

## Supporting Information

# Green Preparation of Shell-Based Biochar and Its Adsorption of Multi-Component Chlorinated Volatile Organic Compounds

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### 1、Materials characterization

The specific surface area and pore size distribution of the samples were measured using the fully automated gas adsorption analyzer ASAP 2020 from Micromeritics Instrument Corporation (USA). The pore structure was characterized by N<sub>2</sub> adsorption-desorption isotherms, and the specific surface area was calculated using the BET method (Testing Parameters: Sample mass: 0.1 g, Analysis adsorptive : N<sub>2</sub>, Analysis bath temp. : -195.640 °C, Equilibration interval: 10 to 15 s). The surface morphology of the materials was examined using a field emission scanning electron microscope (Regulus 8100) from Hitachi Ltd., Japan. The surface functional groups

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20 of the materials were determined using a Fourier transform infrared spectrometer  
 21 (Nicolet iS50 FT-IR) from Thermo Fisher Scientific (USA). The Raman spectra of the  
 22 materials were obtained using a laser Raman spectrometer (RM2000) from Renishaw  
 23 plc (UK), with an excitation wavelength of 532 nm and a scanning range between  
 24 500–3500 cm<sup>-1</sup>. X-ray photoelectron spectroscopy (XPS) was performed using an  
 25 ESCALAB 250 system from Thermo Fisher Scientific (USA), with Al-K $\alpha$  radiation at  
 26 a power of 150 W. The elemental content of the materials was analyzed using an  
 27 elemental analyzer (Vario EL cube) from Elementar Analysensysteme GmbH  
 28 (Germany) via the combustion method. The thermal stability of the shell-derived  
 29 biochar adsorbent was evaluated using a thermogravimetric analyzer (TGA/DSC 3+)  
 30 from Mettler-Toledo Group (Switzerland).

## 31 2、Calculation of adsorption capacity

32 The adsorption capacities of VOCs were calculated by integrating the  
 33 breakthrough curve using the following equation. The breakthrough time was defined  
 34 as the time when the outlet concentration of VOCs was 5% of the inlet concentration,  
 35 and the equilibrium adsorption time was the time required for an equal concentration  
 36 of the VOC at the outlet and inlet.

$$37 \quad q = \frac{FC_0 10^{-9}}{W} \left[ t_s - \int_0^{t_s} \frac{C_i}{C_0} dt \right]$$

38 where  $q$  (g·g<sup>-1</sup>) is the estimated maximum adsorption capacity,  $F$  (mL·min<sup>-1</sup>) is  
 39 the total gas flow,  $C_0$  and  $C_i$  (mg·m<sup>-3</sup>) is the inlet and outlet gas concentration,  
 40 respectively,  $W$  (g) is the mass of adsorbent, and  $t_s$  (min) is the adsorption time.