

**Robust biomimetic MOF featuring a negative pocket for precise recognition of uranyl enabling an ultrahigh U/V selectivity and a rapid uranium extraction from seawater**

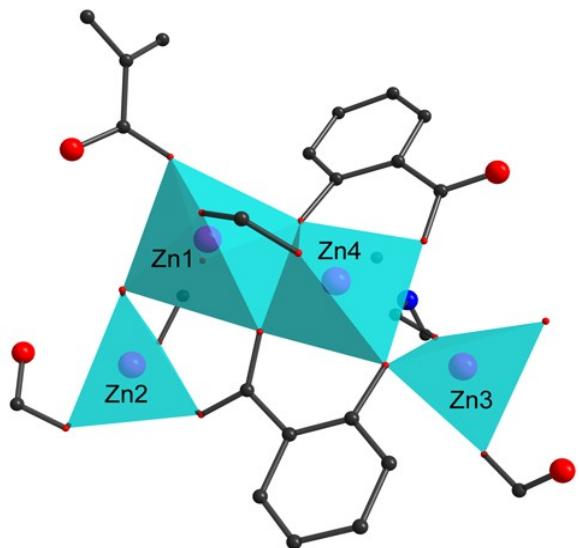
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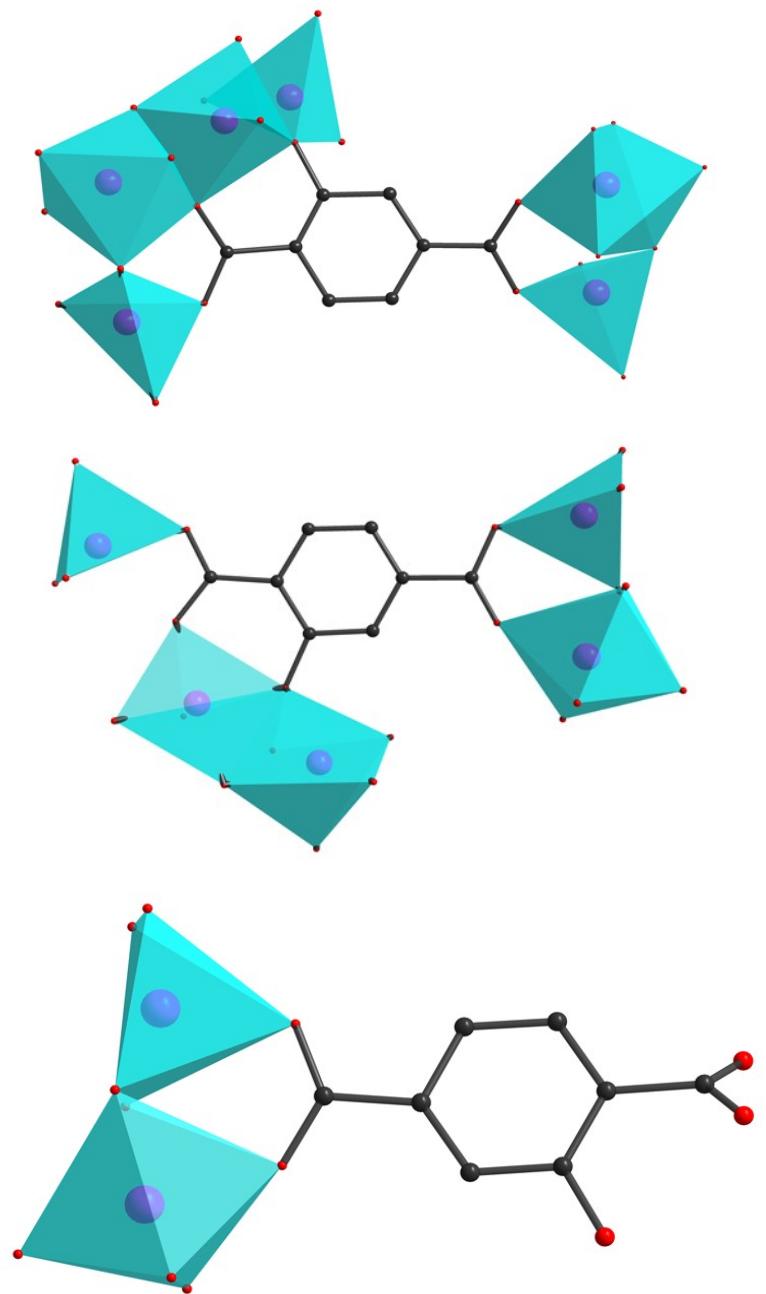
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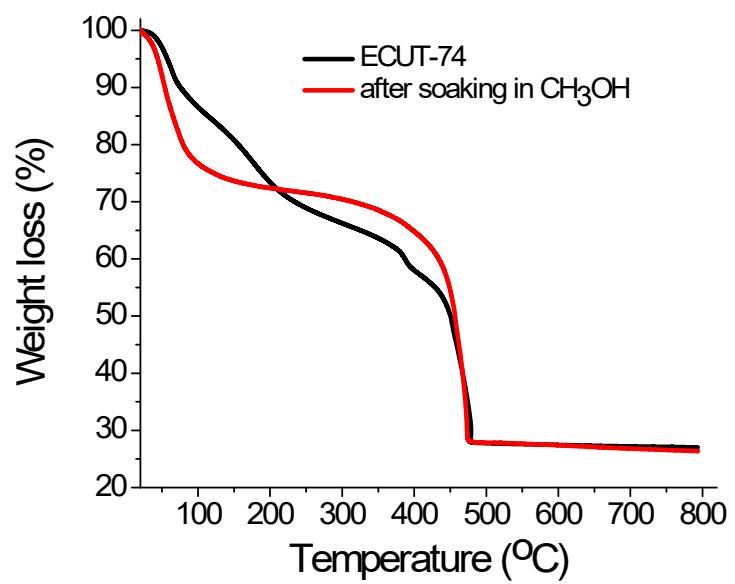
<sup>‡</sup>These authors contributed equally: Anni Ye, Yuxuan Liu, and Lele Gong



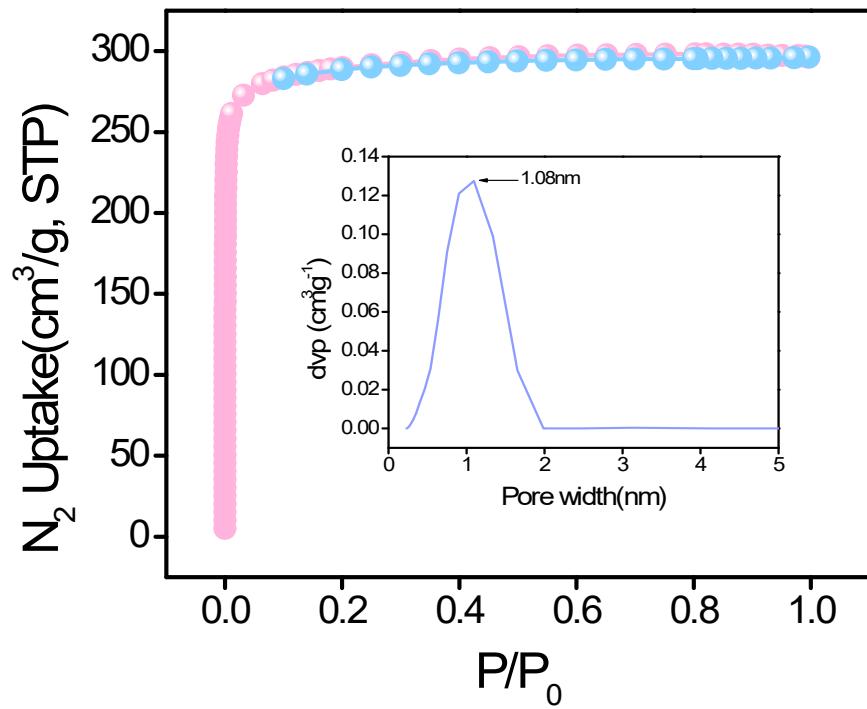
**Fig. S1** View of the coordination surrounding around Zn sites.



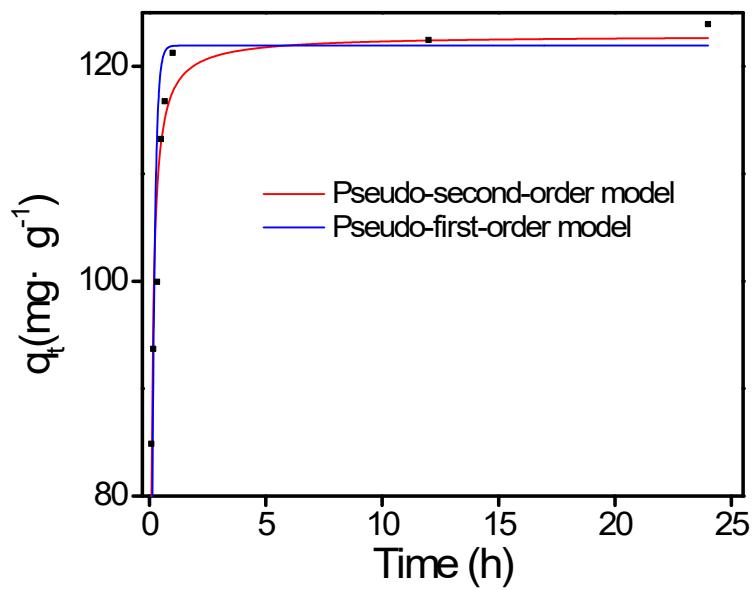
**Fig. S2** View of the coodination modes of  $\text{TP}^{3-}$  and  $\text{H}_2\text{TP}^-$  ligands in  $\mu_6:\eta^1\eta^1\eta^1\eta^1\eta^2\eta^2$ ,  $\mu_5:\eta^1\eta^1\eta^1\eta^1\eta^1\eta^2$ , and  $\mu_2:\eta^1\eta^1\eta^0\eta^0\eta^0$ , respectively.



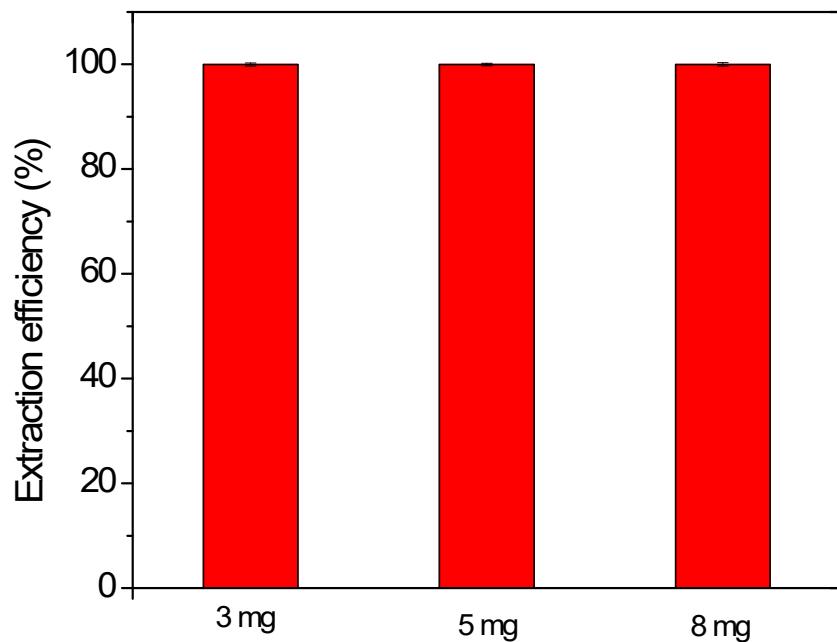
**Fig. S3** TG plots of ECUT-74 and the samples of ECUT-74 after soaking CH<sub>3</sub>OH for three days. This data was measured in air.



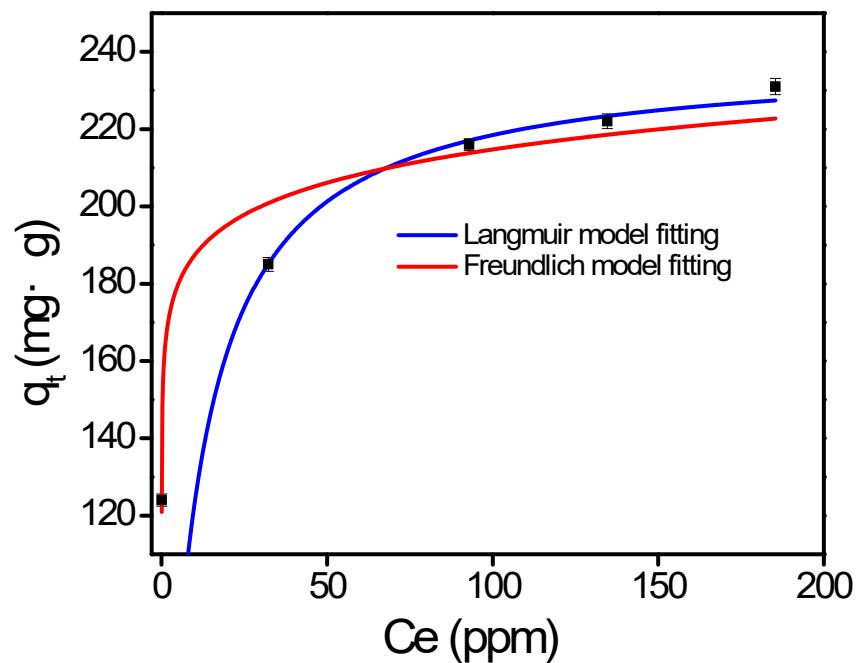
**Fig. S4** N<sub>2</sub> adsorption and desorption isotherms of ECUT-74 at 77 K with the inset of aperture distribution.



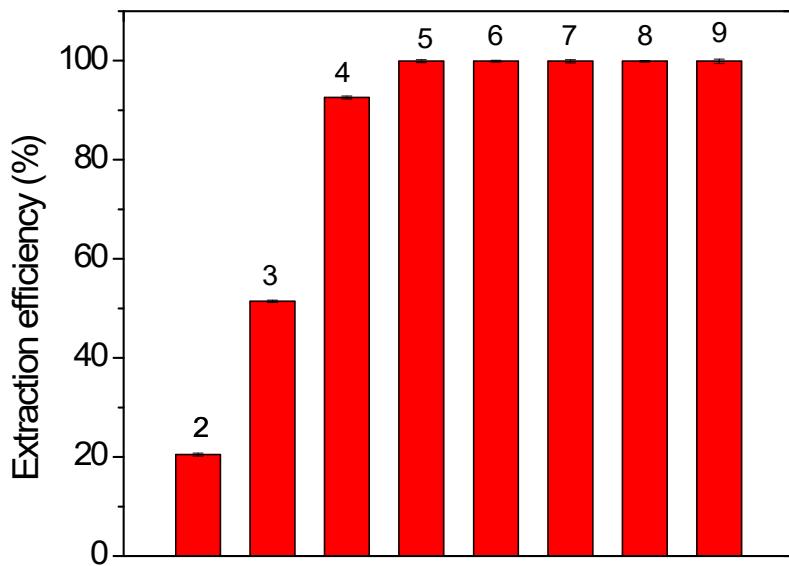
**Fig. S5** A fitting the data of the adsorption kinetics from the 12.4 mg/L uranyl solution by the pseudo-first-order kinetic models and the pseudo-second-order kinetic models, respectively.



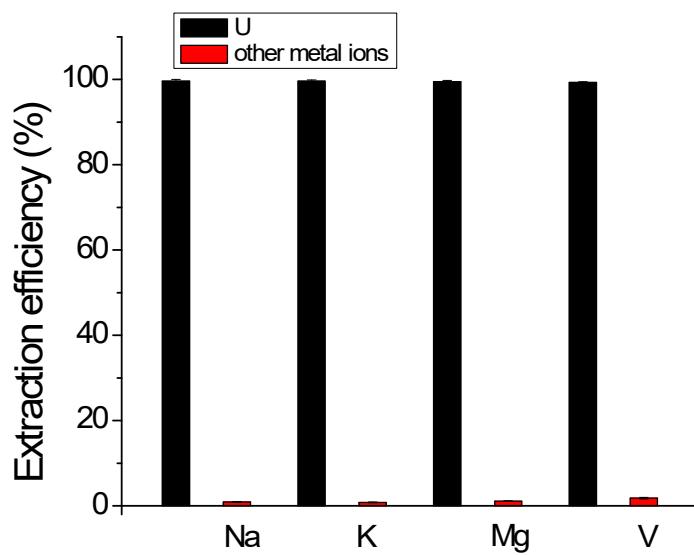
**Fig. S6** The effect of adsorbent dosage on the uranium extraction.



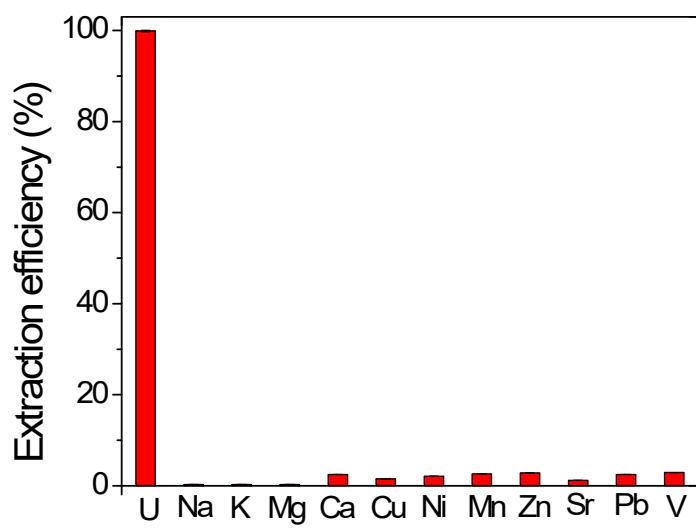
**Fig. S7** A fitting the data of the adsorption isotherm by the Langmuir and Freundlich models, respectively.



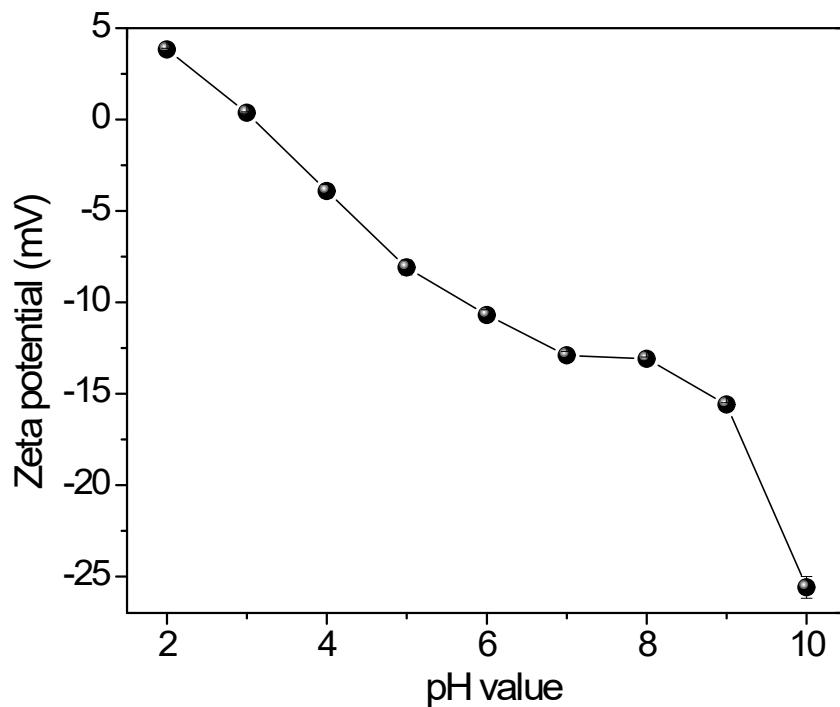
**Fig. S8** The effect of pH value on the uranium extraction.



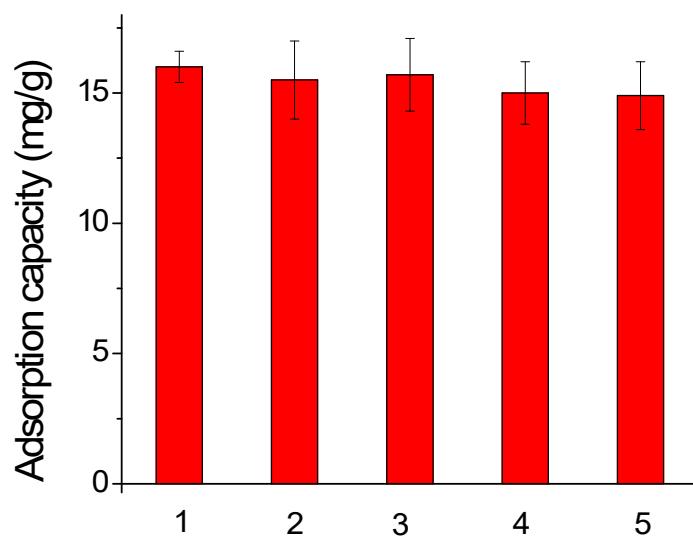
**Fig. S9** Extraction efficiency of uranium and other ions from a binary mixed solution containing 1 mg/L uranyl ions and 100 mg/L other ions (Na, K, Mg, V).



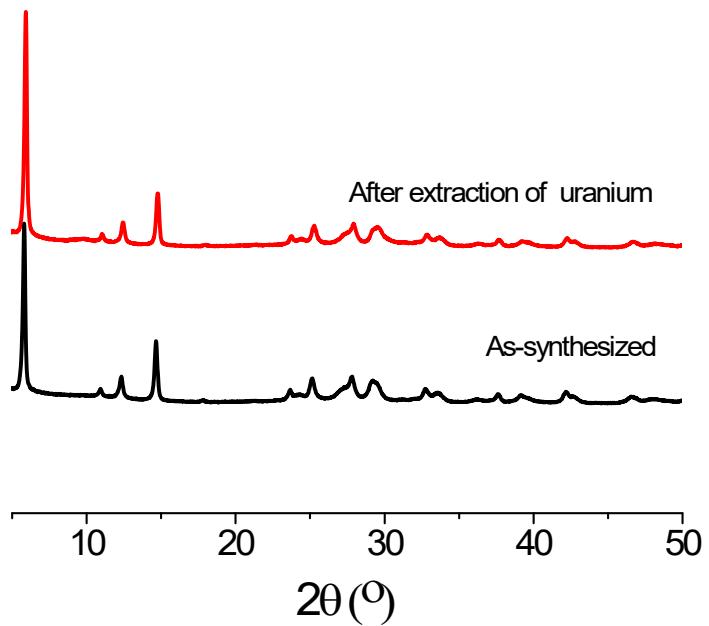
**Fig. S10** Extraction efficiency of uranium and other ions from a 12-ions mixed solution containing 1 mg/L uranyl ions and 1 mg/L other ions (Na, K, Mg, Ca, Cu, Ni, Mn, Zn, Sr, Pb, and V).



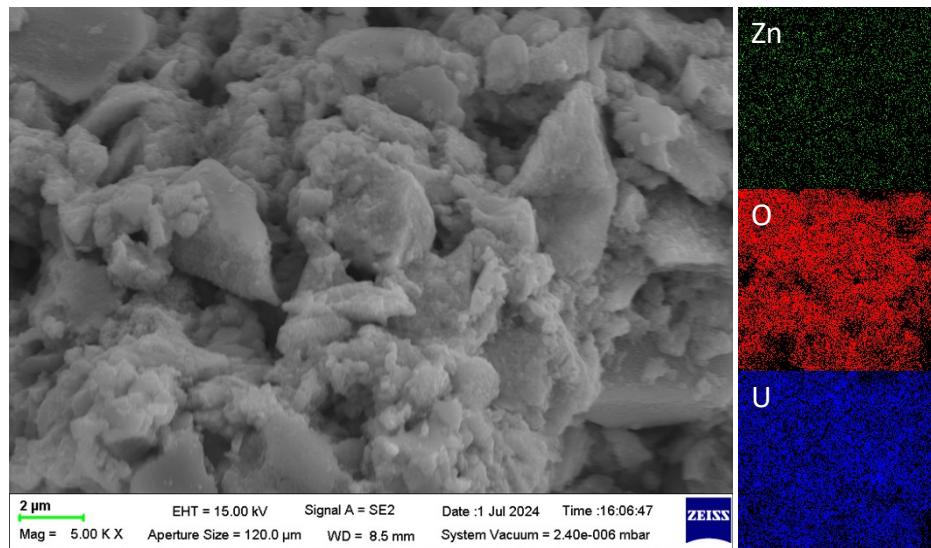
**Fig. S11** Zeta potential of ECUT-74 under pH value of 2-10.



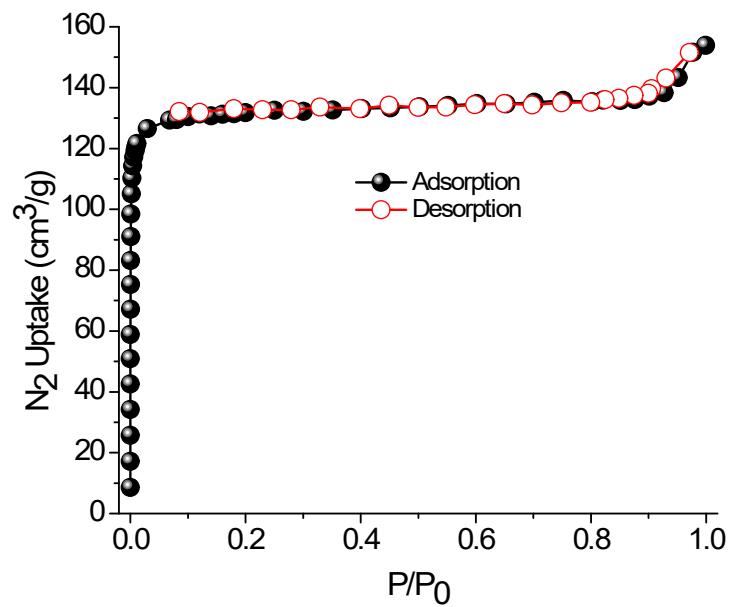
**Fig. S12** Recycle tests of uranium extraction from seawater by ECUT-74. The extracting time is one day.



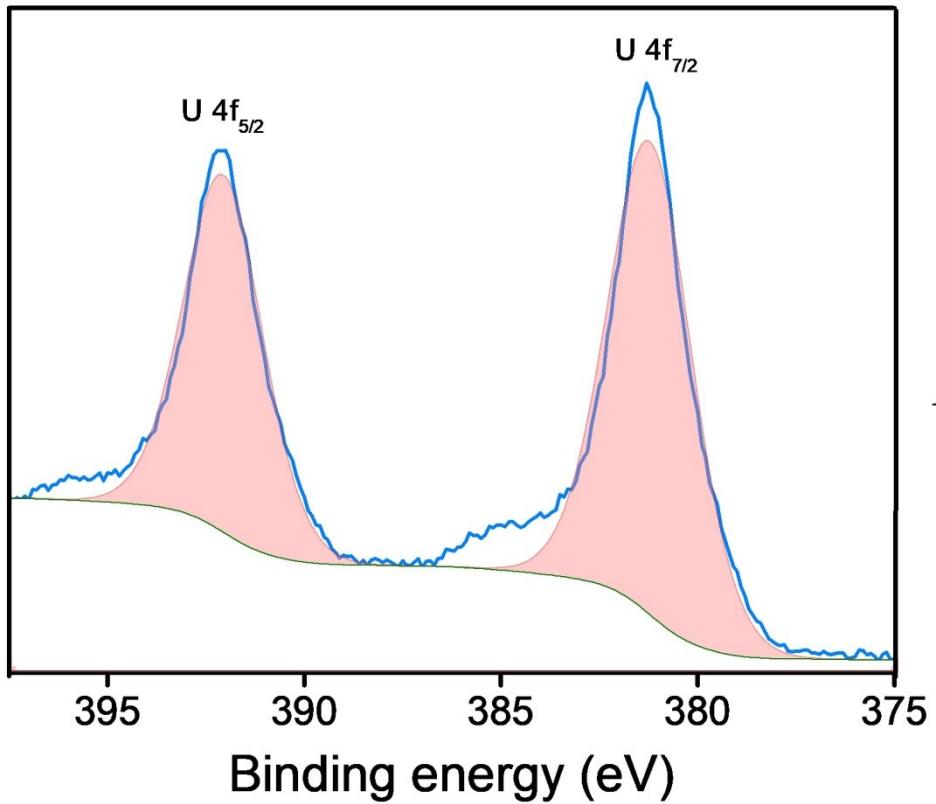
**Fig. S13** A comparison of PXRD between the as-synthesized samples of ECUT-74 and the samples after the recycle of uranium extraction.



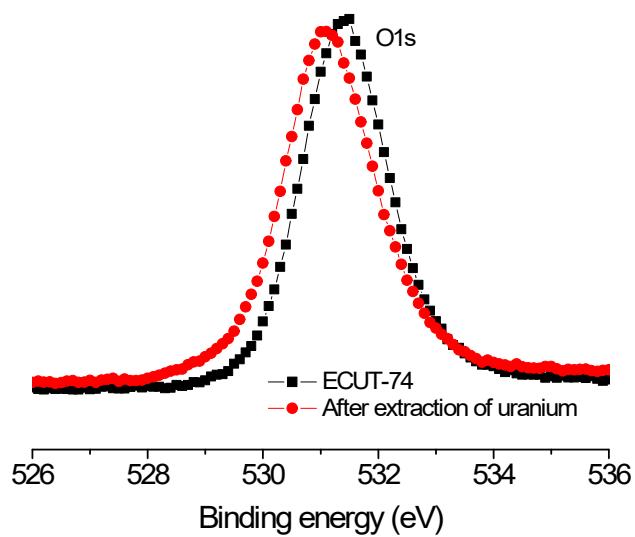
**Fig. S14** SEM-EDS of the samples of ECUT-74 after extraction of uranium.



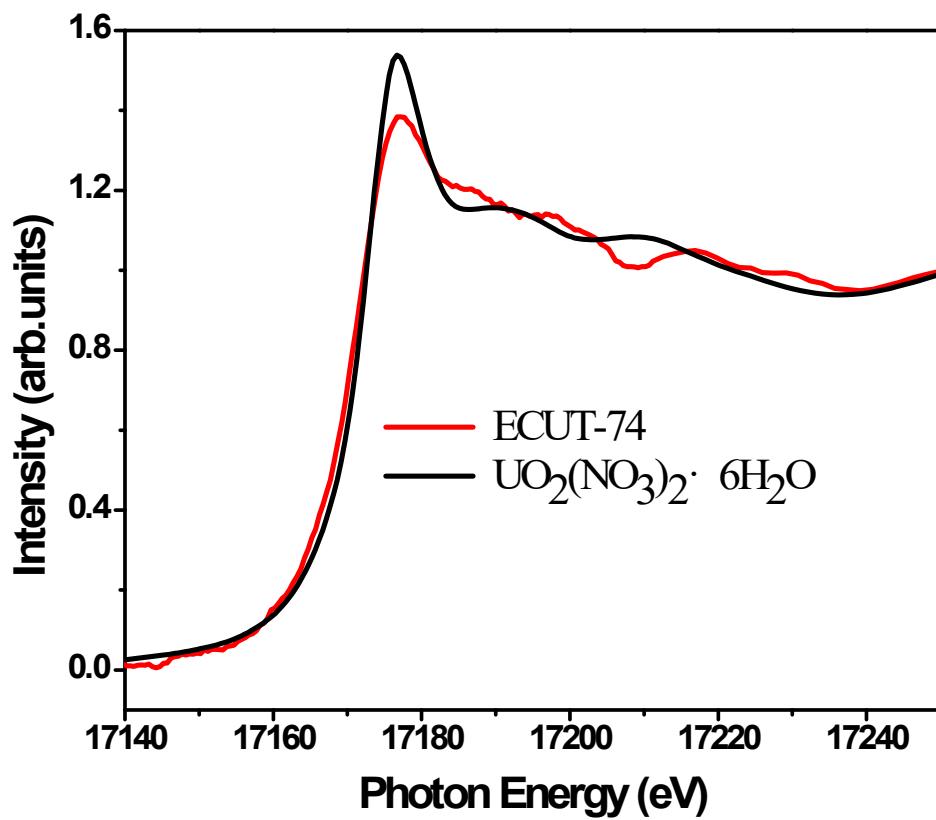
**Fig. S15** N<sub>2</sub> adsorption-desorption isotherm after recycle of uranium extraction.



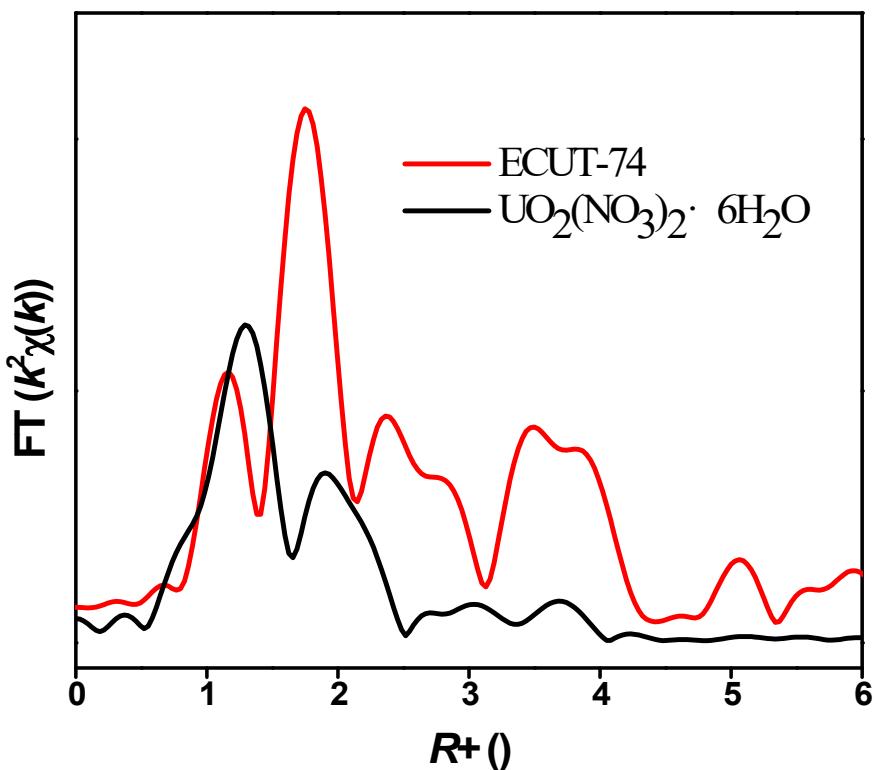
**Fig. S16** XPS U element of the samples of ECUT-74 after extraction of uranium.



**Fig. S17** XPS O element of the samples of ECUT-74 after extraction of uranium.



**Fig. S18** A comparison in XANES between ECUT-74 after extraction of uranium and the  $\text{UO}_2(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ .



**Fig. S19** A comparison in EXAFS between ECUT-74 after extraction of uranium and the  $\text{UO}_2(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ .

**Table S1.** The crystal data of ECUT-74.

Temperature	303(2) K
Wavelength	0.71073 Å
Crystal system, space group	Tetragonal, P4(1)2(1)2
Unit cell dimensions	$a=b=17.1567(4)$ Å $c=33.4185(11)$ Å
Volume	9836.8(5) Å <sup>3</sup>
F(000)	3480
Completeness to theta=25.00	99.8 %
Goodness-of-fit on F <sup>2</sup>	0.996
Final R indices [I>2sigma(I)]	R1=0.0699, wR2=0.1845
CCDC number	2373411

**Table S2.** Zn-O bond lengths in ECUT-74.

O(1)-Zn(4)	1.994(5)
O(1)-Zn(1)	2.004(6)
O(2)-Zn(4)	2.016(6)
O(2)-Zn(1)	2.362(6)
O(3)-Zn(3)	1.983(6)
O(3)-Zn(4)	2.019(6)
O(4)-Zn(2)	1.983(6)
O(5)-Zn(4)	1.954(6)
O(5)-Zn(2)#1	2.417(7)
O(6)-Zn(3)#2	1.935(6)
O(7)-Zn(1)#3	2.030(7)
O(8)-Zn(1)#4	2.040(6)
O(9)-Zn(2)#4	1.949(5)
O(10)-Zn(2)#1	1.978(6)
O(11)-Zn(1)	2.138(8)
O(12)-Zn(4)	2.024(9)
Zn(1)-O(16)#6	2.112(5)
Zn(2)-O(16)#6	1.946(5)
Zn(3)-O(16)	1.990(6)
Zn(3)-O(17)	2.024(12)

**Table S3.** A comparison of  $K_d$  value for uranium extraction among established adsorbents and our case.

Adsorbents	$K_d$ value (mL/g)	References
ECUT-74	$2.1 \times 10^7$	This work
MIGPAF-13	$2.0 \times 10^6$	M1
SMON-PAO	$3.76 \times 10^5$	M2
PIDO/NF	$2.84 \times 10^5$	M3
MS@PIDO/Alg	$1.98 \times 10^4$	M4
POP <sub>I</sub> -AO	$1.1 \times 10^6$	M5
PPA@MISS-PAF-1	$2.18 \times 10^7$	M6
i-MZIF90(50)	$1.22 \times 10^7$	M7

**Table S4.** Fitting the data of the adsorption kinetics from the 12.4 mg/L uranyl solution by the pseudo-first-order kinetic models and the pseudo-second-order kinetic models, respectively.

**Pseudo-first-order model**

$q_e$ : adsorption capacities at equilibrium (mg·g<sup>-1</sup>)

$$q_t = q_e \left(1 - e^{\frac{-k_1 t}{2.303}}\right) \quad q_t: \text{adsorption capacities at time } t \text{ (mg·g}^{-1}\text{)}$$

$k_1$ : pseudo-first-order rate constant for the kinetic model (min<sup>-1</sup>)

**Pseudo-second-order model**

$$q_t = (q_e^2 * k_2 t) / (1 + q_e k_2 t) \quad k_2: \text{pseudo-second-order rate constant of adsorption (mg} \cdot \text{g}^{-1} \cdot \text{min}^{-1}\text{)}$$

Adsorbent	Pseudo-first-order				Pseudo-second-order		
	$q_{e,\text{exp}}$ (mg·g <sup>-1</sup> )	$q_{e,\text{cal}}$ (mg·g <sup>-1</sup> )	$K_1$ (min <sup>-1</sup> )	$R^2$	$q_{e,\text{cal}}$ (mg·g <sup>-1</sup> )	$K_2$ (g·mg <sup>-1</sup> ·min <sup>-1</sup> )	$R^2$
ECUT-74	123.98	121.93	18.424	0.89	124.64	0.1849	0.99

**Table S5.** Fitting the data of the adsorption isotherm by the Langmuir and Freundlich models, respectively.

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**Langmuir model**

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$$Q_e = K_L Q_{max} C_e / (1 + K C_e)$$

$Q_e$ : adsorption capacities at equilibrium ( $\text{mg}\cdot\text{g}^{-1}$ )  
 $Q_{max}$ : Maximum adsorption capacity ( $\text{mg}\cdot\text{g}^{-1}$ )  
 K: Constants related to adsorption ( $\text{mg}\cdot\text{g}^{-1}$ )

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**Freundlich model**

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$$Q_e = K_F C_e^{-n}$$

n: Parameters related to the intensity of adsorption

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Adsorbent	Langmuir model			Freundlich model			
	$Q_{e,exp}(\text{mg}\cdot\text{g}^{-1})$	$K_L(\text{L}\cdot\text{mg}^{-1})$	$Q_{max}(\text{mg}\cdot\text{g}^{-1})$	$R^2$	$K_F(\text{mg}\cdot\text{g}^{-1})$	n	$R^2$
ECUT-74	231	0.10693	238.9	0.99	163.589	0.05908	0.95

**Table S6.** A comparison of U/V for uranium extraction among established adsorbents and our case.

Adsorbents	U/V selectivity	References
ECUT-74	$3.3 \times 10^4$	This work
PPH-OP	$1.0 \times 10^2$	M8
MIGPAF-13	60	M1
UiO-66-3C4N	17	M9
H-ABP	1.3	M10
Zn <sup>2+</sup> -PAO	<1	M11
PAF-170-AO	15	M12
BP-PAO	<1	M13
POP <sub>1</sub> -AO	<4	M5
AO-PIM-1	<1	M14

**Table S7.** A comparison of uranium extraction capacity from natural seawater among established adsorbents and our case.

Adsorbents	Uranium extraction capacity (mg/g)	Extraction time (day)	Uranium extraction capacity <i>per day</i> (mg/g/day)	References
ECUT-74	16	1	16	This work
i-MZIF90(50)	28.2	25	1.13	M7
PPA@MISS-PAF-1	16.97	90	0.19	M6
BP-PAO	11.76	56	0.21	M13
H-ABP	11.5	90	0.13	M10
SMON-PAO	9.59	56	0.17	M2
Zn <sup>2+</sup> -PAO	9.23	28	0.33	M11
PIDO/NF	8.7	56	0.16	M3
COF-4P	24.06	3	8.02	M15
PPH-OP	7.12	21	0.34	M8
AO-PIM-1	9.03	28	0.32	M14
MIGPAF-13	16	56	0.28	M1
TI-COF	8.8	1	8.8	M16
MITpBD	23.6	7	3.37	M17
JNM-101-AO	7.96	8	1.0	M18

**Table S8.** The cost of the raw materials used to synthesize ECUT-74.

The cost of the raw materials from Aladdin Biochemical Technology Co., Ltd	The cost of the raw materials for the synthesis of ECUT-74
2-hydroxyterephthalic acid (1.5 \$/g)	2-hydroxyterephthalic acid (1.08 \$),
Zn(NO <sub>3</sub> ) <sub>2</sub> ·6H <sub>2</sub> O (0.076 \$/g)	Zn(NO <sub>3</sub> ) <sub>2</sub> ·6H <sub>2</sub> O (0.02 \$)
1,4-diazabicyclo[2.2.2]octane (0.04 \$/g)	1,4-diazabicyclo[2.2.2]octane (0.01 \$)
DMF (6.88 \$/L)	DMF (0.27 \$)
glycol (6.56 \$/L)	glycol (0.09 \$)
methanol (4.88 \$/L)	methanol (0.19 \$)
	Total: 1.66 \$/g

**Table S9.** Parameters of the fit of the samples of ECUT-74 after uranium extraction.

Pair	CN	R(Å)	$\sigma^2 \times 10^{-3}$ (Å <sup>-3</sup> )	R factor
U-O <sub>1</sub>	2.0	1.74±0.02	1.0	0.011
U-O <sub>2</sub>	5.5± 1.0	2.40±0.02	2.4	

## References

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