

## Supporting Information

### **Synergistic electronic modulation and Cl<sup>-</sup> shielding of Fe sites for robust seawater electrolysis**

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## Supporting note 1:

### AEMWE measurement

The Ce-NiFeOOH/PO<sub>4</sub><sup>3-</sup> catalyst was sprayed over Ni fibers and carbon paper, forming electrodes (2 cm<sup>2</sup>) that were integrated into an anion exchange membrane (AEM) water electrolysis cell. The anode and cathode were separated using an anion exchange membrane (Sustainion® X37-50-grade T, America). The catalytic AEM cell's performance was evaluated with a power supply (Interface 5000E, Gamry) and 1.0 M KOH + seawater fed in at a flow rate of 60 mL min<sup>-1</sup>. Voltage and current measurements provided information on the cell's operational efficiency.

### Electrolyzer efficiency

H<sub>2</sub> production rate @ 0.5 A cm<sup>-2</sup>

$$= (j \text{ A cm}^{-2})(1 \text{ e}^{-}/1.602 \times 10^{-19} \text{ C})(1 \text{ H}_2/2 \text{ e}^{-})$$

$$= 0.5 \text{ A cm}^{-2} / (1.602 \times 10^{-19} \text{ C} \times 2)$$

$$= 2.59 \times 10^{-6} \text{ mol H}_2 \text{ cm}^{-2} \text{ s}^{-1}$$

LHV of H<sub>2</sub>

$$= 120 \text{ kJ g}^{-1} \text{ H}_2 = 2.42 \times 10^5 \text{ J mol}^{-1} \text{ H}_2$$

H<sub>2</sub> power out

$$= (2.59 \times 10^{-6} \text{ mol cm}^{-2} \text{ s}^{-1}) \times (2.42 \times 10^5 \text{ J mol}^{-1})$$

$$= 0.627 \text{ W cm}^{-2}$$

Electrolyzer Power of Ce-NiFeP||Pt/C

Electrolyzer Power (Ce-NiFeP) @ 0.5 A cm<sup>-2</sup>

$$= (0.5 \text{ A cm}^{-2}) (1.68 \text{ V})$$

$$= 0.84 \text{ W cm}^{-2}$$

Efficiency of Ce-NiFeP||Pt/C

$$= (\text{H}_2 \text{ Power Out}) / (\text{Electrolyzer Power})$$

$$= 0.627 \text{ W cm}^{-2} / 0.84 \text{ W cm}^{-2}$$

$$= 74.6\%$$

Price per gasoline-gallon equivalent (GGE)H<sub>2</sub> @ 0.5A cm<sup>-2</sup>

$$= 1 \text{ GGE H}_2 / \text{H}_2 \text{ production rate} \times \text{Electrolyzer power} \times \text{Electricity bill}$$

$$= 0.997 \text{ kg} / (2.59 \times 10^{-6} \text{ mol H}_2 \cdot \text{cm}^{-2} \text{ s}^{-1} \times 2 \text{ kg/mol}) \times 0.84 \text{ W cm}^{-2} \times \$ 0.02/\text{kWh}$$

$$= \$ 0.90/\text{GGE H}_2$$

#### **Calculation of basic electricity expense for H<sub>2</sub> production <sup>1</sup>**

The total electricity consumption for H<sub>2</sub> production was calculated according to the following equation:

$$W = I \times \int U \, dt \quad (1)$$

Where the W is the total electricity consumption, I is the electrolyzer current, U is the electrolyzer voltage, and t is the reaction time.

The amount of H<sub>2</sub> generation was calculated based on the following equation:

$$V = 22.4 \times I \times t / (Z \times F) \quad (2)$$

Where  $V$  is the volume of produced  $H_2$ ,  $Z$  is the electron transfer number (the value of 2 for HER), and  $F$  is the Faraday constant ( $96485 \text{ Cmol}^{-1}$ ).

According to the above results, the basic electricity expense for  $H_2$  production was calculated as:

$$Q = W / V \text{ (kWh m}^{-3} \text{ H}_2\text{)} \quad (3)$$

For an ideal catalyst, assuming that it has no performance decay during the stability test of water splitting, the calculation of basic electricity expense for  $H_2$  production can be simplified to the formula  $[Q = 2.39 \times U \text{ (kWh m}^{-3} \text{ H}_2\text{)}]$  according to the Eqs. (1-3).

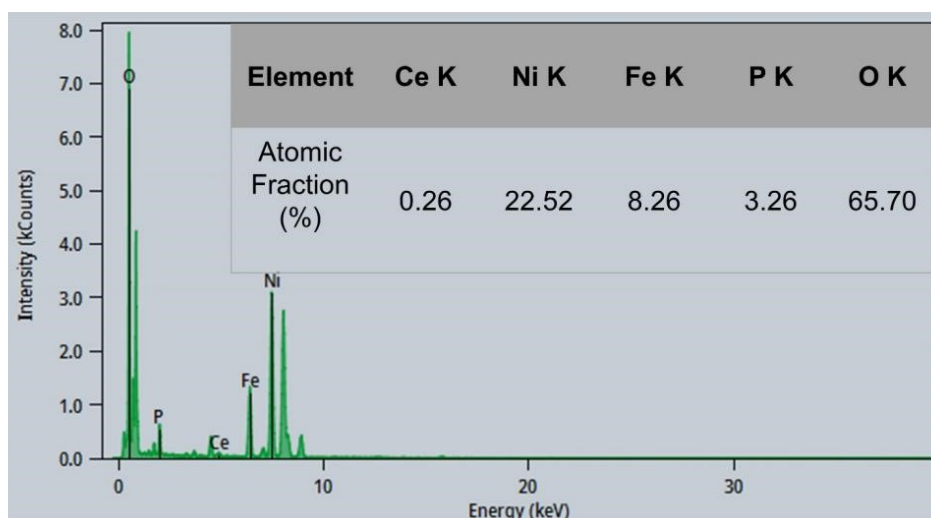


Figure S1. Detailed parameters for TEM EDS of Ce-Ni(Fe)OOH/PO<sub>4</sub><sup>3-</sup>.

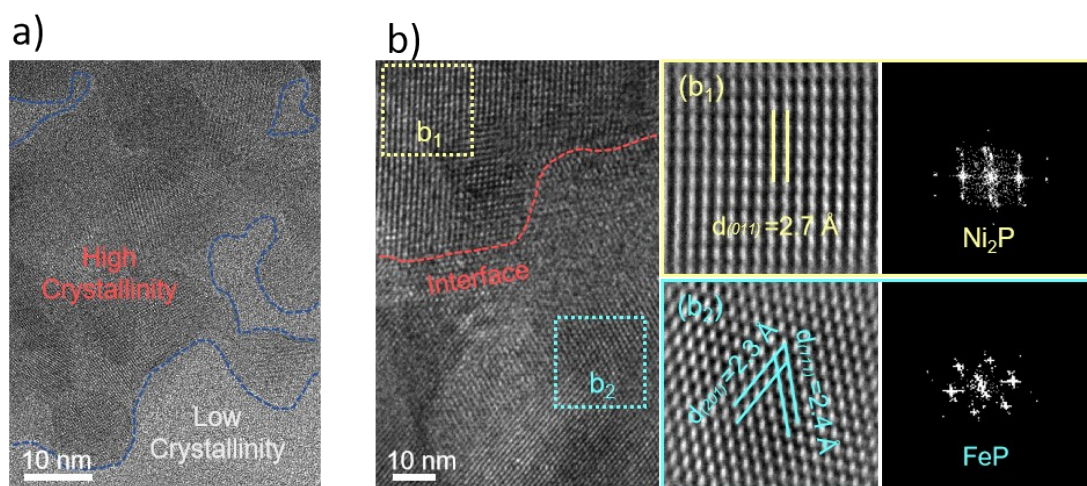


Figure S2. (a) The HR-TEM images of Ce-NiFeP. (b) The enlarged HRTEM image and corresponding Fourier transform pattern.

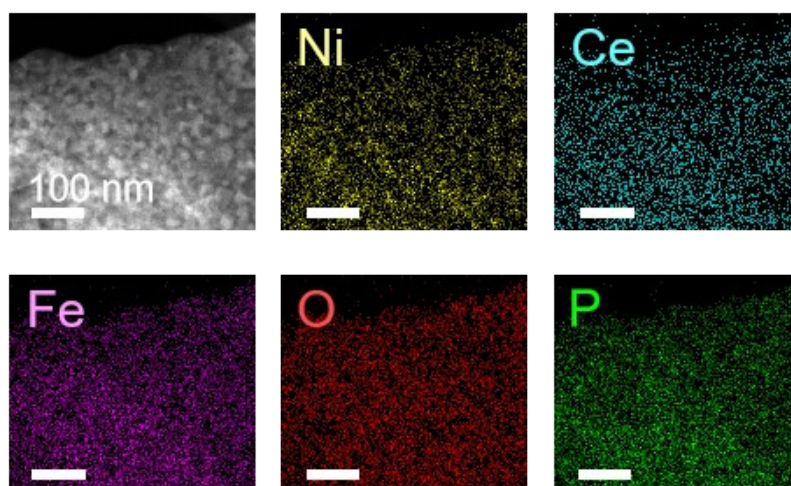


Figure S3. HAADF-STEM with EDS elemental mapping of Ce-NiFeP.

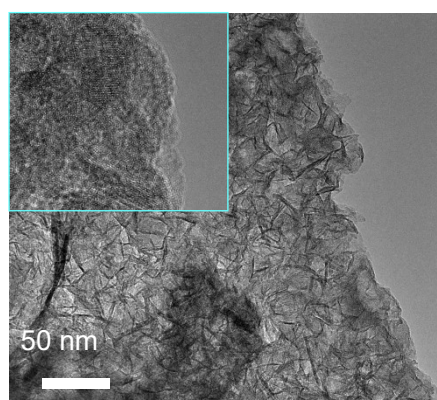


Figure S4. The TEM image of Ce-NiFeOOH/PO<sub>4</sub><sup>3-</sup>.

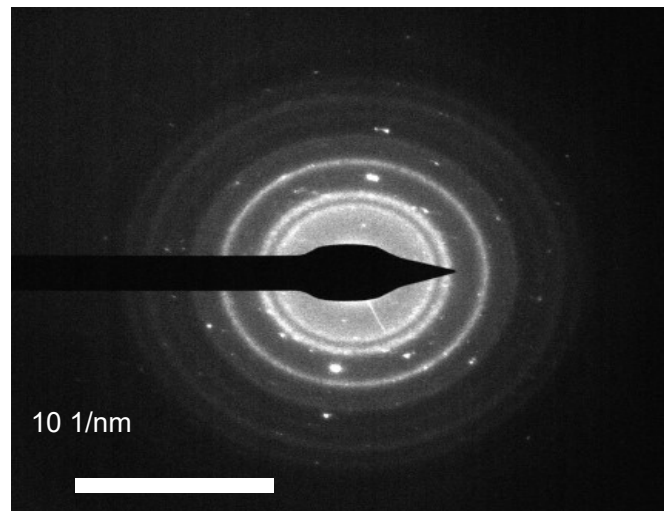


Figure S5. The SAED image of Ce-NiFeOOH/PO<sub>4</sub><sup>3-</sup>.

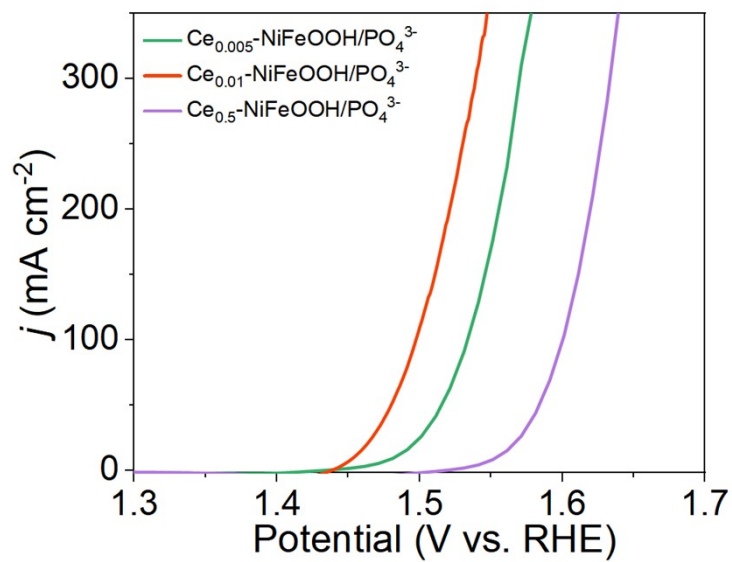


Figure S6. The LSV curves of of Ce-NiFeOOH/PO<sub>4</sub><sup>3-</sup> with different Ce contents.

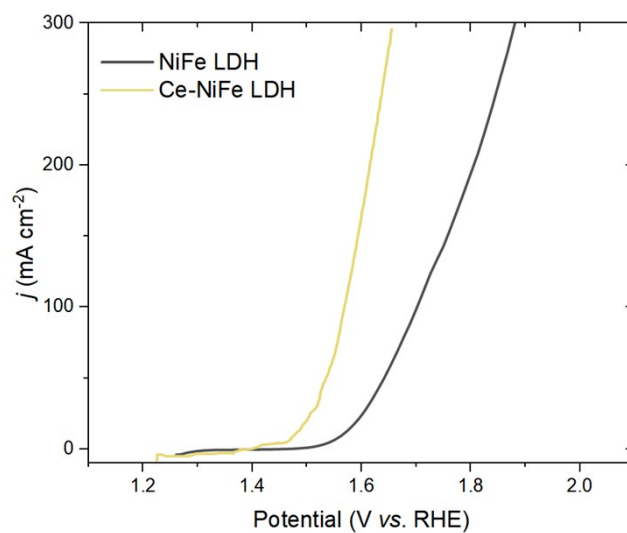


Figure S7. The LSV curves of Ce-NiFe LDH and NiFe LDH.

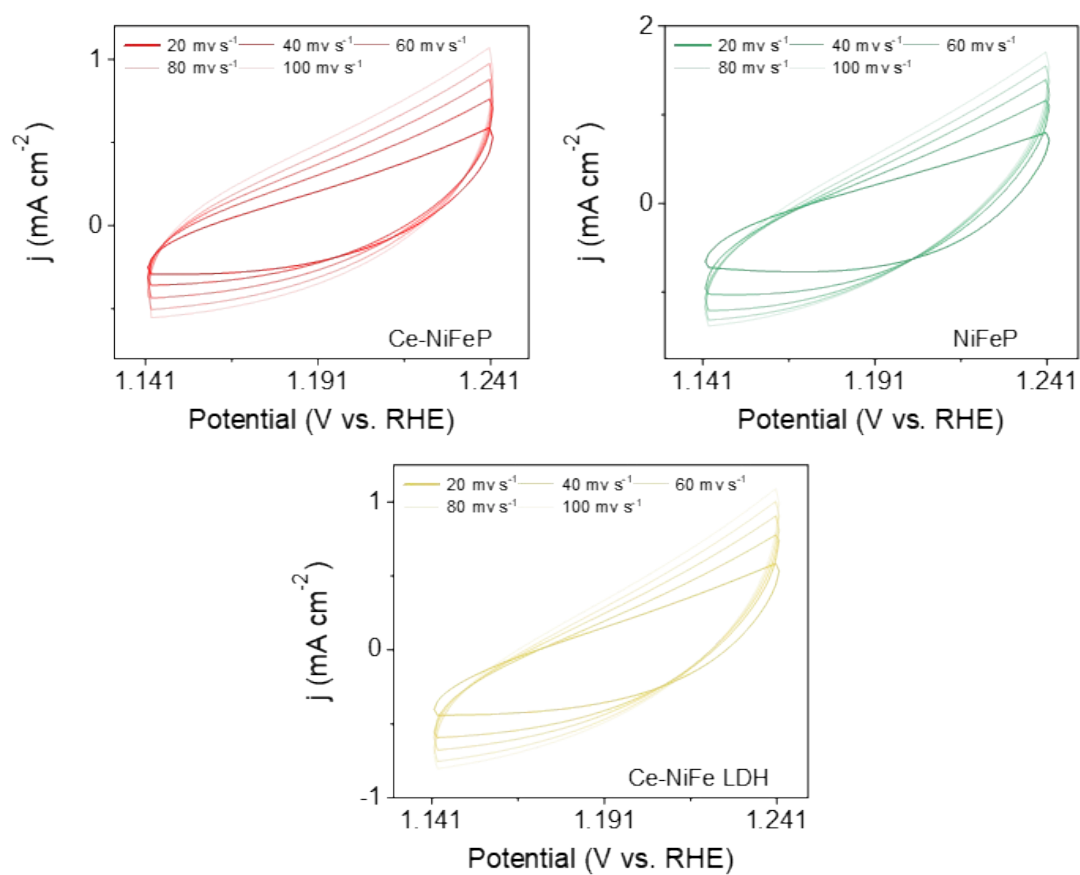


Figure S8. (a-c) CV curves of Ce-NiFeOOH/ $\text{PO}_4^{3-}$ , NiFeOOH and Ce-NiFe LDH electrodes.



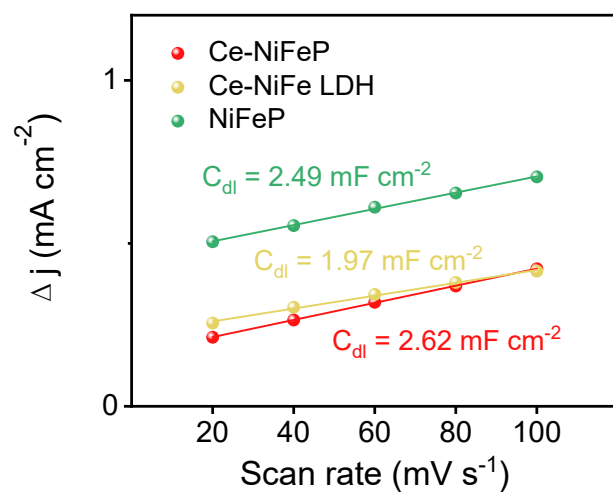


Figure S9.  $C_{dl}$  plots of Ce-NiFeOOH/ $\text{PO}_4^{3-}$ , NiFeOOH and Ce-NiFe LDH.

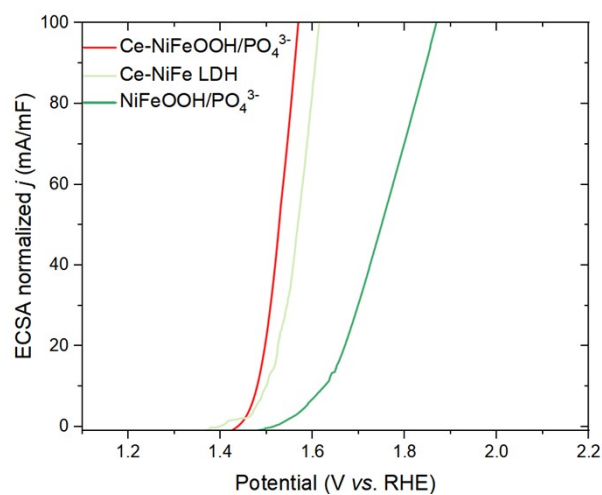


Figure S10. The ECSA normalized LSV curves of Ce-NiFeOOH/ $\text{PO}_4^{3-}$ , Ce-NiFe LDH, and NiFeOOH/ $\text{PO}_4^{3-}$ .

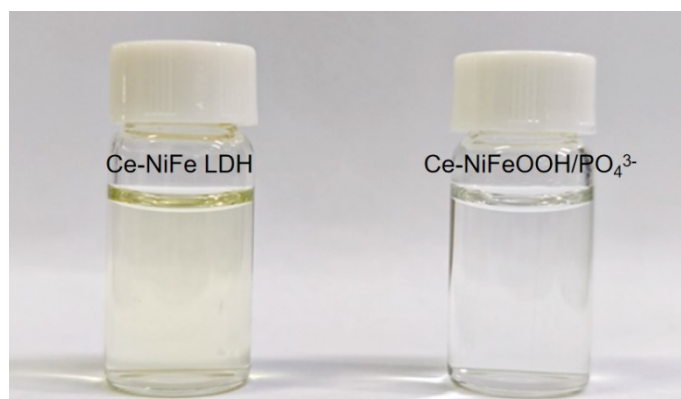


Figure S11. Optical image of  $\text{ClO}^-$  in the electrolyte after long-term stability testing of Ce-NiFe LDH and Ce-NiFeP in 1 M KOH + seawater, respectively.

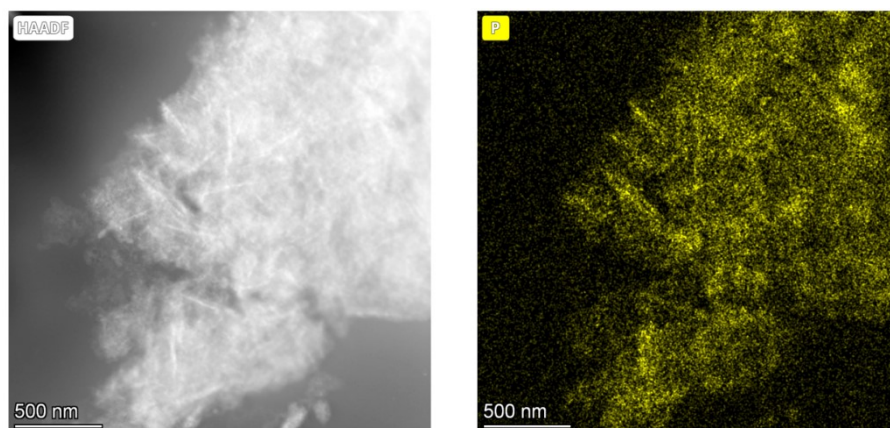


Figure S12. The HADDF-STEM and corresponding EDS mapping image of Ce-NiFeOOH/PO<sub>4</sub><sup>3-</sup> after a 48-hour stability.

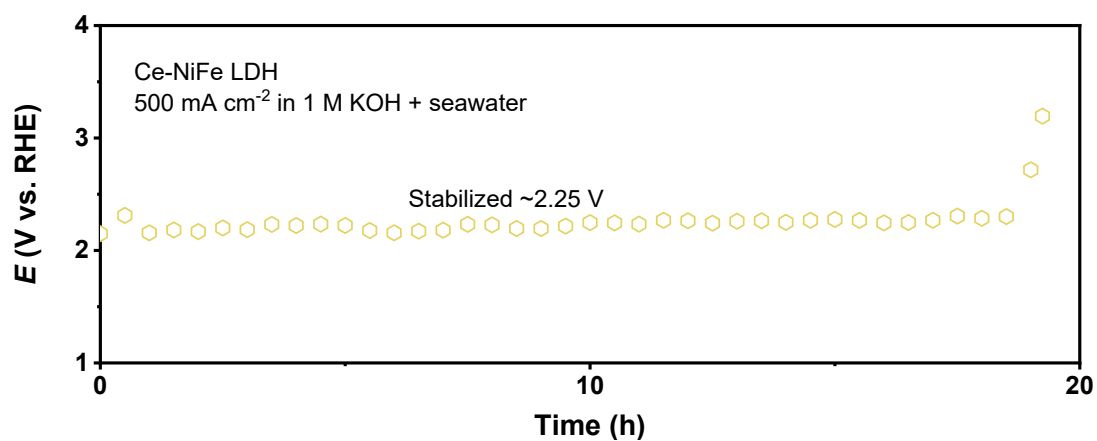


Figure S13. E-T curve of Ce-NiFe LDH in 1 M KOH + seawater electrolyte at 500 mA cm<sup>-2</sup>.

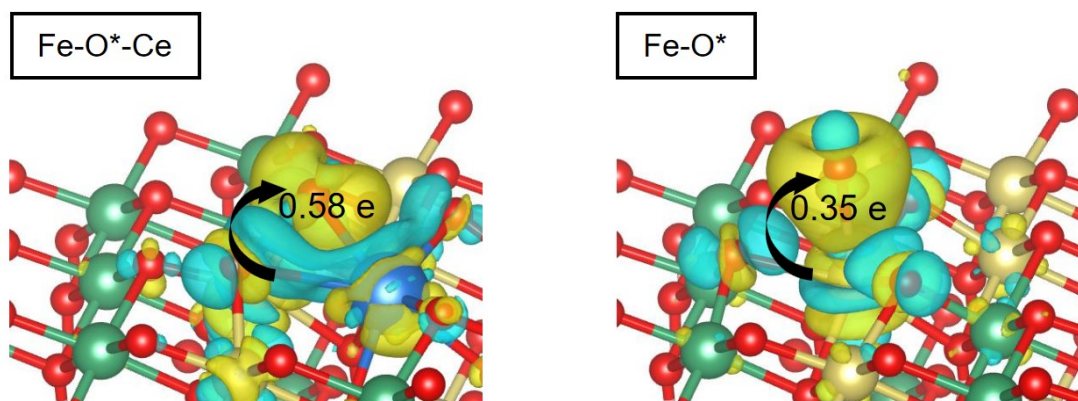


Figure S14. Charge density difference analysis.

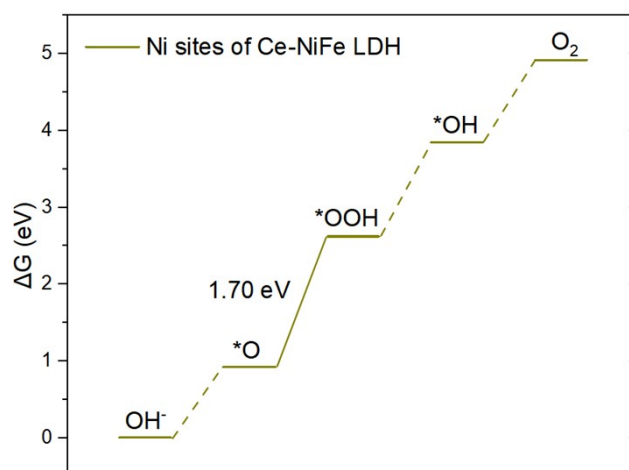


Figure S15. Free energy diagrams for OER on the Ni sites of Ce-Ni(Fe)OOH.

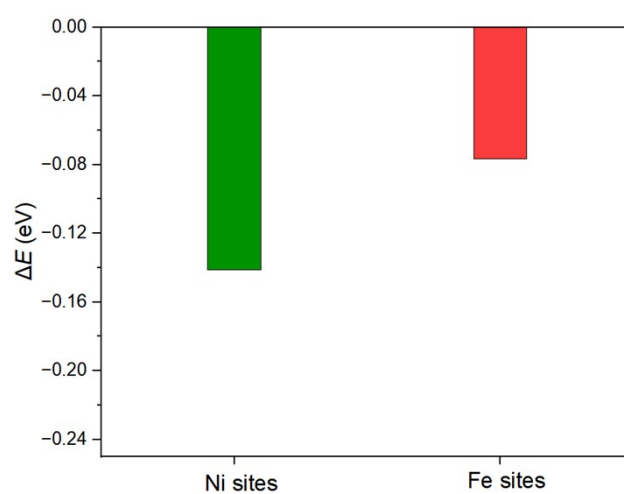


Figure S16. The adsorption energy of  $\text{PO}_4^{3-}$  on the Fe or Ni sites of Ce-Ni(Fe)OOH.

Table S1. Element analysis of Ce-NiFeP and NiFeP by ICP-OES.

Element	Ce-NiFeP			NiFeP	
	Ni	Fe	Ce	Ni	Fe
Element concentration (mg/L)	162.06	56.22	0.62	139.04	48.35
wt (%)	31.7	11.0	0.12	27.6	9.59

Table S2. Comparison of overpotentials of Ce-NiFeOOH/PO<sub>4</sub><sup>3-</sup> at different current density in 1 M KOH, 1 M KOH + 0.5 M NaCl, and 1 M KOH + seawater, respectively.

Electrolyte	10	100	300
	(mA cm <sup>-2</sup> )	(mA cm <sup>-2</sup> )	(mA cm <sup>-2</sup> )
1 M KOH	223	267	309
1 M KOH + 0.5 M NaCl	227	273	318
1 M KOH + seawater	230	286	348

Table S3. Comparison of  $\eta_{@10 \text{ mA cm}^{-2}}$  in the reported literature for Ce-NiFeOOH/PO<sub>4</sub><sup>3-</sup> in 1 M KOH.

Catalyst	$\eta_{@10 \text{ mA cm}^{-2}}$ (mV)	Ref.
Ce-NiFeOOH/PO <sub>4</sub> <sup>3-</sup>	<b>223</b>	<b>This work</b>
MIL-88A/Ni(OH)(2)	250	2
Co <sub>4</sub> N@CeO <sub>2</sub>	263	3

CoSe <sub>2</sub> /MoSe <sub>2</sub>	320	4
R-CoSeO <sub>4</sub>	265	5
3%IrO <sub>x</sub> /NCNT	241	6
H-LSCF	240	7
Ni <sub>3</sub> Fe-BDC	265	8
Fe <sub>3</sub> O <sub>4</sub>	270	9

Table S4. The calculated results for the free energy diagrams.

Free energies	Ce-Ni(Fe)OOH	Ni(Fe)OOH
M*+2H <sub>2</sub> O	0	0
M*OH+H <sub>2</sub> O+H <sup>+</sup>	0.74	0.91
M*O+H <sub>2</sub> O+2H <sup>+</sup>	2.48	2.34
M*OOH+3H <sup>+</sup>	3.57	3.96
M*+O <sub>2</sub> +4H <sup>+</sup>	4.92	4.92

Table S5. Performance comparison of Ce-NiFeOOH/PO<sub>4</sub><sup>3-</sup> with three other reported electrocatalysts in AEM seawater electrolyzers.

Catalyst	Co/P-Fe <sub>3</sub> O <sub>4</sub>	NFCP	NiCoP <sub>v</sub>	Ce-NiFeOOH/PO <sub>4</sub> <sup>3-</sup>
Electrolyzer efficiency at 500 mA cm <sup>-2</sup> (%)	68.5	59.9	51.6	74.6
Price per GGE H <sub>2</sub> at 500 mA cm <sup>-2</sup> (\$)	0.980	1.119	1.150	0.897
<i>E</i> at 500 mA cm <sup>-2</sup> (V)	1.84	2.095	2.43	1.68
<i>j</i> <sub>max</sub> (mA cm <sup>-2</sup> )	1000	500	900	1500
Electricity expense (kWh)	4.38	5.01	5.81	4.02

	<i>Appl. Catal.</i>		<i>Adv. Energy</i>	
	<i>B: Environ.</i>	<i>ACS Catal.</i>	<i>Mater.</i>	This work
Ref.	<b>2024</b> , 357,	<b>2024</b> ,14,18322.	<b>2024</b> ,	
	124269.		14, 2400975	

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