted in an electrolyte composed of 50 mL of BPA solution (20 mg L<sup>-1</sup>) within a sweep range of 1×10<sup>-2</sup> to 1×10<sup>6</sup> Hz. For LSV and i-t measurements, 200 mmol L<sup>-1</sup> boric acid buffer was used as the electrolyte. The current response at the working electrode was recorded while sweeping the potential from 0.2 to 1.4 V at a scan rate of 10 mV s<sup>-1</sup>. Additionally, i-t curves for the Fe-Mn DAC electrode were recorded at 0.5 V vs. Ag/AgCl.

### 4. Determination of PMS consumption

The concentration of PMS remaining in the solution was determined using a colorimetric method. A 0.1 mL reaction sample was collected and filtered through a 0.22  $\mu$ m filter. Subsequently, 0.4 mL ABTS (10 mM), 0.2 mL Co<sup>2+</sup> (10 mM), and 9.4 mL DI water were immediately added to the filtered sample and allowed to react for 10 min. This reaction produced a green-colored ABTS radical cation. The resulting solution was then analyzed using a UV/Vis spectrophotometer (UV1800, Shimadzu, Japan) at its maximum absorbance wavelength of 735 nm.<sup>3</sup>

#### 5. Mathematical formulations and calculations

The pseudo-first-order kinetic rate constant (k) of the degradation was calculated as follows:

$$-\ln(\frac{C_t}{C_0}) = kt$$

Where  $C_0$  and  $C_t$  represent the initial and the instant concentration of BPA.

The turnover frequency of the degradation was calculated as follows:

$$TOF = \frac{k}{\left[catalyst\right]_0}$$

where k is the rate constant of the reaction and [catalyst]<sub>0</sub> is the loading of the catalyst. The initial reaction rate for metal loading was calculated as follows:

$$k_{\rm MC} = k / {\rm wt}\%$$

Where, k is the initial reaction rate, and MC is wt.% metal loading in the catalyst.<sup>[1]</sup> The initial reaction rate per metal site was calculated as follows:

$$k(metal site) = \frac{k \times M}{(m \times wt.\%)}$$

Where k is the initial reaction rate, M is the atomic mass of the metal, m is the catalyst mass used in the reaction, and wt.% is the metal loading in the catalyst.<sup>[1]</sup>

#### 6. Radical probe experiments

In this study, the steady-state concentration of  $SO_4^{--}$ ,  $\cdot OH$ ,  $O_2^{--}$ , and  ${}^1O_2$  in the Fe-Mn DAC/PMS system were calculated using BA, NB, *p*-CBA, and FFA as probe compounds. Since the probe compounds were low concentration compared to BPA (20 mg L<sup>-1</sup> for BPA, 2 mg L<sup>-1</sup> for BA, NB, FFA, and *p*-CBA), which would not affect BPA degradation.<sup>[4]</sup> The calculation methods of steady-state concentration of  $\cdot OH$ ,  $SO_4^{--}$ ,  ${}^1O_2$ ,  $O_2^{--}$  are as follows:

$$(k_{BA, OH} \cdot [\cdot OH]_{ss} + k_{BA, SO_4} \cdot [SO_4^{\cdot -}]_{ss})t = k_{BA}t$$
(1)

$$(k_{NB,OH} [\cdot OH]_{ss} + k_{NB,SO_4} [SO_4]_{ss})t = k_{NB}t$$
(2)

$$(k_{p-CBA,OH} \cdot [\cdot OH]_{ss} + k_{p-CBA,SO_4} \cdot [SO_4^{\cdot -}]_{ss} + k_{pCBA,1O_2} [1_{O_2}]_{ss} + k_{p-CBA,O_2} \cdot [O_2^{\cdot -}]_{ss})t = k_{p-CBA}t$$

(3)

$$(k_{FFA, OH} [ \cdot OH]_{ss} + k_{FFA, SO_4} [SO_4]_{ss} + k_{FFA, 1O_2} [1_{O_2}]_{ss} + k_{FFA, O_2} [O_2]_{ss}]_{ss} = k_{FFA}t$$

$$k_{BA,OH}, k_{BA,SO_4}$$
,  $k_{NB,OH}, k_{NB,SO_4}$ ,  $k_{p-CBA,OH}, k_{p-CBA,SO_4}$ ,  $k_{pCBA,1O_2}, k_{p-CBA,O_2}$ ,  $k_{FFA,OH}, k_{FFA,OH}$ ,  $k_{FFA,OH}, k_{FFA,OH}$ ,  $k_{FFA,OH}, k_{FFA,OH}, k_{FFA,OH}$ ,  $k_{FFA,OH}, k_{FFA,OH}, k_$ 

(4)

$$k_{FFA, SO_4}$$
,  $k_{FFA, 1O_2}$ ,  $k_{FFA, O_2}$  values were taken from the literature.<sup>[2-3]</sup>

The pseudo-first-order reaction rate constant  $(k_{,BA}, k_{,NB}, k_{,p-CBA}, k_{,FFA})$  could be obtained from

the slope of the plots of 
$$-ln \frac{[BA]}{[BA]_0}$$
,  $-ln \frac{[NB]}{[NB]_0}$ ,  $-ln \frac{[p-CBA]}{[p-CBA]_0}$ , and  $-ln \frac{[FFA]}{[FFA]_0}$ , respectively

Then, the steady-state concentrations of the reactive species were obtained by solving equations

1-4 and were listed in Table S5.

### 7. DFT calculations

All theoretical computations were performed using the DFT framework implemented in the Vienna Ab initio Simulation Package (VASP). The Perdew–Burke–Ernzerhof (PBE) generalized gradient approximation was utilized for the exchange-correlation energy, along with the projected augmented wave (PAW) method. Grimme's DFT-D3 method with zero-damping was employed to account for dispersion corrections. For the DFT+U calculations, a magnetic moment of 2.5 was assigned to Fe, while other elements were assigned a moment of 0. A plane-wave basis set with a cutoff energy of 400 eV was used. A 15 Å vacuum layer was incorporated to eliminate interactions between periodic images. For catalyst structure optimizations, the Brillouin zone of the surface unit cell was sampled using Monkhorst–Pack (MP) grids. The convergence criteria were set to  $10^{-6}$  eV for electronic self-consistent iterations and 0.02 eV/Å for atomic forces. A  $1 \times 1 \times 1$  Monkhorst-Pack grid was used to determine the catalyst surface.

Pollutants	Wavelength	Mobile phase (v/v)
BPA	230	Water : Methanol=30:70
4-CP	280	Water : Methanol=40:60
2,4-DCP	280	Water : Acetonitrile=30:70
2,4,6-TCP	284	Water : Methanol=30:70
HBA	270	Water : Methanol=40:60
HBAI	284	Water : Methanol=50:50
ACP	280	Water : Methanol=20:80
IBP	270	Water : Methanol=40:60
OFX	272	Water : Methanol=40:60
BP	280	Water : Methanol=20:80
MQ	276	Water : Methanol=30:70
Phenol	270	Water : Methanol=35:65

**Table S1**HPLC operating conditions for analyzing various pollutants.

2-NP	280	Water : Methanol=20:80
4-NP	280	Water : Methanol=20:80
SMX	265	Water : Acetonitrile =15:85
SMT	175	Water : Methanol=55:45
NB	265	Water : Acetonitrile=50:50
BA	227	Water : Acetonitrile=50:50
FFA	214	Water : Acetonitrile=50:50
<i>p</i> -CBA	239	Water : Acetonitrile=50:50

### Table S2.

Sample	Path	CNa	$R(\text{\AA})^b$	$\sigma^2 (\text{\AA}^2)^c$	$\Delta E_0(\mathrm{eV})^d$	Range of k	Range of k	R factor	
Fe K-edge ( $S_0^2=0.827$ )									
Fe foil	Fe-Fe	8.0*	2.475	0.0052	7.0	20142	1.0-3.0	0.0019	
	Fe-Fe	6.0*	2.854	0.0069		5.0-14.5			
	Fe-O	3.5	1.945	0.0045			1.0-4.0	0.0064	
	Fe-O	2.4	2.110	0.0043					
Fe <sub>2</sub> O <sub>3</sub>	Fe-Fe	4.8	2.961		-2.4	3.0-13.9			
	Fe-Fe	3.8	3.383	0.0067					
	Fe-Fe	5.1	3.692						
	Fe-O	1.6	1.992	0.0105					
	Fe-N	3.2	2.032	0.0105					
Fe-Mn DAC	Fe-Mn	1.0	2.525	0.0205	-1.7	3.0-13.8	1.0-4.0	0.0048	
	Fe-Fe	2.5	3.009	0.0060	0				
	Fe-Fe	3.9	3.524	0.0000					
			Mn	K-edge $(S_0^2)$	=0.881)				
Mn foil	Mn- Mn	12.0*	2.701	0.0085	11.2	3.0-12.0	1.8-3.0	0.0183	
	Mn-O	6.2	2.181	0.0106					
MnO	Mn- Mn	10.5	3.127	0.0086	-5.7	3.0-13.2	1.0-3.2	0.0062	
Fe-Mn DAC	Mn-N	3.2	2.051	0.0076	3.9	2.0.10.0	1028	0.0047	
	Mn-O	1.6	2.073	0.0070					
	Mn-Fe	1.0	2.520						
	Mn- Mn	5.7	3.119	0.0036	0.0036	.0036 13.3	5.0-10.0	1.0-5.8	0.0047
	Mn- Mn	4.4	3.304						

EXAFS fitting parameters at the Fe and Mn K-edge for various samples.

<sup>a</sup>CN, coordination number; <sup>b</sup>R, the distance between absorber and backscatter atoms; <sup>c</sup> $\sigma^2$ , the Debye Waller factor value; <sup>d</sup> $\Delta E_0$ , inner potential correction to account for the difference in the inner potential

between the sample and the reference compound; *R* factor indicates the goodness of the fit.  $S0^2$  was fixed to 0.827 and 0.881, according to the experimental EXAFS fit of Fe foil and Mn foil by fixing *CN* as the known crystallographic value. \* This value was fixed during EXAFS fitting, based on the known structure of Fe and Mn. fitting space: R space; *k*-weight = 3. A reasonable range of EXAFS fitting parameters:  $0.800 < S_0^2 < 1.000$ ; CN > 0;  $\sigma^2 > 0$  Å<sup>2</sup>;  $|\Delta E_0| < 15$  eV; *R* factor < 0.02.

### Table S3.

Comparison of reaction conditions and reaction parameters over the reported DACs, SACs, and nanocatalysts for BPA degradation by PMS activation in the Fenton-like reaction.

No.	Catalysts	BPA (mg L <sup>-1</sup> )	<b>PMS</b> ( g L <sup>-1</sup> )	Catalyst (g)	<b>k</b> (min <sup>-1</sup> )	TOF (min·g) <sup>-1</sup>	<b>TOF/PMS</b> <sub>0</sub> (L min <sup>-1</sup> g <sup>-2</sup> )	Reference
1	Fe-Mn DAC	20	0.20	0.20	1.36	6.8	34.0	This work
2	Fe-Co DAC	20	0.40	0.20	0.94	4.7	11.75	[1]
3	Fe-Co DAC	20	0.25	0.20	0.23	1.15	4.60	[5]
4	Fe-Co NC	20	1.20	0.30	0.19	0.63	0.525	[6]
5	Fe-Cu/OPB	20	0.10	0.30	0.025	0.083	0.83	[7]
6	FeSA–N–C	20	0.40	0.15	0.24	1.6	4.0	[8]
7	Fe <sub>1</sub> /CN	22.80	0.60	0.50	1.43	2.86	4.77	[9]
8	Cu-N <sub>4</sub> /C-B	20	0.40	0.10	0.56	5.6	14.0	[10]
9	Cu–N <sub>4</sub> /C	20	0.20	0.10	0.10	1.02	5.10	[10]
10	Co-TPML	11.40	1.20	0.20	0.147	12	10	[11]
11	Co-NC	10.0	0.30	0.05	0.352	7.04	23.47	[12]

12	FeSA-NC	3.0	0.80	0.02	0.24	12	15.0	[13]
13	Co-N <sub>4</sub> -C	20	0.20	0.10	0.45	4.52	22.60	[14]
14	NiZn@N-G- 900	20	0.20	0.20	0.45	2.67	13.35	[15]
15	10%Ag/C <sub>3</sub> N <sub>4</sub>	20	0.60	0.10	0.05	0.50	0.83	[16]
16	S-doped C <sub>3</sub> N <sub>4</sub>	20	0.60	0.10	0.013	0.13	0.217	[17]
17	CuFe <sub>2</sub> O <sub>4</sub> - Fe <sub>2</sub> O <sub>3</sub>	05	0.70	0.20	1.41	7.05	10.07	[18]
18	DPA-hematite	15	4.0	0.50	0.04	0.08	0.02	[19]
19	Co <sub>3</sub> O <sub>4</sub> -Bi <sub>2</sub> O <sub>3</sub>	20	0.20	0.30	0.12	0.4	2.0	[20]
20	$Mn_{1.8}Fe12O_4$	10	0.40	0.10	0.10	1.0	2.50	[21]
21	$Fe_{0.8}Co_{2.2}O_4$	20	0.40	0.10	0.05	0.5	1.25	[22]
22	O-C <sub>3</sub> N <sub>4</sub>	12	6.0	0.10	0.065	0.65	0.108	[23]
23	$Pd@g-C_3N_4$	20	0.60	0.10	0.038	0.38	0.63	[24]

## Table S4

	Tap Water	<b>River water</b>	Reclaimed water
рН	7.65	7.40	8.34
$\text{HCO}_3^-(\text{mg } \text{L}^{-1})$	28.82	63.60	44.14
$SO_4^{2-}$ (mg L <sup>-1</sup> )	41.63	90.65	21.90
$PO_3^{4-}$ (mg L <sup>-1</sup> )	BDL	0.13	0.01
$NO_{3}^{-}$ (mg L <sup>-1</sup> )	0.46	8.94	49.91
Cl <sup>-</sup> (mg L <sup>-1</sup> )	12.23	94.63	55.71
TOC (mg L <sup>-1</sup> )	-	3.15	4.64

Parameters of the obtained water samples.

\*BDL= Below detection limit

# Table S5.

Reactive species	Steady-state concentration (M)	Contribution ratio (%)
·OH	$1.31 \times 10^{-13}$	0.48
$SO_4$	$5.10  imes 10^{-12}$	0.19
$^{1}O_{2}$	$1.89 \times 10^{-9}$	30.05
O2 <sup></sup>	$8.21 \times 10^{-10}$	69.28

The steady-state concentrations and the contribution ratio of various ROS.



Figure S1. SEM images of Fe-Mn DAC.



**Figure S2.** BPA adsorption on various catalysts in heterogeneous Fenton-like reaction. Reaction conditions: [BPA]=20 mg L<sup>-1</sup>, [catalyst]=0.2 g L<sup>-1</sup>, [PMS]=0.2 g L<sup>-1</sup>, pH=7.0, T=25 °C, adsorption time=30 min.



**Figure S3.** TOC removal by various catalysts in heterogeneous Fenton-like reaction. Reaction conditions: [BPA]=20 mg L<sup>-1</sup>, [catalyst]=0.2 g L<sup>-1</sup>, [PMS]=0.2 g L<sup>-1</sup>, pH=7.0, T=25 °C, reaction time= 10 min.



**Figure S4.** PMS consumption with various catalysts for BPA degradation in heterogeneous Fentonlike reaction. Reaction conditions: [BPA]=20 mg L<sup>-1</sup>, [catalyst]=0.2 g L<sup>-1</sup>, [PMS]=0.2 g L<sup>-1</sup>, pH=7.0, T=25 °C, reaction time= 10 min.



**Figure S5.** Comparison of normalized *k* to metal loading. Reaction conditions: [BPA]= 20 mg L<sup>-1</sup>, [catalyst]= $0.2 \text{ g L}^{-1}$ , [PMS]= $0.2 \text{ g L}^{-1}$ , pH=7.0, T=25 °C.



**Figure S6.** Comparison of normalized *k* to the molar ratio of metal loading per (a) Fe site and (b) Mn site. Reaction conditions:  $[BPA]=20 \text{ mg } \text{L}^{-1}$ ,  $[catalyst]=0.2 \text{ g } \text{L}^{-1}$ ,  $[PMS]=0.2 \text{ g } \text{L}^{-1}$ , pH=7.0, T=25 °C.



**Figure S7.** Effect of pH on the BPA adsorption in Fe-Mn DAC/PMS system. Reaction conditions: [BPA]=20 mg L<sup>-1</sup>, [catalyst]=0.2 g L<sup>-1</sup>, [PMS]=0.2 g L<sup>-1</sup>, T=25 °C, adsorption time=30 min.



**Figure S8.** Stability test of Fe-Mn DAC for BPA degradation. Reaction conditions: [BPA]=20 mg L<sup>-1</sup>, [catalyst]=0.2 g L<sup>-1</sup>, [PMS]=0.2 g L<sup>-1</sup>, pH=7.0, T=25 °C, reaction time=30 min.



Figure S9. FTIR spectrum of transmittance of fresh and recycled Fe-Mn DAC.



Figure S10. EPR spectra in PMS alone.



**Figure S11.** (a) NB, (b) BA, (c) FFA, and (d) *p*-CBA degradation efficiency in Fe-Mn DAC/PMS system. Reaction conditions: [BPA]=20 mg L<sup>-1</sup>, [catalyst]=0.2 g L<sup>-1</sup>, [PMS]=0.2 g L<sup>-1</sup>, pH=7.0, T=25 °C , [probe]= 2.0 mg L<sup>-1</sup>.



Figure S12. *k* of NB, BA, FFA, and *p*-CBA degradation efficiency in Fe-Mn DAC/PMS system. Reaction conditions: [BPA]=20 mg L<sup>-1</sup>, [catalyst]=0.2 g L<sup>-1</sup>, [PMS]=0.2 g L<sup>-1</sup>, pH=7.0, T=25 °C, [probe]= 2.0 mg L<sup>-1</sup>.



**Figure S13.** Linear sweep voltammetry obtained by Fe-Mn DAC as a working electrode in the presence of PMS and BPA.



Figure S14. 2-D electron density distribution structure of (a) Fe-SAC, (b) Mn-SAC, and (c) Fe-Mn DAC.

Figure S15. Charge density difference (top view) in a PMS molecule adsorbed on (a) Fe–SAC, (b) Mn-SAC, (c) Fe-Mn DAC  $_{(Fe \text{ site})}$  and (d) Fe-Mn DAC  $_{(Mn \text{ site})}$ .





**Figure S16.** DFT calculations of PMS adsorption and activation on Fe-SAC and Mn-SAC. Representation of PMS molecule, adsorption energy, and O-O bond stretching on (a) Fe-SAC and (b) Mn-SAC, PDOS of (c) Fe-SAC and (d) Mn-SAC.



Figure S17. Bader charges on (a) Fe-SAC, (b) Mn-SAC, (c) Fe-Mn DAC  $_{(Fe site)}$ , and (d) Fe-Mn DAC  $_{(Mn site)}$ .



Figure S18. Free energy of O transfer in Fe-Mn DAC/PMS system.

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