

## Supplementary Data

### **Facilitating Fe(III)/Fe(II) redox cycle by organic pollutant for enhancement of heterogeneous Fenton-like catalytic performance of iron-containing catalyst**

**Cong Gao<sup>a\*</sup>, Houfen Li<sup>b</sup>, Jize Liu<sup>a</sup>, Wenchao Yang<sup>a</sup>, Hong Chen<sup>b</sup>, Jianbo Han<sup>b</sup>**

<sup>a</sup> Key Laboratory of Coastal Ecology and Environment of State Oceanic Administration, National Marine Environmental Monitoring Center, Dalian 116023, China

<sup>b</sup> College of Environment and Ecology, Taiyuan University of Technology, Taiyuan 030024, China

\* Corresponding authors.

E-mail: [cgao@nmemc.org.cn](mailto:cgao@nmemc.org.cn), [gaocong.200746033@163.com](mailto:gaocong.200746033@163.com)

#### pH<sub>PZC</sub> measurement

MIL-100-Fe powder (0.015 g) was added into 10 mL KNO<sub>3</sub> solution (0.01 M), followed by 24 h of equilibration to ensure complete dispersion of the catalyst particles. After equilibration, the pH value of the resulting suspension was adjusted to a series of target values using HCl (0.4 M) and NaOH (0.4 M). Subsequently, the zeta potential of MIL-100-Fe suspension at each adjusted pH was performed on a Zetasizer nano ZSP (Malvern nano-ZS90, UK). The pH<sub>PZC</sub> of MIL-100-Fe is defined as the pH value at which the zeta potential of MIL-100-Fe was zero, which can be directly obtained from the intersection point of the zeta potential-pH curve with the

vertical axis at 0 mV zeta potential.

### Linear sweep voltammetry (LSV) measurement

LSV measurements were performed using a three-electrode glass cell. The working electrode was a glassy carbon electrode (GCE), the reference electrode was Ag/AgCl<sub>3</sub>/3 M KCl. Pt electrode was used as auxiliary electrode.

Experiment conditions for testing the redox potential of MIL-100-Fe(III)/Fe(II): the sweep range was from 0.9 V to -0.4 V at a scan rate of 0.01 V/s. The experiment was carried out at room temperature in N<sub>2</sub>-saturated 0.1 M Na<sub>2</sub>SO<sub>4</sub> electrolyte at pH 4.0.

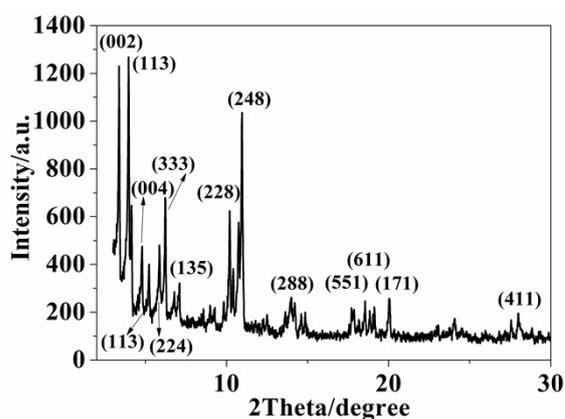


Figure S1. XRD pattern of MIL-100-Fe. (A)

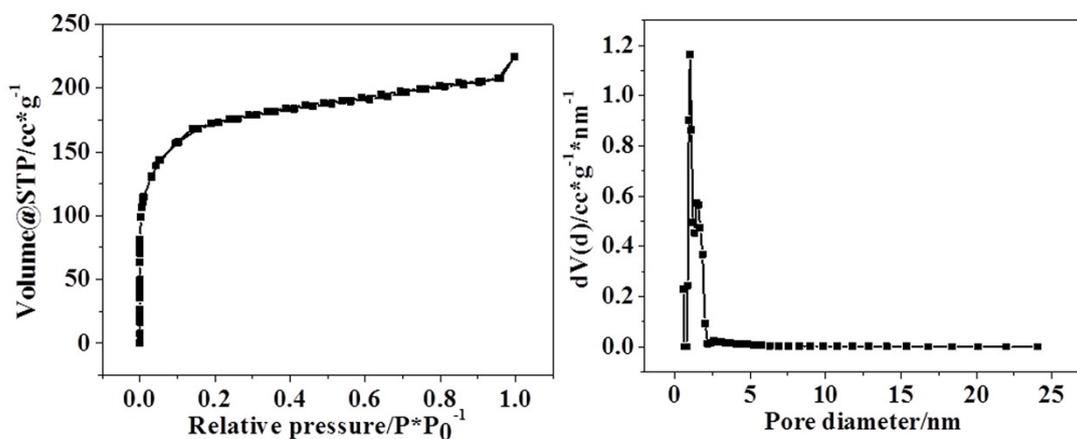


Figure S2. (A) N<sub>2</sub> adsorption–desorption isotherm of MIL-100-Fe; (B) pore size distribution of MIL-100-Fe

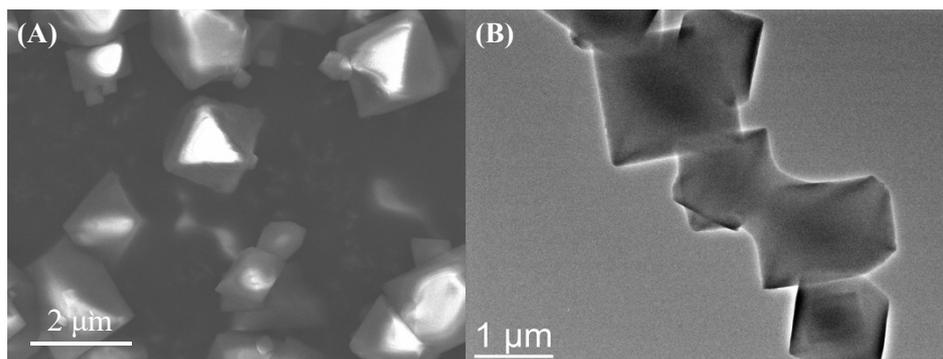


Figure S3. (A) SEM and (B) TEM pictures of MIL-100-Fe.

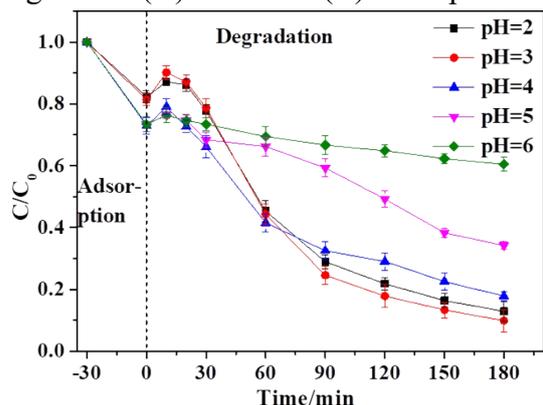


Figure S4. Influence of initial solution pH on the catalytic performance of MB in MIL-100-Fe catalyzed Fenton-like reaction. Reaction condition: [catalyst] = 0.1 g/L, [H<sub>2</sub>O<sub>2</sub>] = 16 mM, [organic pollutants] = 100 mg/L, at room temperature.

Table R1. Comparison of the performance of different Fenton-like catalysts for dye removal

Catalyst	Reaction condition	TOC removal rate	TOC removal rate per unit mass of catalyst	ref
Prussian-blue (PB)-modified - Fe <sub>2</sub> O <sub>3</sub>	pH=5.5, T=298 K, [catalyst]=0.3 g/L, [H <sub>2</sub> O <sub>2</sub> ]=0.4 mol/L, [MB]=20 μg/mL	45%	150%/g L <sup>-1</sup>	[1]
H-Fe-S	[RhB]=2.0*10 <sup>-4</sup> M; [H-Fe-S]=2 g/L; [H <sub>2</sub> O <sub>2</sub> ] = 12 mM, visible light	38%	19%/g L <sup>-1</sup>	[2]
Fe <sub>0</sub> /Fe <sub>3</sub> O <sub>4</sub>	[MB]=100 mg/L, [H <sub>2</sub> O <sub>2</sub> ] = 0.3 M, pH 6.0±0.2,[catalyst]=3 g/L	75%	25%/g L <sup>-1</sup>	[3]
Graphite tailing	[RhB]=100 mg/L, [catalyst]=50 g/L, [H <sub>2</sub> O <sub>2</sub> ]=10 g/L, pH = 3.92	49.02%	0.98%/g L <sup>-1</sup>	[4]

Iron impregnated biochars	[AR1]=50 mg L <sup>-1</sup> , pH 3, [H <sub>2</sub> O <sub>2</sub> ]=16 mM, [catalyst]=4 g L <sup>-1</sup>	86.7%	21.68%/g L <sup>-1</sup>	[5]
	[MB]=100 mg/L, [H <sub>2</sub> O <sub>2</sub> ]=0.133 mL/L, [catalyst]=1.3 g L <sup>-1</sup> , 125 W Hg lamp	21.1%-89.1%	16.2-68.5	[6]
MIL-100-Fe	[MB]=100 mg/L, [catalyst]=0.1 g/L, [H <sub>2</sub> O <sub>2</sub> ]=16 mM, pH= 4	49%	490%/g L <sup>-1</sup>	this study

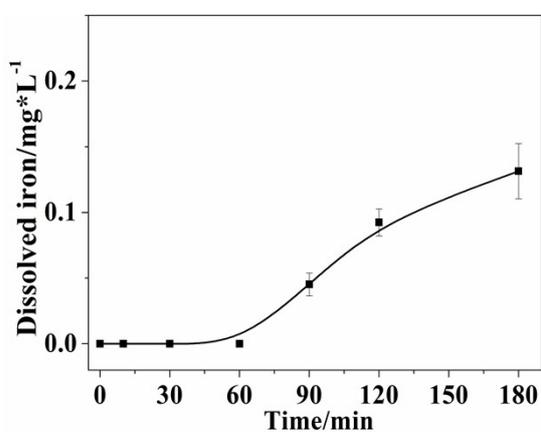


Figure S5. Variation of leached iron ions from MIL-100-Fe during Fenton-like system. Reaction conditions: [catalyst] = 0.1 g/L, [H<sub>2</sub>O<sub>2</sub>] = 16 mM, [MB] = 100 mg/L, pH 4.0 at room temperature.

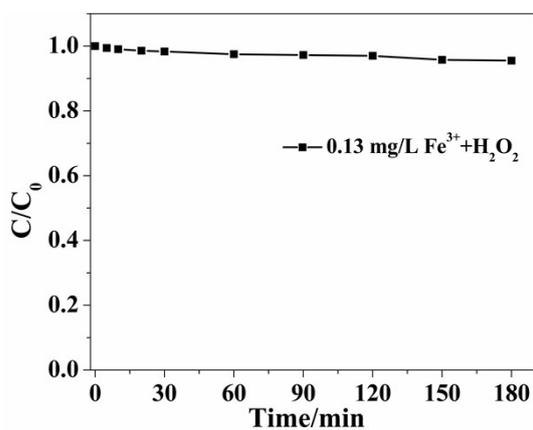


Figure S6. Catalytic degradation of MB in homogeneous Fenton-like reaction. Reaction conditions: [H<sub>2</sub>O<sub>2</sub>] = 16 mM, [MB] = 100 mg/L, pH 4.0 at room temperature.

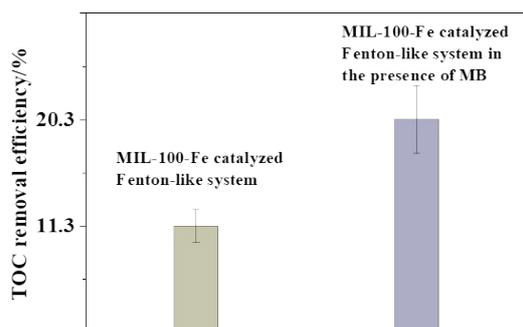


Figure S7. The TOC removal efficiency of the dyeing wastewater by MIL-100-Fe catalyzed Fenton-like reaction. Reaction condition: [catalyst] = 0.1 g/L, [H<sub>2</sub>O<sub>2</sub>] = 16 mM, [MB] = 100 mg/L, pH 4.0 at room temperature.

#### Reference

- [1] H. Wang, Y. Huang. Prussian-blue-modified iron oxide magnetic nanoparticles as effective peroxidase-like catalysts to degrade methylene blue with H<sub>2</sub>O<sub>2</sub>. *J. Hazard. Mater.* 2011, 191, 163-169.
- [2] Y. Gao, H. Gan, G. Zhang, Y. Guo. Visible light assisted Fenton-like degradation of rhodamine B and 4-nitrophenol solutions with a stable poly-hydroxyl-iron/sepiolite Catalyst. *Chem. Eng. J.* 2013, 217, 221-230.
- [3] R.C.C. Costa, F.C.C. Moura, J.D. Ardisson, J.D. Fabris, R.M. Lago. Highly active heterogeneous Fenton-like systems based on Fe<sup>0</sup>/Fe<sub>3</sub>O<sub>4</sub> composites prepared by controlled reduction of iron oxides. *Appl. Catal. B: Environ.* 2008, 83, 131–139.
- [4] C. Bai, W. Gong, D. Feng, M. Xian, Q. Zhou, S. Chen, Z. Ge, Y. Zhou. Natural graphite tailings as heterogeneous Fenton catalyst for the decolorization of rhodamine B. *Chem. Eng. J.* 2012, 197, 306–313.
- [5] K.K. Rubeena, P.H.P. Reddy, A.R. Laiju, P.V. Nidheesh. Iron impregnated biochars as heterogeneous Fenton catalyst for the degradation of acid red 1 dye. *J. Environ. Manage.* 2018, 226, 320-328.
- [6] F.E. Bimbi Junior, C.G. Neves, M.D.L. do Nascimento, E.A. Falcão, W.R.P. Barros. Photo-Fenton-Based Degradation of Methylene Blue Dye Using Hydroxyapatite Nanoparticles Doped with Fe<sub>3</sub>O<sub>4</sub>/γ-Fe<sub>2</sub>O<sub>3</sub>. *J. Braz. Chem. Soc.* 2022, 33, 1441-1455.