

Supporting Information for

Interfacial Interaction of Ag-MnO_x Heterostructure for Efficient CO₂ Electroreduction to CO and Aqueous Zn-CO₂ Batteries

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Experimental section

2.3 Characterizations

The phase structure was recorded by X-ray diffraction (XRD, BRUKER D8 Discover, Cu K α radiation) operating at 20 mA and 40 KV. SEM images were obtained by Field-emission scanning electron microscope (FE-SEM, Thermo Fisher Scientific FEI Quattro S) at 5 KV. The morphology and elemental composition were performed utilizing a transmission electron microscope (TEM, FEI Talos F200S) operated at 200 KV. Raman microscope (Renishaw, Horiba HR Evolution-800) and X-ray photoelectron spectrometer (XPS, Thermo Scientific ESCALAB 250Xi) were used to detect the internal structure and chemical state of synthesized samples. The CO₂ Temperature programmed desorption (CO₂ TPD) experiments were performed by an automatic adsorption device (VDSorb-91i, China) to detect the adsorption/desorption of CO₂. The reaction intermediates were analyzed by the attenuated total reflectance surface enhanced infrared absorption spectroscopy (ATR-SEIRAS, Nicolet iS10).

2.4 Electrochemical Measurements

The CO₂RR experiments were conducted out in an H-type air-tight electrolytic cell fitted with an electrochemical workstation (CHI 660E, CH Instruments, Chenhua Co.) and a proton exchange membrane. Ag/AgCl is the reference electrode and the platinum sheet is the counter electrode. The cathode chamber was saturated with CO₂ (99.999% purity) gas for 30 min, and the flow rate was set to 20 sccm with a mass flow controller (Alicat Scientific, LK2) to maintain the CO₂ flux during the experiment. In the preparation of the working electrode, 10 mg of catalyst was sonicated in a mixture of 600 μ l of DI water, 360 μ l of ethanol and 40 μ l of 5.0 wt. % Nafion for 60 minutes to create a uniform ink. Next, 100 μ L of the formed ink was coated onto carbon paper (1 \times 0.5 \times 2 cm²) and dried at 60 °C, with a loading of \sim 1.0 mg \cdot cm⁻². All potentials were not IR-compensated and were converted to the RHE potential according to:

$$E \text{ (vs. RHE)} = E \text{ (vs. Ag/AgCl)} + 0.059 \times \text{pH} + 0.197$$

Linear scanning voltammetric (LSV) curves were performed on N₂- and CO₂

saturated 0.5 M KHCO₃ electrolytes at a scan rate of 10 mV s⁻¹. The carbon monoxide partial current density is based on the following equation: $j_{\text{CO}} = j * \text{FE}_{\text{CO}}$, wherein j_{CO} represents the partial current density for carbon monoxide, j denotes the total current density, FE_{CO} is the Faraday efficiency of carbon monoxide. The linear portion of the plot of overpotential vs the logarithm of the CO bias current density was fitted to produce Tafel slopes. The electrochemical impedance spectra (EIS) were collected at open circuit potential over a frequency range of 10⁵ Hz to 10 Hz. Cyclic voltammetry (CV) measurements were conducted at varying scan rates (20, 40, 60, 80, 100 mV s⁻¹) to determine the double-layer capacitance (C_{dl}) and assess the electrochemically active surface area (ECSA) of the catalysts, with the equation:

$$\text{ECSA} = C_{\text{dl}} / C_s$$

Wherein C_s denotes the specific capacitance.

2.5 Product Analysis

With a thermal conductivity detector (TCD) and a flame ionization detector (FID), the gas chromatography (GC, FULLI, GC-9790II) was employed to on-line analysis the cathode gas products in the electrolytic cell. The standard gas was diluted into different concentrations to create a standard curve to analyze the content of different gas products. The following formula was used to determine the FE of the reduced product:

$$\text{FE (\%)} = \frac{n N F}{Q_{\text{total}}}$$

Where, n represents the amount of substance in moles, and $N (= 2)$ denotes the number of electrons transferred during the electroreduction of carbon dioxide; F (96500 C mol⁻¹) is the Faradaic constant, and Q_{total} is the total charge that flows through the electrodes during the electrolysis process.

2.6 DFT Calculation

All the Density Functional Theory (DFT)¹ calculations were performed using Vienna Ab initio Simulation Package (VASP)² with the projector augmented wave (PAW)³ method. The Perdew-Burke-Ernzerhof (PBE)⁴ of parameterization of the generalized gradient approximation (GGA)⁵ is adopted to describe the exchange and correlation potential. During the geometry optimization and electronic structure calculations, the cut-off energy of plane-wave basis set is 400 eV, and single gamma-point grid sampling was used for Brillouin zone integration. Atomic positions were optimized until the forces were less than 0.05 eV/Å. The first Brillouin zone was sampled by 1 × 1 × 1 k-mesh and a vacuum thickness of about 15 Å between periodic images was adopted, which were found to be sufficient for accurate results. Grimme's method (DFT-D3)⁶ was carried out to include explicit dispersion correction terms to the energy. The simulated Ag(111) surface contains 4 atomic-layers (100 atoms) and a vacuum layer (~ 15 Å). The manganese oxide clusters were subsequently placed on the Ag surface to obtain the MnO_x/Ag (111) structure. During geometries optimization, the atoms in bottom 2 layers were fixed, and other atoms were fully relaxed until the force on each atom were less than 0.05 eV/Å. The Gibbs Free Energy (ΔG) are calculated using:

$$\Delta G = \Delta E + \Delta \text{ZPE} - T\Delta S$$

where ΔE , ΔZPE , and $T\Delta S$ are the adsorption energy of intermediates, Zero-Point-Energy, and entropy correction under reaction temperature (298.15 K).

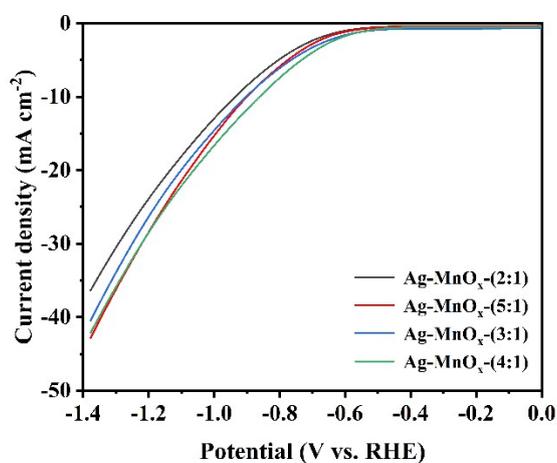


Fig. S1. The LSV curves of catalysts with various Ag/Mn feeding ratios

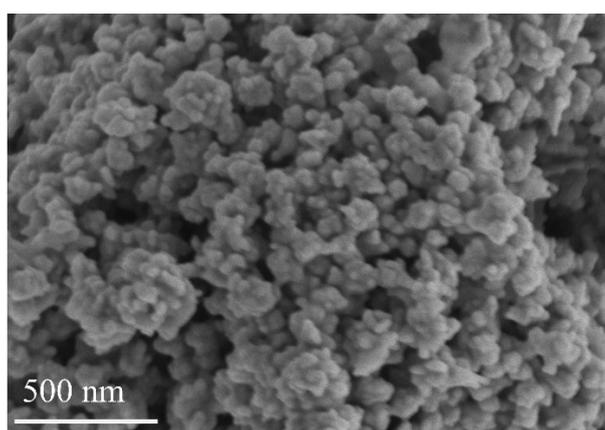


Fig. S2. SEM image of the comparative Ag sample

Table S1 The surface fraction of Mn elements by XPS spectra.

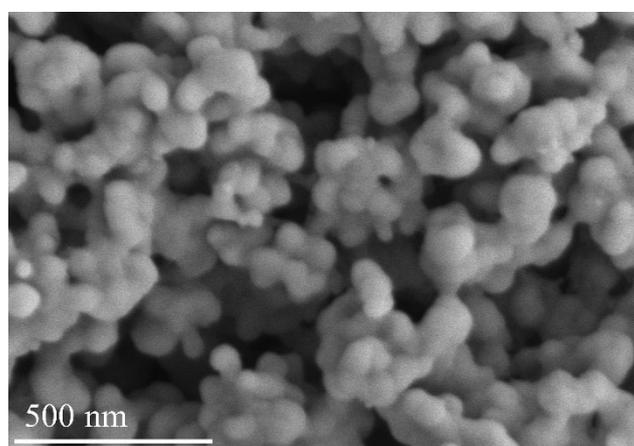
catalyst	Mn 2p _{3/2}			
	Mn ⁴⁺	Mn ³⁺	Mn ²⁺	(Mn ³⁺⁺ Mn ²⁺)/ Mn ⁴⁺
MnO _x	45.8	36.5	17.7	118.1
Ag-MnO _x	34.4	49.2	16.4	190.9

Table S2 The surface fraction of O elements by XPS spectra

catalyst	O 1s		
	O _{sur}	O _{vac}	O _{lat}
MnO _x	11.9	39.9	48.2
Ag-MnO _x	16.4	43.4	40.2

Table S3 Summary of silver-based catalyst performance in recent years

Catalyst	FE _{CO}	j _{CO} (mA cm ⁻²)	Electrode configuration	electrolytes
Ag ₁ /MnO ₂ SAC ⁷	95.7%	3.4 at -0.9 V	H-type cell	0.5 M KHCO ₃
Ag-N _x ⁸	95%	2.5 at -0.377 V	H-type cell	0.1 M KHCO ₃
Cu/Ag (S) ⁹	93%	2.9 at -1.0 V	H-type cell	0.1 M KHCO ₃
Ag-In (OH) ₃ ¹⁰	93%	0.6 at -0.7 V	H-type cell	0.5 M KHCO ₃
Tri-Ag-NPs ¹¹	96.8%	1.25 at -0.856 V	H-type cell	0.1 M KHCO ₃
Ag-BTC ¹²	95%	7.2 at -1.0 V	H-type cell	0.1 M KHCO ₃
PON-Ag ¹³	96.7%	4.4 at -0.69 V	H-type cell	0.5 M KHCO ₃
Porous Ag ¹⁴	96.38%	5.3 at -0.8 V	H-type cell	0.5 M KHCO ₃
Ag-Cu aerogel ¹⁵	89.40%	5.86 at -0.89 V	H-type cell	0.1 M KHCO ₃
Ag layer-Zn ¹⁶	84.2%	2.97 at -1.0 V	H-type cell	0.1 M KHCO ₃
Cu-Ag biphasic ¹⁷	80.25%	4.88 at -0.9 V	H-type cell	0.1 M KHCO ₃
Ag-MnO _x (this work)	97.5%	7.05 at -0.8 V	H-type cell	0.5 M KHCO ₃

**Fig. S3.** SEM image of Ag-MnO_x after stability testing

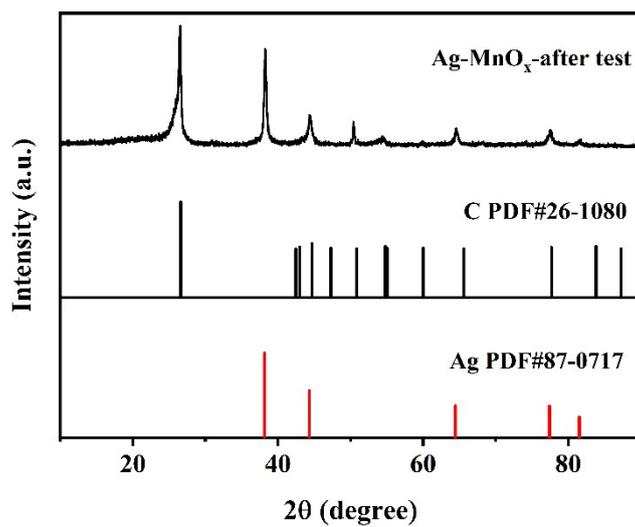


Fig. S4. XRD pattern of Ag-MnO_x after stability testing

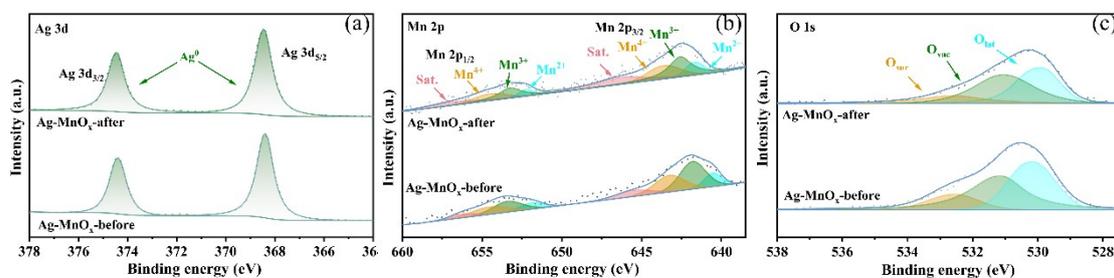


Fig. S5. a) Ag 3d, b) Mn 2p, c) O 1s XPS spectra of the Ag-MnO_x sample before and after stability testing

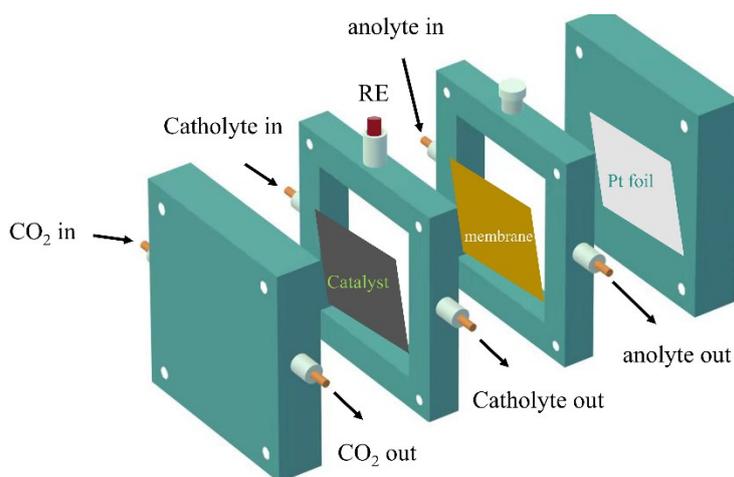


Fig. S6. Flow cell (where, RE is reference electrode.)

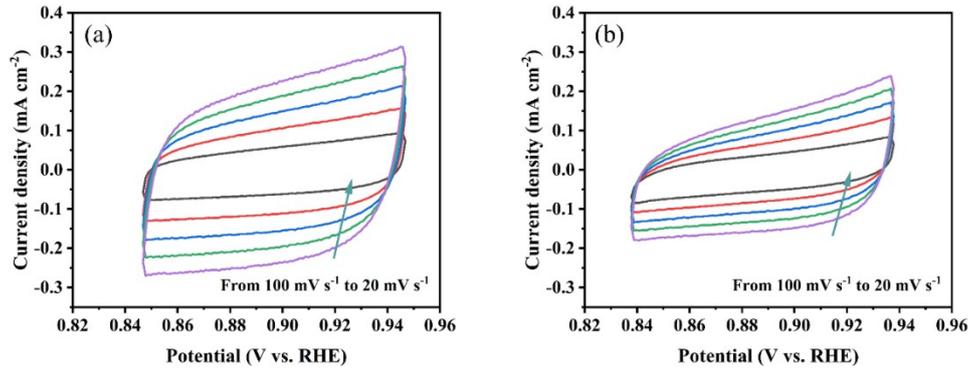


Fig. S7. a) CV of Ag-MnO_x. b) CV of Ag

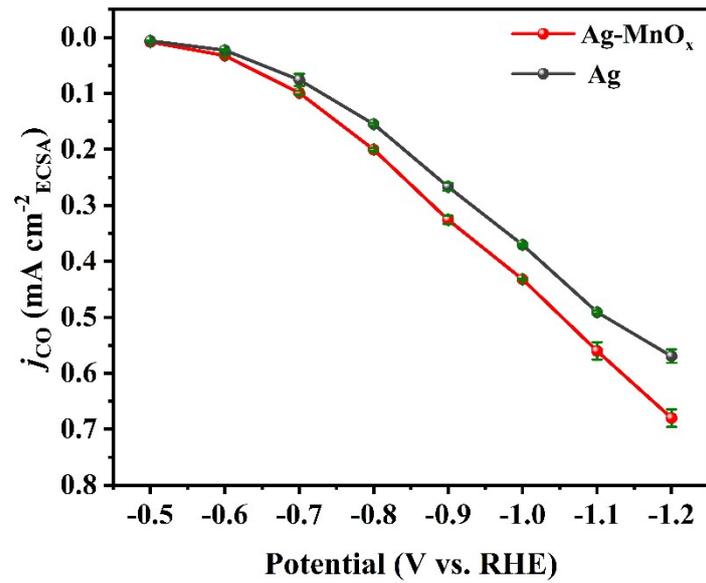


Fig. S8. The ECSA normalized j_{CO} of Ag-MnO_x and Ag

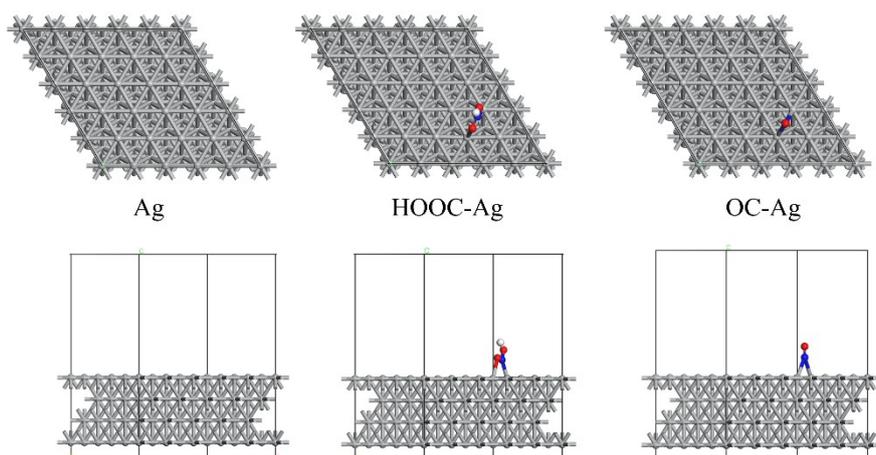


Fig. S9. Optimized structure of Ag, HOOC-Ag and OC-Ag. Silver gray, red, white, and blue spheres represent the Ag, O, H, and C atoms, respectively.

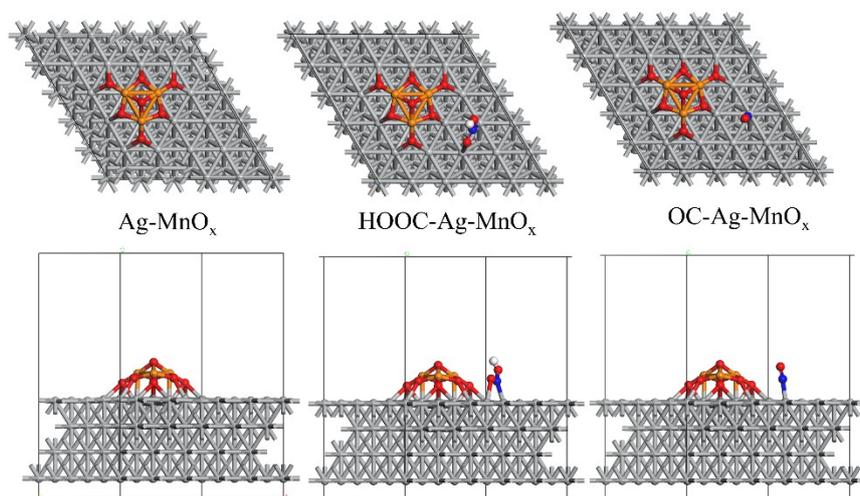


Fig. S10. Optimized structure of Ag-MnO_x, HOOC-Ag-MnO_x and OC-Ag-MnO_x. Silver gray, red, orange, white, and blue spheres represent the Ag, O, Mn, H, and C atoms, respectively.

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